

*The HYDRUS Software Package for Simulating  
the Two- and Three-Dimensional Movement  
of Water, Heat, and Multiple Solutes  
in Variably-Saturated Media*

Technical Manual

Version 1.0

March 2006

PC Progress, Prague, Czech Republic



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## DISCLAIMER

This report documents version 1.0 of HYDRUS, a software package for simulating water, heat and solute movement in two- and three-dimensional variably saturated media. The software has been verified against a large number of test cases. However, no warranty is given that the program is completely error-free. If you do encounter problems with the code, find errors, or have suggestions for improvement, please contact one of the authors at

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## ABSTRACT

Šimůnek, J., M. Th. van Genuchten, and M. Šejna, The HYDRUS Software Package for Simulating Two- and Three Dimensional Movement of Water, Heat, and Multiple Solutes in Variably-Saturated Media, Version 1.0, PC Progress, Prague, Czech Republic, 2006.

This report documents version 1.0 of HYDRUS, a general software package for simulating water, heat, and solute movement in two- and three- dimensional variably saturated media. The software package consists of the computation computer program, and the interactive graphics-based user interface. The HYDRUS program numerically solves the Richards equation for saturated-unsaturated water flow and the convection-dispersion equation for heat and solute transport. The flow equation incorporates a sink term to account for water uptake by plant roots. The heat transport equation considers transport due to conduction and convection with flowing water. The solute transport equations consider convective-dispersive transport in the liquid phase, as well as diffusion in the gaseous phase. The transport equations also include provisions for nonlinear nonequilibrium reactions between the solid and liquid phases, linear equilibrium reactions between the liquid and gaseous phases, zero-order production, and two first-order degradation reactions: one which is independent of other solutes, and one which provides the coupling between solutes involved in sequential first-order decay reactions. In addition, physical nonequilibrium solute transport can be accounted for by assuming a two-region, dual-porosity type formulation which partitions the liquid phase into mobile and immobile regions. Attachment/detachment theory, including the filtration theory, is included to simulate transport of viruses, colloids, and/or bacteria. The program may be used to analyze water and solute movement in unsaturated, partially saturated, or fully saturated porous media. HYDRUS can handle flow regions delineated by irregular boundaries. The flow region itself may be composed of nonuniform soils having an arbitrary degree of local anisotropy. Flow and transport can occur in the vertical plane, the horizontal plane, a three-dimensional region exhibiting radial symmetry about the vertical axis, or fully three-dimensional domain. The water flow part of the model can deal with prescribed head and flux boundaries, boundaries controlled by atmospheric conditions, free drainage boundary conditions, as well as a simplified representation of nodal drains using results of electric analog experiments. The two-dimensional part of this program also includes a Marquardt-Levenberg type parameter optimization algorithm for inverse estimation of soil hydraulic and/or solute transport and reaction parameters from measured transient or steady-state flow and/or transport data for two dimensional problems.

The governing flow and transport equations are solved numerically using Galerkin-type linear finite element schemes. Depending upon the size of the problem, the matrix equations resulting from discretization of the governing equations are solved using either Gaussian elimination for banded matrices, or a conjugate gradient method for symmetric matrices and the ORTHOMIN method for asymmetric matrices.

The program is distributed by means of several different options (Levels). Levels 2D-Light and 2D-Standard are for the programs and the graphical interface for two-dimensional problems with either a structured mesh generator for relatively simple flow domain geometries or a CAD program for more general domain geometries, and the MESHGEN2D mesh generator for an unstructured finite element mesh specifically designed for variably-saturated subsurface flow transport problems, respectively. Levels 3D-Light and 3D-Standard include the two dimensional version and additionally the three dimensional versions for simple hexagonal or more general layered geometries, respectively.

This report serves as both a technical manual and reference document. Detailed instructions are given for data input preparation. The graphical user interface (GUI) of the Hydrus software package is documented in a separate user manual (Šimůnek et al., 2006).



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## LIST OF VARIABLES

$a$	ion activity in soil solution [-]
$a_i$	conversion factor from concentration to osmotic head [ $L^4M^{-1}$ ]
$a_v$	air content [ $L^3L^{-3}$ ]
$\bar{a}$	ion activity on the exchange surfaces [-]
$A$	amplitude of temperature sine wave [K]
$A_e$	area of a triangular element [ $L^2$ ]
$A_{qh}$	parameter in equation (8.1) [ $LT^{-1}$ ]
$A_s$	correction factor [-]
$[A]$	coefficient matrix in the global matrix equation for water flow, [ $LT^{-1}$ ] or [ $L^2T^{-1}$ ] <sup>+</sup>
$b$	normalized root water uptake distribution, [ $L^{-2}$ ] or [ $L^{-3}$ ] <sup>+</sup>
$b'$	arbitrary root water uptake distribution, [ $L^{-2}$ ] or [ $L^{-3}$ ] <sup>+</sup>
$b_i, c_i$	geometrical shape factors [L]
$b_1, b_2, b_3$	empirical parameters to calculate thermal conductivity $\lambda_0$ [ $MLT^{-3}K^{-1}$ ](e.g. $Wm^{-1}K^{-1}$ )
$B_{qh}$	parameter in equation (8.1) [ $L^{-1}$ ]
$\{B\}$	vector in the global matrix equation for water flow, [ $L^2T^{-1}$ ] or [ $L^3T^{-1}$ ] <sup>+</sup>
$c$	solution concentration, [ $ML^{-3}$ ] or [ $N_cL^{-3}$ ]
$c'$	finite element approximation of $c$ [ $ML^{-3}$ ]
$c_i$	initial solution concentration [ $ML^{-3}$ ]
$c_n$	value of the concentration at node $n$ [ $ML^{-3}$ ]
$c_r$	concentration of the sink term [ $ML^{-3}$ ]
$c_0$	prescribed concentration boundary condition [ $ML^{-3}$ ]
$C$	volumetric heat capacity of porous medium [ $ML^{-1}T^{-2}K^{-1}$ ] (e.g. $Jm^{-3}K^{-1}$ )
$C_d$	factor used to adjust the hydraulic conductivity of elements in the vicinity of drains [-]
$C_g$	volumetric heat capacity of gas phase [ $ML^{-1}T^{-2}K^{-1}$ ] (e.g. $Jm^{-3}K^{-1}$ )
$C_n$	volumetric heat capacity of solid phase [ $ML^{-1}T^{-2}K^{-1}$ ] (e.g. $Jm^{-3}K^{-1}$ )
$C_o$	volumetric heat capacity of organic matter [ $ML^{-1}T^{-2}K^{-1}$ ] (e.g. $Jm^{-3}K^{-1}$ )
$C_T$	total solution concentration [ $ML^{-3}$ ] ( $mmol_c l^{-1}$ )
$C_w$	volumetric heat capacity of liquid phase [ $ML^{-1}T^{-2}K^{-1}$ ] (e.g. $Jm^{-3}K^{-1}$ )

$Cr_i^e$	local Courant number [-]
$d$	thickness of stagnant boundary layer [L]
$d_c$	diameter of the sand grains [L]
$d_e$	effective drain diameter [L]
$d_p$	diameter of the particle (e.g., virus, bacteria) ( $= 0.95 \mu\text{m} = 0.95\text{e-}6 \text{ m}$ ) [L]
$D$	side length of the square in the finite element mesh surrounding a drain (elements have adjusted hydraulic conductivities) [L]
$D_g$	ionic or molecular diffusion coefficient in the gas phase [ $\text{L}^2\text{T}^{-1}$ ]
$D_{ij}$	effective dispersion coefficient tensor in the soil matrix [ $\text{L}^2\text{T}^{-1}$ ]
$D_{ij}^g$	diffusion coefficient tensor for the gas phase [ $\text{L}^2\text{T}^{-1}$ ]
$D_{ij}^w$	dispersion coefficient tensor for the liquid phase [ $\text{L}^2\text{T}^{-1}$ ]
$D_L$	longitudinal dispersivity [L]
$D_T$	transverse dispersivity [L]
$D_w$	ionic or molecular diffusion coefficient in free water [ $\text{L}^2\text{T}^{-1}$ ]
$\{D\}$	vector in the global matrix equation for water flow, [ $\text{L}^2\text{T}^{-1}$ ] or [ $\text{L}^3\text{T}^{-1}$ ] <sup>+</sup>
$e_n$	subelements which contain node $n$ [-]
$E$	maximum (potential) rate of infiltration or evaporation under the prevailing atmospheric conditions [ $\text{LT}^{-1}$ ]
$E_a$	activation energy of a reaction or process [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ] ( $\text{m}^2\text{s}^{-2}\text{mol}^{-1}$ )
$f$	fraction of exchange sites assumed to be at equilibrium with the solution concentration [-]
$\{f\}$	vector in the global matrix equation for solute transport, [ $\text{MT}^{-1}\text{L}^{-1}$ ] or [ $\text{MT}^{-1}$ ] <sup>+</sup>
$[F]$	coefficient matrix in the global matrix equation for water flow, [ $\text{L}^2$ ] or [ $\text{L}^3$ ] <sup>+</sup>
$g$	gas concentration [ $\text{ML}^{-3}$ ]
$g$	gravitational acceleration ( $= 9.81 \text{ m s}^{-2}$ ) [ $\text{LT}^{-2}$ ]
$g_{am}$	gas concentration above the stagnant boundary layer [ $\text{ML}^{-3}$ ]
$\{g\}$	vector in the global matrix equation for solute transport, [ $\text{MT}^{-1}\text{L}^{-1}$ ] or [ $\text{MT}^{-1}$ ] <sup>+</sup>
$[G]$	coefficient matrix in the global matrix equation for solute transport, [ $\text{L}^2\text{T}^{-1}$ ] or [ $\text{L}^3\text{T}^{-1}$ ] <sup>+</sup>
$h$	pressure head [L]
$h^*$	scaled pressure head [L]
$h'$	finite element approximation of $h$ [L]

$h_A$	minimum pressure head allowed at the soil surface [L]
$h_n$	nodal values of the pressure head [L]
$h_{ref}$	pressure head at reference temperature $T_{ref}$ [L]
$h_s$	air-entry value in the Brooks and Corey soil water retention function [L]
$h_S$	maximum pressure head allowed at the soil surface [L]
$h_T$	pressure head at soil temperature $T$ [L]
$h_0$	initial condition for the pressure head [L]
$h_{50}$	pressure head at which root water uptake is reduced by 50 % [L]
$h_\phi$	osmotic head [L]
$h_{\phi 50}$	osmotic head at which root water uptake is reduced by 50 % [L]
$h_\Delta$	pressure head at the reversal point in a hysteretic retention function [L]
$H$	Hamaker constant (= $1e-20$ J) [ $ML^2T^{-2}$ ]
$k$	$k$ th chain number [-]
$k$	Boltzman constant (= $1.38048e-23$ J/K) [ $M L^2T^{-2}K^{-1}$ ]
$k_a$	first-order deposition (attachment) coefficient [ $T^{-1}$ ]
$k_d$	first-order entrainment (detachment) coefficient [ $T^{-1}$ ]
$k_g$	empirical constant relating the solution and gas concentrations [-]
$k_s$	empirical constant relating the solution and adsorbed concentrations [ $L^3M^{-1}$ ]
$K$	unsaturated hydraulic conductivity [ $LT^{-1}$ ]
$K^*$	scaled unsaturated hydraulic conductivity [ $LT^{-1}$ ]
$\mathbf{K}^A$	dimensionless anisotropy tensor for the unsaturated hydraulic conductivity $K$ [-]
$K^d$	unsaturated hydraulic conductivity of the main drying branch [ $LT^{-1}$ ]
$K^w$	unsaturated hydraulic conductivity of the main wetting branch [ $LT^{-1}$ ]
$K_{drain}$	adjusted hydraulic conductivity in the elements surrounding a drain [ $LT^{-1}$ ]
$K_{ex}$	dimensionless thermodynamic equilibrium constant [-]
$K_H$	Henry's Law constant [ $MT^2M^{-1}L^{-2}$ ]
$K_{ij}^A$	components of the dimensionless anisotropy tensor $\mathbf{K}^A$ [-]
$K_k$	measured value of the unsaturated hydraulic conductivity at $\theta_k$ [ $LT^{-1}$ ]
$K_r$	relative hydraulic conductivity [-]
$K_{ref}$	hydraulic conductivity at reference temperature $T_{ref}$ [ $LT^{-1}$ ]

$K_s$	saturated hydraulic conductivity [ $LT^{-1}$ ]
$K_s^d$	saturated hydraulic conductivity associated with the main drying branch [ $LT^{-1}$ ]
$K_s^w$	saturated hydraulic conductivity associated with the main wetting branch [ $LT^{-1}$ ]
$K_T$	hydraulic conductivity at soil temperature $T$ [ $LT^{-1}$ ]
$K_v$	Vanselow selectivity coefficient [-]
$K_{12}$	selectivity coefficient [-]
$K_{\Delta}$	unsaturated hydraulic conductivity at the reversal point in a hysteretic conductivity function [ $LT^{-1}$ ]
$l$	pore-connectivity parameter [-]
$L$	length of the side of an element [L]
$L_i$	local coordinate [-]
$L_n$	length of a boundary segment [L]
$L_x$	width of the root zone [L]
$L_z$	depth of the root zone [L]
$m$	parameter in the soil water retention function [-]
$M^0$	cumulative amount of solute removed from the flow region by zero-order reactions, [ $ML^{-1}$ ] or $[M]^+$
$M^1$	cumulative amount of solute removed from the flow region by first-order reactions, [ $ML^{-1}$ ] or $[M]^+$
$M_r$	cumulative amount of solute removed from the flow region by root water uptake, [ $ML^{-1}$ ] or $[M]^+$
$M_t$	amount of solute in the flow region at time $t$ , [ $ML^{-1}$ ] or $[M]^+$
$M_t^e$	amount of solute in element $e$ at time $t$ , [ $ML^{-1}$ ] or $[M]^+$
$M_0$	amount of solute in the flow region at the beginning of the simulation, [ $ML^{-1}$ ] or $[M]^+$
$M_0^e$	amount of solute in element $e$ at the beginning of the simulation, [ $ML^{-1}$ ] or $[M]^+$
$n$	exponent in the soil water retention function [-]
$n^d$	exponent in the soil water retention function; drying branch [-]
$n^w$	exponent in the soil water retention function; wetting branch [-]
$N_c$	number of colloids (particles)
$n_i$	components of the outward unit vector normal to boundary $\Gamma_N$ or $\Gamma_G$ [-]
$n_s$	number of solutes involved in the chain reaction [-]

$N$	total number of nodes [-]
$N_e$	number of subelements $e_n$ , which contain node $n$ [-]
$N_G$	gravitation number [-]
$N_{Lo}$	contribution of particle London-van der Waals attractive forces to particle removal [-]
$N_{Pe}$	Peclet number in the single-collector efficiency coefficient [-]
$N_R$	interception number [-]
$O$	actual rate of inflow/outflow to/from a subregion, $[L^2T^{-1}]$ or $[L^3T^{-1}]^+$
$p$	exponent in the water and osmotic stress response function [-]
$p_t$	period of time necessary to complete one temperature cycle (1 day) [T]
$p_1$	exponent in the water stress response function [-]
$p_2$	exponent in the osmotic stress response function [-]
$p_x$	empirical parameter in the root distribution function [-]
$p_y$	empirical parameter in the root distribution function [-]
$p_z$	empirical parameter in the root distribution function [-]
$Pe_i^e$	local Peclet number [-]
$q_i$	components of the Darcian fluid flux density $[LT^{-1}]$
$Q_n^A$	convective solute flux at node $n$ , $[MT^{-1}L^{-1}]$ or $[MT^{-1}]^+$
$Q_n^D$	dispersive solute flux at node $n$ , $[MT^{-1}L^{-1}]$ or $[MT^{-1}]^+$
$Q_n^T$	total solute flux at node $n$ , $[MT^{-1}L^{-1}]$ or $[MT^{-1}]^+$
$\{Q\}$	vector in the global matrix equation for water flow, $[L^2T^{-1}]$ or $[L^3T^{-1}]^+$
$[Q]$	coefficient matrix in the global matrix equation for solute transport, $[L^2]$ or $[L^3]^+$
$R$	solute retardation factor [-]
$R_u$	universal gas constant $[ML^2T^{-2}K^{-1}M^{-1}]$ ( $=8.314\text{kg m}^2\text{s}^{-2}\text{K}^{-1}\text{mol}^{-1}$ )
$s$	adsorbed solute concentration, [-] or $[N_cM^{-1}]$
$s^e$	adsorbed solute concentration on type-1 sites [-]
$s_i$	initial value of adsorbed solute concentration [-]
$s^k$	adsorbed solute concentration on type-2 sites [-]
$s_{max}$	maximum solid phase concentration $[N_cM^{-1}]$
$S$	sink term $[T^{-1}]$
$S_e$	degree of saturation [-]

$S_{ek}$	degree of saturation at $\theta_k$ [-]
$S_p$	spatial distribution of the potential transpiration rate [ $T^{-1}$ ]
$S_t$	width of soil surface associated with transpiration, [L] or [ $L^2$ ] <sup>+</sup>
$S_T$	cation exchange capacity [ $MM^{-1}$ ] ( $mmol_c kg^{-1}$ )
[ $S$ ]	coefficient matrix in the global matrix equation for solute transport, [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup>
$t$	time [T]
$t^*$	local time within the time period $t_p$ [T]
$t_p$	period of time covering one complete cycle of the temperature sine wave [T] $T$ temperature [K]
$T_a$	actual transpiration rate per unit surface length [ $LT^{-1}$ ]
$\bar{T}$	average temperature at soil surface during period $t_p$ [K]
$T^A$	absolute temperature [K]
$T_i$	initial temperature [K]
$T_p$	potential transpiration rate [ $LT^{-1}$ ]
$T_r^A$	reference absolute temperature [K] ( $293.15K=20^\circ C$ )
$T_0$	prescribed temperature boundary condition [K]
$v$	average pore-water velocity [ $LT^{-1}$ ]
$V$	volume of water in each subregion, [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_{new}$	volume of water in each subregion at the new time level, [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_{old}$	volume of water in each subregion at the previous time level, [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_t$	volume of water in the flow domain at time $t$ , [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_t^e$	volume of water in element $e$ at time $t$ , [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_0$	volume of water in the flow domain at time zero, [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$V_0^e$	volume of water in element $e$ at time zero, [ $L^2$ ] or [ $L^3$ ] <sup>+</sup>
$W$	total amount of energy in the flow region, [ $MLT^{-2}$ ] or [ $ML^2 T^{-2}$ ] <sup>+</sup>
$x^*$	empirical parameter in the root distribution function [L]
$x_i$	spatial coordinates ( $i=1,2,3$ ) [L]
$X_m$	maximum rooting length in the $x$ -direction [L]
$y^*$	empirical parameter in the root distribution function [L]
$Y_m$	maximum rooting length in the $y$ -direction [L]



$z^*$	empirical parameter in the root distribution function [L]
$z_0$	coordinate of the location where the straining process starts [L]
$Z_0$	characteristic impedance of a transmission line analog to drain
$Z_0'$	characteristic impedance of free space ( $\approx 376.7$ ohms)
$Z_m$	maximum rooting length in the $z$ -direction [L]
$\alpha$	coefficient in the soil water retention function [ $L^{-1}$ ]
$\alpha$	dimensionless water stress response function [-]
$\alpha$	sticking efficiency (ratio of the rate of particles that stick to a collector to the rate they strike the collector) [-]
$\alpha^d$	value of $\alpha$ for a drying branch of the soil water retention function [ $L^{-1}$ ]
$\alpha^w$	value of $\alpha$ for a wetting branch of the soil water retention function [ $L^{-1}$ ]
$\alpha^w$	weighing factor [-]
$\alpha_h$	scaling factor for the pressure head [-]
$\alpha_h^*$	temperature scaling factor for the pressure head [-]
$\alpha_K$	scaling factor for the hydraulic conductivity [-]
$\alpha_K^*$	temperature scaling factor for the hydraulic conductivity [-]
$\alpha_\theta$	scaling factor for the water content [-]
$\beta$	empirical constant in adsorption isotherm [-]
$\beta$	empirical factor in the blocking function [-]
$\gamma_g$	zero-order rate constant for solutes in the gas phase [ $ML^{-3}T^{-1}$ ]
$\gamma_i$	activity coefficient in soil solution [ $L^3M^{-1}$ ] ( $1 \text{ mol}^{-1}$ )
$\gamma_s$	zero-order rate constant for solutes adsorbed onto the solid phase [ $T^{-1}$ ]
$\gamma_w$	zero-order rate constants for solutes in the liquid phase [ $ML^{-3}T^{-1}$ ]
$\gamma_e$	boundary segments connected to node $n$
$\Gamma_D$	part of flow domain boundary where Dirichlet type conditions are specified
$\Gamma_G$	part of flow domain boundary where gradient type conditions are specified
$\Gamma_N$	part of flow domain boundary where Neumann type conditions are specified
$\Gamma_C$	part of flow domain boundary where Cauchy type conditions are specified
$\delta_{ij}$	Kronecker delta [-]
$\Delta t$	time increment [T]

$\Delta t_{max}$	maximum permitted time increment [T]
$\Delta t_{min}$	minimum permitted time increment [T]
$\varepsilon$	temporal weighing factor [-]
$\varepsilon_a^c$	absolute error in the solute mass balance, [ML <sup>-1</sup> ] or [M] <sup>+</sup>
$\varepsilon_a^w$	absolute error in the water mass balance, [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup>
$\varepsilon_r^c$	relative error in the solute mass balance [%]
$\varepsilon_r^w$	relative error in the water mass balance [%]
$\varepsilon_0$	permittivity of free space (used in electric analog representation of drains)
$\eta$	empirical constant in adsorption isotherm [L <sup>3</sup> M <sup>-3</sup> ]
$\eta$	single-collector efficiency [-]
$\theta$	volumetric water content [L <sup>3</sup> L <sup>-3</sup> ]
$\theta^*$	scaled volumetric water content [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_a$	parameter in the soil water retention function [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_k$	volumetric water content corresponding to $K_k$ [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_m$	parameter in the soil water retention function [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_m^d$	parameter in soil water retention function; drying branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_m^w$	parameter in soil water retention function; wetting branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_n$	volumetric solid phase fraction [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_o$	volumetric organic matter fraction [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_r$	residual soil water content [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_r^*$	scaled residual soil water content [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_r^d$	residual soil water content of the main drying branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_r^w$	residual soil water content of the main wetting branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_s$	saturated soil water content [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_s^d$	saturated soil water content of the main drying branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_s^w$	saturated soil water content of the main wetting branch [L <sup>3</sup> L <sup>-3</sup> ]
$\theta_{\Delta}$	water content at the reversal point of a hysteretic retention function [L <sup>3</sup> L <sup>-3</sup> ]
$\kappa$	parameter which depends on the type of flow being analyzed, [-] or [L] <sup>+</sup>
$\lambda$	first-order rate constant [T <sup>-1</sup> ]
$\lambda_{ij}$	apparent thermal conductivity tensor of the soil [MLT <sup>-3</sup> K <sup>-1</sup> ] (e.g. Wm <sup>-1</sup> K <sup>-1</sup> )

$\lambda_L$	longitudinal thermal dispersivity [L]
$\lambda_T$	transverse thermal dispersivity [L]
$\lambda_0$	thermal conductivity of porous medium in the absence of flow [ $\text{MLT}^{-3}\text{K}^{-1}$ ] (e.g. $\text{W m}^{-1}\text{K}^{-1}$ )
$\mu$	fluid viscosity (= 0.00093 Pa s) [ $\text{ML}^{-1}\text{T}^{-1}$ ]
$\mu_g$	first-order rate constant for solutes in the gas phase [ $\text{T}^{-1}$ ]
$\mu_{ref}$	dynamic viscosity at reference temperature $T_{ref}$ [ $\text{MT}^{-1}\text{L}^{-1}$ ]
$\mu_s$	first-order rate constant for solutes adsorbed onto the solid phase [ $\text{T}^{-1}$ ]
$\mu_T$	dynamic viscosity at temperature $T$ [ $\text{MT}^{-1}\text{L}^{-1}$ ]
$\mu_w$	first-order rate constant for solutes in the liquid phase [ $\text{T}^{-1}$ ]
$\mu_g'$	first-order rate constant for chain solutes in the gas phase [ $\text{T}^{-1}$ ]
$\mu_s'$	first-order rate constant for chain solutes adsorbed onto the solid phase [ $\text{T}^{-1}$ ]
$\mu_w'$	first-order rate constant for chain solutes in the liquid phase [ $\text{T}^{-1}$ ]
$\xi_i$	activity coefficient on the exchange surfaces [ $\text{MM}^{-1}$ ] ( $\text{kg mol}^{-1}$ )
$\rho$	bulk density of porous medium [ $\text{ML}^{-3}$ ]
$\rho_d$	dimensionless ratio between the side of the square in the finite element mesh surrounding the drain, $D$ , and the effective diameter of a drain, $d_e$ [-]
$\rho_f$	fluid density (= 998 $\text{kg m}^{-3}$ ) [ $\text{ML}^{-3}$ ]
$\rho_{ref}$	density of soil water at reference temperature $T_{ref}$ [ $\text{ML}^{-3}$ ]
$\rho_p$	bacterial density (= 1080 $\text{kg m}^{-3}$ ) [ $\text{ML}^{-3}$ ]
$\rho_T$	density of soil water at temperature $T$ [ $\text{ML}^{-3}$ ]
$\sigma_{ref}$	surface tension at reference temperature $T_{ref}$ [ $\text{MT}^{-2}$ ]
$\sigma_T$	surface tension at temperature $T$ [ $\text{MT}^{-2}$ ]
$\sigma_1$	prescribed flux boundary condition at boundary $\Gamma_N$ [ $\text{LT}^{-1}$ ]
$\sigma_2$	prescribed gradient boundary condition at boundary $\Gamma_G$ [-]
$\tau_a$	tortuosity factor in the gas phase [-]
$\tau_w$	tortuosity factor in the liquid phase [-]
$\phi_n$	linear basis functions [-]
$\phi_n^u$	upstream weighted basis functions [-]
$\psi$	prescribed pressure head boundary condition at boundary $\Gamma_D$ [L]

$\psi$	dimensionless colloid retention function [-]
$\omega$	first-order adsorption rate constant [T <sup>-1</sup> ]
$\omega_a$	angle between principal direction of $K_1^A$ and the $x$ -axis of the global coordinate system [-]
$\omega_s$	performance index used as a criterion to minimize or eliminate numerical oscillations [-]
$\Omega$	flow region
$\Omega_e$	domain occupied by element $e$
$\Omega_R$	region occupied by the root zone

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<sup>+</sup> for plane (2D) and axisymmetric (or 3D) flow, respectively

## 1. INTRODUCTION

The importance of the unsaturated zone as an integral part of the hydrological cycle has long been recognized. The zone plays an inextricable role in many aspects of hydrology, including infiltration, soil moisture storage, evaporation, plant water uptake, groundwater recharge, runoff and erosion. Initial studies of the unsaturated (vadose) zone focused primarily on water supply studies, inspired in part by attempts to optimally manage the root zone of agricultural soils for maximum crop production. Interest in the unsaturated zone has dramatically increased in recent years because of growing concern that the quality of the subsurface environment is being adversely affected by agricultural, industrial and municipal activities. Federal, state and local action and planning agencies, as well as the public at large, are now scrutinizing the intentional or accidental release of surface-applied and soil-incorporated chemicals into the environment. Fertilizers and pesticides applied to agricultural lands inevitably move below the soil root zone and may contaminate underlying groundwater reservoirs. Chemicals migrating from municipal and industrial disposal sites similarly represent environmental hazards. The same is true for radionuclides emanating from nuclear waste disposal facilities.

The past several decades has seen considerable progress in the conceptual understanding and mathematical description of water flow and solute transport processes in the unsaturated zone. A variety of analytical and numerical models are now available to predict water and/or solute transfer processes between the soil surface and the groundwater table. The most popular models remain the Richards' equation for variably saturated flow, and the Fickian-based convection-dispersion equation for solute transport. Deterministic solutions of these classical equations have been used, and likely will continue to be used in the near future, for (1) predicting water and solute movement in the vadose zone, (2) analyzing specific laboratory or field experiments involving unsaturated water flow and/or solute transport, and (3) extrapolating information from a limited number of field experiments to different soil, crop and climatic conditions, as well as to different soil and water management schemes.

Once released into the subsurface environment, industrial and agricultural chemicals are generally subjected to a large number of simultaneous physical, chemical, and biological processes, including sorption-desorption, volatilization, photolysis, and biodegradation, as well as their kinetics. The extent of degradation, sorption and volatilization largely determines the persistence of a pollutant in the subsurface [*Chiou*, 1989]. For example, the fate of organic chemicals in soils is known to be strongly affected by the kinetics of biological degradation. *Alexander and Scow* [1989]

gave a review of some of the equations used to represent the kinetics of biodegradation. These equations include zero-order, half-order, first-order, three-half-order, mixed-order, logistic, logarithmic, Michaelis-Menton, and Monod type (with or without growth) expressions. While most of these expressions have a theoretical bases, they are commonly used only in an empirical fashion by fitting the equations to observed data. Zero- and first-order kinetic equations remain the most popular for describing biodegradation of organic compounds, mostly because of their simplicity and the ease at which they can be incorporated in solute transport models. Conditions for the application of these two equations are described by *Alexander and Scow* [1989].

One special group of degradation reactions involves decay chains in which solutes are subject to sequential (or consecutive) decay reactions. Problems of solute transport involving sequential first-order decay reactions frequently occur in soil and groundwater systems. Examples are the migration of various radionuclides [*Lester et al.*, 1975; *Rogers*, 1978; *Gureghian*, 1981; *Gureghian and Jansen*, 1983], the simultaneous movement of interacting nitrogen species [*Cho*, 1971; *Misra et al.*, 1974; *Wagenet et al.*, 1976; *Tillotson et al.*, 1980], organic phosphate transport [*Castro and Rolston*, 1977], and the transport of certain pesticides and their metabolites [*Bromilow and Leistra*, 1980; *Wagenet and Hutson*, 1987].

While in the past most pesticides were regarded as involatile, volatilization is now increasingly recognized as being an important process affecting the fate of pesticides in field soils [*Glotfelty and Schomburg*, 1989; *Spencer*, 1991]. Another process affecting pesticide fate and transport is the relative reactivity of solutes in the sorbed and solution phases. Several processes such as gaseous and liquid phase molecular diffusion, and convective-dispersive transport, act only on solutes that are not adsorbed. Degradation of organic compounds likely occurs mainly, or even exclusively, in the liquid phase [*Pignatello*, 1989]. On the other side, radioactive decay takes place equally in the solution and adsorbed phases, while other reactions or transformations may occur only or primarily in the sorbed phase.

Several analytical solutions have been published for simplified transport systems involving consecutive decay reactions [*Cho*, 1971; *Wagenet et al.*, 1976; *Harada et al.*, 1980; *Higashi and Pigford*, 1980; *van Genuchten*, 1985]. Unfortunately, analytical solutions for more complex situations, such as for transient water flow or the nonequilibrium solute transport with nonlinear reactions, are not available and/or cannot be derived, in which case numerical models must be employed. To be useful, such numerical models must allow for different reaction rates to take place in the solid, liquid, and gaseous phases, as well as for a correct distribution of the solutes among the different phases.

The purpose of this technical report is to document version 1.0 of the HYDRUS software package simulating **two-** and **three-dimensional** variably-saturated water flow, heat movement, and transport of solutes involved in sequential first-order decay reactions. The software package consists of several computational programs [h2d\_calc.exe (2D direct), h2d\_clci.exe (2D inverse), h2d\_wtld.exe (wetland), and h3d\_calc.exe (3D direct)] and the interactive graphics-based user interface HYDRUS. The HYDRUS program numerically solves the Richards equation for saturated-unsaturated water flow and convection-dispersion type equations for heat and solute transport. The flow equation incorporates a sink term to account for water uptake by plant roots. The heat transport equation considers movement by conduction as well as convection with flowing water. The governing convection-dispersion solute transport equations are written in a very general form by including provisions for nonlinear nonequilibrium reactions between the solid and liquid phases, and linear equilibrium reaction between the liquid and gaseous phases. Hence, both adsorbed and volatile solutes such as pesticides can be considered. The solute transport equations also incorporate the effects of zero-order production, first-order degradation independent of other solutes, and first-order decay/production reactions that provides the required coupling between the solutes involved in the sequential first-order chain. The transport models also account for convection and dispersion in the liquid phase, as well as for diffusion in the gas phase, thus permitting one to simulate solute transport simultaneously in both the liquid and gaseous phases. HYDRUSD at present considers up to fifteen solutes which can be either coupled in a unidirectional chain or may move independently of each other. Physical nonequilibrium solute transport can be accounted for by assuming a two-region, dual porosity type formulation which partition the liquid phase into mobile and immobile regions. Attachment/detachment theory, including the filtration theory, is included to simulate transport of viruses, colloids, and/or bacteria.

The program may be used to analyze water and solute movement in unsaturated, partially saturated, or fully saturated porous media. HYDRUS can handle flow domains delineated by irregular boundaries. The flow region itself may be composed of nonuniform soils having an arbitrary degree of local anisotropy. Flow and transport can occur in the vertical plane, the horizontal plane, a three-dimensional region exhibiting radial symmetry about a vertical axis, or in a three-dimensional region. The water flow part of the model considers prescribed head and flux boundaries, boundaries controlled by atmospheric conditions, free drainage boundary conditions, as well as a simplified representation of nodal drains using results of electric analog experiments. First- or third-type boundary conditions can be implemented in both the solute and heat transport parts of the model. In addition, HYDRUS implements a Marquardt-Levenberg type parameter estimation

scheme for inverse estimation of soil hydraulic and/or solute transport and reaction parameters from measured transient or steady-state flow and/or transport data for two-dimensional problem.

The governing flow and transport equations are solved numerically using Galerkin-type linear finite element schemes. Depending upon the size of the problem, the matrix equations resulting from discretization of the governing equations are solved using either Gaussian elimination for banded matrices, or the conjugate gradient method for symmetric matrices and the ORTHOMIN method for asymmetric matrices [Mendoza *et al.*, 1991]. The program is an extension of the variably saturated flow codes HYDRUS-2D of Šimůnek *et al.* [1999], SWMS\_3D of Šimůnek *et al.* [1995], SWMS\_2D of Šimůnek *et al.* [1992] and CHAIN\_2D of Šimůnek and van Genuchten [1994], which in turn were based in part on the early numerical work of Vogel [1987] and Neuman and colleagues [Neuman, 1972, 1973, Neuman *et al.*, 1974; Neuman, 1975; Davis and Neuman, 1983].

Even with an abundance of well-documented models now being available, one major problem often preventing their optimal use is the extensive work required for data preparation, numerical grid design, and graphical presentation of the output results. Hence, the more widespread use of multi-dimensional models requires ways which make it easier to create, manipulate and display large data files, and which facilitate interactive data management. Introducing such techniques will free users from cumbersome manual data processing, and should enhance the efficiency in which programs are being implemented for a particular example. To avoid or simplify the preparation and management of relatively complex input data files for two- and three-dimensional applications, and to graphically display the final simulation results, we developed an interactive graphics-based user-friendly interface HYDRUS for the MS Windows 95, 98, NT, ME, and XP environments.

The HYDRUS software is distributed in the following forms (Levels):

1) Level **2D-Light** includes the executable code HYDRUS (h2d\_calc.exe and h2d\_clci.exe) and a graphics-based user interface, so as to facilitate data preparation and output display in the MS WINDOWS 95, 98, 2000, NT, and/or XP environments. A mesh generator for relatively simple rectangular domain geometry is made part of option A. The user interface is written in MS Visual C++. Because HYDRUS was written in Microsoft FORTRAN, this code uses several extensions that are not part of ANSI-standard FORTRAN, such as dynamically allocated arrays.

2) Level **2D-Standard** consists of **2D-Light**, but further augmented with a CAD program MESHGEN2D for designing more general domain geometry, and its discretization into an unstructured finite element mesh for a variety of problems involving variably-saturated subsurface flow and transport. Option B is also distributed on a CD ROM and web.



3) Level **3D-Light** includes **2D-Standard** above and a mesh generator for relatively simple hexagonal three-dimensional domain geometry.

4) Level **3D-Standard** includes **3D-Light**, and a mesh generator that can generate unstructured meshes for general two-dimensional geometries, that can be extended into a three dimensional transport domains.

A general overview of the graphics-based interface is described in the accompanying user manual. In addition to the detailed description in the accompanying user manual, extensive on-line help files are available with each module of the user interface.

Demo version of the program, the input and output files of examples discussed in this report, plus many additional examples which illustrate the interface and the program in its full complexity, can be downloaded from [www.hydrus3d.com](http://www.hydrus3d.com).



## 2. VARIABLY SATURATED WATER FLOW

### 2.1. Governing Flow Equation

#### 2.1.1. Uniform Flow

Consider two- and/or three-dimensional isothermal uniform Darcian flow of water in a variably saturated rigid porous medium and assume that the air phase plays an insignificant role in the liquid flow process. The governing flow equation for these conditions is given by the following modified form of the Richards' equation:

$$\frac{\partial \theta}{\partial t} = \frac{\partial}{\partial x_i} \left[ K \left( K_{ij}^A \frac{\partial h}{\partial x_j} + K_{iz}^A \right) \right] - S \quad (2.1)$$

where  $\theta$  is the volumetric water content [ $L^3L^{-3}$ ],  $h$  is the pressure head [L],  $S$  is a sink term [ $T^{-1}$ ],  $x_i$  ( $i=1,2$ ) are the spatial coordinates [L],  $t$  is time [T],  $K_{ij}^A$  are components of a dimensionless anisotropy tensor  $\mathbf{K}^A$ , and  $K$  is the unsaturated hydraulic conductivity function [ $LT^{-1}$ ] given by

$$K(h, x, y, z) = K_s(x, y, z) K_r(h, x, y, z) \quad (2.2)$$

where  $K_r$  is the relative hydraulic conductivity and  $K_s$  the saturated hydraulic conductivity [ $LT^{-1}$ ]. The anisotropy tensor  $K_{ij}^A$  in (2.1) is used to account for an anisotropic medium. The diagonal entries of  $K_{ij}^A$  equal one and the off-diagonal entries zero for an isotropic medium. If (2.1) is applied to planar flow in a vertical cross-section,  $x_1=x$  is the horizontal coordinate and  $x_2=z$  is the vertical coordinate, the latter taken to be positive upward. Einstein's summation convention is used in (2.1) and throughout this report. Hence, when an index appears twice in an algebraic term, this particular term must be summed over all possible values of the index.

#### 2.1.2. Flow in a Dual-Porosity System

Dual-porosity models assume that water flow is restricted to the fractures (or inter-aggregate pores and macropores), and that water in the matrix (intra-aggregate pores or the rock

matrix) does not move at all. These models assume that the matrix, consisting of immobile water pockets, can exchange, retain, and store water, but does not permit convective flow. This conceptualization leads to two-region, dual-porosity type flow and transport models [Philip, 1968; van Genuchten and Wierenga, 1976] that partition the liquid phase into mobile (flowing, inter-aggregate),  $\theta_m$ , and immobile (stagnant, intra-aggregate),  $\theta_{im}$ , regions:

$$\theta = \theta_m + \theta_{im} \quad (2.3)$$

with some exchange of water and/or solutes possible between the two regions, usually calculated by means of a first-order rate equation. We will use here the subscript  $m$  to represent fractures, inter-aggregate pores, or macropores, and the subscript  $im$  to represent the soil matrix, intra-aggregate pores, or the rock matrix.

The dual-porosity formulation for water flow as used in HYDRUS-1D is based on a mixed formulation, which uses Richards equation (2.1) to describe water flow in the fractures (macropores), and a simple mass balance equation to describe moisture dynamics in the matrix as follows [Šimůnek *et al.*, 2003]:

$$\begin{aligned} \frac{\partial \theta_m}{\partial t} &= \frac{\partial}{\partial z} \left[ K(h) \left( \frac{\partial h}{\partial x} + \cos \alpha \right) \right] - S_m - \Gamma_w \\ \frac{\partial \theta_{im}}{\partial t} &= -S_{im} + \Gamma_w \end{aligned} \quad (2.4)$$

where  $S_m$  and  $S_{im}$  are sink terms for both regions, and  $\Gamma_w$  is the transfer rate for water from the inter- to the intra-aggregate pores.

An alternative dual-porosity approach, not implemented in HYDRUS-1D, was suggested by Germann [1985] and Germann and Beven [1985], who used a kinematic wave equation to describe gravitational movement of water in macropores. Although dual-porosity models have been popularly used for solute transport studies (e.g. van Genuchten [1981]), they have not thus far been used to water flow problems.

## 2.2. Root Water Uptake

### 2.2.1. Root Water Uptake without Compensation

The sink term,  $S$ , in (2.1) represents the volume of water removed per unit time from a unit volume of soil due to plant water uptake. *Feddes et al.* [1978] defined  $S$  as

$$S(h) = \alpha(h)S_p \quad (2.5)$$

where the water stress response function  $\alpha(h)$  is a prescribed dimensionless function (Fig. 2.1) of the soil water pressure head ( $0 \leq \alpha \leq 1$ ), and  $S_p$  is the potential water uptake rate [ $T^{-1}$ ]. Figure 2.1 gives a schematic plot of the stress response function as used by *Feddes et al.* [1978]. Notice that water uptake is assumed to be zero close to saturation (i.e., wetter than some arbitrary "anaerobiosis point",  $h_1$ ). For  $h < h_4$  (the wilting point pressure head), water uptake is also assumed to be zero. Water uptake is considered optimal between pressure heads  $h_2$  and  $h_3$ , whereas for pressure head between  $h_3$  and  $h_4$  (or  $h_1$  and  $h_2$ ), water uptake decreases (or increases) linearly with  $h$ . The variable  $S_p$  in (2.5) is equal to the water uptake rate during periods of no water stress when  $\alpha(h) = 1$ . *van Genuchten* [1987] expanded the formulation of Feddes by including osmotic stress as follows

$$S(h, h_\phi) = \alpha(h, h_\phi) S_p \quad (2.6)$$

where  $h_\phi$  is the osmotic head [L], which is assumed here to be given by a linear combination of the concentrations,  $c_i$ , of all solutes present, i.e.,

$$h_\phi = a_i c_i \quad (2.7)$$

in which  $a_i$  are experimental coefficients [ $L^4 M$ ] converting concentrations into osmotic heads. *van Genuchten* [1987] proposed an alternative S-shaped function to describe the water uptake stress response function (Fig. 2.1), and suggested that the influence of the osmotic head reduction can be either additive or multiplicative as follows

$$\alpha(h, h_\phi) = \frac{1}{1 + \left( \frac{h + h_\phi}{h_{50}} \right)^p} \quad h + h_\phi > h_4$$

$$\alpha(h, h_\phi) = 0. \quad h + h_\phi < h_4 \quad (2.8)$$

or

$$\alpha(h, h_\phi) = \frac{1}{1 + (h/h_{50})^{p_1}} \frac{1}{1 + (h_\phi/h_{\phi 50})^{p_2}} \quad (2.9)$$

respectively, where  $p$ ,  $p_1$ , and  $p_2$  are experimental constants. The exponent  $p$  was found to be approximately 3 when applied to salinity stress data only [van Genuchten, 1987]. The parameter  $h_{50}$  in (2.8) and (2.9) represents the pressure head at which the water extraction rate is reduced by 50% during conditions of negligible osmotic stress. Similarly,  $h_{\phi 50}$  represents the osmotic head at which the water extraction rate is reduced by 50% during conditions of negligible water stress. Note that, in contrast to the expression of Feddes *et al.* [1978], this formulation of the stress response function,  $\alpha(h, h_\phi)$ , does not consider a transpiration reduction near saturation. Such a simplification seems justified when saturation occurs for only relatively short periods of time.

When the potential water uptake rate is equally distributed over a two-dimensional rectangular root domain,  $S_p$  becomes

$$S_p = \frac{1}{L_x L_z} S_t T_p \quad (2.10)$$

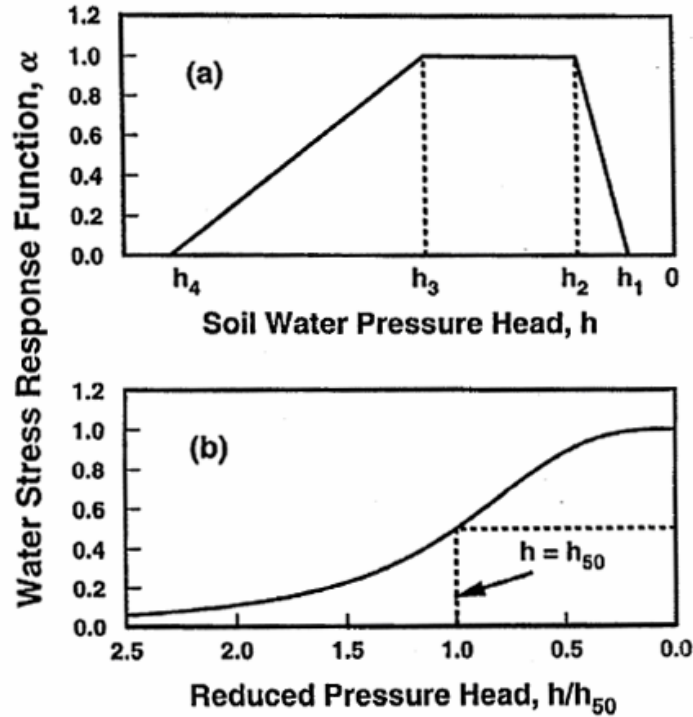


Figure 2.1. Schematic of the plant water stress response function,  $\alpha(h)$ , as used by a) Feddes *et al.* [1978] and b) van Genuchten [1987].

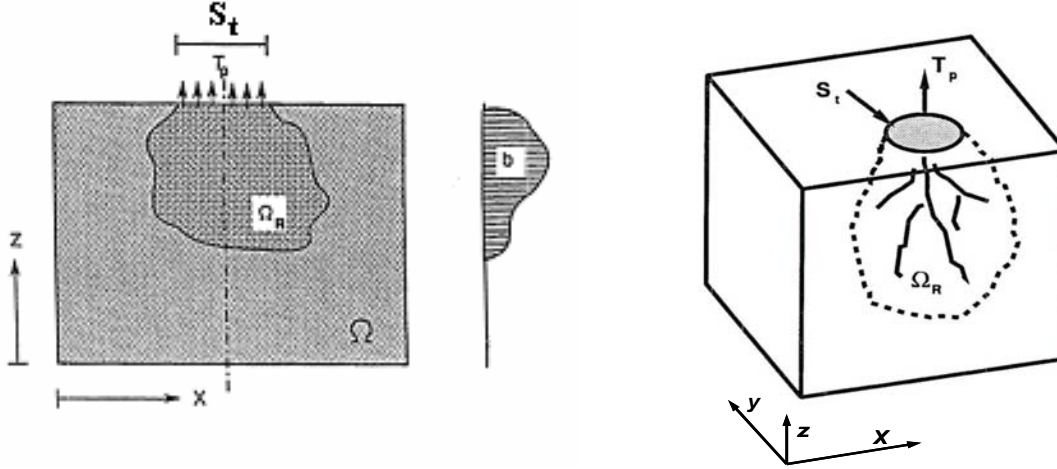


Figure 2.2. Schematic of the potential water uptake distribution function,  $b(x,y,z)$ , in the soil root zone.

where  $T_p$  is the potential transpiration rate [ $LT^{-1}$ ],  $L_z$  is the depth [L] of the root zone,  $L_x$  is the width [L] of the root zone, and  $S_t$  is the width [L] of the soil surface associated with the transpiration process. Notice that  $S_p$  reduces to  $T_p/L_z$  when  $S_t=L_x$ . For three-dimensional problems, (2.10) additionally includes the width of the  $y$ -direction,  $L_y$  [L], and  $S_t$  becomes the soil surface associated with transpiration [ $L^2$ ] (Figure 2.2, right).

Equation (2.10) may be generalized by introducing a non-uniform distribution of the potential water uptake rate over a root zone of arbitrary shape [Vogel, 1987]:

$$S_p = b(x, y, z)S_t T_p \quad (2.11)$$

where  $b(x,y,z)$  is the normalized water uptake distribution [ $L^{-2}$  or  $L^{-3}$ ]. This function describes the spatial variation of the potential extraction term,  $S_p$ , over the root zone (Fig. 2.2), and is obtained from  $b'(x,y,z)$  as follows

$$b(x, y, z) = \frac{b'(x, y, z)}{\int_{\Omega_R} b'(x, y, z) d\Omega} \quad (2.12)$$

where  $\Omega_R$  is the region occupied by the root zone, and  $b'(x,y,z)$  is an arbitrarily prescribed distribution function. Normalizing the uptake distribution ensures that  $b(x,y,z)$  integrates to unity

over the flow domain, i.e.,

$$\int_{\Omega_R} b(x, y, z) d\Omega = 1 \quad (2.13)$$

From (2.11) and (2.13) it follows that  $S_p$  is related to  $T_p$  by the expression

$$\frac{1}{S_t} \int_{\Omega_R} S_p d\Omega = T_p \quad (2.14)$$

The actual water uptake distribution is obtained by substituting (2.11) into (2.5):

$$S(h, h_\phi, x, y, z) = \alpha(h, h_\phi, x, y, z) b(x, y, z) S_t T_p \quad (2.15)$$

whereas the actual transpiration rate,  $T_a$ , is obtained by integrating (2.15) as follows

$$T_a = \frac{1}{S_t} \int_{\Omega_R} S d\Omega = T_p \int_{\Omega_R} \alpha(h, h_\phi, x, y, z) b(x, y, z) d\Omega \quad (2.16)$$

### 2.2.2. Root Water Uptake with Compensation

The ratio of actual to potential transpiration of the root uptake without compensation is defined as follows:

$$\frac{T_a}{T_p} = \frac{1}{T_p} \int_{\Omega_R} S(h, h_\phi, x, y, z) d\Omega = \int_{\Omega_R} \alpha(h, h_\phi, x, y, z) b(x, y, z) d\Omega = \omega \quad (2.17)$$

where  $\omega$  is a dimensionless water stress index [Jarvis, 1989]. Following Jarvis [1989], we introduce a critical value of the water stress index  $\omega_c$ , a so-called the root adaptability factor, which represents a threshold value above which root water uptake reduced in stressed parts of the root zone is fully compensated by increased uptake from other parts. However, some reduction in potential transpiration will occur below this threshold value, although smaller than



for water uptake without compensation.

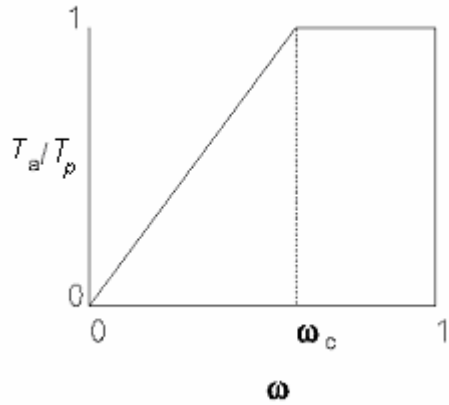


Figure 2.3. Ratio of actual to potential transpiration as a function of the stress index  $\omega$ .

Thus, for the interval when  $\omega$  is larger than the threshold value  $\omega_c$  (Fig. 2.3), one obtains

$$S(h, h_\phi, x, y, z) = \alpha(h, h_\phi, x, y, z) b(x, y, z) \frac{T_p}{\omega}$$

$$\frac{T_a}{T_p} = \frac{\int_{L_R} \alpha(h, h_\phi, x, y, z) b(x, y, z) dx}{\omega} = \frac{\omega}{\omega} = 1 \quad (2.18)$$

While for the interval when  $\omega$  is smaller than the threshold value  $\omega_c$ , one has

$$S(h, h_\phi, x, y, z) = \alpha(h, h_\phi, x, y, z) b(x, y, z) \frac{T_p}{\omega_c}$$

$$\frac{T_a}{T_p} = \frac{\int_{L_R} \alpha(h, h_\phi, x, y, z) b(x, y, z) dx}{\omega_c} = \frac{\omega}{\omega_c} < 1 \quad (2.19)$$

When the parameter  $\omega_c$  is equal to one we hence have noncompensated root water uptake, and when  $\omega_c$  is equal to zero we obtain fully compensated uptake.

### 2.2.3. Spatial Root Distribution Functions

Following two- and three-dimensional root distribution functions are implemented into HYDRUS [Vrugt *et al.*, 2001, 2002]:

$$b(x, z) = \left(1 - \frac{z}{Z_m}\right) \left(1 - \frac{x}{X_m}\right) e^{-\left(\frac{p_z}{Z_m}|z^* - z| + \frac{p_x}{X_m}|x^* - x|\right)} \quad (2.20)$$

$$b(x, y, z) = \left(1 - \frac{x}{X_m}\right) \left(1 - \frac{y}{Y_m}\right) \left(1 - \frac{z}{Z_m}\right) e^{-\left(\frac{p_x}{X_m}|x^* - x| + \frac{p_y}{Y_m}|y^* - y| + \frac{p_z}{Z_m}|z^* - z|\right)} \quad (2.21)$$

where  $X_m$ ,  $Y_m$ , and  $Z_m$  are the maximum rooting lengths in the  $x$ -,  $y$ -, and  $z$ - directions [L], respectively;  $x$ ,  $y$ , and  $z$  are distances from the origin of the tree in the  $x$ -,  $y$ -, and  $z$ - directions [L], respectively;  $p_x$  [-],  $p_y$  [-],  $p_z$  [-],  $x^*$  [L],  $y^*$  [L], and  $z^*$  [L] are empirical parameters, and  $b(x, z)$  and  $b(x, y, z)$  denote two- and three-dimensional spatial distribution of the potential root water uptake [-]. Following Vrugt *et al.* [2002], we set  $p_x$ ,  $p_y$  and  $p_z$  to unity for  $z > z^*$ ,  $x > x^*$  and  $y > y^*$ , respectively. Vrugt *et al.* [2001] showed that the root water uptake in (2.20) is extremely flexible and allows spatial variations of water uptake as influenced by non-uniform water application (e.g. drip irrigation) and root length density patterns. See Vrugt *et al.* [2001, 2002] for different configurations of normalized spatial distribution of potential root water uptake.

### 2.3. The Unsaturated Soil Hydraulic Properties

The unsaturated soil hydraulic properties,  $\theta(h)$  and  $K(h)$ , in (2.1) are in general highly nonlinear functions of the pressure head. HYDRUS permits the use of five different analytical models for the hydraulic properties [Brooks and Corey, 1964; van Genuchten, 1980; and Vogel and Císlerová, 1988; Kosugi, 1995, Durner, 1994].

The soil water retention,  $\theta(h)$ , and hydraulic conductivity,  $K(h)$ , functions according to Brooks and Corey [1964] are given by

$$S_e = \begin{cases} |\alpha h|^{-n} & h < -1/\alpha \\ 1 & h \geq -1/\alpha \end{cases} \quad (2.22)$$

$$K = K_s S_e^{2/n+2} \quad (2.23)$$

respectively, where  $S_e$  is the effective water content,

$$S_e = \frac{\theta - \theta_r}{\theta_s - \theta_r} \quad (2.24)$$

in which  $\theta_r$  and  $\theta_s$  denote the residual and saturated water content, respectively;  $K_s$  is the saturated hydraulic conductivity,  $\alpha$  is the inverse of the air-entry value (or bubbling pressure),  $n$  is a pore-size distribution index, and  $l$  is a pore-connectivity parameter assumed to be 2.0 in the original study of *Brooks and Corey* [1964]. The parameters  $\alpha$ ,  $n$  and  $l$  in HYDRUS are considered to be merely empirical coefficients affecting the shape of the hydraulic functions.

HYDRUS also implements the soil-hydraulic functions of *van Genuchten* [1980] who used the statistical pore-size distribution model of *Mualem* [1976] to obtain a predictive equation for the unsaturated hydraulic conductivity function in terms of soil water retention parameters. The expressions of *van Genuchten* [1980] are given by

$$\theta(h) = \begin{cases} \theta_r + \frac{\theta_s - \theta_r}{[1 + |\alpha h|^n]^m} & h < 0 \\ \theta_s & h \geq 0 \end{cases} \quad (2.25)$$

$$K(h) = K_s S_e^l [1 - (1 - S_e^{1/m})^m]^2 \quad (2.26)$$

where

$$m = 1 - 1/n, \quad n > 1 \quad (2.27)$$

The above equations contain six independent parameters:  $\theta_r$ ,  $\theta_s$ ,  $\alpha$ ,  $n$ ,  $K_s$ , and  $l$ . The pore-connectivity parameter  $l$  in the hydraulic conductivity function was estimated [*Mualem*, 1976] to be about 0.5 as an average for many soils.

A third set of hydraulic equations implemented in HYDRUS are those by *Vogel and Císlerová* [1988] who modified the equations of *van Genuchten* [1980] to add flexibility in the description of the hydraulic properties near saturation. The soil water retention,  $\theta(h)$ , and hydraulic

conductivity,  $K(h)$ , functions of *Vogel and Císlarová* [1988] are given by (Fig. 2.4)

$$\theta(h) = \begin{cases} \theta_a + \frac{\theta_m - \theta_a}{(1 + |\alpha h|^n)^m} & h < h_s \\ \theta_s & h \geq h_s \end{cases} \quad (2.28)$$

and

$$K(h) = \begin{cases} K_s K_r(h) & h \leq h_s \\ K_k + \frac{(h - h_k)(K_s - K_k)}{h_s - h_k} & h_k < h < h_s \\ K_s & h \geq h_s \end{cases} \quad (2.29)$$

respectively, where

$$K_r = \frac{K_k}{K_s} \left( \frac{S_e}{S_{ek}} \right)^{1/2} \left[ \frac{F(\theta_r) - F(\theta)}{F(\theta_r) - F(\theta_k)} \right]^2 \quad (2.30)$$

$$F(\theta) = \left[ 1 - \left( \frac{\theta - \theta_a}{\theta_m - \theta_a} \right)^{1/m} \right]^m \quad (2.31)$$

$$S_{ek} = \frac{\theta_k - \theta_r}{\theta_s - \theta_r} \quad (2.32)$$

The above equations allow for a non-zero minimum capillary height,  $h_s$ , by replacing the parameter  $\theta_s$  in van Genuchten's retention function by a fictitious (extrapolated) parameter  $\theta_m$  slightly larger than  $\theta_s$  as shown in Figure 2.4. While this change from  $\theta_s$  to  $\theta_m$  has little or no effect on the retention curve, the effect on the shape and value of the hydraulic conductivity function can be considerable, especially for fine-textured soils when  $n$  is relatively small (e.g.,  $1.0 < n < 1.3$ ). To increase the flexibility of the analytical expressions, the parameter  $\theta_r$  in the retention function was replaced by the fictitious (extrapolated) parameter  $\theta_a \leq \theta_r$ . The approach maintains the physical meaning of  $\theta_r$  and  $\theta_s$  as measurable quantities. Equation (2.30) assumes that the predicted hydraulic conductivity function is matched to a measured value of the hydraulic conductivity,  $K_k = K(\theta_k)$ , at some water content,  $\theta_k$ , less than or equal to the saturated water content, i.e.,  $\theta_k \leq \theta_s$  and  $K_k \leq K_s$  [*Vogel and Císlarová*, 1988; *Luckner et al.*, 1989]. Inspection of (2.28) through (2.30) shows that the hydraulic

characteristics contain 9 unknown parameters:  $\theta_r$ ,  $\theta_s$ ,  $\theta_a$ ,  $\theta_m$ ,  $\alpha$ ,  $n$ ,  $K_s$ ,  $K_k$ , and  $\theta_k$ . When  $\theta_a = \theta_r$ ,  $\theta_m = \theta_k = \theta_s$  and  $K_k = K_s$ , the soil hydraulic functions of *Vogel and Císlarová* [1988] reduce to the original expressions of *van Genuchten* [1980].

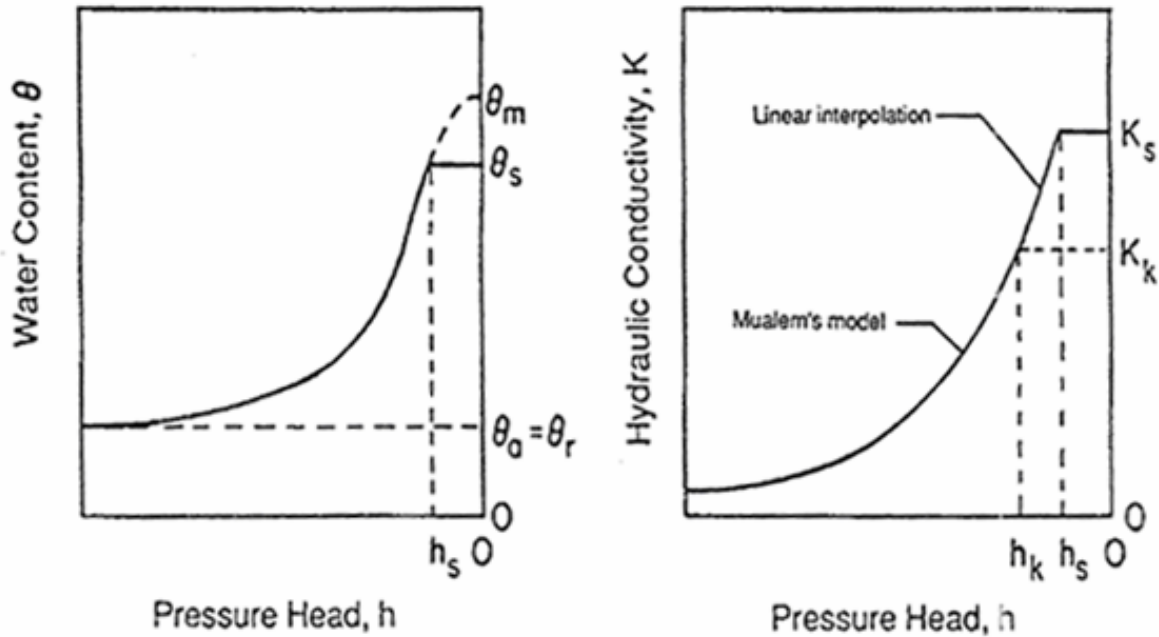


Figure 2.4. Schematics of the soil water retention (a) and hydraulic conductivity (b) functions as given by equations (2.28) and (2.29), respectively.

Version 3.0 of Hydrus allows the soil hydraulic properties to be defined also according to *Kosugi* [1996], who suggested the following lognormal distribution model for  $S_e(h)$ :

$$S_e = \frac{\theta - \theta_r}{\theta_s - \theta_r} = \begin{cases} \frac{1}{2} \operatorname{erfc} \left\{ \frac{\ln(h/\alpha)}{\sqrt{2n}} \right\} & (h < 0) \\ 1 & (h \geq 0) \end{cases} \quad (2.33)$$

Application of Mualem's pore-size distribution model [*Mualem*, 1976] now leads to the following hydraulic conductivity function:

$$K = \begin{cases} K_s S_e^{1/2} \left\{ \frac{1}{2} \operatorname{erfc} \left[ \frac{\ln(h/\alpha)}{\sqrt{2n}} + n \right] \right\}^2 & (h < 0) \\ K_s & (h \geq 0) \end{cases} \quad (2.34)$$

Note that in in this text we use symbols  $\alpha$  instead of  $h_0$  and  $n$  instead of  $\sigma$  as used in *Kosugi* [1996].

*Durner* [1994] divided the porous medium into two (or more) overlapping regions and suggested to use for each of these regions a van Genuchten-Mualem type function [*van Genuchten*, 1980] of the soil hydraulic properties. Linear superposition of the functions for each particular region gives then the functions for the composite multimodal pore system [*Durner et al.*, 1999]:

$$S_e = w_1 [1 + (\alpha_1 h)^{n_1}]^{-m_1} + w_2 [1 + (\alpha_2 h)^{n_2}]^{-m_2} \quad (2.35)$$

Combining this retention model with *Mualem's* [1976] pore-size distribution model leads now to:

$$K(S_e) = K_s \frac{(w_1 S_{e_1} + w_2 S_{e_2})^l \left( w_1 \alpha_1 [1 - (1 - S_{e_1}^{1/m_1})^{m_1}] + w_2 \alpha_2 [1 - (1 - S_{e_2}^{1/m_2})^{m_2}] \right)^2}{(w_1 \alpha_1 + w_2 \alpha_2)^2} \quad (2.36)$$

where  $w_i$  are the weighting factors for the two overlapping regions, and  $\alpha_i$ ,  $n_i$ ,  $m_i$  ( $=1-1/n_i$ ), and  $l$  are empirical parameters of the separate hydraulic functions ( $i=1,2$ ).

An example of composite retention and hydraulic conductivity functions for two overlapping porous media is shown in Figure 2.5. Note that the pressure head axes are on a log scale, which causes the near-saturated values to be significantly enlarged. The fracture domain in this example represents only 2.5% of the entire pore space, but accounts for almost 90% of the hydraulic conductivity close to saturation. Curves similar to those in Figure 2.5 have been used also for fractured rock by *Peters and Klavetter* [1988], *Pruess and Wang* [1987], and *Flint et al.* [2001], among others.

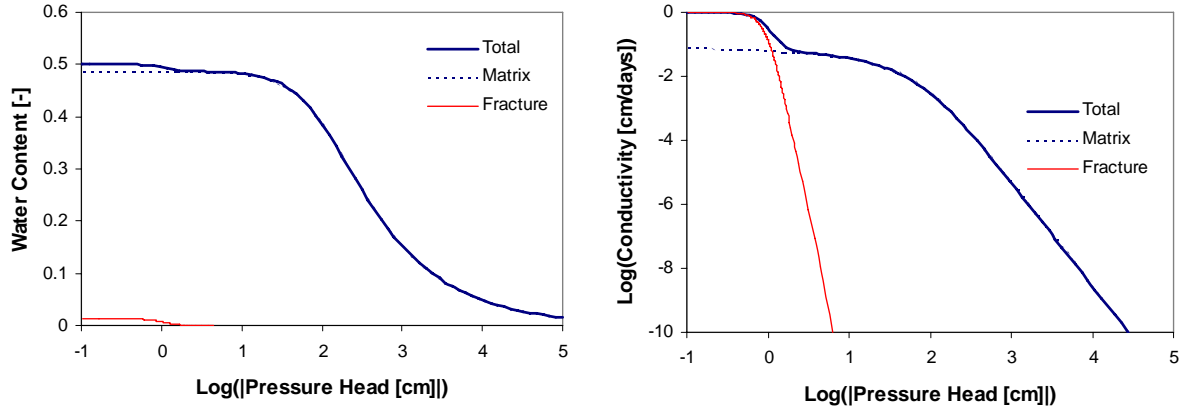


Figure 2.5. Example of composite retention (left) and hydraulic conductivity (right) functions ( $\theta_r=0.00$ ,  $\theta_s=0.50$ ,  $\alpha_1=0.01 \text{ cm}^{-1}$ ,  $n_1=1.50$ ,  $l=0.5$ ,  $K_s=1 \text{ cm d}^{-1}$ ,  $w_1=0.975$ ,  $w_2=0.025$ ,  $\alpha_2=1.00 \text{ cm}^{-1}$ ,  $n_2=5.00$ ).

#### 2.4. Scaling in the Soil Hydraulic Functions

HYDRUS implements a scaling procedure designed to simplify the description of the spatial variability of the unsaturated soil hydraulic properties in the flow domain. The code assumes that the hydraulic variability in a given area can be approximated by means of a set of linear scaling transformations which relate the individual soil hydraulic characteristics  $\theta(h)$  and  $K(h)$  to reference characteristics  $\theta^*(h^*)$  and  $K^*(h^*)$ . The technique is based on the similar media concept introduced by *Miller and Miller* [1956] for porous media which differ only in the scale of their internal geometry. The concept was extended by *Simmons et al.* [1979] to materials which differ in morphological properties, but which exhibit 'scale-similar' soil hydraulic functions. Three independent scaling factors are embodied in HYDRUS. These three scaling parameters may be used to define a linear model of the actual spatial variability in the soil hydraulic properties as follows [*Vogel et al.*, 1991]:

$$\begin{aligned}
 K(h) &= \alpha_K K^*(h^*) \\
 \theta(h) &= \theta_r + \alpha_\theta [\theta^*(h^*) - \theta_r^*] \\
 h &= \alpha_h h^*
 \end{aligned}
 \tag{2.37}$$

in which, for the most general case,  $\alpha_\theta$ ,  $\alpha_h$  and  $\alpha_K$  are mutually independent scaling factors for the water content, the pressure head and the hydraulic conductivity, respectively. Less general scaling methods arise by invoking certain relationships between  $\alpha_\theta$ ,  $\alpha_h$  and/or  $\alpha_K$ . For example, the original

Miller-Miller scaling procedure is obtained by assuming  $\alpha_\theta=1$  (with  $\theta_r^* = \theta_r$ ), and  $\alpha_K=\alpha_h^{-2}$ . A detailed discussion of the scaling relationships given by (2.37), and their application to the hydraulic description of heterogeneous soil profiles, is given by *Vogel et al.* [1991].

## 2.5. Temperature Dependence of the Soil Hydraulic Functions

A similar scaling technique as described above is used in HYDRUS to express the temperature dependence of the soil hydraulic functions. Based on capillary theory that assumes that the influence of temperature on the soil water pressure head can be quantitatively predicted from the influence of temperature on surface tension, *Philip and de Vries* [1957] derived the following equation

$$\frac{dh}{dT} = \frac{h}{\sigma} \frac{d\sigma}{dT} \quad (2.38)$$

where  $T$  is temperature [K] and  $\sigma$  is the surface tension at the air-water interface [ $\text{MT}^{-2}$ ]. From (2.38) it follows that

$$h_T = \frac{\sigma_T}{\sigma_{ref}} h_{ref} = \alpha_h^* h_{ref} \quad (2.39)$$

where  $h_T$  and  $h_{ref}$  ( $\sigma_T$  and  $\sigma_{ref}$ ) are pressure heads (surface tensions) at temperature  $T$  and reference temperature  $T_{ref}$ , respectively; and  $\alpha_h^*$  is the temperature scaling factor for the pressure head.

Following *Constantz* [1982], the temperature dependence of the hydraulic conductivity can be expressed as

$$K_T(\theta) = \frac{\mu_{ref}}{\mu_T} \frac{\rho_T}{\rho_{ref}} K_{ref}(\theta) = \alpha_K^* K_{ref}(\theta) \quad (2.40)$$

where  $K_{ref}$  and  $K_T$  denote hydraulic conductivities at the reference temperature  $T_{ref}$  and soil temperature  $T$ , respectively;  $\mu_{ref}$  and  $\mu_T$  ( $\rho_{ref}$  and  $\rho_T$ ) represent the dynamic viscosity [ $\text{ML}^{-1}\text{T}^{-1}$ ] (density of soil water [ $\text{ML}^{-3}$ ]) at temperatures  $T_{ref}$  and  $T$ , respectively; and  $\alpha_K^*$  is the temperature scaling factor for the hydraulic conductivity.



## 2.6. Hysteresis in the Soil Hydraulic Properties

Applications of unsaturated flow models often assume unique, single-valued (non-hysteretic) functions for  $\theta(h)$  and  $K(h)$  to characterize the hydraulic properties at a certain point in the soil profile. While such a simplification may be acceptable for some flow simulations, many cases require a more realistic description involving hysteresis in the soil hydraulic properties. The HYDRUS code incorporates hysteresis by using the empirical model introduced by *Scott et al.* [1983]. This model was also employed by *Kool and Parker* [1987], who modified the formulation to account for air entrapment. The present version of HYDRUS further extends the model of *Kool and Parker* according to *Vogel et al.* [1996] by considering also hysteresis in the hydraulic conductivity function.

The adopted procedure for modeling hysteresis in the retention function requires that both the main drying and main wetting curves be known (Fig. 2.6). These two curves are described with (2.26) using the parameter vectors  $(\theta_r^d, \theta_s^d, \theta_m^d, \alpha^d, n^d)$  and  $(\theta_r^w, \theta_s^w, \theta_m^w, \alpha^w, n^w)$ , respectively, where the subscripts  $d$  and  $w$  indicate wetting and drying, respectively. The following restrictions are expected to hold in most practical applications:

$$\theta_r^d = \theta_r^w, \alpha^d \leq \alpha^w \quad (2.41)$$

We also invoke the often-assumed restriction

$$n^d = n^w \quad (2.42)$$

If data are lacking, one may use  $\alpha^w = 2\alpha^d$  as a reasonable first approximation [*Kool and Parker*, 1987; *Nielsen and Luckner*, 1992]. We further assume

$$\theta_m^w = \theta_r + \frac{\theta_s^w - \theta_r}{\theta_s^d - \theta_r} (\theta_m^d - \theta_r) \quad (2.43)$$

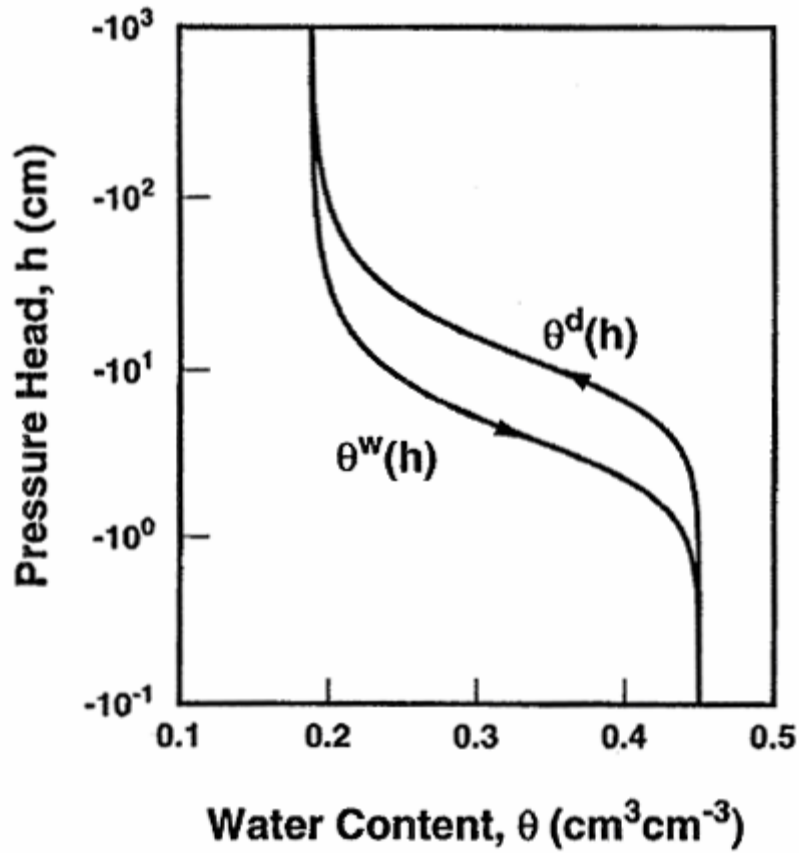


Figure 2.6. Example of a water retention curve showing hysteresis. Shown are the boundary wetting curve,  $\theta^w(h)$ , and the boundary drying curve,  $\theta^d(h)$ .

so that the parameters  $\theta_s$  and  $\alpha$  are the only independent parameters describing hysteresis in the retention function. According to the hysteresis model, drying scanning curves are scaled from the main drying curve, and wetting scanning curves from the main wetting curve. The scaling factors for the drying scanning curves can be obtained by considering the main drying curve as a reference curve in scaling equation (2.37) (keeping  $\alpha_h = 1$  to scale only in the water content direction), i.e.:

$$\theta(h) = \theta_r' + \alpha_\theta [\theta^d(h) - \theta_r^d] \quad (2.44)$$

and forcing each scanning curve,  $\theta(h)$ , to pass through the point  $(\theta_\Delta, h_\Delta)$  characterizing the latest reversal from wetting to drying. Substituting this reversal point into (2.44), and assuming that  $\theta_r = \theta_r^d$ , leads to

$$\alpha_\theta = \frac{\theta_\Delta - \theta_r}{\theta^d(h_\Delta) - \theta_r} \quad (2.45)$$

Note that the scaling procedure results in a fictitious value of the parameter  $\theta_s'$  for the drying scanning curve (this parameter may be located outside of the main hysteresis loop). The scaling relationship is similarly for the wetting scanning curves

$$\theta(h) = \theta_r' + \alpha_\theta [\theta^w(h) - \theta_r] \quad (2.46)$$

in which the fictitious parameter  $\theta_r'$  is now used (again possibly scaled outside of the main loop). The scaling factor  $\alpha_\theta$  for a particular scanning curve can be obtained by substituting the reversal point  $(\theta_\Delta, h_\Delta)$  and the full saturation point  $(\theta_s, 0)$  into (2.46), and subtracting the two resulting equations to eliminate  $\theta_r'$  to give

$$\alpha_\theta = \frac{\theta_\Delta - \theta_s}{\theta^w(h_\Delta) - \theta_s'} \quad (2.47)$$

The parameter  $\theta_r'$  is subsequently determined from (2.46) as  $\theta_r' = \theta_s - \alpha_\theta(\theta_s^w - \theta_r)$ . If the main hysteresis loop is not closed at saturation, the water content at saturation for a particular wetting scanning curve is evaluated using the empirical relationship of *Aziz and Settari* [1979]

$$\theta_s = \theta_s^d - \frac{\theta_s^d - \theta_\Delta}{1 + R(\theta_s^d - \theta_\Delta)}, \quad R = \frac{1}{\theta_s^d - \theta_s^w} - \frac{1}{\theta_s^d - \theta_r^d} \quad (2.48)$$

An analogous hysteretic procedure can be applied to the unsaturated hydraulic conductivity function  $K(h)$ . The main branches  $K^d(h)$  and  $K^w(h)$  of the hysteresis loop are characterized by the same set of parameters as the corresponding retention curves  $\theta^d(h)$  and  $\theta^w(h)$ , and by the saturated conductivities  $K_s^d$  and  $K_s^w$  according to Eq. (2.26). For drying scanning curves we obtain from (2.37)

$$K(h) = \alpha_K K^d(h) \quad (2.49)$$

From knowledge of the reversal point  $(h_{\Delta}, K_{\Delta})$  we obtain

$$\alpha_K = \frac{K_{\Delta}}{K^d(h_{\Delta})} \quad (2.50)$$

For a wetting scanning curve we have now

$$K(h) = K_r' + \alpha_K K^w(h) \quad (2.51)$$

where  $K_r'$  is a fictitious parameter. Substituting the reversal point  $(h_{\Delta}, K_{\Delta})$  and the saturation point  $(0, K_s)$  into (2.40) and solving for  $\alpha_K$  yields

$$\alpha_K = \frac{K_{\Delta} - K_s}{K^w(h_{\Delta}) - K_s^w} \quad (2.52)$$

The fictitious conductivity parameter  $K_r'$  may be obtained from (2.51) as  $K_r' = K_s - \alpha_K K_s^w$ . If the main hysteresis loop is not closed at saturation, the hydraulic conductivity at saturation for a wetting scanning curve is evaluated using equations similar to (2.48), i.e.,

$$K_s = K_s^d - \frac{K_s^d - K_{\Delta}}{1 + R(K_s^d - K_{\Delta})}, \quad R = \frac{1}{K_s^d - K_s^w} - \frac{1}{K_s^d} \quad (2.53)$$

While relatively simple to implement, the above model has been found to suffer from a so-called pumping effect, in which the hysteresis loops can move to physically unrealistic parts of the retention function. As an alternative, we also incorporated in HYDRUS the hysteresis model of *Lenhard et al.* [1991] and *Lenhard and Parker* [1992] that eliminates pumping by keeping track of historical reversal points. We greatly acknowledge the help of Robert Lenhard in this effort.

## 2.7. Initial and Boundary Conditions

The solution of Eq. (2.1) requires knowledge of the initial distribution of the pressure head within the flow domain,  $\Omega$ :

$$h(x, y, z, t) = h_0(x, y, z) \quad \text{for } t = 0 \quad (2.54)$$

where  $h_0$  is a prescribed function of  $x$  and  $z$ .

### 2.7.1. System-Independent Boundary Conditions

HYDRUS implements three types of conditions to describe system-independent interactions along the boundaries of the flow region. These conditions are specified pressure head (Dirichlet type) boundary conditions of the form

$$h(x, y, z, t) = \psi(x, y, z, t) \quad \text{for } (x, y, z) \in \Gamma_D \quad (2.55)$$

specified flux (Neumann type) boundary conditions given by

$$-[K(K_{ij}^A \frac{\partial h}{\partial x_j} + K_{iz}^A)]n_i = \sigma_1(x, y, z, t) \quad \text{for } (x, y, z) \in \Gamma_N \quad (2.56)$$

and specified gradient boundary conditions

$$(K_{ij}^A \frac{\partial h}{\partial x_j} + K_{iz}^A)n_i = \sigma_2(x, y, z, t) \quad \text{for } (x, y, z) \in \Gamma_G \quad (2.57)$$

where  $\Gamma_D$ ,  $\Gamma_N$ , and  $\Gamma_G$  indicate Dirichlet, Neumann, and gradient type boundary segments, respectively;  $\psi$  [L],  $\sigma_1$  [LT<sup>-1</sup>], and  $\sigma_2$  [-] are prescribed functions of  $x$ ,  $z$  and  $t$ ; and  $n_i$  are the components of the outward unit vector normal to boundary  $\Gamma_N$  or  $\Gamma_G$ . As pointed out by *McCord* [1991], the use of the term "Neumann type boundary condition" for the flux boundary is not very appropriate since this term should hold for a gradient type condition (see also Section 3.2 for solute

transport). However, since the use of the Neumann condition is standard in the hydrologic literature [Neuman, 1972; Neuman *et al.*, 1974], we shall also use this term to indicate flux boundaries throughout this report. HYDRUS implements the gradient boundary condition only in terms of a unit vertical hydraulic gradient simulating free drainage from a relatively deep soil profile. This situation is often observed in field studies of water flow and drainage in the vadose zone [Sisson, 1987; McCord, 1991]. McCord [1991] states that the most pertinent application of (2.57) is its use as a bottom outflow boundary condition for situations where the water table is situated far below the domain of interest.

### 2.7.2. System-Dependent Boundary Conditions

In addition to the system-independent boundary conditions given by (2.55), (2.56), and (2.57), HYDRUS considers three different types of system-dependent boundary conditions which cannot be defined a priori. One of these involves soil-air interfaces, which are exposed to atmospheric conditions. The potential fluid flux across these interfaces is controlled exclusively by external conditions. However, the actual flux depends also on the prevailing (transient) soil moisture conditions. Soil surface boundary conditions may change from prescribed flux to prescribed head type conditions (and vice-versa). In the absence of surface ponding, the numerical solution of (2.1) is obtained by limiting the absolute value of the flux such that the following two conditions are satisfied [Neuman *et al.*, 1974]:

$$|K(K_{ij}^A \frac{\partial h}{\partial x_j} + K_{iz}^A)n_i| \leq E \quad (2.58)$$

and

$$h_A \leq h \leq h_S \quad (2.59)$$

where  $E$  is the maximum potential rate of infiltration or evaporation under the current atmospheric conditions,  $h$  is the pressure head at the soil surface, and  $h_A$  and  $h_S$  are, respectively, minimum and maximum pressure heads allowed under the prevailing soil conditions. The value for  $h_A$  is determined from the equilibrium conditions between soil water and atmospheric water vapor, whereas  $h_S$  is usually set equal to zero. HYDRUS assumes that any excess water on the soil surface is immediately removed. When one of the end points of (2.59) is reached, a prescribed head boundary condition will be used to calculate the actual surface flux. Methods of calculating  $E$  and  $h_A$

on the basis of atmospheric data have been discussed by *Feddes et al.* [1974].

A second type of system-dependent boundary condition considered in HYDRUS is a seepage face through which water leaves the saturated part of the flow domain. In this case, the length of the seepage face is not known a priori. HYDRUS assumes that the pressure head is always uniformly equal to zero along a seepage face. Additionally, the code assumes that water leaving the saturated zone across a seepage face is immediately removed by overland flow or some other removal process.

Finally, a third class of system-dependent boundary conditions in HYDRUS concerns tile drains. Similarly as for seepage phase, HYDRUS assumes that as long as a drain is located in the saturated zone, the pressure head along the drain will be equal to zero; the drain then acts as a pressure head sink. However, the drain will behave as a nodal sink/source with zero recharge when located in the unsaturated zone. More information can be found in Section 5.3.7.

In addition to system-dependent boundary conditions available in version 2.x of HYDRUS-2D, several new options are available in HYDRUS:

- a) While in version 2.0, all boundary conditions (i.e., fluxes or pressure heads) changed in abrupt steps, the new version allows boundary pressure heads to change smoothly with time. Abrupt changes in the pressure heads lead to sudden changes in fluxes, while smoothly changing pressure heads provide smoothly changing fluxes. An example of such a boundary condition is the water level in a stream or furrow.
- b) While version 2.0 only allowed either time-variable pressure heads or time-variable fluxes on a particular part of the boundary, the new version allows boundary conditions to change from variable pressure heads to a zero flux and vice-versa. This boundary condition can be used for example for a disc permeameter where the specified head changes to a zero flux during time periods when the permeameter is re-supplied with water. The zero flux is initiated by specifying a value larger than 999999.
- c) When a time-variable pressure head boundary condition is specified along a boundary, then the specified value is assigned to the lowest nodal point of a particular boundary, while pressure heads at other nodes are adjusted based on the  $z$ -coordinate. When this option is selected, then nodes with calculated negative pressure heads are not associated with a Dirichlet boundary condition, but rather with a zero flux. A fluctuating water level in a stream or furrow is an example of this type of boundary condition. While positive pressure head values are below the water table, negative values occur above the water table.

- d) This is similar to c) except that an atmospheric boundary condition is assigned to nodes with negative calculated pressure heads.
- e) This is similar to c) except that a seepage face boundary condition is assigned to nodes with negative calculated pressure heads.
- f) When this type of system-dependent boundary condition is selected, then HYDRUS treats the time-variable flux boundary conditions similarly as atmospheric fluxes. This means that pressure heads have two limiting values, with the maximum pressure head equal to hCritS and the minimum pressure head equal to hCritA.
- g) While in version 2.x of the code, the flux across the nonactive part of the seepage face was always equal to zero, the new version can apply atmospheric boundary conditions on a nonactive seepage face.
- h) When heat transport is simulated simultaneously with water flow and atmospheric boundary conditions, then snow accumulation on top of the soil surface can be simulated. The code then assumes that when the air temperature is below -2 C all precipitation is in the form of snow. When the air temperature is above +2 C all precipitation is in the form of liquid, while a linear transition is used between the two limiting temperatures (-2,2). The code further assumes that when the air temperature is above zero, the existing snow layer (if it exists) melts proportionally to the air temperature.

Boundary condition options a) through g) can be used only with the first time-variable head condition.

## 2.8. Water Mass Transfer

The mass transfer rate,  $\Gamma_w$ , in (2.4) for water between the fracture and matrix regions in several dual-porosity studies (e.g. Phillip [1968]; Šimůnek et al. [2003]) has been assumed to be proportional to the difference in effective saturations of the two regions using the first-order rate equation:

$$\Gamma_w = \frac{\partial \theta_{im}}{\partial t} = \omega [S_e^m - S_e^{im}] \quad (2.60)$$

where  $\theta_{im}$  is the matrix water content,  $\omega$  is a first-order rate coefficient ( $T^{-1}$ ), and  $S_e^m$  and  $S_e^{im}$  are effective fluid saturations of the mobile (fracture) and immobile (matrix) regions, respectively.



Equation (2.60) assumes that the mass transfer rate is proportional to the difference in effective water contents, rather than pressure heads [Gerke and van Genuchten, 1993b], which should provide a more realistic description of the exchange rate between the fracture and matrix regions. An inherent assumption of (2.60) is that the water retention properties of the matrix and the fracture domains are identical. For this reason, equation (2.60) must be used with some caution and probably only for dual-porosity models. The approach has nevertheless been used successfully in multiple studies (e.g., Köhne et al. [2004, 2005]).

An important advantage of (2.60) is the fact that the dual-porosity model based on this mass transfer equation requires significantly fewer parameters since one does not need to know the retention function for the matrix region explicitly, but only its residual and saturated water contents. Coupling (2.60) with a dual-porosity nonequilibrium flow model leads to the usual soil hydraulic parameters needed for the equilibrium model, two additional parameters characterizing the matrix region (i.e. its residual,  $\theta_r^{im}$ , and saturated,  $\theta_s^{im}$ , water contents), and the first-order mass transfer coefficient  $\omega$ . By additionally assuming that the residual water content of the fracture region is equal to zero (and hence that residual water is present only in the immobile region), one could further decrease the number of model parameters.

When the rate of exchange of water between the fracture and matrix regions is assumed to be proportional to the difference in pressure heads between the two pore regions [Gerke and van Genuchten, 1993a], the coupling term,  $\Gamma_w$ , becomes:

$$\Gamma_w = \alpha_w (h_f - h_m) \quad (2.61)$$

in which  $\alpha_w$  is a first-order mass transfer coefficient [ $L^{-1}T^{-1}$ ]. Since pressure heads are now needed for both regions, this approach requires retention curves for both pore regions. For porous media with well-defined geometries, the first-order mass transfer coefficient,  $\alpha_w$ , can be defined as follows [Gerke and van Genuchten, 1993b]:

$$\alpha_w = \frac{\beta}{d^2} K_a \gamma_w \quad (2.62)$$

where  $d$  is an effective ‘diffusion’ pathlength (i.e. half the aggregate width or half the fracture spacing) [L],  $\beta$  is a shape factor that depends on the geometry [-], and  $\gamma_w$  is a scaling factor (=0.4) obtained by matching the results of the first-order approach at the half-time level of the cumulative infiltration curve to the numerical solution of the horizontal infiltration equation

(Gerke and van Genuchten, 1993b). *Gerke and van Genuchten* [1996] evaluated the effective hydraulic conductivity  $K_a$  [ $\text{LT}^{-1}$ ] of the fracture-matrix interface using a simple arithmetic average involving both  $h_f$  and  $h_m$  as follows

$$K_a(h) = 0.5 [K_a(h_f) + K_a(h_m)] \quad (2.63)$$

The use of (2.62) implies that the medium contains geometrically well-defined rectangular or other types of macropores or fractures (e.g. *Edwards et al.* [1979], *van Genuchten and Dalton* [1986], and *Gerke and van Genuchten* [1996]). While geometrically based models are conceptually attractive, they may be too difficult to use for field applications, partly because structured soils and rocks usually contain mixtures of aggregates and matrix blocks of various sizes and shapes, but also because the parameters in (2.62) may not be identifiable. Hence, rather than using (2.62) directly, one could also lump  $\beta$ ,  $d$ , and  $\gamma_w$  into one effective hydraulic conductivity  $K_a^*$  of the fracture-matrix interface to give

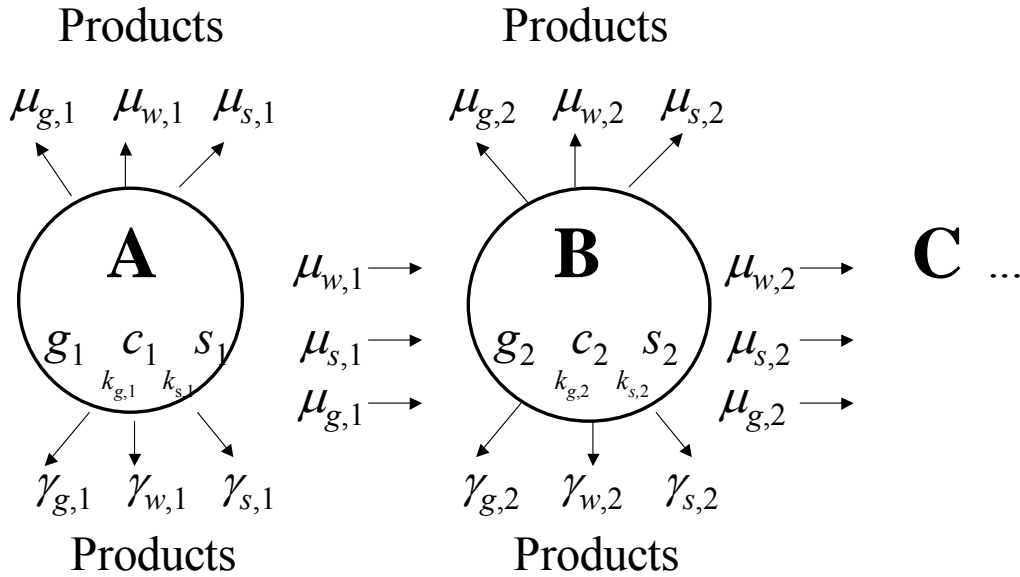
$$\alpha_w = K_a^*(h) \quad (2.64)$$

in which case  $K_a^*$  can be used as a calibration parameter (this variable is an input parameter to HYDRUS).

### 3. NONEQUILIBRIUM TRANSPORT OF SOLUTES INVOLVED IN SEQUENTIAL FIRST-ORDER DECAY REACTIONS

#### 3.1. Governing Transport Equation

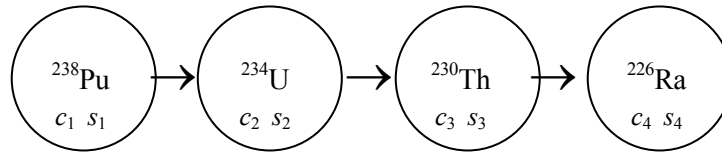
We assume that solutes can exist in all three phases (liquid, solid, and gaseous) and that the decay and production processes can be different in each phase. Interactions between the solid and liquid phases may be described by nonlinear nonequilibrium equations, while interactions between the liquid and gaseous phases are assumed to be linear and instantaneous. We further assume that the solutes are transported by convection and dispersion in the liquid phase, as well as by diffusion in the gas phase. A general structure of the system of first-order decay reactions for three solutes (A, B and C) is as follows [Šimůnek and van Genuchten, 1995]:



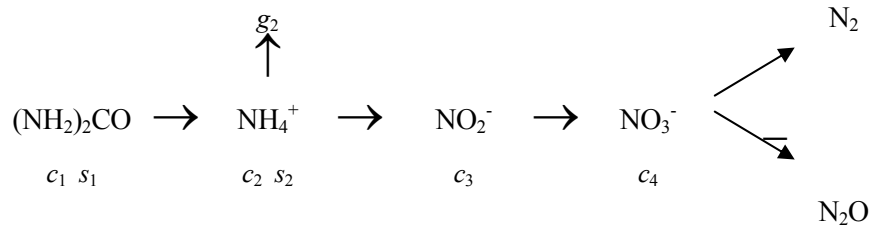
where  $c$ ,  $s$ , and  $g$  represent concentrations in the liquid, solid, and gaseous phases, respectively; the subscripts  $s$ ,  $w$ , and  $g$  refer to solid, liquid and gaseous phases, respectively; straight arrows represent the different zero-order ( $\gamma$ ) and first-order ( $\mu$ ,  $\mu'$ ) rate reactions, and circular arrows ( $k_g$ ,  $k_s$ ) indicate equilibrium distribution coefficients between phases.

Typical examples of sequential first-order decay chains are:

1. Radionuclides [van Genuchten, 1985]

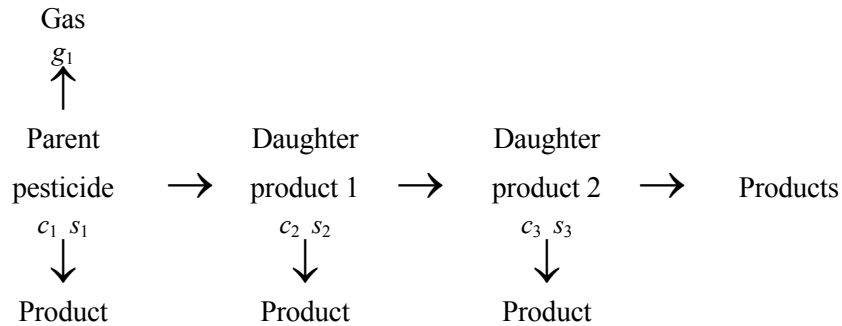


2. Nitrogen [Tillotson et al., 1980]

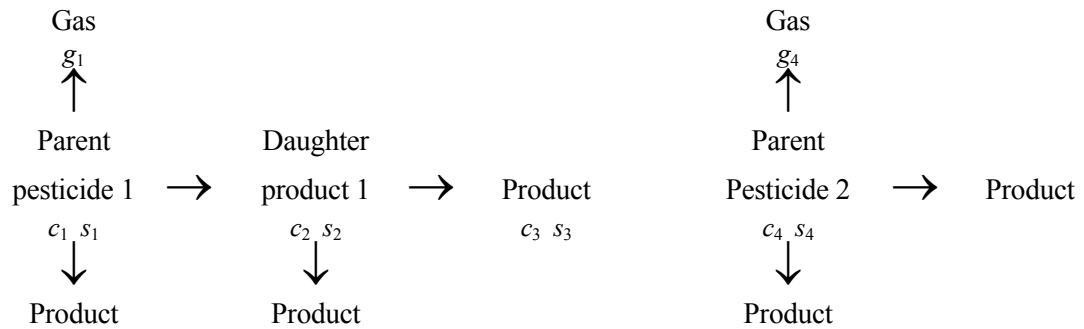


3. Pesticides [Wagenet and Hutson, 1987]:

a) Uninterrupted chain - one reaction path:



b) Interrupted chain - two independent reaction paths:



HYDRUS at present considers up to fifteen solutes, which can be either coupled in a unidirectional chain or may move independently of each other.

The partial differential equations governing nonequilibrium chemical transport of solutes involved in a sequential first-order decay chain during transient water flow in a variably saturated rigid porous medium are taken as

$$\begin{aligned} \frac{\partial \theta c_1}{\partial t} + \frac{\partial \rho s_1}{\partial t} + \frac{\partial a_v g_1}{\partial t} = \frac{\partial}{\partial x_i} \left( \theta D_{ij,1}^w \frac{\partial c_1}{\partial x_j} \right) + \frac{\partial}{\partial x_i} \left( a_v D_{ij,1}^g \frac{\partial g_1}{\partial x_j} \right) - \frac{\partial q_i c_1}{\partial x_i} - S c_{r,1} - \\ - (\mu_{w,1} + \mu'_{w,1}) \theta c_1 - (\mu_{s,1} + \mu'_{s,1}) \rho s_1 - (\mu_{g,1} + \mu'_{g,1}) a_v g_1 + \gamma_{w,1} \theta + \gamma_{s,1} \rho + \gamma_{g,1} a_v \end{aligned} \quad (3.1)$$

$$\begin{aligned} \frac{\partial \theta c_k}{\partial t} + \frac{\partial \rho s_k}{\partial t} + \frac{\partial a_v g_k}{\partial t} = \frac{\partial}{\partial x_i} \left( \theta D_{ij,k}^w \frac{\partial c_k}{\partial x_j} \right) + \frac{\partial}{\partial x_i} \left( a_v D_{ij,k}^g \frac{\partial g_k}{\partial x_j} \right) - \frac{\partial q_i c_k}{\partial x_i} - \\ - (\mu_{w,1} + \mu'_{w,k}) \theta c_k - (\mu_{s,k} + \mu'_{s,k}) \rho s_k - (\mu_{g,k} + \mu'_{g,k}) a_v g_k + \mu'_{w,k-1} \theta c_{k-1} + \\ + \mu'_{s,k-1} \rho s_{k-1} + \mu'_{g,k-1} a_v g_{k-1} + \gamma_{w,k} \theta + \gamma_{s,k} \rho + \gamma_{g,k} a_v - S c_{r,k} \quad k \in (2, n_s) \end{aligned} \quad (3.2)$$

where  $c$ ,  $s$ , and  $g$  are solute concentrations in the liquid [ $\text{ML}^{-3}$ ], solid [ $\text{MM}^{-1}$ ], and gaseous [ $\text{ML}^{-3}$ ], phases, respectively;  $q_i$  is the  $i$ -th component of the volumetric flux density [ $\text{LT}^{-1}$ ],  $\mu_w$ ,  $\mu_s$ , and  $\mu_g$  are first-order rate constants for solutes in the liquid, solid, and gas phases [ $\text{T}^{-1}$ ], respectively;  $\mu_w'$ ,  $\mu_s'$ , and  $\mu_g'$  are similar first-order rate constants providing connections between individual chain species,  $\gamma_w$ ,  $\gamma_s$ , and  $\gamma_g$  are zero-order rate constants for the liquid [ $\text{ML}^{-3}\text{T}^{-1}$ ], solid [ $\text{T}^{-1}$ ], and gas [ $\text{ML}^{-3}\text{T}^{-1}$ ] phases, respectively;  $\rho$  is the soil bulk density [ $\text{ML}^{-3}$ ],  $a_v$  is the air content [ $\text{L}^3\text{L}^{-3}$ ],  $S$  is the sink term in the water flow equation (2.1),  $c_r$  is the concentration of the sink term [ $\text{ML}^{-3}$ ],  $D_{ij}^w$  is the dispersion coefficient tensor [ $\text{L}^2\text{T}^{-1}$ ] for the liquid phase, and  $D_{ij}^g$  is the diffusion coefficient tensor [ $\text{L}^2\text{T}^{-1}$ ] for the gas phase. As before, the subscripts  $w$ ,  $s$ , and  $g$  correspond with the liquid, solid and gas phases, respectively; while the subscript  $k$  represents the  $k$ th chain number, and  $n_s$  is the number of solutes involved in the chain reaction. The indicial notation used in this report assumes summations over indices  $i$  and  $j$  ( $i, j = 1, 2$ ), but not over index  $k$ . The nine zero- and first-order rate constants in (3.1) and (3.2) may be used to represent a variety of reactions or transformations including biodegradation, volatilization, and precipitation.

HYDRUS assumes nonequilibrium interaction between the solution ( $c$ ) and adsorbed ( $s$ ) concentrations, and equilibrium interaction between the solution ( $c$ ) and gas ( $g$ ) concentrations of the solute in the soil system. The adsorption isotherm relating  $s_k$  and  $c_k$  is described by a generalized nonlinear equation of the form

$$s_k = \frac{k_{s,k} c_k^{\beta_k}}{1 + \eta_k c_k^{\beta_k}} \quad k \in (1, n_s) \quad (3.3)$$

$$\frac{\partial s_k}{\partial t} = \frac{k_{s,k} \beta_k c_k^{\beta_k - 1}}{(1 + \eta_k c_k^{\beta_k})^2} \frac{\partial c_k}{\partial t} + \frac{c_k^{\beta_k}}{1 + \eta_k c_k^{\beta_k}} \frac{\partial k_{s,k}}{\partial t} - \frac{k_{s,k} c_k^{2\beta_k}}{(1 + \eta_k c_k^{\beta_k})^2} \frac{\partial \eta_k}{\partial t} + \frac{k_{s,k} c_k^{\beta_k} \ln c_k}{(1 + \eta_k c_k^{\beta_k})^2} \frac{\partial \beta_k}{\partial t}$$

where  $k_{s,k}$  [ $L^3 M^{-1}$ ],  $\beta_k$  [-] and  $\eta_k$  [ $L^3 M^{-1}$ ] are empirical coefficients. The Freundlich, Langmuir, and linear adsorption equations are special cases of equation (3.3). When  $\beta_k=1$ , equation (3.3) becomes the Langmuir equation, when  $\eta_k=0$ , equation (3.3) becomes the Freundlich equation, and when both  $\beta_k=1$  and  $\eta_k=0$ , equation (3.3) leads to a linear adsorption isotherm. Solute transport without adsorption is described with  $k_{s,k}=0$ . While the coefficients  $k_{s,k}$ ,  $\beta_k$ , and  $\eta_k$  in equation (3.3) are assumed to be independent of concentration, they are permitted to change as a function of time through their dependency on temperature. This feature will be discussed later.

The concentrations  $g_k$  and  $c_k$  are related by a linear expression of the form

$$g_k = k_{g,k} c_k \quad k \in (1, n_s) \quad (3.4)$$

where  $k_{g,k}$  is an empirical constant [-] equal to  $(K_H R_u T^A)^{-1}$  [Stumm and Morgan, 1981] in which  $K_H$  is Henry's Law constant [ $MT^2 M^{-1} L^{-2}$ ],  $R_u$  is the universal gas constant [ $ML^2 T^{-2} K^{-1} M^{-1}$ ] and  $T^A$  is absolute temperature [K].

### 3.1.1. Chemical Nonequilibrium

The concept of two-site sorption [Selim et al., 1977; van Genuchten and Wagenet, 1989] is implemented in HYDRUS to permit consideration of nonequilibrium adsorption-desorption reactions. The two-site sorption concept assumes that the sorption sites can be divided into two fractions:

$$s_k = s_k^e + s_k^k \quad k \in (1, n_s) \quad (3.5)$$

Sorption,  $s_k^e$  [MM<sup>-1</sup>], on one fraction of the sites (the type-1 sites) is assumed to be instantaneous, while sorption,  $s_k^k$  [MM<sup>-1</sup>], on the remaining (type-2) sites is considered to be time-dependent. At equilibrium we have for the type-1 (equilibrium) and type-2 (kinetic) sites, respectively

$$s_k^e = f s_k \quad k \in (1, n_s) \quad (3.6)$$

where  $f$  is the fraction of exchange sites assumed to be in equilibrium with the solution phase [-]. Because type-1 sorption sites are always at equilibrium, differentiation of (3.6) gives immediately the sorption rate for the type-1 equilibrium sites:

$$s_k^k = (1 - f) s_k \quad k \in (1, n_s) \quad (3.7)$$

$$\frac{\partial s_k^e}{\partial t} = f \frac{\partial s_k}{\partial t} \quad k \in (1, n_s) \quad (3.8)$$

Sorption on the type-2 nonequilibrium sites is assumed to be a first-order kinetic rate process. Following *Toride et al.* [1993], the mass balance equation for the type-2 sites in the presence of production and degradation is given by

$$\frac{\partial s_k^k}{\partial t} = \omega_k \left[ (1 - f) \frac{k_{s,k} c_k^{\beta_k}}{1 + \eta_k c_k^{\beta_k}} - s_k^k \right] - (\mu_{s,k} + \mu'_{s,k}) s_k^k + (1 - f) \gamma_{s,k} \quad k \in (1, n_s) \quad (3.9)$$

where  $\omega_k$  is the first-order rate constant for the  $k$ th solute [T<sup>-1</sup>].

Substituting (3.3) through (3.9) into (3.1) and (3.2), and using the continuity equation describing the isothermal Darcian flow of water in a variably saturated porous medium, i.e.,

$$\frac{\partial \theta}{\partial t} = - \frac{\partial q_i}{\partial x_i} - S \quad (3.10)$$

leads to the following equation

$$-\theta R_k \frac{\partial c_k}{\partial t} - q_i \frac{\partial c_k}{\partial x_i} + \frac{\partial}{\partial x_i} \left( \theta D_{ij,k} \frac{\partial c_k}{\partial x_j} \right) + F_k c_k + G_k = 0 \quad k \in (1, n_s) \quad (3.11)$$

in which  $D_{ij}$  [ $L^2T^{-1}$ ] is an effective dispersion coefficient tensor given by

$$\theta D_{ij,k} = \theta D_{ij,k}^w + a_v D_{ij,k}^g k_{g,k} \quad k \in (1, n_s) \quad (3.12)$$

The coefficients  $F_k$  and  $G_k$  in (3.11) are defined as

$$F_k(c_k) = -(\mu_{w,k} + \mu'_{w,k})\theta - (\mu_{s,k} + \mu'_{s,k})\rho f \frac{k_{s,k} c_k^{\beta_k - 1}}{1 + \eta_k c_k^{\beta_k}} - (\mu_{g,k} + \mu'_{g,k})a_v k_{g,k} + \\ + S + k_{g,k} \frac{\partial \theta}{\partial t} - a_v \frac{\partial k_{g,k}}{\partial t} - \omega_k \rho \frac{(1-f)k_{s,k} c_k^{\beta_k - 1}}{1 + \eta_k c_k^{\beta_k}} - g_k(c_k) \quad k \in (1, n_s) \quad (3.13)$$

$$G_1(c_1) = \gamma_{w,1}\theta + \gamma_{s,1}f\rho + \gamma_{g,1}a_v - Sc_{r,1} + \omega_1 \rho s_1^k$$

$$G_k(c_k) = (\mu'_{w,k-1}\theta + \mu'_{s,k-1}f\rho \frac{k_{s,k-1} c_{k-1}^{\beta_{k-1} - 1}}{1 + \eta_{k-1} c_{k-1}^{\beta_{k-1}}} + \mu'_{g,k-1}a_v k_{g,k-1})c_{k-1} + \\ + \mu'_{s,k-1}\rho s_{k-1}^k + \gamma_{w,k}\theta + \gamma_{s,k}f\rho + \gamma_{g,k}a_v - Sc_{r,k} + \omega_k \rho s_k^k \quad k \in (2, n_s) \quad (3.14)$$

where the variable  $g_k$  accounts for possible changes in the adsorption parameters caused by temperature changes in the system as follows (see also section 3.4):

$$g_k(c_k) = \rho f \left( \frac{c_k^{\beta_k - 1}}{1 + \eta_k c_k^{\beta_k}} \frac{\partial k_{s,k}}{\partial t} - \frac{k_{s,k} c_k^{2\beta_k - 1}}{(1 + \eta_k c_k^{\beta_k})^2} \frac{\partial \eta_k}{\partial t} + \frac{k_{s,k} \ln c_k c_k^{\beta_k - 1}}{(1 + \eta_k c_k^{\beta_k})^2} \frac{\partial \beta_k}{\partial t} \right) \quad k \in (1, n_s) \quad (3.15)$$

The retardation factor  $R_k$  [-] in (3.11) is given by



$$R_k(c_k) = 1 + \frac{\rho f k_{s,k} \beta_k c_k^{\beta_k - 1}}{\theta (1 + \eta_k c_k^{\beta_k})^2} + \frac{a_v k_{g,k}}{\theta} \quad k \in (1, n_s) \quad (3.16)$$

### 3.1.2. Physical Nonequilibrium

The concept of two-region, dual-porosity type solute transport [van Genuchten and Wierenga, 1976] is implemented in HYDRUS to permit consideration of physical nonequilibrium transport. The two-region concept assumes that the liquid phase can be partitioned into mobile (flowing),  $\theta_m$  [L<sup>3</sup>L<sup>-3</sup>], and immobile (stagnant),  $\theta_{im}$  [L<sup>3</sup>L<sup>-3</sup>], regions:

$$\theta = \theta_m + \theta_{im} \quad (3.17)$$

and that solute exchange between the two liquid regions can be modeled as a first-order process, i.e.,

$$\left[ \theta_{im} + \rho(1-f) \frac{k_{s,k} \beta_k c_{k,im}^{\beta_k - 1}}{(1 + \eta_k c_{k,im}^{\beta_k})^2} \right] \frac{\partial c_{k,im}}{\partial t} = \omega_k (c_k - c_{k,im}) + \gamma_{w,k} \theta_{im} + (1-f) \rho \gamma_{s,k} - \left[ \theta_{im} (\mu_{w,k} + \mu'_{w,k}) + \rho (\mu_{s,k} + \mu'_{s,k}) (1-f) \frac{k_{s,k} c_{k,im}^{\beta_k - 1}}{\eta_k c_{k,im}^{\beta_k}} \right] c_{k,im} \quad k \in (1, n_s) \quad (3.18)$$

where  $c_{im}$  [ML<sup>-3</sup>] is the concentration in the immobile region and  $\omega_k$  is the mass transfer coefficient for the  $k$ th solute [T<sup>-1</sup>].

Substituting (3.17) and (3.18) into (3.1) and (3.2), the latter two equations modified for mobile and immobile regions as shown by van Genuchten and Wagenet [1989], leads to equation (3.11) in which  $\theta$  is replaced with  $\theta_m$  and with the coefficients  $F_k$  and  $G_k$  redefined as follows

$$F_k(c_k) = -(\mu_{w,k} + \mu'_{w,k}) \theta_m - (\mu_{s,k} + \mu'_{s,k}) \rho f \frac{k_{s,k} c_k^{\beta_k - 1}}{1 + \eta_k c_k^{\beta_k}} - (\mu_{g,k} + \mu'_{g,k}) a_v k_{g,k} - \omega_k \quad (3.19)$$

$$\begin{aligned}
G_1(c_1) &= \gamma_{w,1}\theta_m + \gamma_{s,1}f\rho + \gamma_{g,1}a_v - Sc_{r,1} + \omega_1c_{1,im} - \rho fg_1(c_1) \\
G_k(c_k) &= [\mu'_{w,k-1}\theta_m + \mu'_{s,k-1}f\rho \frac{k_{s,k-1}c_{k-1}^{\beta_{k-1}-1}}{1 + \eta_{k-1}c_{k-1}^{\beta_{k-1}}} + \mu'_{g,k-1}a_vk_{g,k-1}]c_{k-1} + \\
&+ [\mu'_{w,k-1}\theta_{im} + \mu'_{s,k-1}(1-f)\rho \frac{k_{s,k-1}c_{k-1,im}^{\beta_{k-1}-1}}{1 + \eta_{k-1}c_{k-1,im}^{\beta_{k-1}}}]c_{k-1,im} + \\
&+ \gamma_{w,k}\theta_m + \gamma_{s,k}f\rho + \gamma_{g,k}a_v - Sc_{r,k} + \omega_k c_{k,im} - \rho fg_k(c_k) \quad k \in (2, n_s)
\end{aligned} \tag{3.20}$$

In order to solve equation (3.11), it is necessary to know the water content  $\theta$  and the volumetric flux  $q$ . Both variables are obtained from solutions of the Richards' equation. The above equations may appear to be relatively complicated. However, by selecting proper values of particular coefficients (i.e.,  $\gamma_w, \gamma_s, \gamma_g, \mu_w, \mu_s, \mu_g, \mu_w', \mu_s', \mu_g', \eta, k_s, k_g, f, \beta, \omega$ ) the entire system can be simplified significantly. Assuming for example that  $\mu_w', \mu_s', \mu_g', \eta$ , and  $k_g$  are zero, and  $f$  and  $\beta$  are equal to one, the entire system of equations (3.1) through (3.20) simplifies into a set of equations describing the transport of mutually independent solutes, i.e., single-ion transport as applicable to:

$$\theta R \frac{\partial c}{\partial t} = \frac{\partial}{\partial x_i} \left( \theta D_{ij}^w \frac{\partial c}{\partial x_j} \right) - \frac{\partial q_i c}{\partial x_i} + Fc + G \tag{3.21}$$

### 3.1.3. Attachment-Detachment Model

Virus, colloid, and bacteria transport and fate models commonly employ a modified form of the convection-dispersion equation. In this study we define the mass balance equation for these applications as:

$$\frac{\partial \theta c}{\partial t} + \rho \frac{\partial s_e}{\partial t} + \rho \frac{\partial s_1}{\partial t} + \rho \frac{\partial s_2}{\partial t} = \frac{\partial}{\partial x_i} \left( \theta D_{ij}^w \frac{\partial c}{\partial x_j} \right) - \frac{\partial q_i c}{\partial x_i} - \mu_w \theta c - \mu_s \rho (s_e + s_1 + s_2) \tag{3.22}$$

where  $c$  is the (colloid, virus, bacteria) concentration in the aqueous phase [ $N_c L^{-3}$ ],  $s$  is the solid phase (colloid, virus, bacteria) concentration [ $N_c M^{-1}$ ], subscripts  $e, 1$ , and  $2$  represent equilibrium and two kinetic sorption sites, respectively,  $N_c$  is a number of colloids (particles), and  $\mu_w$  and  $\mu_s$  represent inactivation and degradation processes in the liquid and solid phases, respectively.

While sorption to equilibrium sites can be described similarly as before using (3.3), mass

transfer between the aqueous and both solid kinetic phases can be described as (note that we now dropped subscripts 1 and 2):

$$\rho \frac{\partial s}{\partial t} = \theta k_a \psi c - k_d \rho s \quad (3.23)$$

where  $k_a$  is the first-order deposition (attachment) coefficient [ $T^{-1}$ ],  $k_d$  is the first-order entrainment (detachment) coefficient [ $T^{-1}$ ], and  $\psi$  is a dimensionless colloid retention function [-]. The attachment and detachment coefficients in (3.23) have been found to strongly depend upon water content, with attachment significantly increasing as the water content decreases.

To simulate reductions in the attachment coefficient due to filling of favorable sorption sites,  $\psi$  is sometimes assumed to decrease with increasing colloid mass retention. A Langmuirian dynamics [Adamczyk *et al.*, 1994] equation has been proposed for  $\psi$  to describe this blocking phenomenon:

$$\psi = \frac{s_{\max} - s}{s_{\max}} = 1 - \frac{s}{s_{\max}} \quad (3.24)$$

in which  $s_{\max}$  is the maximum solid phase concentration [ $N_c M^{-1}$ ]. Blocking coefficients listed below are implemented only into a two-dimensional formulation. Conversely, enhanced colloid retention during porous medium ripening can theoretically be described using a functional form of  $\psi$  that increases with increasing mass of retained colloids:

$$\psi = \max(1, s^{s_{\max}}) \quad (3.25)$$

*Johnson and Elimelech* [1995] proposed the so-called random sequential adsorption model to describe blocking of the sorption sites:

$$\begin{aligned}
\psi &= 1 - 4a + 3.308a^2 + 1.4069a^3 & \text{for } s < 0.8s_{\max} \\
\psi &= \frac{(1 - bs)^3}{2d_c^2 b^3} & \text{for } s > 0.8s_{\max} \\
b &= \frac{1}{s_{\max}} \\
a &= 0.546 \frac{s}{s_{\max}}
\end{aligned} \tag{3.26}$$

Finally, *Bradford et al.* [2003] hypothesized that the influence of straining and attachment processes on colloid retention can be separated into two distinct components. They suggested the following depth-dependent blocking coefficient for the straining process:

$$\psi = \left( \frac{d_c + z - z_0}{d_c} \right)^{-\beta} \tag{3.27}$$

where  $d_c$  is the diameter of the sand grains [L],  $z_0$  is the coordinate of the location where the straining process starts [L] (the surface of the soil profile, or interface between soil layers), and  $\beta$  is an empirical factor (with an optimal value of 0.43 [*Bradford et al.*, 2003]) [-].

The attachment coefficient is often calculated using filtration theory [*Logan et al.*, 1995], a quasi-empirical formulation in terms of the median grain diameter of the porous medium (often termed the collector), the pore-water velocity, and collector and collision (or sticking) efficiencies accounting for colloid removal due to diffusion, interception and gravitational sedimentation [*Rajagopalan and Tien*, 1976; *Logan et al.*, 1995]:

$$k_a = \frac{3(1-\theta)}{2d_c} \eta \alpha v \tag{3.28}$$

where  $d_c$  is the diameter of the sand grains [L],  $\alpha$  is the sticking efficiency (ratio of the rate of particles that stick to a collector to the rate they strike the collector) [-],  $v$  is the pore water velocity [ $LT^{-1}$ ], and  $\eta$  is the single-collector efficiency [-]:

$$\eta = 4A_s^{1/3} N_{Pe}^{-2/3} + A_s N_{Lo}^{1/8} N_R^{15/8} + 0.00338 A_s N_G^{1.2} N_R^{-0.4} \tag{3.29}$$

where the first, second, and third terms represent removal by diffusion, interception, and gravitational sedimentation, respectively, and where  $N_{Pe}$  is the Peclet number [-],  $N_R$  is the interception number [-],  $N_G$  is the gravitation number [-],  $N_{Lo}$  accounts for the contribution of particle London-van der Walls attractive forces to particle removal [-], and  $A_s$  is a correction factor [-] as follows:

$$A_s = \frac{2(1-\gamma^5)}{2-3\gamma+3\gamma^5-2\gamma^6} \quad (3.30)$$

$$\gamma = (1-\theta)^{1/3}$$

The dimensionless Peclet number in (3.29) is calculated as follows:

$$N_{Pe} = \frac{3\pi\mu d_p d_c q}{kT} \quad (3.31)$$

where  $\mu$  is the fluid viscosity (= 0.00093 Pa s) [ $ML^{-1}T^{-1}$ ],  $d_p$  is the diameter of the particle (e.g., virus, bacteria) (= 0.95  $\mu m$  = 0.95e-6 m) [L],  $q$  is the Darcy's flux [ $LT^{-1}$ ],  $k$  is the Boltzman constant (= 1.38048e-23 J/K) [ $M L^2 T^{-2} K^{-1}$ ], and  $T$  is the temperature (= 298 K) [K]. Finally, the interception number,  $N_R$ , the gravitation number,  $N_G$ , and the number representing London-van der Walls attractive forces,  $N_{Lo}$ , in (3.29) are calculated using:

$$N_R = \frac{d_p}{d_c} \quad (3.32)$$

$$N_G = \frac{g(\rho_p - \rho_f)d_p^2}{18\mu q} \quad (3.33)$$

$$N_{Lo} = \frac{4H}{9\pi\mu d_p^2 q} \quad (3.34)$$

where  $H$  is the Hamaker constant (= 1e-20 J) [ $ML^2T^{-2}$ ],  $g$  is the gravitational acceleration (= 9.81  $m s^{-2}$ ) [ $LT^{-2}$ ],  $\rho_p$  is the bacterial density (= 1080  $kg m^{-3}$ ) [ $ML^{-3}$ ], and  $\rho_f$  is the fluid density (= 998  $kg m^{-3}$ ) [ $ML^{-3}$ ].

The model described above using equation (3.22) can be used in many different ways.

For example, one can assume that the soil has two sorption sites,  $s_1$  and  $s_2$ , each having their own attachment and detachment constants. This model has been used to describe virus transport in sand dunes by *Schijven and Šimůnek* [2002]. Sorption sites  $s_1$  and  $s_2$  can be used to describe straining and attachment, respectively, as was done by *Bradford et al.* [2002, 2003, 2004]. One may also assume that one sorption site represents sorption to the solid phase, while the other site represents removal of particles by means of attachment to the air-water interface.

### 3.2. Initial and Boundary Conditions

The solution of (3.11) requires knowledge of the initial concentration within the flow region,  $\Omega$ , i.e.,

$$\begin{aligned} c(x, y, z, 0) &= c_i(x, y, z) \\ s^k(x, y, z, 0) &= s_i^k(x, y, z) \\ c_{im}(x, y, z, 0) &= c_{im,i}(x, y, z) \end{aligned} \quad (3.35)$$

where  $c_i$  [ $\text{ML}^{-3}$ ],  $c_{im,i}$  [ $\text{ML}^{-3}$ ] and  $s_i^k$  [-] are prescribed functions of  $x$  and  $z$ . The initial condition for  $s_i^k$  must be specified only when nonequilibrium adsorption is considered. The subscript  $k$  is dropped in (3.35) and throughout the remainder of this report, thus assuming that the transport-related equations in the theoretical development and numerical solution apply to each of the solutes in the decay chain.

Two types of boundary conditions (Dirichlet and Cauchy type conditions) can be specified along the boundary of  $\Omega$ . First-type (or Dirichlet type) boundary conditions prescribe the concentration along a boundary segment  $\Gamma_D$ :

$$c(x, y, z, t) = c_0(x, y, z, t) \quad \text{for } (x, y, z) \in \Gamma_D \quad (3.36)$$

whereas third-type (Cauchy type) boundary conditions may be used to prescribe the concentration flux along a boundary segment  $\Gamma_C$  as follows:

$$-\theta D_{ij} \frac{\partial c}{\partial x_j} n_i + q_i n_i c = q_i n_i c_0 \quad \text{for } (x, y, z) \in \Gamma_C \quad (3.37)$$

in which  $q_i n_i$  represents the outward fluid flux,  $n_i$  is the outward unit normal vector and  $c_0$  is the concentration of the incoming fluid [ML<sup>-3</sup>]. In some cases, for example when  $\Gamma_C$  is an impermeable boundary ( $q_i n_i=0$ ) or when water flow is directed out of the region, (3.37) reduces to a second-type (Neumann type) boundary condition of the form:

$$\theta D_{ij} \frac{\partial c}{\partial x_j} n_i = 0 \quad \text{for } (x, y, z) \in \Gamma_N \quad (3.38)$$

A different type of boundary condition is needed for volatile solutes when they are present in both the liquid and gas phases. This situation requires a third-type boundary condition which has on the right-hand side an additional term to account for gas diffusion through a stagnant boundary layer of thickness  $d$  [L] on the soil surface. The additional solute flux is proportional to the difference in gas concentrations above and below this boundary layer [Jury *et al.*, 1983]. This modified boundary condition has the form

$$-\theta D_{ij} \frac{\partial c}{\partial x_j} n_i + q_i n_i c = q_i n_i c_0 + \frac{D_g}{d} (k_g c - g_{atm}) \quad \text{for } (x, y, z) \in \Gamma_C \quad (3.39)$$

where  $D_g$  is the molecular diffusion coefficient in the gas phase [L<sup>2</sup>T<sup>-1</sup>] and  $g_{atm}$  is the gas concentration above the stagnant boundary layer [ML<sup>-3</sup>]. We note that Jury *et al.* [1983] assumed  $g_{atm}$  to be zero. Similarly as for (3.37), (3.39) reduces to a second-type (Neumann type) boundary condition when water flow is zero or directed out of the region:

$$-\theta D_{ij} \frac{\partial c}{\partial x_j} n_i = \frac{D_g}{d} (k_g c - g_{atm}) \quad \text{for } (x, y, z) \in \Gamma_N \quad (3.40)$$

Equations (3.39) and (3.40) can only be used when the additional gas diffusion flux is positive. Jury *et al.* [1983] discussed how to estimate the thickness of the boundary layer,  $d$ , and recommended  $d=0.5$  cm as a good average value for a bare surface.

### 3.3. Effective Dispersion Coefficient

The components of the dispersion tensor in the liquid phase,  $D_{ij}^w$ , are given by [Bear, 1972]

$$\theta D_{ij}^w = D_T |q| \delta_{ij} + (D_L - D_T) \frac{q_j q_i}{|q|} + \theta D_w \tau_w \delta_{ij} \quad (3.41)$$

where  $D_w$  is the molecular diffusion coefficient in free water [ $L^2T^{-1}$ ],  $\tau_w$  is a tortuosity factor in the liquid phase [-],  $q$  is the absolute value of the Darcian fluid flux density [ $LT^{-1}$ ],  $\delta_{ij}$  is the Kronecker delta function ( $\delta_{ij}=1$  if  $i=j$ , and  $\delta_{ij}=0$  if  $i \neq j$ ), and  $D_L$  and  $D_T$  are the longitudinal and transverse dispersivities, respectively [L]. After adding the diffusion contribution from the gas phase, the individual components of the effective dispersion tensor in the soil matrix for three-dimensional transport are as follows:

$$\begin{aligned} \theta D_{xx} &= D_L \frac{q_x^2}{|q|} + D_T \frac{q_y^2}{|q|} + D_T \frac{q_z^2}{|q|} + \theta D_w \tau_w + a_v D_g k_g \tau_g \\ \theta D_{yy} &= D_L \frac{q_y^2}{|q|} + D_T \frac{q_x^2}{|q|} + D_T \frac{q_z^2}{|q|} + \theta D_w \tau_w + a_v D_g k_g \tau_g \\ \theta D_{zz} &= D_L \frac{q_z^2}{|q|} + D_T \frac{q_{xy}^2}{|q|} + D_T \frac{q_z^2}{|q|} + \theta D_w \tau_w + a_v D_g k_g \tau_g \\ \theta D_{xy} &= (D_L - D_T) \frac{q_x q_y}{|q|} \\ \theta D_{xz} &= (D_L - D_T) \frac{q_x q_z}{|q|} \\ \theta D_{yz} &= (D_L - D_T) \frac{q_y q_z}{|q|} \end{aligned} \quad (3.42)$$

where  $D_g$  is the molecular diffusion coefficient in the gas phase [ $L^2T^{-1}$ ] and  $\tau_g$  is a tortuosity factor in the gas phase [-]. Terms with  $y$  in (3.42) are equal to zero in a two-dimensional formulation.

The tortuosity factors for both phases are evaluated in HYDRUS as a function of the water and gas contents using the relationship of Millington and Quirk [1961]:



$$\begin{aligned}\tau_w &= \frac{\theta^{7/3}}{\theta_s^2} \\ \tau_g &= \frac{a_v^{7/3}}{\theta_s^2}\end{aligned}\tag{3.43}$$

### 3.4. Temperature Dependence of Transport and Reaction Coefficients

Several of the diffusion ( $D_w, D_g$ ), zero-order production ( $\gamma_w, \gamma_s, \gamma_g$ ), first-order degradation ( $\mu_w', \mu_s', \mu_g', \mu_w, \mu_s$ , and  $\mu_g$ ), and adsorption ( $k_s, k_g, \beta, \eta, \omega$ ) coefficients may be strongly dependent upon temperature. HYDRUS assumes that this dependency can be expressed by the Arrhenius equation [Stumm and Morgan, 1981]. After some modification, this equation can be expressed in the general form

$$a_T = a_r \exp \left[ \frac{E_a(T^A - T_r^A)}{R_u T^A T_r^A} \right]\tag{3.44}$$

where  $a_r$  and  $a_T$  are the values of the coefficient being considered at a reference absolute temperature  $T_r^A$  and absolute temperature  $T^A$ , respectively;  $R_u$  is the universal gas constant, and  $E_a$  [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ] is the activation energy of the particular reaction or process being modeled.



## 4. HEAT TRANSPORT

### 4.1. Governing Heat Transport Equations

Neglecting the effects of water vapor diffusion, two- and three-dimensional heat transport can be described as [*Sophocleous*, 1979]:

$$C(\theta) \frac{\partial T}{\partial t} = \frac{\partial}{\partial x_i} \left( \lambda_{ij}(\theta) \frac{\partial T}{\partial x_j} \right) - C_w q_i \frac{\partial T}{\partial x_i} \quad (4.1)$$

where  $\lambda_{ij}(\theta)$  is the apparent thermal conductivity of the soil [ $\text{MLT}^{-3}\text{K}^{-1}$ ] (e.g.  $\text{Wm}^{-1}\text{K}^{-1}$ ) and  $C(\theta)$  and  $C_w$  are the volumetric heat capacities [ $\text{ML}^{-1}\text{T}^{-2}\text{K}^{-1}$ ] (e.g.  $\text{Jm}^{-3}\text{K}^{-1}$ ) of the porous medium and the liquid phase, respectively. Volumetric heat capacity is defined as the product of the bulk density and gravimetric heat capacity. The first term on the right-hand side of (4.1) represents heat flow due to conduction and the second term accounts for heat being transported by flowing water. We do not consider the transfer of latent heat by vapor movement. According to *de Vries* [1963] the volumetric heat capacity can be expressed as

$$C_p(\theta) = C_n \theta_n + C_o \theta_o + C_w \theta + C_g a_v \approx (1.92\theta_n + 2.51\theta_o + 4.18\theta) 10^6 \quad (\text{J m}^{-3}\text{C}^{-1}) \quad (4.2)$$

where  $\theta$  refers to a volumetric fraction [ $\text{L}^3\text{L}^{-3}$ ], and subscripts  $n$ ,  $o$ ,  $g$ ,  $w$  represent solid phase, organic matter, gas phase and liquid phase, respectively.

### 4.2. Apparent Thermal Conductivity Coefficient

The apparent thermal conductivity,  $\lambda_{ij}(\theta)$ , combines the thermal conductivity  $\lambda_0(\theta)$  of the porous medium (solid plus water) in the absence of flow, and the macrodispersivity which is assumed to be a linear function of the velocity [*de Marsily*, 1986]. In analogy with the dispersion coefficient for solute transport, the apparent thermal conductivity  $\lambda_{ij}(\theta)$  is given by [*Šimůnek and Suarez*, 1993b]

$$\lambda_{ij}(\theta) = \lambda_T C_w |q| \delta_{ij} + (\lambda_L - \lambda_T) c_w \frac{q_j q_i}{|q|} + \lambda_0(\theta) \delta_{ij} \quad (4.3)$$

where  $q$  is the absolute value of the Darcian fluid flux density [ $LT^{-1}$ ],  $\delta_{ij}$  is the Kronecker delta function as before, and  $\lambda_L$  and  $\lambda_T$  are the longitudinal and transverse thermal dispersivities [ $L$ ], respectively. The individual components of the thermal conductivity tensor for three-dimensional transport are as follows:

$$\begin{aligned} \lambda_{xx} &= \lambda_L C_w \frac{x_x^2}{|q|} + \lambda_T C_w \frac{x_y^2}{|q|} + \lambda_T C_w \frac{x_z^2}{|q|} + \lambda_0 \\ \lambda_{yy} &= \lambda_L C_w \frac{x_y^2}{|q|} + \lambda_T C_w \frac{x_x^2}{|q|} + \lambda_T C_w \frac{x_z^2}{|q|} + \lambda_0 \\ \lambda_{zz} &= \lambda_L C_w \frac{x_z^2}{|q|} + \lambda_T C_w \frac{x_y^2}{|q|} + \lambda_T C_w \frac{x_x^2}{|q|} + \lambda_0 \\ \lambda_{xy} &= (\lambda_L - \lambda_T) C_w \frac{q_x q_y}{|q|} \\ \lambda_{xz} &= (\lambda_L - \lambda_T) C_w \frac{q_x q_z}{|q|} \\ \lambda_{yz} &= (\lambda_L - \lambda_T) C_w \frac{q_y q_z}{|q|} \end{aligned} \quad (4.4)$$

The volumetric heat capacity of the liquid phase is included here in the definition of the thermal conductivity in order to have the dimensions of the thermal dispersivities in the length units [*de Marsily*, 1986]. The thermal conductivity,  $\lambda_0(\theta)$ , accounts for the tortuosity of the porous medium, and is described with the simple equation [*Chung and Horton*, 1987]

$$\lambda_0(\theta) = b_1 + b_2 \theta_w + b_3 \theta_w^{0.5} \quad (4.5)$$

where  $b_1$ ,  $b_2$  and  $b_3$  are empirical parameters [ $MLT^{-3}K^{-1}$ ] (e.g.  $Wm^{-1}K^{-1}$ ).

### 4.3. Initial and Boundary Conditions

Equation (4.1) will be solved subject to the general initial condition

$$T(x, y, z, 0) = T_i(x, y, z) \quad (4.6)$$

where  $T_i$  is a prescribed function of  $x$  and  $z$ .

Two types of boundary conditions (Dirichlet and Cauchy type conditions) can again be specified along the boundary of  $\Omega$ . First-type (or Dirichlet type) boundary conditions prescribe the temperature along a boundary segment  $\Gamma_D$ :

$$T(x, y, z, t) = T_0(x, y, z, t) \quad \text{for } (x, y, z) \in \Gamma_D \quad (4.7)$$

whereas third-type (Cauchy type) boundary conditions prescribe the heat flux along a boundary segment  $\Gamma_C$  as follows

$$-\lambda_{ij} \frac{\partial T}{\partial x_j} n_i + T_c q_i n_i = T_0 C_w q_i n_i \quad \text{for } (x, y, z) \in \Gamma_C \quad (4.8)$$

in which  $q_i n_i$  represents the outward fluid flux,  $n_i$  is the outward unit normal vector and  $T_0$  is the temperature of the incoming fluid. When  $\Gamma_C$  is an impermeable boundary ( $q_i n_i = 0$ ) or when water flow is directed out of the region, (4.8) reduces to a second-type (Neumann type) boundary condition of the form:

$$\lambda_{ij} \frac{\partial T}{\partial x_j} n_i = 0 \quad \text{for } (x, y, z) \in \Gamma_N \quad (4.9)$$

The atmospheric boundary condition for soil temperature is assumed to be given by a sine function as follows [Kirkham and Powers, 1972]:

$$T_0 = \bar{T} + A \sin\left(\frac{2\pi t^*}{t_p} - \frac{7\pi}{12}\right) \quad (4.10)$$

where  $t_p$  is the period of time [T] necessary to complete one cycle of the sine wave (taken to be 1 day),  $\bar{T}$  is the average temperature at the soil surface [K] during period  $t_p$ ,  $A$  is the amplitude of the sine wave [K], and  $t^*$  is the local time [T] within the period  $t_p$ . The second term within the argument of the sine function is included to allow the highest temperature to occur at 1 p.m.

## 5. NUMERICAL SOLUTION OF THE WATER FLOW EQUATION

The Galerkin finite element method with linear basis functions is used to obtain a solution of the flow equation (2.1) subject to the imposed initial and boundary conditions. Since the Galerkin method is relatively standard and has been covered in detail elsewhere [Neuman, 1975; Zienkiewicz, 1977; Pinder and Gray, 1977], only the most pertinent steps in the solution process are given here.

### 5.1. Space Discretization

The flow region is divided into a network of triangular (2D) or tetrahedral (3D) elements. The corners of these elements are taken to be the nodal points. The dependent variable, the pressure head function  $h(x,y,z,t)$ , is approximated by a function  $h'(x,y,z,t)$  as follows

$$h'(x, y, z, t) = \sum_{n=1}^N \phi_n(x, y, z) h_n(t) \quad (5.1)$$

where  $\phi_n$  are piecewise linear basis functions satisfying the condition  $\phi_n(x_m, z_m) = \delta_{nm}$ ,  $h_n$  are unknown coefficients representing the solution of (2.1) at the nodal points, and  $N$  is the total number of nodal points.

The Galerkin method postulates that the differential operator associated with the Richards' equation (2.1) is orthogonal to each of the  $N$  basis functions, i.e.,

$$\int_{\Omega} \left\{ \frac{\partial \theta}{\partial t} - \frac{\partial}{\partial x_i} \left[ K \left( K_{ij}^A \frac{\partial h}{\partial x_j} + K_{iz}^A \right) \right] + S \right\} \phi_n d\Omega = 0 \quad (5.2)$$

Applying Green's first identity to (5.2), and replacing  $h$  by  $hN$ , leads to

$$\begin{aligned}
& \sum_e \int_{\Omega_e} \left( \frac{\partial \theta}{\partial t} \phi_n + K K_{ij}^A \frac{\partial h'}{\partial x_j} \frac{\partial \phi_n}{\partial x_i} \right) d\Omega = \\
& \sum_e \int_{\Gamma_e} K \left( K_{ij}^A \frac{\partial h'}{\partial x_j} + K_{iz}^A \right) n_i \phi_n d\Gamma + \sum_e \int_{\Omega_e} \left( -K K_{iz}^A \frac{\partial \phi_n}{\partial x_i} - S \phi_n \right) d\Omega
\end{aligned} \tag{5.3}$$

where  $\Omega_e$  represents the domain occupied by element  $e$ , and  $\Gamma_e$  is a boundary segment of element  $e$ . Natural flux-type (Neumann) and gradient type boundary conditions can be immediately incorporated into the numerical scheme by specifying the line integral in equation (5.3).

After imposing additional simplifying assumptions to be discussed later, and performing integration over the elements, the procedure leads to a system of time-dependent ordinary differential equations with nonlinear coefficients. In matrix form, these equations are given by

$$[F] \frac{d\{\theta\}}{dt} + [A]\{h\} = \{Q\} - \{B\} - \{D\} \tag{5.4}$$

where

$$\begin{aligned}
A_{nm} &= \sum_e K_l K_{ij}^A \int_{\Omega_e} \phi_l \frac{\partial \phi_n}{\partial x_i} \frac{\partial \phi_m}{\partial x_j} d\Omega = \\
&= \sum_e \frac{\kappa}{4A_e} \bar{K} \left[ K_{xx}^A b_m b_n + K_{xz}^A (c_m b_n + b_m c_n) + K_{zz}^A c_m c_n \right] \quad \text{for 2D} \\
&= \sum_e \frac{\bar{K}}{36V_e} \left[ K_{xx}^A b_m b_n + K_{yy}^A c_m c_n + K_{zz}^A d_n d_m + K_{xy}^A (b_m c_n + c_m b_n) + \right. \\
&\quad \left. + K_{xz}^A (b_n d_m + d_n b_m) + K_{yz}^A (c_m d_n + d_m c_n) \right] \quad \text{for 3D}
\end{aligned} \tag{5.5}$$

$$\begin{aligned}
B_n &= \sum_e K_l K_{iz}^A \int_{\Omega_e} \phi_l \frac{\partial \phi_n}{\partial x_i} d\Omega = \sum_e \frac{\kappa}{2} \bar{K} (K_{xz}^A b_n + K_{zz}^A c_n) \quad \text{for 2D} \\
&= \sum_e \frac{\bar{K}}{6} (K_{xz}^A b_n + K_{yz}^A c_n + K_{zz}^A d_n) \quad \text{for 3D}
\end{aligned} \tag{5.6}$$



$$\begin{aligned}
F_{nm} &= \delta_{nm} \sum_e \int_{\Omega_e} \phi_n d\Omega = \delta_{nm} \sum_e \frac{K}{3} A_e && \text{for 2D} \\
&= \delta_{nm} \sum_e \frac{V_e}{4} && \text{for 3D}
\end{aligned} \tag{5.7}$$

$$Q_n = -\sum_e \sigma_{1l} \int_{\Gamma_e} \phi_l \phi_n d\Gamma = -\sum_e \sigma_{1n} L_n \tag{5.8}$$

$$\begin{aligned}
D_n &= \sum_e S_l \int_{\Omega_e} \phi_l \phi_n d\Omega = \sum_e \frac{K}{12} A_e (3\bar{S} + S_n) && \text{for 2D} \\
&= \sum_e \frac{V_e}{20} (4\bar{S} + S_n) && \text{for 3D}
\end{aligned} \tag{5.9}$$

where the overlined variables represent average values over an element  $e$ , the subscripts  $i$  and  $j$  are space direction indices ( $i, j = 1, 2, 3$ ). For a two-dimensional problem:

$$l = 1, 2, \dots, N \quad m = 1, 2, \dots, N \quad n = 1, 2, \dots, N$$

$$\begin{aligned}
b_i &= z_j - z_k & c_i &= x_k - x_j \\
b_j &= z_k - z_i & c_j &= x_i - x_k \\
b_k &= z_i - z_j & c_k &= x_j - x_i
\end{aligned} \tag{5.10}$$

$$A_e = \frac{c_k b_j - c_j b_k}{2} \quad \bar{K} = \frac{K_i + K_j + K_k}{3} \quad \bar{S} = \frac{S_i + S_j + S_k}{3}$$

For tetrahedral element vertexed by nodes 1, 2, 3, and 4 of a three-dimensional problem:

$$\begin{aligned}
b_1 &= (y_4 - y_2)(z_3 - z_2) - (y_3 - y_2)(z_4 - z_2) \\
b_2 &= (y_4 - y_3)(z_1 - z_3) - (y_1 - y_3)(z_4 - z_3) \\
b_3 &= (y_2 - y_4)(z_1 - z_4) - (y_1 - y_4)(z_2 - z_4) \\
b_4 &= (y_2 - y_1)(z_3 - z_1) - (y_3 - y_1)(z_2 - z_1)
\end{aligned} \tag{5.11}$$

$$\begin{aligned}
c_1 &= (x_3 - x_2)(z_4 - z_2) - (x_4 - x_2)(z_3 - z_2) \\
c_2 &= (x_1 - x_3)(z_4 - z_3) - (x_4 - x_3)(z_1 - z_3) \\
c_3 &= (x_1 - x_4)(z_2 - z_4) - (x_2 - x_4)(z_1 - z_4) \\
c_4 &= (x_3 - x_1)(z_2 - z_1) - (x_2 - x_1)(z_3 - z_1) \\
d_1 &= (x_4 - x_2)(y_3 - y_2) - (x_3 - x_2)(y_4 - y_2) \\
d_2 &= (x_4 - x_3)(y_1 - y_3) - (x_1 - x_3)(y_4 - y_3) \\
d_3 &= (x_2 - x_4)(y_1 - y_4) - (x_1 - x_4)(y_2 - y_4) \\
d_4 &= (x_2 - x_1)(y_3 - y_1) - (x_3 - x_1)(y_2 - y_1)
\end{aligned}$$

$$V_e = (x_4 - x_1)b_4 + (y_4 - y_1)c_4 + (z_4 - z_1)d_4$$

$$\bar{K} = \frac{K_1 + K_2 + K_3 + K_4}{4} \quad \bar{S} = \frac{S_1 + S_2 + S_3 + S_4}{4} \tag{5.12}$$

Equation (5.8) is valid for a flux-type boundary condition. For a gradient-type boundary condition the variable  $\sigma_1$  in (5.8) must be replaced by the product of the hydraulic conductivity  $K$  and the prescribed gradient  $\sigma_2$  ( $=1$ ). Equations (5.5) through (5.9) hold for flow in a three-dimensional Cartesian  $(x,y,z)$  domain, a two-dimensional Cartesian  $(x,z)$  domain, as well as for flow in an axisymmetric  $(x,z)$  system in which  $x$  is used as the radial coordinate. For two-dimensional plane flow we have

$$\kappa = 1 \quad \lambda_n = \frac{L_n}{2} \tag{5.13}$$

while for axisymmetric flow (using two-dimensional formulation)

$$\kappa = 2\pi \frac{x_i + x_j + x_k}{3} \quad \lambda_n = L_n \pi \frac{x'_n + 2x_n}{3} \quad (5.14)$$

The subscripts  $i, j$  and  $k$  in equations (5.10) and (5.14) represent the three corners of a triangular element  $e$ .  $A_e$  is the area of a two-dimensional element  $e$ ,  $V_e$  is the volume of a three-dimensional element  $e$ ,  $\bar{K}$  and  $\bar{S}$  are the average hydraulic conductivity and root water extraction values over element  $e$ ,  $L_n$  is the length of the boundary segment connected to node  $n$ , and  $x'_n$  is the  $x$ -coordinate of a boundary node adjacent to node  $n$ . The symbol  $\sigma_n$  in equation (5.8) stands for the flux [ $\text{LT}^{-1}$ ] across the boundary in the vicinity of boundary node  $n$  (positive when directed outward of the system). The boundary flux is assumed to be uniform over each boundary segment. The entries of the vector  $Q_n$  are zero at all internal nodes, which do not act as sources or sinks for water.

The numerical procedure leading to (5.4) incorporates two important assumptions in addition to those related to the Galerkin finite element approach. One assumption concerns the time derivatives of the nodal values of the water content in (5.4). These time derivatives were weighted according to

$$\frac{d\theta_n}{dt} = \frac{\sum_e \int_{\Omega_e} \frac{\partial \theta}{\partial t} \phi_n d\Omega}{\sum_e \int_{\Omega_e} \phi_n d\Omega} \quad (5.15)$$

This assumption implements mass-lumping, which has been shown to improve the rate of convergence of the iterative solution process [e.g., *Neuman, 1973*].

A second assumption in the numerical scheme is related to the anisotropy tensor  $\mathbf{K}^A$  which is taken to be constant over each element. By contrast, the water content  $\theta$ , the hydraulic conductivity  $K$ , the soil water capacity  $C$ , and the root water extraction rate  $S$ , at a given point in time are assumed to vary linearly over each element,  $e$ . For example, the water content is expanded over each element as follows:

$$\begin{aligned}
\theta(x, z) &= \sum_{n=1}^3 \theta(x_n, z_n) \phi_n(x, z) && \text{for } (x, z) \in \Omega_e \\
\theta(x, y, z) &= \sum_{n=1}^4 \theta(x_n, y_n, z_n) \phi_n(x, y, z) && \text{for } (x, y, z) \in \Omega_e
\end{aligned} \tag{5.16}$$

where  $n$  stands for the corners of element  $e$ . The advantage of linear interpolation is that no numerical integration is needed to evaluate the coefficients in (5.4).

## 5.2. Time Discretization

Integration of (5.4) in time is achieved by discretizing the time domain into a sequence of finite intervals and replacing the time derivatives by finite differences. An implicit (backward) finite difference scheme is used for both saturated and unsaturated conditions:

$$[F] \frac{\{\theta\}_{j+1} - \{\theta\}_j}{\Delta t_j} + [A]_{j+1} \{h\}_{j+1} = \{Q\}_j - \{B\}_{j+1} - \{D\}_j \tag{5.17}$$

where  $j+1$  denotes the current time level at which the solution is being considered,  $j$  refers to the previous time level, and  $\Delta t_j = t_{j+1} - t_j$ . Equation (5.17) represents the final set of algebraic equations to be solved. Since the coefficients  $\theta$ ,  $A$ ,  $B$ ,  $D$ , and  $Q$  ( $Q$  for only gradient-type boundary conditions) are functions of  $h$ , the set of equations is generally highly nonlinear. Note that the vectors  $D$  and  $Q$  are evaluated at the old time level.

## 5.3. Numerical Solution Strategy

### 5.3.1. Iterative Process

Because of the nonlinear nature of (5.17), an iterative process must be used to obtain solutions of the global matrix equation at each new time step. For each iteration a system of linearized algebraic equations is first derived from (5.17), which, after incorporation of the boundary

conditions, is solved using either Gaussian elimination or the conjugate gradient method (see Section 8.5). The Gaussian elimination process takes advantage of the banded and symmetric features of the coefficient matrices in (5.17). After inversion, the coefficients in (5.17) are re-evaluated using the first solution, and the new equations are again solved. The iterative process continues until a satisfactory degree of convergence is obtained, i.e., until at all nodes in the saturated (or unsaturated) region the absolute change in pressure head (or water content) between two successive iterations becomes less than some small value determined by the imposed absolute pressure head (or water content) tolerance [Šimůnek and van Genuchten, 1994]. The first estimate (at zero iteration) of the unknown pressure heads at each time step is obtained by extrapolation from the pressure head values at the previous two time levels.

### 5.3.2. Treatment of the Water Capacity Term

The iteration process is extremely sensitive to the method used for evaluating the water content term ( $\Delta\theta/\Delta t$ ) in equation (5.17). The present version of HYDRUS code uses the "mass-conservative" method proposed by Celia *et al.* [1990]. Their method has been shown to provide excellent results in terms of minimizing the mass balance error. The mass-conservative method proceeds by separating the water content term into two parts:

$$[F] \frac{\{\theta\}_{j+1} - \{\theta\}_j}{\Delta t_j} = [F] \frac{\{\theta\}_{j+1}^{k+1} - \{\theta\}_{j+1}^k}{\Delta t_j} + [F] \frac{\{\theta\}_{j+1}^k - \{\theta\}_j}{\Delta t_j} \quad (5.18)$$

where  $k+1$  and  $k$  denote the current and previous iteration levels, respectively; and  $j+1$  and  $j$  the current and previous time levels, respectively. Notice that the second term on the right hand side of (5.18) is known prior to the current iteration. The first term on the right hand side can be expressed in terms of the pressure head, so that (5.18) becomes

$$[F] \frac{\{\theta\}_{j+1} - \{\theta\}_j}{\Delta t_j} = [F][C]_{j+1} \frac{\{h\}_{j+1}^{k+1} - \{h\}_{j+1}^k}{\Delta t_j} + [F] \frac{\{\theta\}_{j+1}^k - \{\theta\}_j}{\Delta t_j} \quad (5.19)$$

where  $C_{nm} = \delta_{nm} C_n$ , in which  $C_n$  represents the nodal value of the soil water capacity. The first term

on the right hand side of (5.19) should vanish at the end of the iteration process if the numerical solution converges. This particular feature guarantees relatively small mass balance errors in the solution.

### 5.3.3. Time Control

Three different time discretizations are introduced in HYDRUS: (1) time discretizations associated with the numerical solution, (2) time discretizations associated with the implementation of boundary conditions, and (3) time discretizations which provide printed output of the simulation results (e.g., nodal values of dependent variables, water and solute mass balance components, and other information about the flow regime).

Discretizations 2 and 3 are mutually independent; they generally involve variable time steps as described in the input data file. Discretization 1 starts with a prescribed initial time increment,  $\Delta t$ . This time increment is automatically adjusted at each time level according to the following rules [Mls, 1982; Vogel, 1987]:

- a. Discretization 1 must coincide with time values resulting from discretizations 2 and 3.
- b. Time increments cannot become less than a preselected minimum time step,  $\Delta t_{min}$ , nor exceed a maximum time step,  $\Delta t_{max}$  (i.e.,  $\Delta t_{min} \leq \Delta t \leq \Delta t_{max}$ ).
- c. If, during a particular time step, the number of iterations necessary to reach convergence is  $\leq 3$ , the time increment for the next time step is increased by multiplying  $\Delta t$  by a predetermined constant  $> 1$  (usually between 1.1 and 1.5). If the number of iterations is  $\geq 7$ ,  $\Delta t$  for the next time level is multiplied by a constant  $< 1$  (usually between 0.3 and 0.9).
- d. If, during a particular time step, the number of iterations at any time level becomes greater than a prescribed maximum (usually between 10 and 50), the iterative process for that time level is terminated. The time step is subsequently reset to  $\Delta t/3$ , and the iterative process restarted.

The selection of optimal time steps,  $\Delta t$ , is also influenced by the solution scheme for solute transport (see Section 6.4.6).

#### 5.3.4. Treatment of Pressure Head Boundary Conditions

Finite element equations corresponding to Dirichlet nodes where the pressure head is prescribed can, at least in principle, be eliminated from the global matrix equation. An alternative and numerically simpler approach is to replace the Dirichlet finite element equations by dummy expressions of the form [Neuman, 1974]

$$\delta_{nm} h_m = \psi_n \quad (5.20)$$

where  $\delta_{nm}$  is the Kronecker delta and  $\psi_n$  is the prescribed value of the pressure head at node  $n$ . The values of  $h_n$  in all other equations are set equal to  $\psi_n$  and the appropriate entries containing  $\psi_n$  in the left hand side matrix are incorporated into the known vector on the right-hand side of the global matrix equation. When done properly, this rearrangement will preserve symmetry in the matrix equation. This procedure is applied only when Gaussian elimination is used to solve the matrix equations. When the conjugate gradient solver is used, then the finite element equation representing the Dirichlet node is modified as follows. The right hand side of this equation is set equal to the prescribed pressure head multiplied by a large number ( $10^{30}$ ), and entry on the left hand side representing the Dirichlet node is set equal to this large number. After solving for all pressure heads, the value of the flux  $Q_n$  can be calculated explicitly and accurately from the original finite element equation associated with node  $n$  [e.g., Lynch, 1984].

#### 5.3.5. Flux and Gradient Boundary Conditions

The values of the fluxes  $Q_n$  at nodal points along prescribed flux and gradient boundaries are computed according to equation (5.8). Internal nodes which act as Neumann type sources or sinks have values of  $Q_n$  equal to the imposed fluid injection or extraction rate.

#### 5.3.6. Atmospheric Boundary Conditions and Seepage Faces

Atmospheric boundaries are simulated by applying either prescribed head or prescribed flux boundary conditions depending upon whether equation (2.58) or (2.59) is satisfied [Neuman, 1974].

If (2.59) is not satisfied, node  $n$  becomes a prescribed head boundary. If, at any point in time during the computations, the calculated flux exceeds the specified potential flux in (2.47), the node will be assigned a flux equal to the potential value and treated again as a prescribed flux boundary.

All nodes expected to be part of a seepage face during code execution must be identified a priori. During each iteration, the saturated part of a potential seepage face is treated as a prescribed pressure head boundary with  $h=0$ , while the unsaturated part is treated as a prescribed flux boundary with  $Q=0$ . The lengths of the two surface segments are continually adjusted [Neuman, 1974] during the iterative process until the calculated values of  $Q$  (equation (5.8)) along the saturated part, and the calculated values of  $h$  along the unsaturated part, are all negative, thus indicating that water is leaving the flow region through the saturated part of the surface boundary only.

### 5.3.7. Tile Drains as Boundary Conditions

The representation of tile drains as boundary conditions is based on studies by *Vimoke et al.* [1963] and *Fipps et al.* [1986]. The approach uses results of electric analog experiments conducted by *Vimoke and Taylor* [1962] who reasoned that drains can be represented by nodal points in a regular finite element mesh, provided adjustments are made in the hydraulic conductivity,  $K$ , of neighboring elements. The adjustments should correspond to changes in the electric resistance of conducting paper as follows

$$K_{drain} = KC_d \quad (5.21)$$

where  $K_{drain}$  is the adjusted conductivity [ $LT^{-1}$ ], and  $C_d$  is the correction factor [-].  $C_d$  is determined from the ratio of the effective radius,  $d_e$  [L], of the drain to the side length,  $D$  [L], of the square formed by finite elements surrounding the drain node [Vimoke et al., 1962]:

$$C_d = \frac{Z'_0}{Z_0} \approx \frac{\sqrt{\mu_0 / \varepsilon_0}}{138 \log_{10} \rho_d + 6.48 - 2.34A - 0.48B - 0.12C} \quad (5.22)$$

where  $Z'_0$  is the characteristic impedance of free space ( $\approx 376.7$  ohms),  $\mu_0$  is the permeability of free space,  $\varepsilon_0$  is the permittivity of free space, and  $Z_0$  is the characteristic impedance of a transmission



line analog of the drain. The coefficients in (5.22) are given by

$$\begin{aligned} \rho_d &= \frac{D}{d} & A &= \frac{1+0.405\rho_d^{-4}}{1-0.405\rho_d^{-4}} \\ B &= \frac{1+0.163\rho_d^{-8}}{1-0.163\rho_d^{-8}} & C &= \frac{1+0.067\rho_d^{-12}}{1-0.067\rho_d^{-12}} \end{aligned} \quad (5.23)$$

where  $d_e$  is the effective drain diameter to be calculated from the number and size of small openings in the drain tube [Mohammad and Skaggs, 1984], and  $D$  is the size of the square in the finite element mesh surrounding the drain having adjusted hydraulic conductivities. The approach above assumes that the node representing a drain must be surrounded by finite elements (either triangular or quadrilateral), which form a square whose hydraulic conductivities are adjusted according to (5.21). This method of implementing drains by means of a boundary condition gives an efficient, yet relatively accurate, prediction of the hydraulic head in the immediate vicinity of the drain, as well as of the drain flow rate [Fipps *et al.*, 1986]. More recent studies have shown that the correction factor,  $C_d$ , could be further reduced by a factor of 2 [Rogers and Fouss, 1989] or 4 [Tseng, 1994, personal communication]. These two studies compared numerical simulations of the flow of ponded water into a tile drain system with an analytical solution given by Kirkham [1949]. Pressure head contours calculated numerically with the original correction factor  $C_d$  (5.22), as well as with the additionally reduced correction factor  $C_d/4$ , were compared with the analytical results in Šimůnek *et al.* [1994].

### 5.3.8. Water Balance Computations

The HYDRUS code performs water balance computations at prescribed times for several preselected subregions of the flow domain. The water balance information for each subregion consists of the actual volume of water,  $V$  ( $[L^2]$  or  $[L^3]$ ), in that subregion, and the rate,  $O$  ( $[L^2T^{-1}]$  or  $[L^3T^{-1}]$ ), of inflow or outflow to or from the subregion.  $V$  and  $O$  are given by

$$\begin{aligned}
V &= \sum_e \kappa A_e \frac{\theta_i + \theta_j + \theta_k}{3} && \text{for 2D} \\
V &= \sum_e V_e \frac{\theta_i + \theta_j + \theta_k + \theta_l}{4} && \text{for 3D}
\end{aligned} \tag{5.24}$$

and

$$O = \frac{V_{new} - V_{old}}{\Delta t} \tag{5.25}$$

respectively, where  $\theta_i$ ,  $\theta_j$ ,  $\theta_k$ , and  $\theta_l$  are water contents evaluated at the corner nodes of element  $e$ , and where  $V_{new}$  and  $V_{old}$  are volumes of water in the subregion computed at the current and previous time levels, respectively. The summation in (5.24) is taken over all elements within the subregion.

The absolute error in the mass balance is calculated as

$$\mathcal{E}_a^w = V_t - V_0 + S_t \int_0^t T_a dt - \int_0^t \sum_{n_r} Q_n dt \tag{5.26}$$

where  $V_t$  and  $V_0$  are the volumes of water in the flow domain at time  $t$  and zero, respectively, as calculated with (5.24). The third term on the right-hand side represents the cumulative root water uptake amount, while the fourth term gives the cumulative flux through nodes,  $n_r$ , located along the boundary of the flow domain or at internal source and sink nodes.

The accuracy of the numerical solution is evaluated in terms of the relative error,  $\mathcal{E}_r^w$  [%], in the water mass balance as follows:

$$\mathcal{E}_r^w = \frac{|\mathcal{E}_a^w|}{\max \left[ \sum_e |V_t^e - V_0^e|, S_t \int_0^t T_a dt + \int_0^t \sum_{n_r} |Q_n| dt \right]} \tag{5.27}$$

where  $V_t^e$  and  $V_0^e$  are the volumes of water in element  $e$  at times  $t$  and zero, respectively. Note that HYDRUS does not relate the absolute error to the volume of water in the flow domain, but instead to the maximum value of two quantities. The first quantity represents the sum of the absolute changes in water content over all elements, whereas the second quantity is the sum of the absolute

values of all fluxes in and out of the flow domain. This criterion is much stricter than the usual criterion involving the total volume of water in the flow domain. This is because cumulative boundary fluxes are often much smaller than the volume in the domain, especially at the beginning of the simulation.

### 5.3.9. Computation of Nodal Fluxes

Components of the Darcian flux are computed at each time level during the simulation only when the water flow and solute transport equations are solved simultaneously. When the flow equation is being solved alone, the flux components are calculated only at selected print times. The  $x$ - and  $z$ -components of the nodal fluxes for a two-dimensional problem are computed for each node  $n$  according to:

$$\begin{aligned}
 q_x &= -\frac{K_n}{N_e} \sum_{e_n} \left[ \frac{\gamma_i^x h_i + \gamma_j^x h_j + \gamma_k^x h_k}{2A_e} + K_{xz}^A \right] \\
 q_z &= -\frac{K_n}{N_e} \sum_{e_n} \left[ \frac{\gamma_i^z h_i + \gamma_j^z h_j + \gamma_k^z h_k}{2A_e} + K_{zz}^A \right] \\
 \gamma_n^x &= K_{xx}^A b_n + K_{xz}^A c_n \\
 \gamma_n^z &= K_{xz}^A b_n + K_{zz}^A c_n
 \end{aligned} \tag{5.28}$$

and  $x$ -,  $y$ - and  $z$ -components for a three-dimensional problem as follows:

$$\begin{aligned}
q_x &= -\frac{K_n}{N_e} \sum_{e_n} \left[ \frac{\gamma_i^x h_i + \gamma_j^x h_j + \gamma_k^x h_k + \gamma_l^x h_l}{6V_e} + K_{xz}^A \right] \\
q_y &= -\frac{K_n}{N_e} \sum_{e_n} \left[ \frac{\gamma_i^y h_i + \gamma_j^y h_j + \gamma_k^y h_k + \gamma_l^y h_l}{6V_e} + K_{yz}^A \right] \\
q_z &= -\frac{K_n}{N_e} \sum_{e_n} \left[ \frac{\gamma_i^z h_i + \gamma_j^z h_j + \gamma_k^z h_k + \gamma_l^z h_l}{6V_e} + K_{zz}^A \right] \\
\gamma_n^x &= K_{xx}^A b_n + K_{xy}^A c_n + K_{xz}^A d_n \\
\gamma_n^y &= K_{xy}^A b_n + K_{yy}^A c_n + K_{yz}^A d_n \\
\gamma_n^z &= K_{xz}^A b_n + K_{yz}^A c_n + K_{zz}^A d_n
\end{aligned} \tag{5.29}$$

where  $N_e$  is the number of sub-elements  $e_n$  adjacent to node  $n$ . Einstein's summation convention is not used in (5.28).

### 5.3.10. Water Uptake by Plant Roots

HYDRUS considers the root zone to consist of all nodes,  $n$ , for which the potential root water uptake distribution,  $b$  (see Section 2.2), is greater than zero. The root water extraction rate is assumed to vary linearly over each element; this leads to approximation (5.9) for the root water extraction term  $D_n$  in the global matrix equation. The values of the actual root extraction rate  $S_n$  in (5.9) are evaluated with (2.15). In order to speed up the calculations, the extraction rates  $S_n$  are calculated at the old time level and are not updated during the iterative solution process at a given time step. HYDRUS calculates the total rate of transpiration per unit soil surface length using the equation

$$\begin{aligned}
T_a &= \frac{1}{S_t} \sum_e \kappa A_e \bar{S}_e && \text{for 2D} \\
T_a &= \frac{1}{S_t} \sum_e V_e \bar{S}_e && \text{for 3D}
\end{aligned} \tag{5.30}$$

in which the summation takes place over all elements within the root zone.

### 5.3.11. Evaluation of the Soil Hydraulic Properties

At the beginning of a numerical simulation, HYDRUS generates for each soil type in the flow domain a table of water contents, hydraulic conductivities, and specific water capacities from the specified set of hydraulic parameters. The values of  $\theta_i$ ,  $K_i$  and  $C_i$  in the table are evaluated at prescribed pressure heads  $h_i$  within a specified interval  $(h_a, h_b)$ . The entries in the table are generated such that

$$\frac{h_{i+1}}{h_i} = \text{constant} \quad (5.31)$$

which means that the spacing between two consecutive pressure head values increases in a logarithmic fashion. Values for the hydraulic properties,  $\theta(h)$ ,  $K(h)$  and  $C(h)$ , are computed during the iterative solution process using linear interpolation between the entries in the table. If an argument  $h$  falls outside the prescribed interval  $(h_a, h_b)$ , the hydraulic characteristics are evaluated directly from the hydraulic functions, i.e., without interpolation. The above interpolation technique was found to be much faster computationally than direct evaluation of the hydraulic functions over the entire range of pressure heads, except when very simple hydraulic models were used.

### 5.3.12. Implementation of Hydraulic Conductivity Anisotropy

Since the hydraulic conductivity anisotropy tensor,  $\mathbf{K}^A$ , is assumed to be symmetric, it is possible to define at any point in the flow domain a local coordinate system for which the tensor  $\mathbf{K}^A$  is diagonal (i.e., having zeroes everywhere except on the diagonal). The diagonal entries  $K_1^A$  and  $K_2^A$  (and  $K_3^A$  for 3D) of  $\mathbf{K}^A$  are referred to as the principal components of  $\mathbf{K}^A$ .

The HYDRUS code permits one to vary the orientation of the local principal directions from element to element. For this purpose, the local coordinate axes are subjected to a rotation such that they coincide with the principal directions of the tensor  $\mathbf{K}^A$ . The principal components  $K_1^A$  and  $K_2^A$  (and  $K_3^A$  for 3D), together with the angle  $\omega_a$  (the cosines of angles) between the principal direction of  $K_1^A$  and the  $x$ -axis (axes) of the global coordinate system, are specified for each element. Each locally determined tensor  $\mathbf{K}^A$  is transformed to the global coordinate system at the beginning of the

simulation using the following rules for a two-dimensional problem:

$$\begin{aligned}
 K_{xx}^A &= K_1^A \cos^2 \omega_a + K_2^A \sin^2 \omega_a \\
 K_{zz}^A &= K_1^A \sin^2 \omega_a + K_2^A \cos^2 \omega_a \\
 K_{xz}^A &= (K_2^A - K_1^A) \sin \omega_a \cos \omega_a
 \end{aligned}
 \tag{5.32}$$

and for a three-dimensional problem:

$$\begin{aligned}
 K_{xx}^A &= K_1^A a_{11} a_{11} + K_2^A a_{12} a_{12} + K_3^A a_{13} a_{13} \\
 K_{yy}^A &= K_1^A a_{12} a_{12} + K_2^A a_{22} a_{22} + K_3^A a_{23} a_{23} \\
 K_{zz}^A &= K_1^A a_{13} a_{13} + K_2^A a_{23} a_{23} + K_3^A a_{33} a_{33} \\
 K_{xy}^A &= K_1^A a_{11} a_{12} + K_2^A a_{12} a_{22} + K_3^A a_{13} a_{23} \\
 K_{xz}^A &= K_1^A a_{11} a_{13} + K_2^A a_{12} a_{23} + K_3^A a_{13} a_{33} \\
 K_{yz}^A &= K_1^A a_{12} a_{13} + K_2^A a_{22} a_{23} + K_3^A a_{23} a_{33}
 \end{aligned}
 \tag{5.33}$$

where  $a_{ij}$  represents cosine of angle between the  $i$ th principal direction of the tensor  $\mathbf{K}^A$  and the  $j$ -axis of the global coordinate system.

### 5.3.13. Steady-State Analysis

All transient flow problems are solved by time marching until a prescribed time is reached. The steady-state problem can be solved in the same way, i.e., by time marching until two successive solutions differ less than some prescribed pressure head tolerance. HYDRUS implements a faster way of obtaining the steady-state solution without having to go through a large number of time steps. The steady-state solution for a set of imposed boundary conditions is obtained directly during one set of iterations at the first time step by equating the time derivative term in the Richards' equation (2.1) to zero.

## 6. NUMERICAL SOLUTION OF THE SOLUTE TRANSPORT EQUATION

The Galerkin finite element method is also used to solve the solute and heat transport equations (equations (3.11) and (4.1), respectively) subject to appropriate initial and boundary conditions. Since the heat transport equation (4.1) has the same mathematical form as the (linearized) solute transport equation (3.11), the numerical solution will be given here only for solute transport. The solution procedure largely parallels the approach used in Section 5 for the flow equation.

### 6.1. Space Discretization

The dependent variable, the concentration function  $c(x,y,z,t)$ , is approximated by a finite series  $c'(x,y,z,t)$  of the form

$$c'(x, y, z, t) = \sum_{n=1}^N \phi_n(x, y, z) c_n(t) \quad (6.1)$$

where  $\phi_n$  are the selected linear basis functions,  $c_n$  are the unknown time dependent coefficients which represent solutions of (5.11) at the finite element nodal points and, as before,  $N$  is the total number of nodal points. Application of the standard Galerkin method leads to the following set of  $N$  equations

$$\int_{\Omega} \left[ -\theta R \frac{\partial c}{\partial t} - q_i \frac{\partial c}{\partial x_i} + \frac{\partial}{\partial x_i} \left( \theta D_{ij} \frac{\partial c}{\partial x_j} \right) + Fc + G \right] \phi_n d\Omega = 0 \quad (6.2)$$

Application of Green's theorem to the second derivatives in (6.2) and substitution of  $c$  by  $c'$  results in the following system of time-dependent differential equations

$$\begin{aligned} \sum_e \int_{\Omega_e} \left[ \left( -\theta R \frac{\partial c'}{\partial t} - q_i \frac{\partial c'}{\partial x_i} + Fc' + G \right) \phi_n - \theta D_{ij} \frac{\partial c'}{\partial x_j} \frac{\partial \phi_n}{\partial x_i} \right] d\Omega + \\ + \sum_e \int_{\Gamma_N^e} \theta D_{ij} \frac{\partial c'}{\partial x_j} n_i \phi_n d\Gamma = 0 \end{aligned} \quad (6.3)$$

or in matrix form:

$$[Q] \frac{d\{c\}}{dt} + [S]\{c\} + \{f\} = -\{Q^D\} \quad (6.4)$$

where

$$\begin{aligned} Q_{nm} &= \delta_{nm} \sum_e (-\theta R)_l \int_{\Omega_e} \phi_l \phi_n \phi_m d\Omega = -\sum_e \frac{\kappa A_e}{12} (3\bar{\theta} \bar{R} + \theta_n R_n) \delta_{nm} && \text{for 2D} \\ &= -\sum_e \frac{V_e}{20} (4\bar{\theta} \bar{R} + \theta_n R_n) \delta_{nm} && \text{for 3D} \end{aligned} \quad (6.5)$$

$$\begin{aligned} S_{nm} &= \sum_e \left[ (-q_i)_l \int_{\Omega_e} \phi_l \phi_n \frac{\partial \phi_m}{\partial x_i} d\Omega - (\theta D_{ij})_l \int_{\Omega_e} \phi_l \frac{\partial \phi_n}{\partial x_i} \frac{\partial \phi_m}{\partial x_j} d\Omega + F_l \int_{\Omega_e} \phi_l \phi_n \phi_m d\Omega \right] = \\ &= \sum_e \left\{ -\frac{\kappa b_m}{24} (3\bar{q}_x + q_{xn}) - \frac{\kappa c_m}{24} (3\bar{q}_z + q_{zn}) + \frac{\kappa A_e}{60} (3\bar{F} + F_n + F_m)(1 + \delta_{nm}) - \right. \\ &\quad \left. - \frac{\kappa}{4A_e} [b_m b_n \theta \bar{D}_{xx} + (b_m c_n + c_m b_n) \theta \bar{D}_{xz} + c_m c_n \theta \bar{D}_{zz}] \right\} && \text{for 2D} \\ &= \sum_e \left\{ -\frac{b_m}{120} (4\bar{q}_x + q_{xn}) - \frac{c_m}{120} (4\bar{q}_y + q_{yn}) - \frac{d_m}{120} (4\bar{q}_z + q_{zn}) + \right. \\ &\quad \left. + \frac{V_e}{120} (4\bar{F} + F_n + F_m)(1 + \delta_{nm}) - \right. \\ &\quad \left. - \frac{1}{36V_e} [b_m b_n \theta \bar{D}_{xx} + c_m c_n \theta \bar{D}_{yy} + d_m d_n \theta \bar{D}_{zz} + (b_m c_n + c_m b_n) \theta \bar{D}_{xy} + \right. \\ &\quad \left. + (b_m d_n + d_m b_n) \theta \bar{D}_{xz} + (c_m d_n + d_m c_n) \theta \bar{D}_{yz}] \right\} && \text{for 3D} \end{aligned} \quad (6.6)$$



$$\begin{aligned}
f_n &= \sum_e G_l \int_{\Omega_e} \phi_l \phi_n d\Omega = \sum_e \frac{\kappa A_e}{12} (3\bar{G} + G_n) && \text{for 2D} \\
&= \sum_e \frac{V_e}{20} (4\bar{G} + G_n) && \text{for 3D}
\end{aligned} \tag{6.7}$$

in which the overlined variables represent average values over a given element  $e$ . The notation in the above equations is similar as in (5.10). The boundary integral in (6.3) represents the dispersive flux,  $Q_n^D$ , across the boundary and will be discussed later in Section 6.3.4.

The derivation of equations (6.5) through (6.7) invoked several important assumptions in addition to those involved in the Galerkin finite element approach [Huyakorn and Pinder, 1983; van Genuchten, 1978]. First, the different coefficients under the integral signs ( $\theta R$ ,  $q_i$ ,  $\theta D_{ij}$ ,  $F$ ,  $G$ ) were expanded linearly over each element, similarly as for the dependent variable, i.e., in terms of their nodal values and associated basis functions. Second, mass lumping was invoked by redefining the nodal values of the time derivative in (6.4) as weighted averages over the entire flow region:

$$\frac{dc_n}{dt} = \frac{\sum_e \int_{\Omega_e} \theta R \frac{\partial c}{\partial t} \phi_n d\Omega}{\sum_e \int_{\Omega_e} \theta R \phi_n d\Omega} \tag{6.8}$$

## 6.2. Time Discretization

The Galerkin method is used only for approximating the spatial derivatives while the time derivatives are discretized by means of finite differences. A first-order approximation of the time derivatives leads to the following set of algebraic equations:

$$[Q]_{j+\varepsilon} \frac{\{c\}_{j+1} - \{c\}_j}{\Delta t} + \varepsilon [S]_{j+1} \{c\}_{j+1} + (1-\varepsilon) [S]_j \{c\}_j + \varepsilon \{f\}_{j+1} + (1-\varepsilon) \{f\}_j = 0 \tag{6.9}$$

where  $j$  and  $j+1$  denote the previous and current time levels, respectively;  $\Delta t$  is the time increment, and  $\varepsilon$  is a time weighing factor. The incorporation of the dispersion flux,  $Q_n^D$ , into matrix  $[Q]$  and

vector  $\{f\}$  is discussed in Section 6.3.4. The coefficient matrix  $[Q]_{j+\varepsilon}$  is evaluated using weighted averages of the current and previous nodal values of  $\theta$  and  $R$ . Equation (6.9) can be rewritten in the form:

$$[G]\{c\}_{j+1} = \{g\} \quad (6.10)$$

where

$$[G] = \frac{1}{\Delta t}[Q]_{j+\varepsilon} + \varepsilon[S]_{j+1} \quad (6.11)$$

$$\{g\} = \frac{1}{\Delta t}[Q]_{j+\varepsilon}\{c\}_j - (1-\varepsilon)[S]_j\{c\}_j - \varepsilon\{f\}_{j+1} - (1-\varepsilon)\{f\}_j$$

Higher-order approximations for the time derivative in the transport equation were derived by *van Genuchten* [1976, 1978]. The higher-order effects may be incorporated into the transport equation by introducing time-dependent dispersion corrections as follows

$$D_{ij}^- = D_{ij} - \frac{q_i q_j \Delta t}{6\theta^2 R} \quad (6.12)$$

$$D_{ij}^+ = D_{ij} + \frac{q_i q_j \Delta t}{6\theta^2 R}$$

where the superscripts + and - indicate evaluation at the old and new time levels, respectively.

### 6.3. Numerical Solution for Linear Nonequilibrium Solute Transport

The same solution procedure as described in Sections 6.1 and 6.2 is used here for either linear equilibrium or nonlinear (both equilibrium and nonequilibrium) solute transport. However, linear nonequilibrium transport is implemented somewhat differently. First, equation (3.9), simplified for linear adsorption, is discretized using finite differences as follows

$$\begin{aligned} \frac{s^{t+\Delta t} - s^t}{\Delta t} = & \varepsilon[\omega(1-f)k_s c - \omega s^k - \mu_s s^k + (1-f)\gamma]^{t+\Delta t} + \\ & + (1-\varepsilon)[\omega(1-f)k_s c - \omega s^k - \mu_s s^k + (1-f)\gamma]^t \end{aligned} \quad (6.13)$$

The new adsorbed concentration for type-2 sorption sites follows directly from (6.13):

$$s^{t+\Delta t} = s^t \frac{2 - \Delta t(\omega + \mu_s)^t}{2 + \Delta t(\omega + \mu_s)^{t+\Delta t}} + \frac{\Delta t(1-f)[(\omega k_s c)^{t+\Delta t} + (\omega k_s c)^t + \gamma^{t+\Delta t} + \gamma^t]}{2 + \Delta t(\omega + \mu_s)^{t+\Delta t}} \quad (6.14)$$

This term is incorporated directly into  $F$  and  $G$  so that they have the following values:

$$F_*^{t+\Delta t} = F^{t+\Delta t} - \left\{ \frac{\rho\omega\Delta t(1-f)\omega k_s}{2 + \Delta t(\omega + \mu_s)} \right\}^{t+\Delta t} \quad (6.15)$$

$$G_*^{t+\Delta t} = G^{t+\Delta t} + \rho\omega^{t+\Delta t} \left\{ s^t \frac{2 - \Delta t(\omega + \mu_s)^t}{2 + \Delta t(\omega + \mu_s)^{t+\Delta t}} + \frac{\Delta t(1-f)[(\omega k_s c)^t + \gamma^{t+\Delta t} + \gamma^t]}{2 + \Delta t(\omega + \mu_s)^{t+\Delta t}} \right\} \quad (6.16)$$

where  $F_*^{t+\Delta t}$  and  $G_*^{t+\Delta t}$  are the values of parameters  $F$  and  $G$  for linear nonequilibrium solute transport, and  $F^{t+\Delta t}$  and  $G^{t+\Delta t}$  are the original values of  $F$  and  $G$ . The above procedure avoids having to solve two simultaneous equations for linear nonequilibrium transport. Once the transport equation with the modified  $F$  and  $G$  parameters is solved using the methods discussed earlier to yield the concentration  $c^{t+\Delta t}$ , equation (6.14) is used to update the adsorbed concentration  $s^{t+\Delta t}$ .

For physical nonequilibrium (dual-porosity) transport, equation (3.18), simplified for linear adsorption, is discretized using finite differences as follows

$$A \frac{c_{im}^{t+\Delta t} - c_{im}^t}{\Delta t} = \varepsilon [\omega(c - c_{im}) - Bc_{im} + E]^{t+\Delta t} + (1 - \varepsilon) [\omega(c - c_{im}) - Bc_{im} + E]^t$$

where

$$\begin{aligned} A &= \theta_{im} + (1 - f)\rho k_s \\ B &= \theta_{im}\mu_w + (1 - f)\rho k_s \mu_s \\ E &= \theta_{im}\gamma_w + (1 - f)\rho \gamma_s \end{aligned}$$

(6.17)

The new concentration in the immobile region follows directly from (6.13):

$$c_{im}^{t+\Delta t} = c_{im}^t \frac{2A - \Delta t(\omega + B)^t}{2A + \Delta t(\omega + B)^{t+\Delta t}} + \frac{\Delta t [(\omega c_{im})^{t+\Delta t} + (\omega c_{im})^t + E^{t+\Delta t} + E^t]}{2A + \Delta t(\omega + B)^{t+\Delta t}} \quad (6.18)$$

Similarly as for the chemical nonequilibrium case, equation (6.18) is incorporated directly into  $F$  and  $G$  to obtain following values:

$$F_*^{t+\Delta t} = F^{t+\Delta t} - \left\{ \frac{\omega \Delta t \omega}{2A + \Delta t(\omega + B)} \right\}^{t+\Delta t} \quad (6.19)$$

$$G_*^{t+\Delta t} = G^{t+\Delta t} + \omega^{t+\Delta t} \left\{ c_{im}^t \frac{2A - \Delta t(\omega + B)^t}{2A + \Delta t(\omega + B)^{t+\Delta t}} + \frac{\Delta t [(\omega c)^t + E^{t+\Delta t} + E^t]}{2A + \Delta t(\omega + B)^{t+\Delta t}} \right\} \quad (6.20)$$

The numerical solution for the attachment/detachment approach to nonequilibrium solute transport is handled similarly.

## 6.4. Numerical Solution Strategy

### 6.4.1. Solution Process

The solution process at each time step proceeds as follows. First, an iterative procedure is used to obtain the solution of the Richards' equation (2.1) (see Section 5.3.1). After achieving convergence, the solution of the transport equation (6.10) is implemented. This is done by first determining the nodal values of the fluid flux from nodal values of the pressure head by applying Darcy's law. Nodal values of the water content and the fluid flux at the previous time level are already known from the solution at the previous time step. Values for the water content and the fluid flux are subsequently used as input to the transport equations (first for heat transport and then for solute transport), leading to the system of linear algebraic equations given by (6.10). The structure of the final set of equations depends upon the value of the temporal weighing factor,  $\varepsilon$ . The explicit ( $\varepsilon=0$ ) and fully implicit ( $\varepsilon=1$ ) schemes require that the global matrix  $[G]$  and the vector  $\{g\}$  be evaluated at only one time level (the previous or current time level). All other schemes require evaluation at both time levels. Also, all schemes except for the explicit formulation ( $\varepsilon=0$ ) lead to an asymmetric banded matrix  $[G]$ . The associated set of algebraic equations is solved using either a standard asymmetric matrix equation solver [e.g., *Neuman*, 1972], or the ORTHOMIN method [*Mendoza et al.*, 1991], depending upon the size of final matrix. By contrast, the explicit scheme leads to a diagonal matrix  $[G]$ , which is much easier to solve (but generally requires smaller time steps).

Since the heat transport equation is linear, there is no need for an iterative solution process for heat flow. The same is true for the transport of solutes undergoing only linear sorption reactions. On the other hand, iteration is needed when a nonlinear reaction between the solid and liquid phase is considered. The iteration procedure for solute transport is very similar to that for water flow. The coefficients in (6.10) are re-evaluated using each iteration, and the new equations are again solved using results of the previous iteration. The iterative process continues until a satisfactory degree of convergence is obtained, i.e., until at all nodes the absolute change in concentration between two successive iterations becomes less than some small value determined by the imposed relative and absolute concentration tolerances.

### 6.4.2. Upstream Weighted Formulation

Upstream weighing is provided as an option in the HYDRUS to minimize some of the problems with numerical oscillations when relatively steep concentration fronts are being simulated. For this purpose the second (flux) term of equation (6.3) is not weighted by regular linear basis functions  $\phi_n$ , but instead using the nonlinear functions  $\phi_n^u$  [Yeh and Tripathi, 1990]

$$\begin{aligned}\phi_1^u &= L_1 - 3\alpha_3^w L_2 L_1 + 3\alpha_2^w L_3 L_1 \\ \phi_2^u &= L_2 - 3\alpha_1^w L_3 L_2 + 3\alpha_3^w L_1 L_2 \\ \phi_3^u &= L_3 - 3\alpha_2^w L_1 L_3 + 3\alpha_1^w L_2 L_3\end{aligned}\quad \text{for 2D}$$

(6.21)

$$\begin{aligned}\phi_1^u &= L_1 - 3\alpha_{12}^w L_2 L_1 + 3\alpha_{14}^w L_4 L_1 + 3\alpha_{13}^w L_1 L_3 \\ \phi_2^u &= L_2 - 3\alpha_{23}^w L_3 L_2 + 3\alpha_{12}^w L_1 L_2 + 3\alpha_{24}^w L_2 L_4 \\ \phi_3^u &= L_3 - 3\alpha_{34}^w L_4 L_3 + 3\alpha_{23}^w L_2 L_3 - 3\alpha_{13}^w L_1 L_3 \\ \phi_4^u &= L_4 - 3\alpha_{14}^w L_4 L_1 + 3\alpha_{34}^w L_3 L_4 - 3\alpha_{24}^w L_2 L_4\end{aligned}\quad \text{for 3D}$$

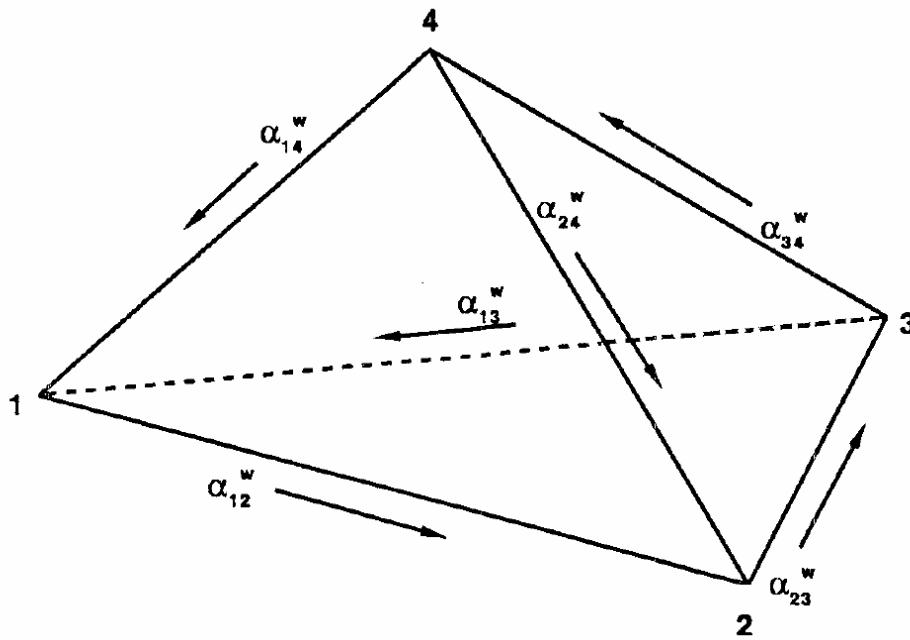


Figure 6.1. Direction definition for the upstream weighting factors  $\alpha_{ij}^w$ .

where  $\alpha_i^w$  is a weighing factor associated with the length of the element size opposite to node  $i$ ,  $\alpha_{ij}^w$  is a weighing factor associated with the line connecting nodes  $i$  and  $j$  (Figure 6.1) and  $L_i$  are the local coordinates. The weighing factors are evaluated using the equation of *Christie et al.* [1976]:

$$\alpha_i^w = \coth\left(\frac{uL}{2D}\right) - \frac{2D}{uL} \quad (6.22)$$

where  $u$ ,  $D$  and  $L$  are the flow velocity, dispersion coefficient and length associated with side  $i$ . The weighing functions  $\phi^i$  ensure that relatively more weight is placed on the flow velocities of nodes located at the upstream side of an element. Evaluating the integrals in (6.3) shows that the following additional terms must be added to the entries of the global matrix  $S_{nm}$  in equation (6.6) in two-dimensional formulation:

$$S_{1j}^{e'} = S_{1j}^e - \frac{b_j}{40} [2q_{x1}(\alpha_2^w - \alpha_3^w) + q_{x2}(\alpha_2^w - 2\alpha_3^w) + q_{x3}(2\alpha_2^w - \alpha_3^w)] - \frac{c_j}{40} [2q_{z1}(\alpha_2^w - \alpha_3^w) + q_{z2}(\alpha_2^w - 2\alpha_3^w) + q_{z3}(2\alpha_2^w - \alpha_3^w)] \quad (6.23)$$

$$S_{2j}^{e'} = S_{2j}^e - \frac{b_j}{40} [q_{x1}(2\alpha_3^w - \alpha_1^w) + 2q_{x2}(\alpha_3^w - \alpha_1^w) + q_{x3}(\alpha_3^w - 2\alpha_1^w)] - \frac{c_j}{40} [q_{z1}(2\alpha_3^w - \alpha_1^w) + 2q_{z2}(\alpha_3^w - \alpha_1^w) + q_{z3}(\alpha_3^w - 2\alpha_1^w)] \quad (6.24)$$

$$S_{3j}^{e'} = S_{3j}^e - \frac{b_j}{40} [q_{x1}(\alpha_1^w - 2\alpha_2^w) + q_{x2}(2\alpha_1^w - \alpha_2^w) + 2q_{x3}(\alpha_1^w - \alpha_2^w)] - \frac{c_j}{40} [q_{z1}(\alpha_1^w - 2\alpha_2^w) + q_{z2}(2\alpha_1^w - \alpha_2^w) + 2q_{z3}(\alpha_1^w - \alpha_2^w)] \quad (6.25)$$

and in three-dimensional formulation

$$S_{1j}^{e'} = S_{1j}^e - \frac{b_j}{240} [q_{x1}(-2\alpha_{12}^w + 2\alpha_{14}^w + 2\alpha_{13}^w) + q_{x2}(-2\alpha_{12}^w + \alpha_{14}^w + \alpha_{13}^w) + q_{x3}(-\alpha_{12}^w + \alpha_{14}^w + 2\alpha_{13}^w) + q_{x4}(-\alpha_{12}^w + 2\alpha_{14}^w + \alpha_{13}^w)] - \frac{c_j}{240} [-q_{y1}(\dots\dots\dots) + \dots] - \frac{d_j}{240} [-q_{z1}(\dots\dots\dots) + \dots] \quad (6.26)$$

$$\begin{aligned}
S_{2j}^{e'} = S_{2j}^e - \frac{b_j}{240} [q_{x1}(-\alpha_{23}^w + 2\alpha_{112}^w + \alpha_{24}^w) + q_{x2}(-2\alpha_{23}^w + 2\alpha_{12}^w + 2\alpha_{24}^w) + \\
+ q_{x3}(-2\alpha_{23}^w + \alpha_{12}^w + \alpha_{24}^w) + q_{x4}(-\alpha_{23}^w + \alpha_{12}^w + 2\alpha_{24}^w)] - \\
- \frac{c_j}{240} [-q_{y1}(\dots\dots\dots) + \dots] - \frac{d_j}{240} [-q_{z1}(\dots\dots\dots) + \dots]
\end{aligned} \quad (6.27)$$

$$\begin{aligned}
S_{3j}^{e'} = S_{3j}^e - \frac{b_j}{240} [q_{x1}(-\alpha_{34}^w + \alpha_{23}^w - 2\alpha_{13}^w) + q_{x2}(-\alpha_{34}^w + 2\alpha_{23}^w - \alpha_{13}^w) + \\
+ q_{x3}(-2\alpha_{34}^w + 2\alpha_{23}^w - 2\alpha_{13}^w) + q_{x4}(-2\alpha_{34}^w + \alpha_{23}^w - \alpha_{13}^w)] - \\
- \frac{c_j}{240} [-q_{y1}(\dots\dots\dots) + \dots] - \frac{d_j}{240} [-q_{z1}(\dots\dots\dots) + \dots]
\end{aligned} \quad (6.28)$$

$$\begin{aligned}
S_{4j}^{e'} = S_{4j}^e - \frac{b_j}{240} [q_{x1}(-2\alpha_{14}^w + \alpha_{34}^w - \alpha_{24}^w) + q_{x2}(-\alpha_{14}^w + \alpha_{34}^w - 2\alpha_{24}^w) + \\
+ q_{x3}(-\alpha_{14}^w + 2\alpha_{34}^w - \alpha_{24}^w) + q_{x4}(-2\alpha_{14}^w + 2\alpha_{34}^w - 2\alpha_{24}^w)] - \\
- \frac{c_j}{240} [-q_{y1}(\dots\dots\dots) + \dots] - \frac{d_j}{240} [-q_{z1}(\dots\dots\dots) + \dots]
\end{aligned} \quad (6.29)$$

The weighing factors are applied only to those element sides that are inclined within 10 degrees from the flow direction.

### 6.4.3. Implementation of First-Type Boundary Conditions

Individual equations in the global matrix equation which correspond to nodes at which the concentration is prescribed are replaced by new equations:

$$\delta_{nm} c_m = c_{n0} \quad (6.30)$$

where  $c_{n0}$  is the prescribed value of the concentration at node  $n$ . This is done only when Gaussian elimination is used to solve the matrix equation. A similar procedure as for water flow (described in Section 5.3.4) is applied when the ORTHOMIN method is used. Because of asymmetry of the global matrix  $[G]$ , no additional manipulations are needed in the resulting system of equations as was the case for the water flow solution.



The total material flux,  $Q_n^T$ , through a boundary at node  $n$  consists of the dispersive flux,  $Q_n^D$ , and the convective flux,  $Q_n^A$ :

$$Q_n^T = Q_n^D + Q_n^A \quad (6.31)$$

The dispersive boundary nodal flux is not known explicitly but must be calculated from equation (6.4). Hence, the dispersion flux,  $Q_n^D$ , for node  $n$  can be calculated as

$$Q_n^D = -\left[ \varepsilon S_{nm}^{j+1} + (1-\varepsilon) S_{nm}^j \right] c_m^j - \varepsilon f_n^{j+1} - (1-\varepsilon) f_n^j - Q_{nm}^{j+\varepsilon} \frac{c_n^{j+1} - c_n^j}{\Delta t} \quad (6.32)$$

The convective flux is evaluated as

$$Q_n^A = Q_n c_n \quad (6.33)$$

where the fluid flux  $Q_n$  is known from the solution of the water flow equation.

#### 6.4.4. Implementation of Third-Type Boundary Conditions

Equation (3.37) is rewritten as follows

$$\theta D_{ij} \frac{\partial c'}{\partial x_j} n_i = q_i n_i (c - c_0) \quad (6.34)$$

When substituted into the last term of (6.3), the boundary integral becomes

$$\sum_e \int_{\Gamma_N^e} \theta D_{ij} \frac{\partial c'}{\partial x_j} n_i \phi_n d\Gamma = Q_n c_n - Q_n c_{n0} \quad (6.35)$$

The first term on the right-hand side of (6.35) represents the convective flux. This term is incorporated into the coefficient matrix  $[S]$  of (6.4). The last term of (6.35) represents the total material flux, which is added to the known vector  $\{f\}$ .

At nodes where free outflow of water and its dissolved solutes takes place, the exit concentration  $c_0$  is equal to the local (nodal) concentration  $c_n$ . In this case the dispersive flux becomes zero and the total material flux through the boundary is evaluated as

$$Q_n^T = Q_n c_n \quad (6.36)$$

The Cauchy boundary condition for volatile solutes is treated in a similar way. Equation (3.39) is rewritten as follows

$$\theta D_{ij} \frac{\partial c'}{\partial x_j} n_i = q_i n_i (c - c_0) - \frac{D_g}{d} (k_g c - g_{atm}) \quad (6.37)$$

Again, when substituted into the last term of (6.3), the boundary integral becomes

$$\sum_e \int_{\Gamma_N^e} \theta D_{ij} \frac{\partial c'}{\partial x_j} n_i \phi_n d\Gamma = Q_n c_n - Q_n c_{n0} - \frac{D_g \Delta L}{d} (k_g c_n - g_{atm}) \quad (6.38)$$

where  $\Delta L$  is the length of the boundary associated with node  $n$ . The last term of (6.38) representing the gas diffusion flux through the stagnant boundary layer at the soil surface is directly added to the vector  $\{f\}$  in equation (6.9), whereas the term containing  $k_g$  and unknown concentration  $c_n$  is incorporated into the coefficient matrix  $[S]$ . The other terms on the right-hand side of (6.38) are treated in the same way as described above for equation (6.35).

#### 6.4.5. Mass Balance Calculations

The total amount of mass in the entire flow domain, or in a preselected subregion, is given by

$$M = \sum_e \int_{\Omega_e} (\theta c + a_v g + \rho s) d\Omega = \sum_e \int_{\Omega_e} \left[ \left( \theta + a_v k_g + \rho f \frac{k_s c^{\beta-1}}{1 + \eta c^\beta} \right) c + \rho s^k \right] d\Omega \quad (6.39)$$

The summation is taken over all elements within the specified region. The equations in this section pertain only to the equilibrium or chemical nonequilibrium models; the mass balance equations for physical nonequilibrium transport are very similar as those for chemical nonequilibrium.

The cumulative amounts  $M^0$  and  $M^1$  of solute removed from the flow region by zero- and first-order reactions, respectively, are calculated as follows

$$M_1^0 = - \int_0^t \sum_e \int_{\Omega_e} (\gamma_{w,1} \theta + \gamma_{s,1} \rho + \gamma_{g,1} a_v) d\Omega dt$$

$$M_1^k = - \int_0^t \sum_e \int_{\Omega_e} \left[ \left( \mu'_{w,k-1} \theta + \mu'_{s,k-1} \rho f \frac{k_{s,k-1} c_{k-1}^{\beta_{k-1}-1}}{1 + \eta_{k-1} c_{k-1}^{\beta_{k-1}}} + \mu'_{g,k-1} a_v k_{g,k-1} \right) c_{k-1} + \right. \quad (6.40)$$

$$\left. + \mu'_{s,k-1} \rho s_{k-1}^k + \gamma_{w,k} \theta + \gamma_{s,k} \rho + \gamma_{g,k} a_v \right] d\Omega dt$$

$$M^1 = \int_0^t \sum_e \int_{\Omega_e} \left\{ (\mu_w + \mu'_w) \theta + (\mu_s + \mu'_s) \rho f \frac{k_s c^{\beta-1}}{1 + \eta c^\beta} + (\mu_g + \mu'_g) a_v k_g \right\} c + \quad (6.41)$$

$$+(\mu_s + \mu'_s) \rho s^k \} d\Omega dt$$

whereas the cumulative amount  $M_r$  of solute taken up by plant roots is given by

$$M_r = \int_0^t \sum_{e_R} \int_{\Omega_e} S c_s d\Omega dt \quad (6.42)$$

where  $e_R$  represents the elements making up the root zone.

Finally, when all boundary material fluxes, decay reactions, and root uptake mass fluxes have been computed, the following mass balance should hold for the flow domain as a whole:

$$M_t - M_0 = \int_0^t \sum_{n_T} Q_n^T dt + M^0 + M^1 - M_r \quad (6.43)$$

where  $M_t$  and  $M_0$  are the amounts of solute in the flow region at times  $t$  and zero, respectively, as calculated with (6.39), and  $n_\Gamma$  represents nodes located along the boundary of the flow domain or at internal sinks and/or sources. The difference between the left- and right-hand sides of (6.43) represents the absolute error,  $\varepsilon_a^c$ , in the solute mass balance. Similarly as for water flow, the accuracy of the numerical solution for solute transport is evaluated by using the relative error,  $\varepsilon_r^c$  [%], in the solute mass balance as follows

$$\varepsilon_r^c = \frac{100|\varepsilon_a^c|}{\max \left[ \sum_e |M_t^e - M_0^e|, |M^0| + |M^1| + |M_r| + \int_0^t \sum_{n_\Gamma} |Q_n^T| dt \right]} \quad (6.44)$$

where  $M_0^e$  and  $M_t^e$  are the amounts of solute in element  $e$  at times 0 and  $t$ , respectively. Note again that HYDRUS does not relate the absolute error to the total amount of mass in the flow region. Instead, the program uses as a reference the maximum value of (1) the absolute change in element concentrations as summed over all elements, and (2) the sum of the absolute values of all cumulative solute fluxes across the flow boundaries including those resulting from sources and sinks in the flow domain.

The total amount of heat energy in the entire flow domain, or in a preselected subregion, is given by

$$W = \sum_e \int_{\Omega_e} (c_n \theta_n + c_o \theta_o + C_w \theta + C_g a_v) T^A d\Omega \quad (6.45)$$

where  $T^A$  is the absolute temperature [K]. The summation is taken over all elements within the specified region.

#### 6.4.6. Oscillatory Behavior

Numerical solutions of the transport equation often exhibit oscillatory behavior and/or excessive numerical dispersion near relatively sharp concentration fronts. These problems can be especially serious for convection-dominated transport characterized by small dispersivities. One way to partially circumvent numerical oscillations is to use upstream weighing as discussed in Section 6.4.2. Undesired oscillations can often be prevented also by selecting an appropriate combination of space and time discretizations. Two dimensionless numbers may be used to characterize the space and time discretizations. One of these is the grid Peclet number,  $Pe_i^e$ , which defines the predominant type of the solute transport (notably the ratio of the convective and dispersive transport terms) in relation to coarseness of the finite element grid:

$$Pe_i^e = \frac{q_i \Delta x_i}{\theta D_{ii}} \quad (6.46)$$

where  $\Delta x_i$  is the characteristic length of a finite element. The Peclet number increases when the convective part of the transport equation dominates the dispersive part, i.e., when a relatively steep concentration front is present. To achieve acceptable numerical results, the spatial discretization must be kept relatively fine to maintain a low Peclet number. Numerical oscillation can be virtually eliminated when the local Peclet numbers do not exceed about 5. However, acceptably small oscillations may be obtained with local Peclet numbers as high as 10 [Huyakorn and Pinder, 1983]. Undesired oscillation for higher Peclet numbers can be effectively eliminated by using upstream weighing (see Section 6.4.2).

A second dimensionless number which characterizes the relative extent of numerical oscillations is the Courant number,  $Cr_i^e$ . The Courant number is associated with the time discretization as follows

$$Cr_i^e = \frac{q_i \Delta t}{\theta R \Delta x_i} \quad (6.47)$$

Three stabilizing options are used in HYDRUS to avoid oscillations in the numerical solution of the solute transport equation [Šimůnek and van Genuchten, 1994]. One option is

upstream weighing (see Section 6.4.2), which effectively eliminates undesired oscillations at relatively high Peclet numbers. A second option for minimizing or eliminating numerical oscillations uses the criterion developed by *Perrochet and Berod* [1993]

$$Pe \cdot Cr \leq \omega_s = 2 \quad (6.48)$$

where  $\omega_s$  is the performance index [-]. This criterion indicates that convection-dominated transport problems having large  $Pe$  numbers can be safely simulated provided  $Cr$  is reduced according to (6.48) [*Perrochet and Berod*, 1993]. When small oscillations in the solution can be tolerated,  $\omega_s$  can be increased to about 5 or 10.

A third stabilization option implemented in HYDRUS also utilizes criterion (6.48). However, instead of decreasing  $Cr$  to satisfy equation (6.48), this option introduces artificial dispersion to decrease the Peclet number. The amount of additional longitudinal dispersion,  $\bar{D}_L$  [L], is given by [*Perrochet and Berod*, 1993]

$$\bar{D}_L = \frac{|q|\Delta t}{\theta R \omega_s} - D_L - \frac{\theta D_d \tau}{|q|} \quad (6.49)$$

The maximum permitted time step is calculated for all three options, as well as with the additional requirement that the Courant number must remain less than or equal to 1. The time step calculated in this way is subsequently used as one of the time discretization rules (rule No. B) discussed in section 5.3.3.

## 7. PARAMETER OPTIMIZATION

Parameter optimization is an indirect approach for estimating the unsaturated soil hydraulic and/or solute transport parameters from transient flow and/or transport data. Inverse methods are typically based upon the minimization of a suitable objective function, which expresses the discrepancy between the observed values and the predicted system response. Soil hydraulic properties for this purpose are assumed to be described by an analytical model with unknown parameter values (see Section 2.3). The system response is represented by a numerical solution of the flow equation, augmented with the parameterized hydraulic functions, selected transport parameters, and suitable initial and boundary conditions. Initial estimates of the optimized system parameters are then iteratively improved during the minimization process until a desired degree of precision is obtained. This methodology was originally applied to one-step and multi-step column outflow data generated in the laboratory [see for example *Kool et al.*, 1985; *van Dam et al.*, 1994], and laboratory or field transport data during steady-state water flow [*van Genuchten*, 1981; *Toride et al.*, 1995]. HYDRUS implements parameter optimization also for estimating the solute transport and reaction parameters from transient water flow and/or solute transport experiments.

### 7.1. Definition of the Objective Function

The objective function  $\Phi$  to be minimized during the parameter estimation process may be defined as [*Šimůnek et al.*, 1998]:

$$\begin{aligned} \Phi(\mathbf{b}, \mathbf{q}, \mathbf{p}) = & \sum_{j=1}^{m_q} v_j \sum_{i=1}^{n_{qj}} w_{i,j} [g_j^*(\mathbf{x}, t_i) - g_j(\mathbf{x}, t_i, \mathbf{b})]^2 + \\ & + \sum_{j=1}^{m_p} v_j \sum_{i=1}^{n_{pj}} \bar{w}_{ij} [p_j^*(\theta_i) - p_j(\theta_i, \mathbf{b})]^2 + \\ & + \sum_{j=1}^{n_b} \hat{v}_j [b_j^* - b_j]^2 \end{aligned} \quad (7.1)$$

where the first term on the right-hand side represents deviations between the measured and calculated space-time variables (e.g., observed pressure heads, water contents, and/or concentrations at different locations and/or time in the flow domain, or the actual or cumulative flux versus time

across a boundary of specified type). In this term,  $m_q$  is the number of different sets of measurements,  $n_{qj}$  is the number of measurements in a particular measurement set,  $q_j^*(\mathbf{x}, t_i)$  represents specific measurements at time  $t_i$  for the  $j$ th measurement set at location  $\mathbf{x}(r, z)$ ,  $q_j(\mathbf{x}, t_i, \mathbf{b})$  are the corresponding model predictions for the vector of optimized parameters  $\mathbf{b}$  (e.g.,  $\theta_r$ ,  $\theta_s$ ,  $\alpha$ ,  $n$ ,  $K_s$ ,  $D_l$ ,  $k_{g,k}$ , ...), and  $v_j$  and  $w_{i,j}$  are weights associated with a particular measurement set or point, respectively. The second term of (7.1) represents differences between independently measured and predicted soil hydraulic properties (e.g., retention,  $\theta(h)$  and/or hydraulic conductivity,  $K(\theta)$  or  $K(h)$  data), while the terms  $m_p$ ,  $n_{pj}$ ,  $p_j^*(\theta_i)$ ,  $p_j(\theta_i, \mathbf{b})$ ,  $\overline{v_{jj}}$  and  $\overline{w_{i,j}}$  have similar meanings as for the first term but now for the soil hydraulic properties. The last term of (7.1) represents a penalty function for deviations between prior knowledge of the soil hydraulic parameters,  $b_j^*$ , and their final estimates,  $b_j$ , with  $n_b$  being the number of parameters with prior knowledge and  $\hat{v}_j$  representing pre-assigned weights. Estimates, which make use of prior information (such as those used in the third term of (7.1)) are known as Bayesian estimates. We note that the covariance (weighting) matrices, which provide information about the measurement accuracy, as well as any possible correlation between measurement errors and/or parameters, are assumed to be diagonal in this study. The weighting coefficients  $v_j$ , which minimize differences in weighting between different data types because of different absolute values and numbers of data involved, are given by [Clausnitzer and Hopmans, 1995]:

$$v_j = \frac{1}{n_j \sigma_j^2} \quad (7.2)$$

which causes the objective function to become the average weighted squared deviation normalized by the measurement variances  $\sigma_j^2$ .

## 7.2. Marquardt-Levenberg Optimization Algorithm

Minimization of the objective function  $\Phi$  is accomplished by using the Levenberg-Marquardt nonlinear minimization method (a weighted least-squares approach based on Marquardt's maximum neighborhood method) [Marquardt, 1963]. This method combines the Newton and steepest descend methods, and generates confidence intervals for the optimized parameters. The



method was found to be very effective and has become a standard in nonlinear least-squares fitting among soil scientists and hydrologists [*van Genuchten*, 1981; *Kool et al.*, 1985, 1987].

### 7.3. Statistics of the Inverse Solution

As part of the inverse solution, HYDRUS produces a correlation matrix which specifies degree of correlation between the fitted coefficients. The correlation matrix quantifies changes in model predictions caused by small changes in the final estimate of a particular parameter, relative to similar changes as a result of changes in the other parameters. The correlation matrix reflects the nonorthogonality between two parameter values. A value of  $\pm 1$  suggests a perfect linear correlation whereas 0 indicates no correlation at all. The correlation matrix may be used to select which parameters, if any, are best kept constant in the parameter estimation process because of high correlation.

An important measure of the goodness of fit is the  $r^2$  value for regression of the observed,  $\hat{y}_i$ , versus fitted,  $y_i(\mathbf{b})$ , values:

$$r^2 = \frac{\left[ \sum w_i \hat{y}_i y_i - \frac{\sum \hat{y}_i \sum y_i}{\sum w_i} \right]^2}{\left[ \sum w_i \hat{y}_i^2 - \frac{(\sum \hat{y}_i)^2}{\sum w_i} \right] \left[ \sum w_i y_i^2 - \frac{(\sum y_i)^2}{\sum w_i} \right]} \quad (7.3)$$

The  $r^2$  value is a measure of the relative magnitude of the total sum of squares associated with the fitted equation; a value of 1 indicates a perfect correlation between the fitted and observed values.

HYDRUS provides additional statistical information about the fitted parameters such as the mean, standard error, T-value, and the lower and upper confidence limits (given in output file FIT.OUT). The standard error,  $s(b_j)$ , is estimated from knowledge of the objective function, the number of observations, the number of unknown parameters to be fitted, and an inverse matrix [*Daniel and Wood*, 1971]. The T-value is obtained from the mean and standard error using the equation

$$T = \frac{b_j}{s(b_j)} \quad (7.4)$$

The values for  $T$  and  $s(b_j)$  provide absolute and relative measures of the deviations around the mean. HYDRUS also specifies the upper and lower bounds of the 95% confidence level around each fitted parameter  $b_j$ . It is desirable that the real value of the target parameter always be located in a narrow interval around the estimated mean as obtained with the optimization program. Large confidence limits indicate that the results are not very sensitive to the value of a particular parameter.

Finally, because of possible problems related to convergence and parameter uniqueness, we recommend to routinely rerun the program with different initial parameter estimates to verify that the program indeed converges to the same global minimum in the objective function. This is especially important for field data sets, which often exhibit considerable scatter in the measurements, or may cover only a narrow range of soil water contents, pressure heads, and/or concentrations. Whereas HYDRUS will not accept initial estimates that are out of range, it is ultimately the user's responsibility to select meaningful initial estimates. Parameter optimization is implemented only for two-dimensional problems.

## 8. PROBLEM DEFINITION

### 8.1. Construction of Finite Element Mesh

The finite element mesh is constructed by dividing the flow region for two-dimensional problems into quadrilateral and/or triangular elements or for three-dimensional problems into tetrahedral, hexahedral and/or triangular prismatic elements (Fig. 8.1) whose shapes are defined by the coordinates of the nodes that form the element corners. The program automatically subdivides the quadrilaterals into triangles (or hexahedrals and triangular prisms into tetrahedrals), which are then treated as subelements. Two different ways are possible to subdivide the hexahedrals into tetrahedrals, whereas six different possibilities exist for subdividing the triangular prisms into tetrahedrals (see Fig. 8.1).

If two neighboring hexahedral elements are subdivided in the same way (e.g., options 2a or 2b in Fig. 8.1), the newly formed edges on a common surface will cross each other, a feature which is not allowed. Two neighboring hexahedral elements should therefore always use both options 2a and 2b as shown in Figure 8.1, so that the newly formed edges on the common surface will coincide. Therefore, it is necessary to give not only the corner nodes, which define an element, but also the code, which specifies how a particular element is to be subdivided into subelements (this is done automatically if the graphical user interface is used). It is necessary to always realize how the neighboring elements are going to be subdivided, and to input also the proper code specifying the subdivision. Having high flexibility in terms of possible subdivisions into subelements is important, especially for unstructured finite element meshes using triangular prisms.

Transverse lines [Neuman, 1974] formed by element boundaries must transect the mesh along the general direction of its shortest dimension. These transverse lines should be continuous and non-intersecting, but need not be straight. The nodes are numbered sequentially from 1 to  $NumNP$  (total number of nodes) by proceeding along each transverse line in the same direction. Elements are numbered in a similar manner. The maximum number of nodes on any transverse line,  $IJ$ , is used to determine the effective size of the finite element matrix (i.e., its band width). To minimize memory and time requirements,  $IJ$  should be kept as small as possible. The above rules for defining the finite element mesh apply only when Gaussian elimination is used to solve the matrix equations. Iterative methods (such as the conjugate gradient and ORTHOMIN methods) are not so restrictive since only non-zero entries in the coefficient matrix are stored in memory, and since the computational efficiency is less dependent upon the bandwidth of the matrix as compared to direct

equation solvers.

The finite element dimensions must be adjusted to a particular problem. They should be made relatively small in directions where large hydraulic gradients are expected. Region with sharp gradients are usually located in the vicinity of the internal sources or sinks, or close to the soil surface where highly variable meteorological factors can cause fast changes in pressure head. Hence, we recommend normally using relatively small elements at and near the soil surface. The size of elements can gradually increase with depth to reflect the generally much slower changes in pressure heads at deeper depths. The element dimensions should also depend upon the soil hydraulic properties. For example, coarse-textured soils having relatively high  $n$ -values and small  $\alpha$ -values (see Eqs. (2.26) and (2.28)) generally require a finer discretization than fine-textured soils. We also recommend using elements having approximately equal sizes to decrease numerical errors. For axisymmetric three-dimensional flow systems, the vertical axis must coincide with, or be to the left of, the left boundary of the mesh. No special restrictions are necessary to facilitate the soil root zone.

## 8.2. Coding of Soil Types and Subregions

*Soil Types* - An integer code beginning with 1 and ending with  $NMat$  (the total number of soil materials) is assigned to each soil type in the flow region. The appropriate material code is subsequently assigned to each nodal point  $n$  of the finite element mesh. Interior material interfaces do not coincide with element boundaries. When different material numbers are assigned to the corner nodes of a certain element, material properties of this element will be averaged automatically by the finite element algorithm. This procedure will somewhat smooth soil interfaces.

A set of soil hydraulic parameters and solute transport characteristics must be specified for each soil material. Also, the user must define for each element the principal components of the conductivity anisotropy tensor, as well as the angle between the local and global coordinate systems.

As explained in Section 2.3, one additional way of changing the unsaturated soil hydraulic properties in the flow domain is to introduce scaling factors associated with the water content, the pressure head and the hydraulic conductivity. The scaling factors are assigned to each nodal point  $n$  in the flow region.

*Subregions* - Water and solute mass balances are computed separately for each specified subregion. The subregions may or may not coincide with the material regions. Subregions are characterized by an integer code which runs from 1 to  $N Lay$  (the total number of subregions). A subregion code is assigned to each element in the flow domain.

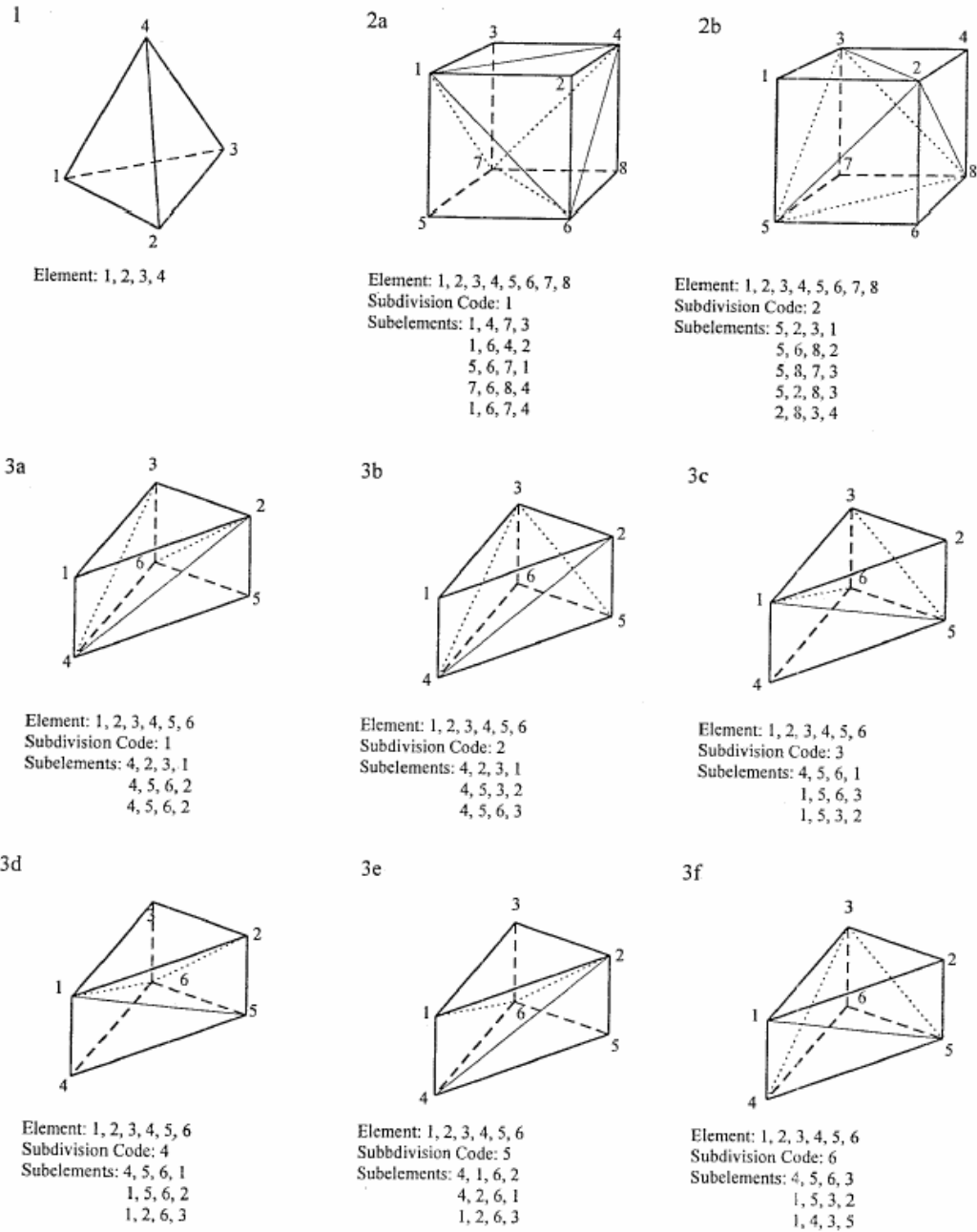


Figure 8.1. Finite elements and subelements used to discretize the 3-D domain: 1) tetrahedral, 2) hexahedral, 3) triangular prism.

### 8.3. Coding of Boundary Conditions

Flow boundary conditions were programmed in a fairly similar way as done in the UNSAT1 and UNSAT2 models of *Neuman* [1972] and *Neuman et al.* [1974], and in the SWMS\_2D [*Šimůnek et al.*, 1992] and CHAIN\_2D [*Šimůnek and van Genuchten*, 1994] codes. A boundary code,  $Kode(n)$ , must be assigned to each node,  $n$ . If node  $n$  is to have a prescribed pressure head during a time step (Dirichlet boundary condition),  $Kode(n)$  must be set positive during that time step. If the volumetric flux of water entering or leaving the system at node  $n$  is prescribed during a time step (Neumann boundary condition),  $Kode(n)$  must be negative or zero.

*Constant Boundary Conditions* - The values of constant boundary conditions for a particular node,  $n$ , are given by the initial values of the pressure head,  $h(n)$ , in case of Dirichlet boundary conditions, or by the initial values of the recharge/discharge flux,  $Q(n)$ , in case of Neumann boundary conditions. Table 8.1 summarizes the use of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  for various types of nodes.

Table 8.1. Initial settings of  $Kode(n)$ ,  $Q(n)$ , and  $h(n)$  for constant boundary conditions.

Node Type	$Kode(n)$	$Q(n)$	$h(n)$
Internal; not sink/source	0	0.0	Initial Value
Internal; sink/source (Dirichlet condition)	1	0.0	Prescribed
Internal; sink/source (Neumann condition)	-1	Prescribed	Initial Value
Impermeable Boundary	0	0.0	Initial Value
Specified Head Boundary	1 <sup>+</sup>	0.0	Prescribed
Specified Flux Boundary	-1 <sup>*</sup>	Prescribed	Initial Value

<sup>+</sup> 5 may also be used

<sup>\*</sup> -5 may also be used

*Variable Boundary Conditions* - Three types of variable boundary conditions can be imposed:

1. Atmospheric boundary conditions for which  $Kode(n)=\pm 4$ ,
2. Variable pressure head boundary conditions for which  $Kode(n)=+3, +7, +8, +9$ , and
3. Variable flux boundary conditions for which  $Kode(n)=-3, -7, -8, \text{ and } -9$ .

These conditions can be specified along any part of the boundary. It is not possible to specify more than one time-dependent boundary condition for each type. Initial settings of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  for the time-dependent boundary conditions are given in Table 8.2.

Table 8.2. Initial settings of  $Kode(n)$ ,  $Q(n)$ , and  $h(n)$  for variable boundary conditions.

Node Type	$Kode(n)$	$Q(n)$	$h(n)$
Atmospheric Boundary	-4	0.0	Initial Value
Variable Head Boundary	+3, +7, +8, +9	0.0	Initial Value
Variable Flux Boundary	-3, -7, -8, -9	0.0	Initial Value

Atmospheric boundary conditions are implemented when  $Kode(n)=\pm 4$ , in which case time-dependent input data for the precipitation,  $Prec$ , and evaporation,  $rSoil$ , rates must be specified in the input file ATMOSPH.IN. The potential fluid flux across the soil surface is determined by  $rAtm=rSoil-Prec$ . The actual surface flux is calculated internally by the program. Two limiting values of surface pressure head must also be provided:  $hCritS$  which specifies the maximum allowed pressure head at the soil surface (usually 0.0), and  $hCritA$  which specifies the minimum allowed surface pressure head (defined from equilibrium conditions between soil water and atmospheric vapor). The program automatically switches the value of  $Kode(n)$  from -4 to +4 if one of these two limiting points is reached. Table 8.3 summarizes the use of the variables  $rAtm$ ,  $hCritS$  and  $hCritA$  during program execution.  $Width(n)$  in the table denotes the length of the boundary segment associated with node  $n$ .

Table 8.3. Definition of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  when an atmospheric boundary condition is applied.

$Kode(n)$	$Q(n)$	$h(n)$	Event
-4	$-Width(n)*r_{Atm}$	Unknown	$r_{Atm}=r_{Soil}-Prec$
+4	Unknown	$h_{CritA}$	Evaporation capacity is exceeded
+4	Unknown	$h_{CritS}$	Infiltration capacity is exceeded

Variable head and flux boundary conditions along a certain part of the boundary are implemented when  $Kode(n)=+3, +7, +8, +9$ , and  $-3, -7, -8$ , and  $-9$ , respectively. In that case, the input file ATMOSPH.IN must contain the prescribed time-dependent values of the pressure head,  $ht_i$ , or the flux,  $rt_i$ , imposed along the boundary. The values of  $ht_i$  or  $rt_i$  are assigned to particular nodes at specified times according to rules given in Table 8.4. Variable flux boundary conditions with  $Kode(n)=+3$  are treated similarly as atmospheric boundary conditions, i.e., with limited pressure head values of  $h_{CritA}$  and  $h_{CritS}$ .

Table 8.4. Definition of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  when variable head or flux boundary conditions are applied.

Node Type	$Kode(n)$	$Q(n)$	$h(n)$
Variable Head Boundary	+3, +7, +8, +9	Unknown	$ht_i$
Variable Flux Boundary	-3, -7, -8, -9	$-Width(n)*rt_i$	Unknown

*Water Uptake by Plant Roots* - The program calculates the rate at which plants extract water from the soil root zone by evaluating the term  $D$  (equation (5.9)) in the finite element formulation. The code requires that  $Kode(n)$  be set equal to 0 or negative for all nodes in the root zone. Values of the potential transpiration rate,  $r_{Root}$ , must be specified at preselected times in the input file ATMOSPH.IN. Actual transpiration rates are calculated internally by the program as discussed in



Section 2.2. The root uptake parameters are taken from an input file SELECTOR.IN. Values of the function  $Beta(n)$ , which describes the potential water uptake distribution over the root zone (equation (2.9)), must be specified for each node in the flow domain (see the description of input Block I in Table 10.8 of Section 10). All parts of the flow region where  $Beta(n) > 0$  are treated as the soil root zone.

*Deep Drainage from the Soil Profile* - Vertical drainage,  $q(h)$ , across the lower boundary of the soil profile is sometimes approximated by a flux which depends on the position of groundwater level (e.g., *Hopmans and Stricker*, 1989). If available, such a relationship can be implemented in the form of a variable flux boundary condition for which  $Kode(n) = -6$ . This boundary condition is implemented in HYDRUS by setting the logical variable  $qGWL$  in the input file BOUNDARY.IN equal to ".true.". The discharge rate  $Q(n)$  assigned to node  $n$  is determined by the program as  $Q(n) = -Width(n) * q(h)$  where  $h$  is the local value of the pressure head, and  $q(h)$  is given by

$$q(h) = -A_{qh} \exp(B_{qh} |h - GWL0L|) \quad (8.1)$$

where  $A_{qh}$  and  $B_{qh}$  are empirical parameters which must be specified in the input file BOUNDARY.IN, together with  $GWL0L$  which represents the reference position of the groundwater level (usually set equal to the  $z$ -coordinate of the soil surface).

*Free Drainage* - Unit vertical hydraulic gradient boundary conditions can be implemented in the form of a variable flux boundary condition for which  $Kode(n) = -6$ . This boundary condition is implemented in HYDRUS by setting the logical variable  $FreeD$  in the input file BOUNDARY.IN equal to ".true.". The program determines the discharge rate  $Q(n)$  assigned to node  $n$  as  $Q(n) = -Width(n) * K(h)$ , where  $h$  is the local value of the pressure head, and  $K(h)$  is the hydraulic conductivity corresponding to this pressure head.

*Seepage Faces* - The initial settings of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  for nodes along a seepage face are summarized in Table 8.5. All potential seepage faces must be identified before starting the numerical simulation. This is done by providing a list of nodes along each potential seepage face (see input Block J as defined in Table 10.10 of Section 10).

Table 8.5. Initial setting of  $Kode(n)$ ,  $Q(n)$ , and  $h(n)$  for seepage faces.

Node Type	$Kode(n)$	$Q(n)$	$h(n)$
Seepage Face (initially saturated)	+2	0.0	0.0
Seepage Face (initially unsaturated)	-2	0.0	Initial Value

*Drains* - Table 8.6 summarizes the initial settings of the variables  $Kode(n)$ ,  $Q(n)$  and  $h(n)$  for nodes representing drains. All drains must be identified before starting the numerical simulation. This is done by providing a list of nodes representing drains, together with a list of elements around each drain whose hydraulic conductivities are to be adjusted according to discussion in Section 5.3.7 (see also input Block J as defined in Table 10.10 of Section 10).

Table 8.6. Initial setting of  $Kode(n)$ ,  $Q(n)$ , and  $h(n)$  for drains.

Node Type	$Kode(n)$	$Q(n)$	$h(n)$
Drain (initially saturated)	+5	0.0	0.0
Drain (initially unsaturated)	-5	0.0	Initial Value

*Solute and Heat Transport Boundary Conditions* - The original version 1.1. of SWMS\_2D [Šimůnek et al., 1992] assumed a strict relationship between the boundary conditions for water flow and solute transport. A first-type boundary condition for water flow forced the boundary condition for solute transport also to be of the first-type. Similarly, a second-type boundary condition for water flow induced a second- or third-type boundary condition for solute transport depending upon direction of the water flux. These strict relationships between the boundary conditions for water flow

and solute transport have been abandoned in later versions. Selection of the type of boundary condition for the solute transport is now much more independent of the boundary condition implemented for water flow. The type of boundary condition to be invoked for solute or heat transport is specified by the input variable *KodCB* or *KodTB*, respectively. A positive sign of this variable means that a first-type boundary condition will be used. When *KodCB* (*KodTB*) is negative, HYDRUS selects a third-type boundary condition when the calculated water flux is directed into the region, or a second-type boundary condition when the water flux is zero or directed out of the region. One exception to these rules occurs for atmospheric boundary conditions when  $Kode(n)=\pm 4$  and  $Q(n)<0$ . HYDRUS assumes that solutes can leave the flow region across atmospheric boundaries only by gas diffusion. The solute flux in this situation becomes zero, i.e.,  $c_0=0$  in equation (6.34). Cauchy and Neumann boundary conditions are automatically applied to internal sinks/sources depending upon the direction of water flow. The dependence or independence of the solute and heat boundary conditions on time or the system is still defined through the variable *Kode(n)* as discussed above.

Although HYDRUS can implement first-type boundary conditions, we recommend users to invoke third-type conditions where possible. This is because third-type conditions, in general, are physically more realistic and preserve solute mass in the simulated system (e.g., *van Genuchten and Parker* [1984]; *Leij et al.* [1991]).

For the user's convenience, Table 8.7 summarizes possible values of the different boundary codes and their association with specific water flow and solute transport boundary conditions.

#### 8.4. Program Memory Requirements

One single parameter statement is used at the beginning of the code to define the problem dimensions. All major arrays in the program are adjusted automatically according to these dimensions. This feature makes it possible to change the dimensions of the problem to be simulated without having to recompile all program subroutines. Different problems can be investigated by changing the dimensions in the parameter statement at the beginning of the main program, and subsequently linking all previously compiled subroutines with the main program when creating an executable file. Table 8.8 lists the array dimensions, which must be defined in the parameter statement.

Table 8.7. Summary of Boundary Coding.

	Boundary Type	Water Flow		Solute Transport	
		Kode	Input	KodCB	Input
Time-independent	Impermeable	0	initial $h(n)$ , $Q(n)=0$	NA	NA
	Constant head	1	prescribed $h(n)$ , $Q(n)=0$	$\neq 0$	$cBound(i)$
	Constant flux	-1	initial $h(n)$ , prescribed $Q(n)$	$\neq 0$ (inflow)	$cBound(i)$
	Source/sink (Dirichlet)	1	prescribed $h(n)$ , $Q(n)=0$	$\neq 0$ (Source)	$cBound(6)$
	Source/sink (Neumann)	-1	initial $h(n)$ , prescribed $Q(n)$	$\neq 0$ (Source)	$cBound(6)$
	Seepage Face (saturated)	2	$h(n)=0$ , $Q(n)=0$	0	-
	Seepage Face (unsaturated)	-2	initial $h(n)$ , $Q(n)=0$	0	-
	Drains (saturated)	5	$h(n)=0$ , $Q(n)=0$	0	-
	Drains (unsaturated)	-5	initial $h(n)$ , $Q(n)=0$	0	-
Time-dependent	Changing head	3, 7, 8, 9	$h(t)$ , initial $h(n)$ , $Q(n)=0$	$\neq 0$	$c_h(t)$
	Changing flux	-3, -7, -8, -9	$q(t)$ , initial $h(n)$ , $Q(n)=0$	$\neq 0$ (inflow)	$c_r(t)$
	Atmospheric boundary	-4	$Prec$ , $rSoil$ , $h_A$ , $h_S$ , initial $h(n)$ , $Q(n)=0$	0	$cPrec(t)$
	Root zone	0	$rRoot$ , initial $h(n)$ , $Q(n)=0$	NA	$cBound(5)$
	Deep drainage	-6	$Aqh$ , $Bqh$ , $GWL0L$ , initial $h(n)$ , $Q(n)=0$	0	-
	Free drainage	-6	initial $h(n)$ , $Q(n)=0$	0	-

$i = 1, 2, \dots, 9$

Table 8.8. List of array dimensions in HYDRUS.

Dimension	Description
<i>NumNPD</i>	Maximum number of nodes in finite element mesh
<i>NumEID</i>	Maximum number of elements in finite element mesh
<i>MBandD</i>	Maximum dimension of the bandwidth of matrix <i>A</i> when Gaussian elimination is used. Maximum number of nodes adjacent to a particular node, including itself, when iterative matrix solvers are used.
<i>NumBPD</i>	Maximum number of boundary nodes for which <i>Kode(n)≠0</i>
<i>NSeepD</i>	Maximum number of seepage faces
<i>NumSPD</i>	Maximum number of nodes along a seepage face
<i>NDrD</i>	Maximum number of drains
<i>NEIDrD</i>	Maximum number of elements surrounding a drain
<i>NMatD</i>	Maximum number of materials
<i>NTabD</i>	Maximum number of items in the table of hydraulic properties generated by the program for each soil material
<i>NumKD</i>	Maximum number of available code number values (equals 6 in present version)
<i>NSD</i>	Maximum number of solutes (equals 6 in present version)
<i>NObsD</i>	Maximum number of observation nodes for which the pressure head, the water content, temperature and concentration are printed at each time level
<i>MNorth</i>	Maximum number of orthogonalizations performed when iterative solvers are used

### 8.5. Matrix Equation Solvers

Discretization of the governing partial differential equations for water flow (2.1), solute transport (3.11) and heat movement (4.1) leads to the system of linear equations

$$[A] \{x\} = \{b\} \quad (8.2)$$

in which matrix  $[A]$  is symmetric for water flow and asymmetric for solute and heat transport.

The original version of SWMS\_2D [Šimůnek *et al.*, 1992] uses Gaussian elimination to solve both systems of linear algebraic equations. The invoked solvers took advantage of the banded nature of the coefficient matrices and, in the case of water flow, of the symmetric properties of the matrix. Such direct solution methods have several disadvantages as compared to iterative methods. Direct methods require a fixed number of operations (depending upon the size of the matrix), which increases approximately by the square of the number of nodes [Mendoza *et al.*, 1991]. Iterative methods, on the other hand, require a variable number of repeated steps, which increases at a much smaller rate (about 1.5) with the size of a problem [Mendoza *et al.*, 1991]. A similar reduction also holds for the memory requirement since iterative methods do not require one to store non-zero matrix elements. Memory requirements, therefore, increase at a much smaller rate with the size of the problem when iterative solvers are used [Mendoza *et al.*, 1991]. Round-off errors also represent less of a problem for iterative methods as compared to direct methods. This is because round-off errors in iterative methods are self-correcting [Letniowski, 1989]. Finally, for time-dependent problems, a reasonable approximation of the solution (i.e., the solution at the previous time step) exists for iterative methods, but not for direct methods [Letniowski, 1989]. In general, direct methods are more appropriate for relatively small problems, while iterative methods are more suitable for larger problems.

Many iterative methods have been used in the past for handling large sparse matrix equations. These methods include Jacobi, Gauss-Seidel, alternating direction implicit (ADI), block successive over-relaxation (BSSOR), successive line over-relaxation (SLOR), and strongly implicit procedures (SIP), among others [Letniowski, 1989]. More powerful preconditioned accelerated iterative methods, such as the preconditioned conjugate gradient method (PCG) [Behie and Vinsome, 1982], were introduced more recently. Sudicky and Huyakorn [1991] gave three advantages of the PCG procedure as compared to other iterative methods: PCG can be readily modified for finite element methods with irregular grids, the method does not require iterative parameters, and PCG usually outperforms its iterative counterparts for situations involving relatively stiff matrix conditions.

HYDRUS implements both direct and iterative methods for solving the system of linear algebraic equations given by (8.2). Depending upon the size of matrix  $[A]$ , we use either direct Gaussian elimination or the preconditioned conjugate gradient method [Mendoza *et al.*, 1991] for water flow and the ORTHOMIN (preconditioned conjugate gradient squared) procedure [Mendoza *et al.*, 1991] for solute transport. Gaussian elimination is used if either the bandwidth of matrix  $[A]$  is

smaller than 20, or the total number of nodes is smaller than 500. The iterative methods used in HYDRUS were adopted from the ORTHOFEM software package of *Mendoza et al.* [1991].

The preconditioned conjugate gradient and ORTHOMIN methods consist of two essential parts: initial preconditioning, and the iterative solution with either conjugate gradient or ORTHOMIN acceleration [*Mendoza et al.*, 1991]. Incomplete lower-upper (ILU) preconditioning is used in ORTHOFEM when matrix  $[A]$  is factorized into lower and upper triangular matrices by partial Gaussian elimination. The preconditioned matrix is subsequently repeatedly inverted using updated solution estimates to provide a new approximation of the solution. The orthogonalization-minimization acceleration technique is used to update the solution estimate. This technique insures that the search direction for each new solution is orthogonal to the previous approximate solution, and that either the norm of the residuals (for conjugate gradient acceleration [*Meijerink and van der Vorst*, 1981]) or the sum of the squares of the residuals (for ORTHOMIN [*Behie and Vinsome*, 1982]) is minimized. More details about the two methods is given in the user's guide of ORTHOFEM [*Mendoza et al.*, 1991] or in *Letniowski* [1989]. *Letniowski* [1989] also gives a comprehensive review of accelerated iterative methods, as well as of the preconditional techniques.





## 9. EXAMPLE PROBLEMS

### 9.1. Direct Example Problems

Eight example problems are presented in this section. The first three examples are identical to those provided previously with the first version of SWMS\_2D [Šimůnek *et al.*, 1992]. The other four examples in this section are identical to those provided with CHAIN\_2D [Šimůnek and van Genuchten, 1994], and are included mainly for mathematical verification purposes, and for demonstrating new features of HYDRUS, i.e., non-equilibrium and nonlinear adsorption, sequential first-order decay reactions, solute diffusion in the gas phase, and/or heat transport. These examples have also been used with versions 1 and 2 of HYDRUS-2D [Šimůnek *et al.*, 1996, 1999]. Finally, example 8 is a fully three-dimensional problem. Examples 1 through 6 are solved using both two- and three-dimensional solvers.

Examples 1 and 2 provide comparisons of the water flow part of HYDRUS code with results from both the UNSAT2 code of Neuman [1974] and the SWATRE code of Belmans *et al.* [1983]. Examples 3a and 3b serve to verify the accuracy of the solute transport part of HYDRUS by comparing numerical results against those obtained with two- and three-dimensional analytical solutions during steady-state groundwater flow. The results obtained with the HYDRUS codes (2D and 3D) for these three examples are identical to the results obtained with SWMS\_2D. Example 4 serves to verify the accuracy of HYDRUS by comparing numerical results for a problem with three solutes involved in a sequential first-order decay chain against results obtained with an analytical solution during one-dimensional steady-state water flow [van Genuchten, 1985]. Example 5 considers one-dimensional transport of a solute undergoing nonlinear cation adsorption. Numerical results are compared with experimental data and previous numerical solutions obtained with the MONOC code of Selim *et al.* [1987] and the HYDRUS code of Kool and van Genuchten [1991]. Example 6 serves to verify the accuracy of HYDRUS in describing nonequilibrium adsorption by comparing numerical results against experimental data and previous numerical predictions during one-dimensional steady-state water flow [van Genuchten, 1981]. Example 7 demonstrates numerical results for a field infiltration experiment involving a two-layered axisymmetric three-dimensional flow domain. The infiltrating water was assumed to have a higher temperature than the soil, and to contain an organic compound (parent pesticide) which in the soil profile degraded into two sequential daughter products. Example 8 shows numerical results for contaminant transport in an unconfined aquifer subjected to well pumping.

### 9.1.1. Example 1 - Column Infiltration Test

This example simulates a one-dimensional laboratory infiltration experiment discussed by *Skaggs et al.* [1970]. The example was used later by *Davis and Neuman* [1983] as a test problem for the UNSAT2 code. Hence, the example provides a means of comparing results obtained with the HYDRUS and UNSAT2 codes.

Figure 9.1 gives graphical representations of the soil column and the finite element mesh used for the numerical simulations with two- and three-dimensional solvers. The soil water retention and relative hydraulic conductivity functions of the sandy soil are presented in Figure 9.2. The sand was assumed to be at an initial pressure head of -150 cm. The soil hydraulic properties were assumed to be homogenous and isotropic with a saturated hydraulic conductivity of 0.0433 cm/min. The column was subjected to ponded infiltration (a Dirichlet boundary condition) at the soil surface, resulting in one-dimensional vertical water flow. The open bottom boundary of the soil column was simulated by implementing a no-flow boundary condition during unsaturated flow ( $h < 0$ ), and a seepage face with  $h = 0$  when the bottom boundary becomes saturated (this last condition was not reached during the simulation). The impervious sides of the column were simulated by imposing no-flow boundary conditions.

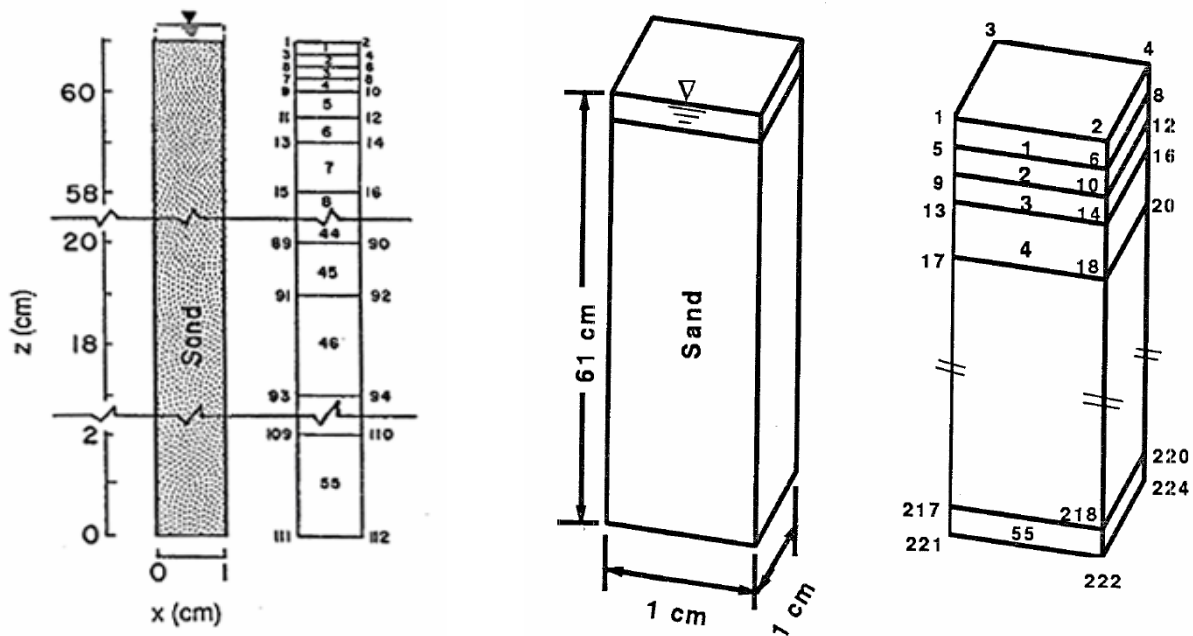


Figure 9.1. Flow system and finite element mesh for example 1 (2D left, 3D right).

The simulation was carried out for 90 min, which corresponds to the total time duration of the experiment. Figure 9.3 shows the calculated instantaneous ( $q_0$ ) and cumulative ( $I_0$ ) infiltration rates simulated with HYDRUS. The calculated results agree closely with those obtained by *Davis and Neuman* [1983] using their UNSAT2 code.

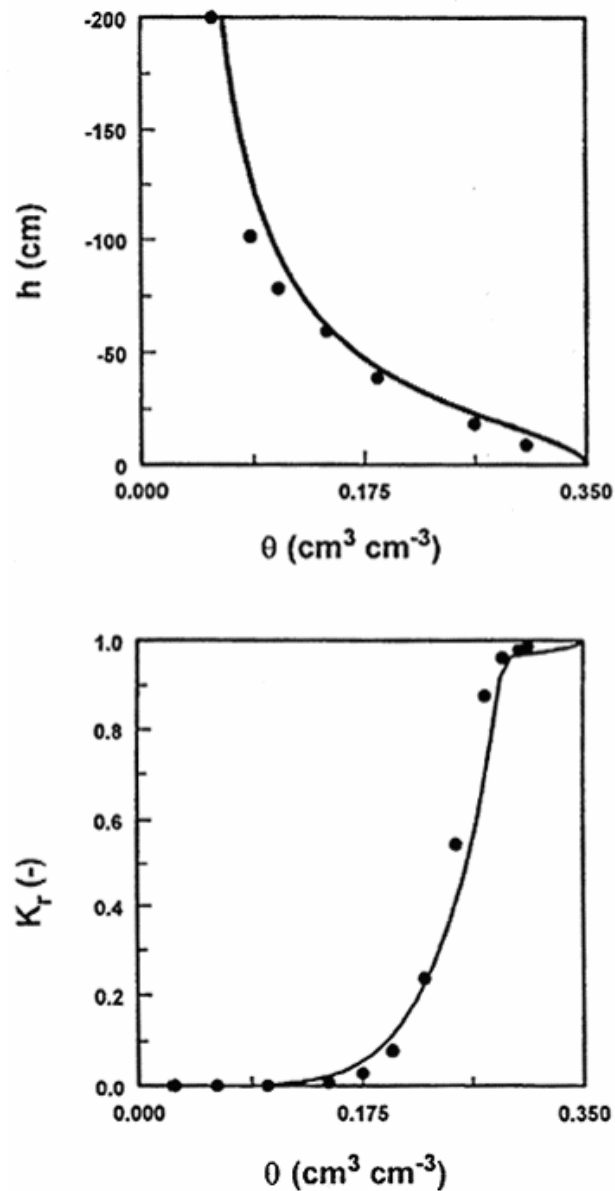


Figure 9.2. Retention and relative hydraulic conductivity functions for example 1. The solid circles are UNSAT2 input data [*Davis and Neuman*, 1983].

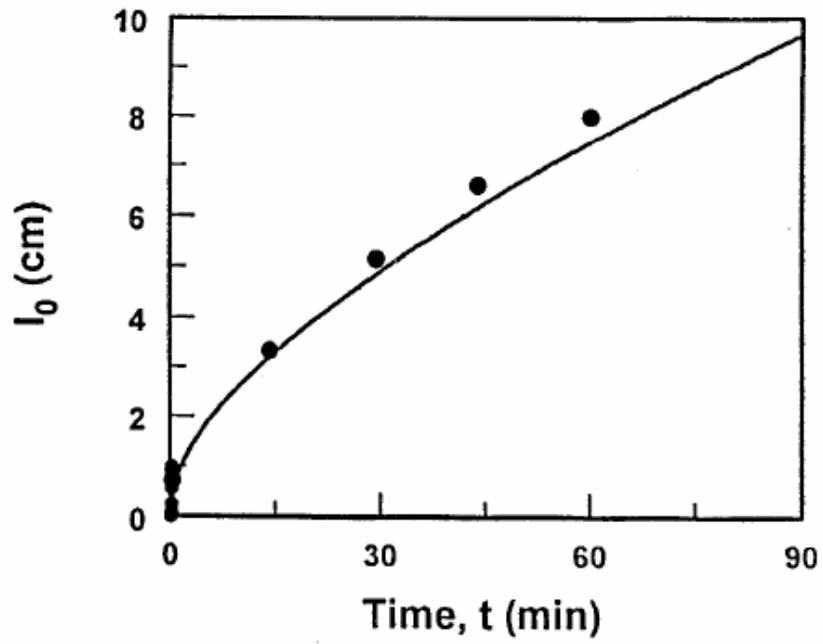
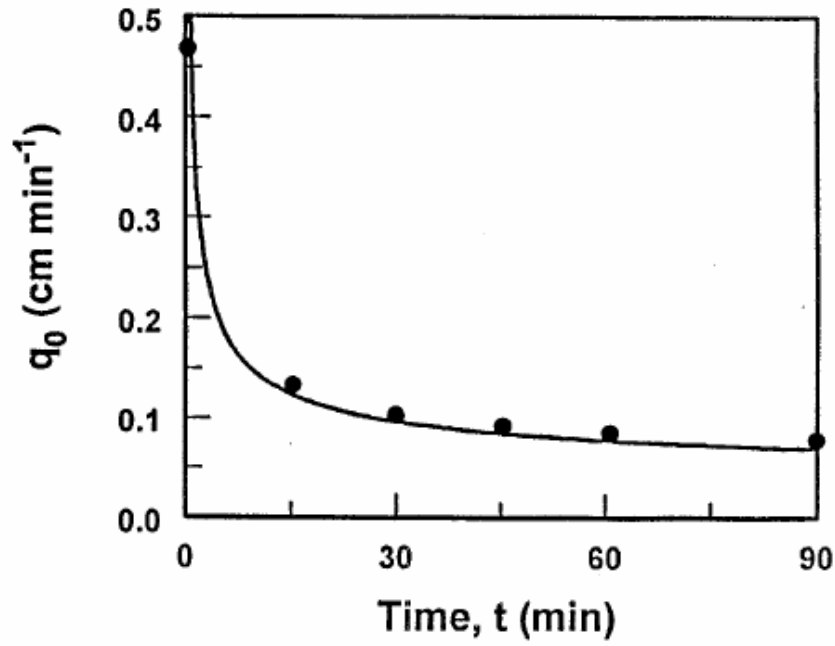


Figure 9.3. Instantaneous,  $q_0$ , and cumulative,  $I_0$ , infiltration rates simulated with the HYDRUS (solid lines) and UNSAT2 (solid circles) codes for example 1.

### 9.1.2. Example 2 - Water Flow in a Field Soil Profile Under Grass

This example considers one-dimensional water flow in a field profile of the Hupselse Beek watershed in the Netherlands. Atmospheric data and observed ground water levels provided the required boundary conditions for the numerical model. Calculations were performed for the period of April 1 to September 30 of the relatively dry year 1982. Simulation results obtained with HYDRUS will be compared with those generated with the SWATRE computer program [Feddes *et al.*, 1978, Belmans *et al.*, 1983].

The soil profile (Fig. 9.4) consisted of two layers: a 40-cm thick A-horizon, and a B/C-horizon which extended to a depth of about 300 cm. The depth of the root zone was 30 cm. The mean scaled hydraulic functions of the two soil layers in the Hupselse Beek area [Cislerová, 1987; Hopmans and Stricker, 1989] are presented in Figure 9.5.

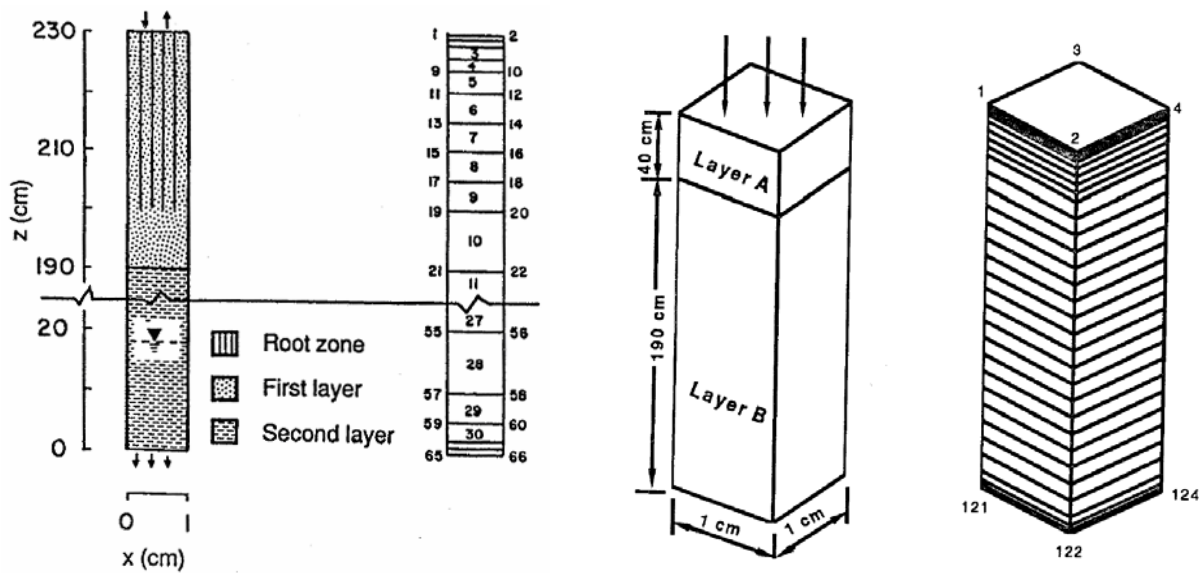


Figure 9.4. Flow system and finite element mesh for example 2 (2D left, 3D right).

The soil surface boundary conditions involved actual precipitation and potential transpiration rates for a grass cover. The surface fluxes were incorporated by using average daily rates distributed uniformly over each day. The bottom boundary condition consisted of a prescribed drainage flux - groundwater level relationship,  $q(h)$ , as given by equation(8.1). The groundwater level was initially set at 55 cm below the soil surface. The initial moisture profile was taken to be in equilibrium with the initial ground water level.

Figure 9.6 presents input values of the precipitation and potential transpiration rates. Calculated cumulative transpiration and cumulative drainage amounts as obtained with the HYDRUS and SWATRE codes are shown in Figure 9.7. The pressure head at the soil surface and the arithmetic mean pressure head of the root zone during the simulated season are presented in Figure 9.8. Finally, Figure 9.9 shows variations in the calculated groundwater level with time.

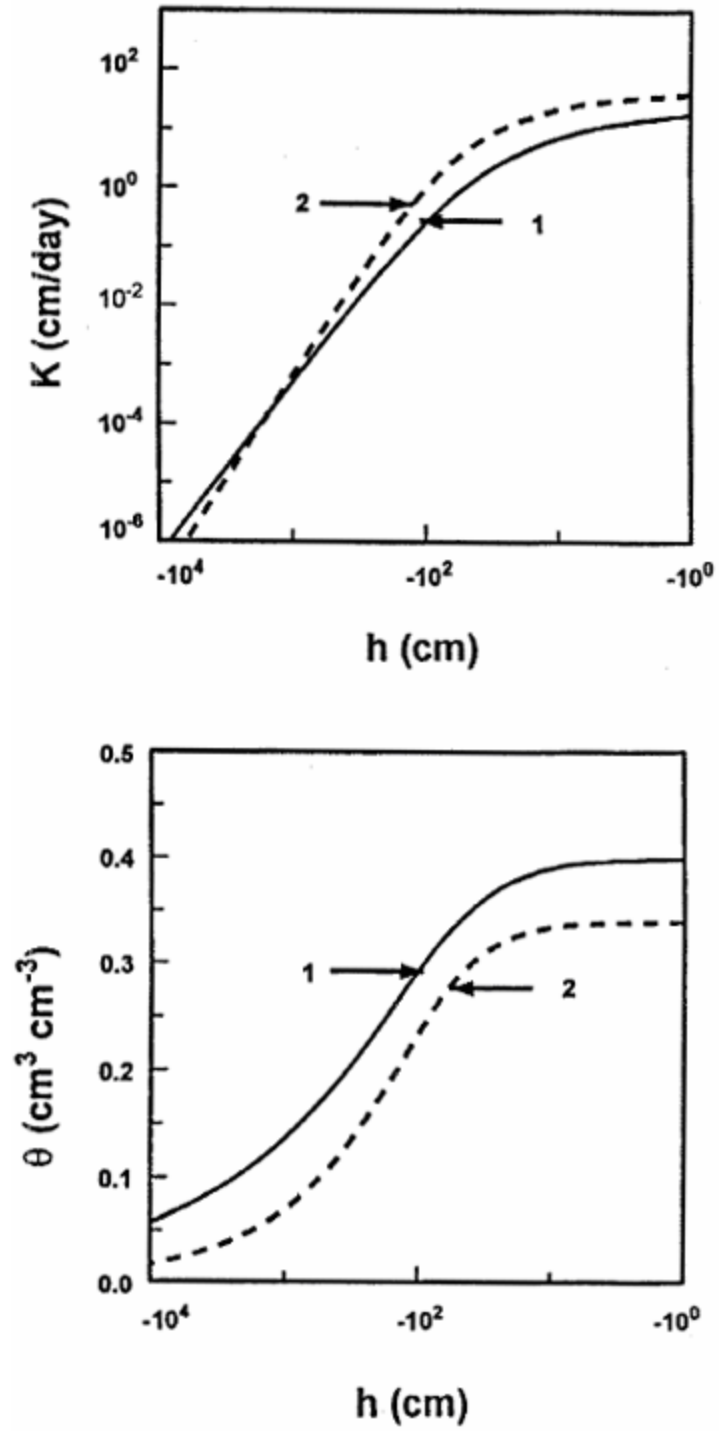


Figure 9.5. Unsaturated hydraulic properties of the first and second soil layers for example 2.

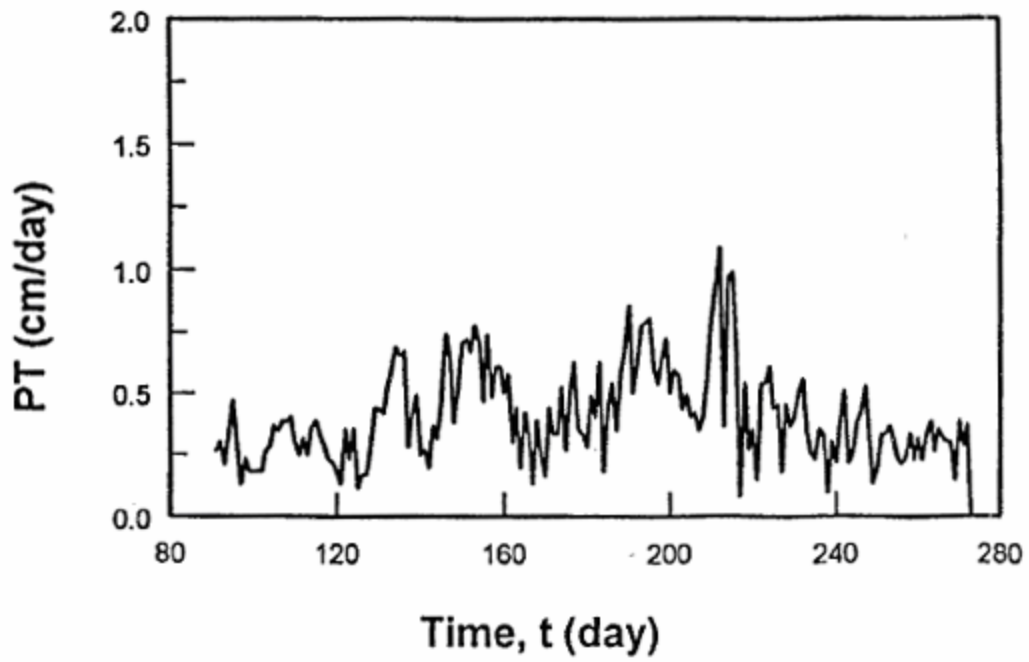
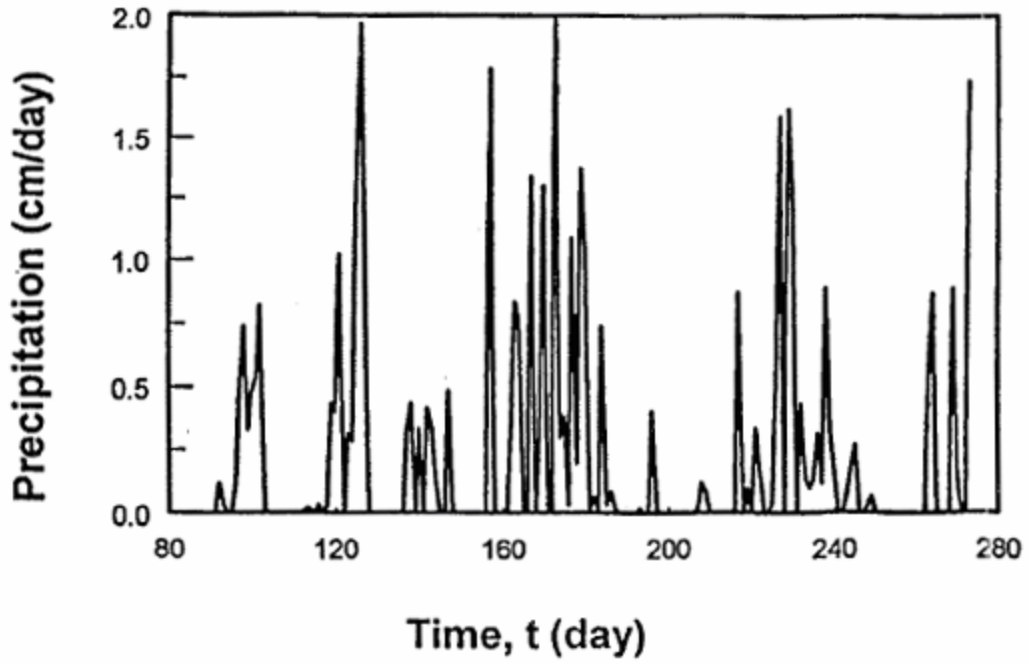


Figure 9.6. Precipitation and potential transpiration rates for example 2.



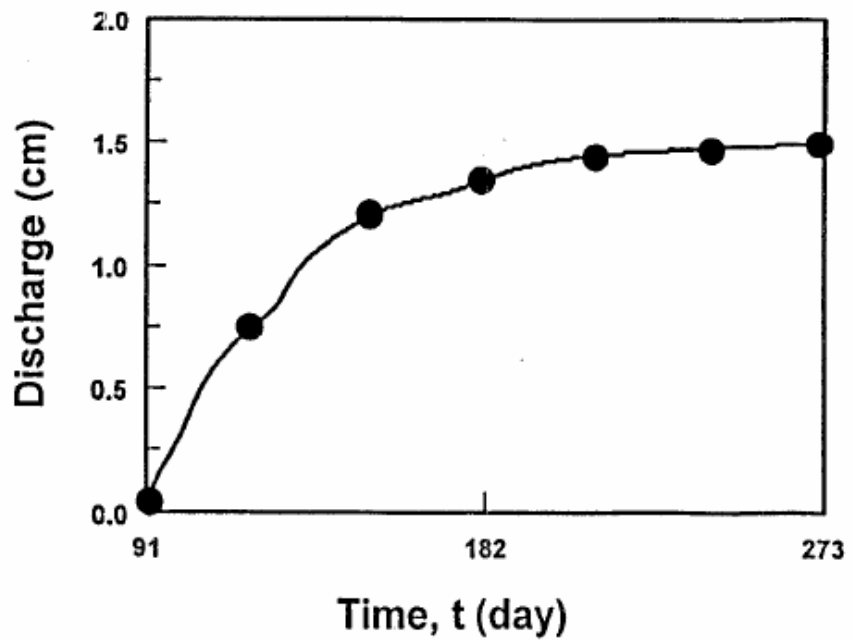
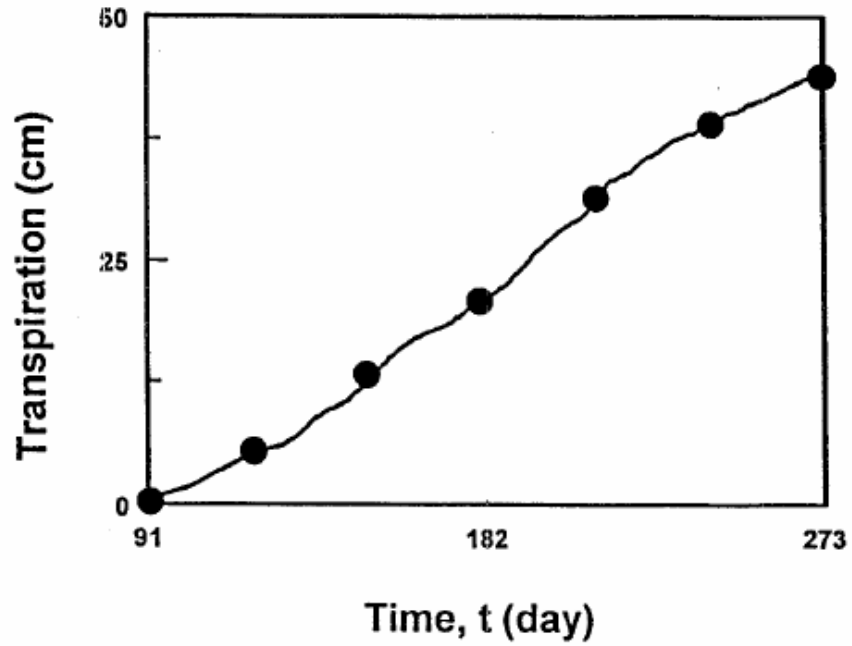


Figure 9.7. Cumulative values for the actual transpiration and bottom discharge rates for example 2 as simulated with HYDRUS (solid line) and SWATRE (solid circles).

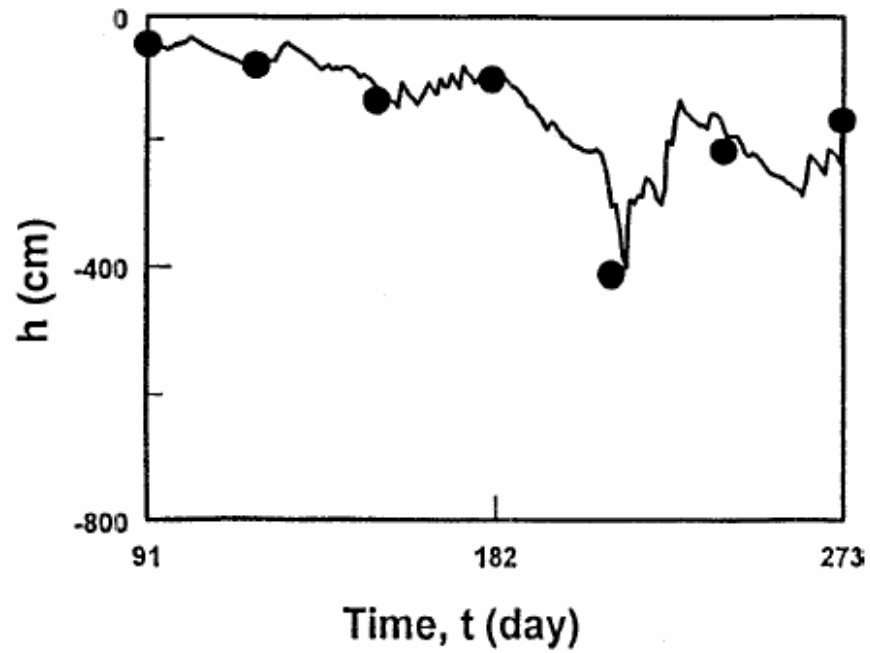
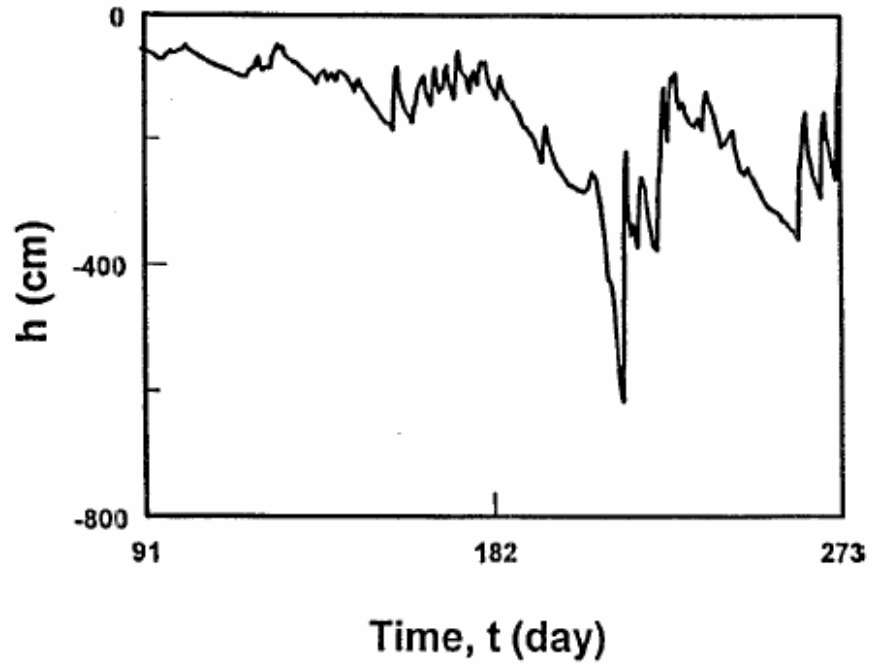


Figure 9.8. Pressure head at the soil surface and mean pressure head of the root zone for example 2 as simulated with HYDRUS (solid lines) and SWATRE (solid circles).

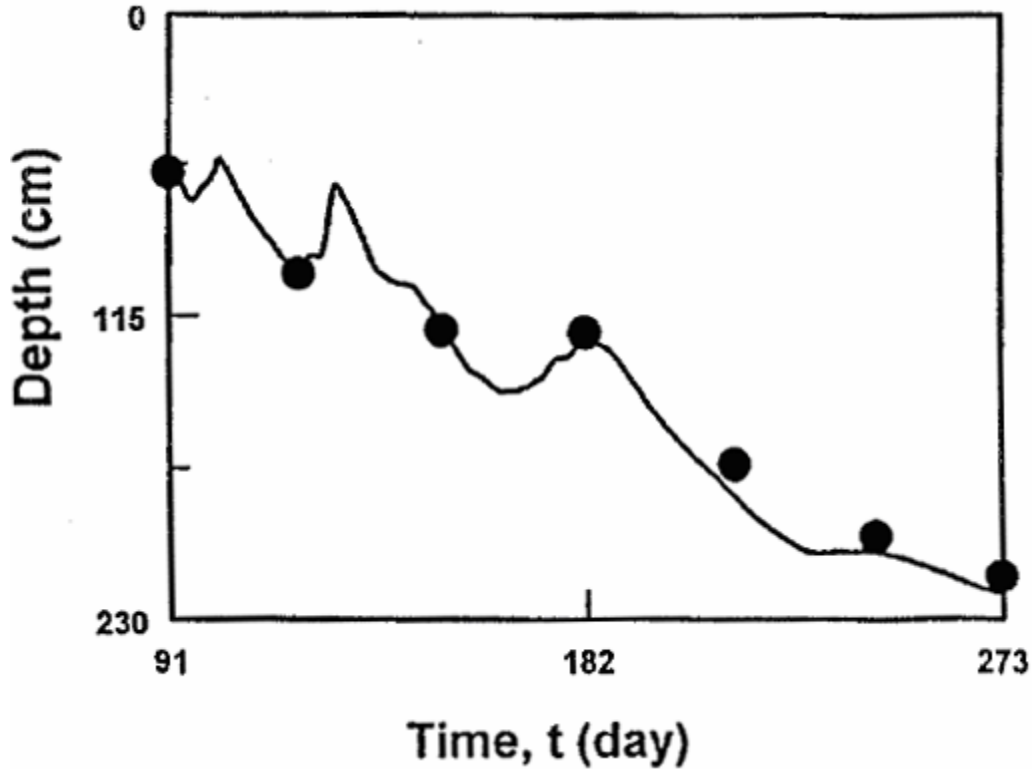


Figure 9.9. Location of the groundwater table versus time for example 2 as simulated with the HYDRUS (solid line) and SWATRE (solid circles) computer programs.

### 9.1.3a. Example 3A - Two-Dimensional Solute Transport

This example was used to verify the mathematical accuracy of the solute transport part of HYDRUS. *Cleary and Ungs* [1978] published several analytical solutions for two-dimensional dispersion problems. One of these solutions holds for solute transport in a homogeneous, isotropic porous medium during steady-state unidirectional groundwater flow. The solute transport equation (3.11) for this situation reduces to

$$D_T \frac{\partial^2 c}{\partial x^2} + D_L \frac{\partial^2 c}{\partial z^2} - v \frac{\partial c}{\partial z} - \lambda R c = R \frac{\partial c}{\partial t} \quad (9.1)$$

where  $\lambda$  is a first-order degradation constant,  $D_L$  and  $D_T$  are the longitudinal and transverse

dispersion coefficients, respectively;  $v$  is the average pore water velocity ( $q_z/\theta$ ) in the flow direction, and  $z$  and  $x$  are the spatial coordinates parallel and perpendicular to the direction of flow. The initially solute-free medium is subjected to a solute source,  $c_0$ , of unit concentration. The source covers a length  $2a$  along the inlet boundary at  $z=0$ , and is located symmetrically about the coordinate  $x=0$ . The transport region of interest is the half- plane ( $z \geq 0; -\infty \leq x \leq \infty$ ). The boundary conditions may be written as:

$$\begin{aligned}
 c(x, 0, t) &= c_0 & -a \leq x \leq a \\
 c(x, 0, t) &= 0 & \text{other values of } x \\
 \lim_{z \rightarrow \infty} \frac{\partial c}{\partial z} &= 0 \\
 \lim_{x \rightarrow \pm\infty} \frac{\partial c}{\partial x} &= 0
 \end{aligned}
 \tag{9.2}$$

The analytical solution of the above transport problem is [Javandel *et al.*, 1984, Leij and Bradford, 1994]

$$\begin{aligned}
 c(x, z, t) &= \frac{c_0 z}{4 (\pi D_L)^{1/2}} \exp\left(\frac{vz}{2D_L}\right) \int_0^{t/R} \exp\left[-\left(\lambda R + \frac{v^2}{4D_L}\right)\tau - \frac{z^2}{4D_L \tau}\right] \tau^{-3/2} \\
 &\quad \cdot \left[ \operatorname{erf}\left(\frac{a-x}{2(D_T \tau)^{1/2}}\right) + \operatorname{erf}\left(\frac{a+x}{2(D_T \tau)^{1/2}}\right) \right] d\tau
 \end{aligned}
 \tag{9.3}$$

The input transport parameters for two simulations are listed in Table 9.1. The width of the source was assumed to be 100 m. Because of symmetry, calculations were carried out only for the quarter plane where  $x \geq 0$  and  $z \geq 0$ .

Figure 9.10 shows the calculated concentration front (taken at a concentration of 0.1) at selected times for the first set of transport parameters in Table 9.1. Note the close agreement between the analytical and numerical results. Excellent agreement is also obtained for the calculated concentration distributions after 365 days at the end of the simulation (Fig. 9.11). Figures 9.12 and 9.13 show similar results for the second set of transport parameters listed in Table 9.1.

Table 9.1. Input parameters for example 3A.

Parameter	Example 3a	Example 3b
$v$ [m/day]	0.1	1.0
$D_T$ [m <sup>2</sup> /day]	1.0	0.5
$D_L$ [m <sup>2</sup> /day]	1.0	1.0
$\lambda$ [day <sup>-1</sup> ]	0.0	0.01
$R$ [-]	1.0	3.0
$c_0$ [-]	1.0	1.0

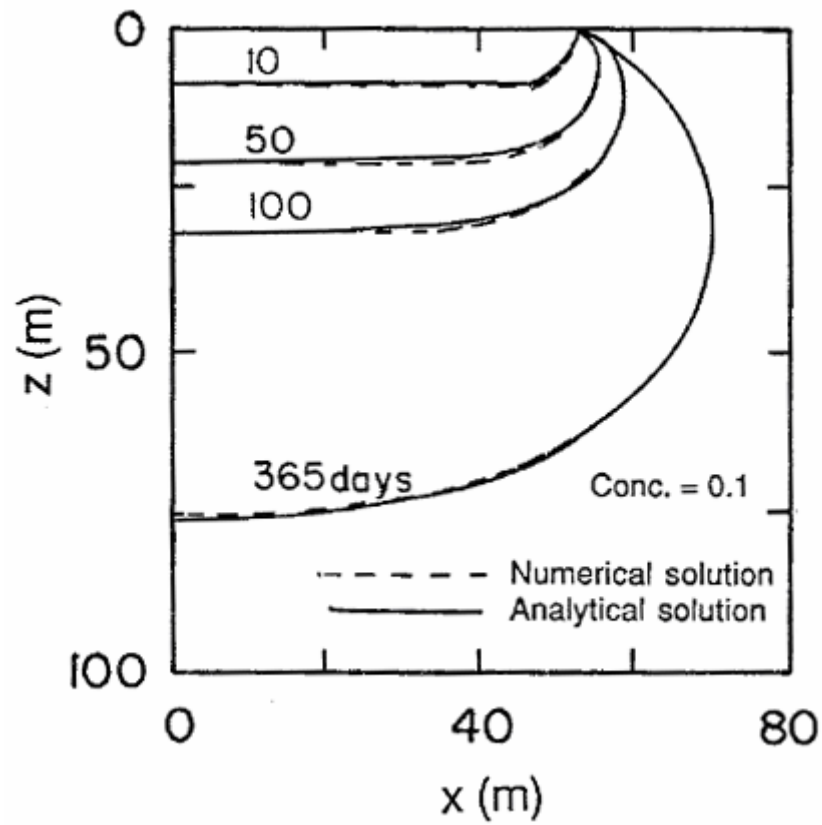


Figure 9.10. Advancement of the concentration front ( $c=0.1$ ) for example 3a as calculated with HYDRUS (dotted lines) and the analytical solution (solid lines).

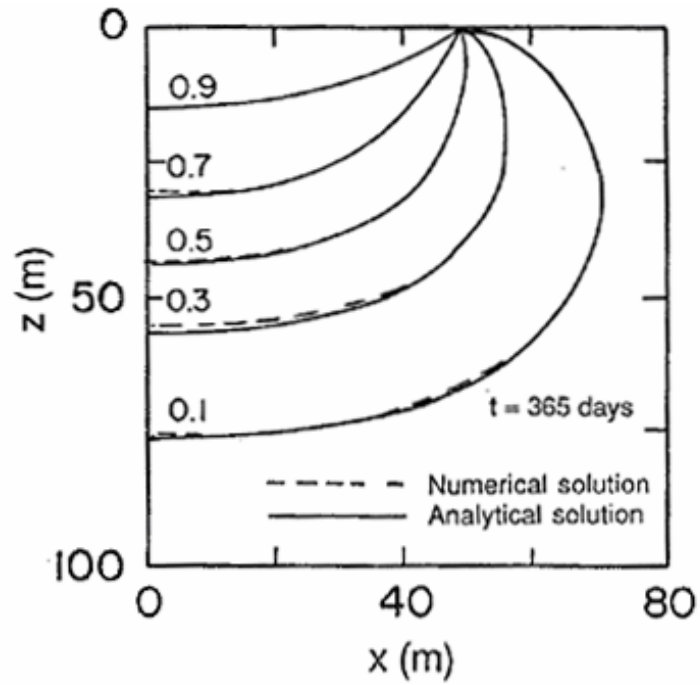


Figure 9.11. Concentration profile at the end of the simulation ( $t=365$  days) for example 3a calculated with HYDRUS (dotted lines) and the analytical solution (solid lines).

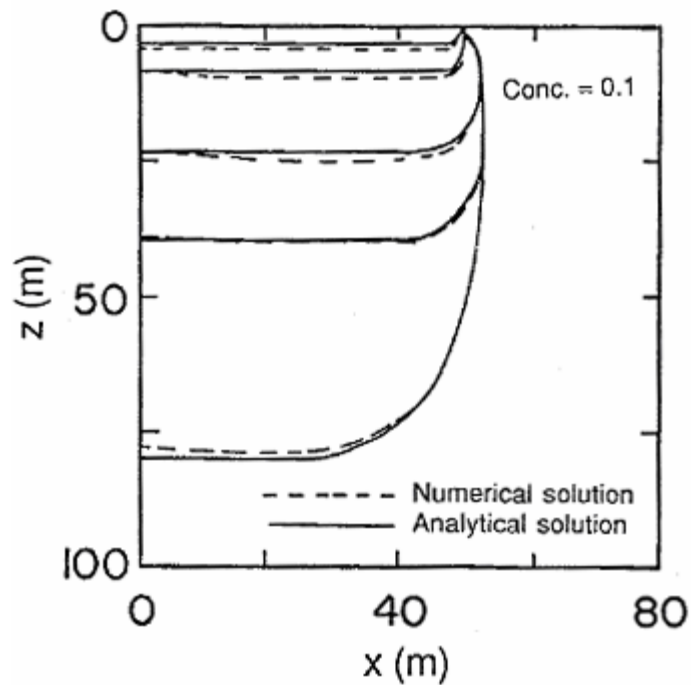


Figure 9.12. Advancement of the concentration front ( $c=0.1$ ) for example 3b as calculated with HYDRUS (dotted lines) and the analytical solution (solid lines).

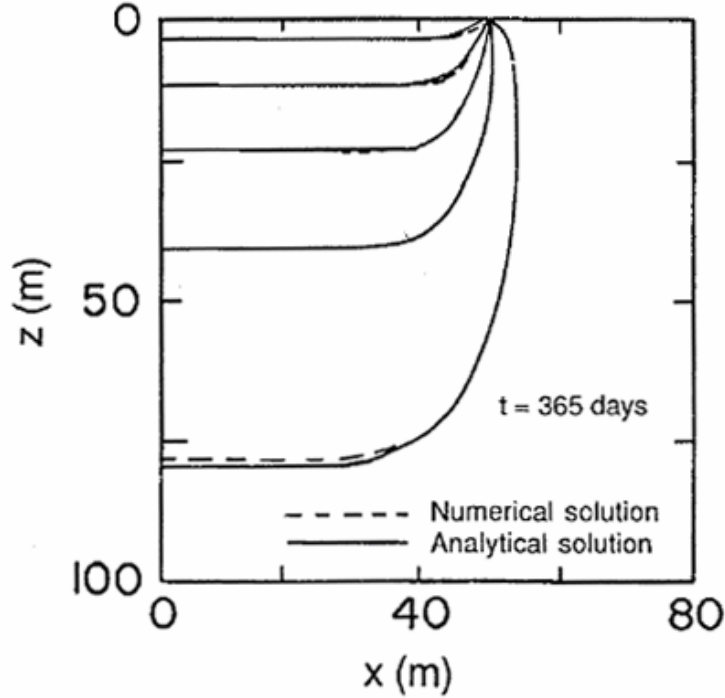


Figure 9.13. Concentration profile at the end of the simulation ( $t=365$  days) for example 3b as calculated with HYDRUS (dotted lines) and the analytical solution (solid lines).

### 9.1.3b. Example 3B - Three-Dimensional Solute Transport

This example was used to verify the mathematical accuracy of the solute transport part of SWMS\_3D. *Leij et al.* [1991] published several analytical solutions for three-dimensional dispersion problems. One of these solutions holds for solute transport in a homogeneous, isotropic porous medium during steady-state unidirectional groundwater flow (Figure 9.14). The solute transport equation (3.1) for this situation reduces to

$$R \frac{\partial c}{\partial t} = D_T \frac{\partial^2 c}{\partial x^2} + D_T \frac{\partial^2 c}{\partial y^2} + D_L \frac{\partial^2 c}{\partial z^2} - v \frac{\partial c}{\partial z} - \mu c + \lambda \quad (9.4)$$

where  $\lambda$  and  $\mu$  are a zero- and first-order degradation constants, respectively;  $D_L$  and  $D_T$  are the longitudinal and transverse dispersion coefficients, respectively;  $v$  ( $= q_z/\theta$ ) is the average pore water velocity in the flow direction, and  $z$  is the spatial coordinate parallel to the direction of flow, while  $x$  and  $y$  are the spatial coordinates perpendicular to the flow direction. The initially

solute-free medium is subjected to a solute source,  $c_0$ , of unit concentration. The rectangular surface source has dimensions  $2a$  and  $2b$  along the inlet boundary at  $z=0$ , and is located symmetrically about the coordinates  $x=0$  and  $y=0$  (Figure 9.14). The transport region of interest is the half-space ( $z \geq 0$ ;  $-\infty \leq x \leq \infty$ ,  $-\infty \leq y \leq \infty$ ). The boundary conditions may be written as:

$$\begin{aligned}
 c(x, y, 0, t) &= c_0 & -a \leq x \leq a, \quad -b \leq y \leq b \\
 c(x, y, 0, t) &= 0 & \text{other values of } x, y \\
 \lim_{z \rightarrow \infty} \frac{\partial c}{\partial z} &= 0 \\
 \lim_{z \rightarrow \pm\infty} \frac{\partial c}{\partial x} &= 0 \\
 \lim_{z \rightarrow \pm\infty} \frac{\partial c}{\partial y} &= 0
 \end{aligned} \tag{9.5}$$

The analytical solution of the above transport problem is [Leij and Bradford, 1994]

$$\begin{aligned}
 c(x, y, z, t) &= \frac{c_0}{4} \int_{P(t)}^t \left[ \frac{Rz^2}{4\pi D_L \tau^3} \right]^{1/2} \exp \left[ -\frac{\mu\tau}{R} - \frac{(Rz - v\tau)^2}{4RD_L\tau} \right] \\
 &\quad \left[ \operatorname{erfc} \left[ \frac{x-a}{2(D_T\tau/R)^{1/2}} \right] - \operatorname{erfc} \left[ \frac{x+a}{2(D_T\tau/R)^{1/2}} \right] \right] \\
 &\quad \left[ \operatorname{erfc} \left[ \frac{y-b}{2(D_T\tau/R)^{1/2}} \right] - \operatorname{erfc} \left[ \frac{y+b}{2(D_T\tau/R)^{1/2}} \right] \right] d\tau + \\
 &\quad + \frac{\lambda}{2R} \int_0^t \exp \left[ -\frac{\mu\tau}{R} \right] \left[ \operatorname{erfc} \left[ \frac{v\tau - Rz}{2(RD_L\tau)^{1/2}} \right] - \exp \left[ \frac{vz}{D_L} \right] \operatorname{erfc} \left[ \frac{Rz + v\tau}{2(RD_L\tau)^{1/2}} \right] \right] d\tau
 \end{aligned} \tag{9.6}$$

where  $P(t) = 0$  if  $t < t_0$  and  $P(t) = t - t_0$  if  $t > t_0$ , and where  $t_0$  is the duration of solute pulse. The input transport parameters for two simulations are listed in Table 9.1. The width of the source was assumed to be 100 m in both the  $x$  and  $y$  directions. Because of symmetry, calculations were carried out only for part of the transport domain where  $x \geq 0$ ,  $y \geq 0$  and  $z \geq 0$ .



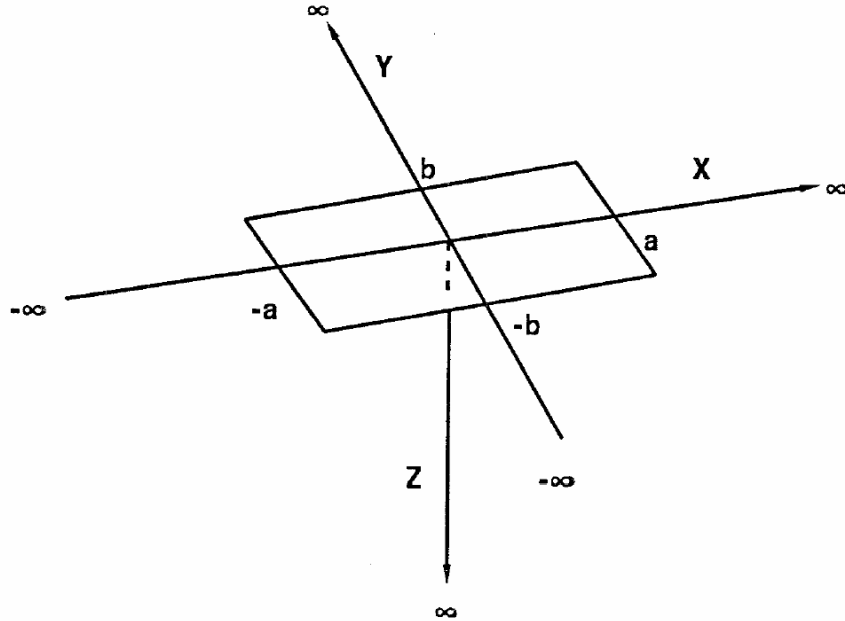


Figure 9.14. Schematic of the transport system for example 3B.

We will not show here the comparison of analytical and numerical results for these three-dimensional problems, since the obtained figures are fairly similar to Figures 9.11 through 9.14. The agreement between the analytical and numerical results is also at the same order as those shown in Figures 9.11 through 9.14.

#### 9.1.4. Example 4 - One-Dimensional Solute Transport with Nitrification Chain

This example was used to verify in part the mathematical accuracy of the solute transport part of HYDRUS. Numerical results will be compared with results generated with an analytical solution published by *van Genuchten* [1985] for one-dimensional convective-dispersive transport of solutes involved in sequential first-order decay reactions. The analytical solution holds for solute transport in a homogeneous, isotropic porous medium during steady-state unidirectional groundwater flow. Solute transport equations (3.1) and (3.2) for this situation reduce to

$$R_1 \frac{\partial c_1}{\partial t} = D \frac{\partial^2 c_1}{\partial x^2} - v \frac{\partial c_1}{\partial x} - \mu_1 R_1 c_1 \quad (9.7)$$

$$R_i \frac{\partial c_i}{\partial t} = D \frac{\partial^2 c_i}{\partial x^2} - v \frac{\partial c_i}{\partial x} + \mu_{i-1} R_{i-1} c_{i-1} - \mu_i R_i c_i \quad i = 2, 3 \quad (9.8)$$

where  $\mu$  is a first-order degradation constant,  $D$  is the dispersion coefficient,  $v$  is the average pore water velocity ( $q_x/\theta$ ) in the flow direction,  $x$  is the spatial coordinate in the direction of flow, and where it is assumed that 3 solutes participate in the decay chain. The specific example used here applies to the three-species nitrification chain



and is the same as described by *van Genuchten* [1985], and earlier by *Cho* [1971]. The boundary conditions may be written as:

$$\begin{aligned} \left( -D \frac{\partial c_1}{\partial x} + v c_1 \right) &= v c_{0,1}(0, t) \\ \left( -D \frac{\partial c_i}{\partial x} + v c_i \right) &= 0 \quad i = 2, 3 \\ \lim_{x \rightarrow \infty} \frac{\partial c_i}{\partial x} &= 0 \quad i = 1, 2, 3 \end{aligned} \quad (9.10)$$

The experiment involves the application of a  $\text{NH}_4^+$  solution to an initially solute-free medium ( $c_i = 0$ ). The input transport parameters for the simulation are listed in Table 9.2.

Figure 9.15 shows concentration profiles for all three solutes at time 200 hours, calculated both numerically with HYDRUS and analytically with the CHAIN code of *van Genuchten* [1985]. Figure 9.16 shows the concentration profiles at three different times (50, 100, and 200 hours) for  $\text{NH}_4^+$ ,  $\text{NO}_2^-$ , and  $\text{NO}_3^-$ , respectively. The numerical results in each case duplicated the analytical results.

Table 9.2. Input parameters for example 4.

Parameter	Value
$v$ [cm/hour]	1.0
$D$ [cm <sup>2</sup> /hour]	0.18
$\mu_1$ [hour <sup>-1</sup> ]	0.005
$\mu_2$ [hour <sup>-1</sup> ]	0.1
$\mu_3$ [hour <sup>-1</sup> ]	0.0
$R_1$ [-]	2.0
$R_2$ [-]	1.0
$R_3$ [-]	1.0
$c_i$ [-]	0.0
$c_{0,1}$ [-]	1.0

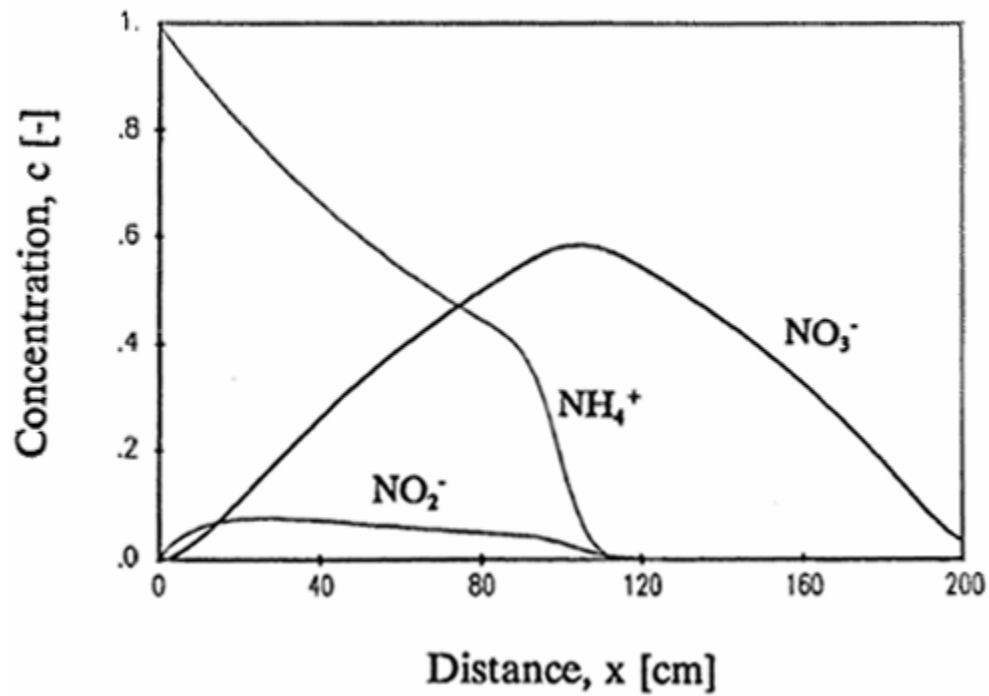


Figure 9.15. Analytically and numerically calculated concentration profiles for  $\text{NH}_4^+$ ,  $\text{NO}_2^-$ , and  $\text{NO}_3^-$  after 200 hours for example 4.

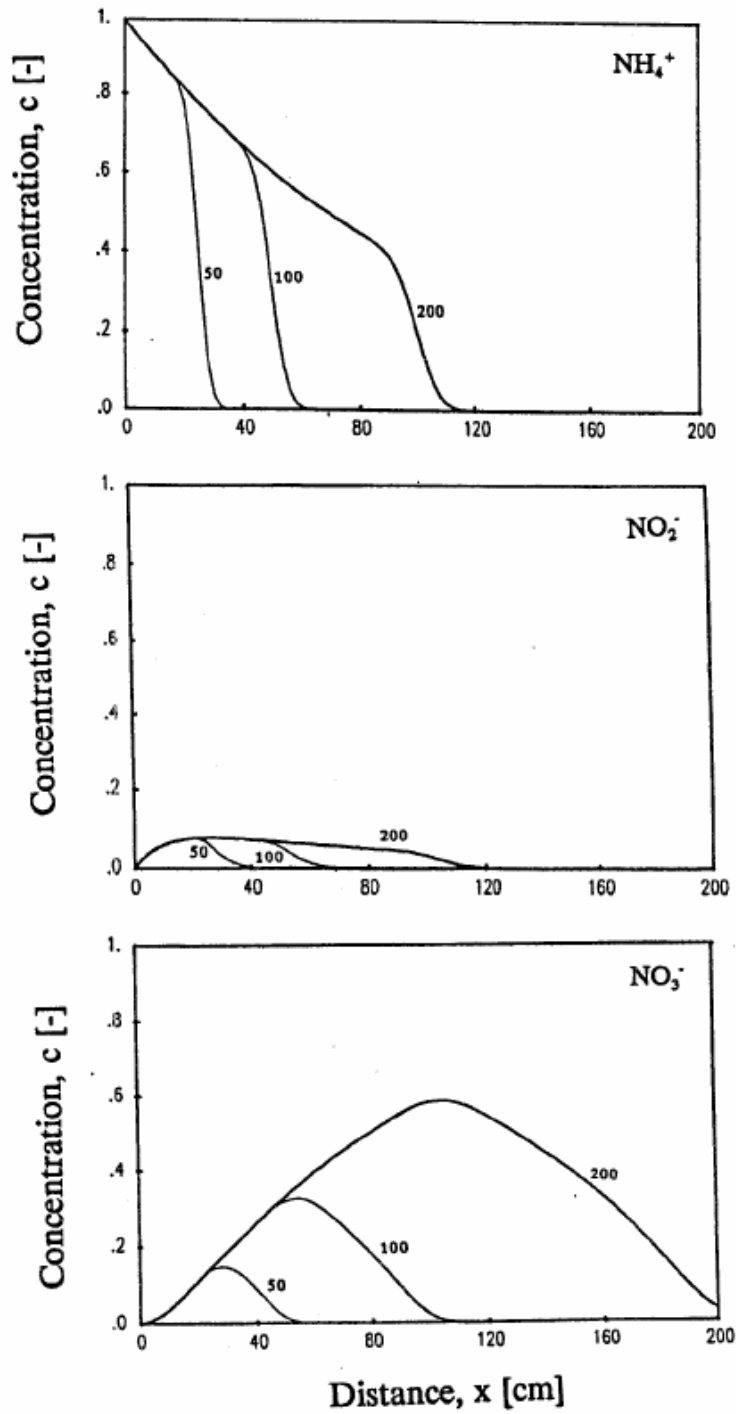


Figure 9.16. Analytically and numerically calculated concentration profiles for  $\text{NH}_4^+$  (top),  $\text{NO}_2^-$  (middle),  $\text{NO}_3^-$  (bottom) after 50, 100, and 200 hours for example 4.

### 9.1.5. Example 5 - One-Dimensional Solute Transport with Nonlinear Cation Adsorption

The experiment discussed in this example was conducted by *Selim et al.* [1987], and used later for validation of the HYDRUS code [*Kool and van Genuchten*, 1991]. The soil in this experiment was Abist loam. A 10.75-cm long soil column was first saturated with a 10 mmol<sub>c</sub>L<sup>-1</sup> CaCl<sub>2</sub> solution. The experiment consisted of applying a 14.26 pore volume pulse ( $t=358.05$  hours) of 10 mmol<sub>c</sub>L<sup>-1</sup> MgCl<sub>2</sub> solution, followed by the original CaCl<sub>2</sub> solution. The adsorption isotherm was determined with the help of batch experiments [*Selim et al.*, 1987], and fitted with the Freundlich equation (3.3) [*Kool and van Genuchten*, 1991]. The Freundlich isotherm parameters, as well as other transport parameters for this problem, are listed in Table 9.3. First- and second-type boundary conditions were applied at the top and bottom of the soil column, respectively.

The observed Mg breakthrough curve is shown in Figure 9.17, together with simulated breakthrough curves obtained with HYDRUS, the MONOC code of *Selim et al.* [1987] and the version 3.1 of the HYDRUS code of *Kool and van Genuchten* [1991]. The results indicate a reasonable prediction of the measured breakthrough curve using HYDRUS, and close correspondence between the simulated results obtained with the HYDRUS and MONOC models. The HYDRUS results became identical to those generated with HYDRUS-3.1 when a third-type boundary condition was invoked at the top of the soil column.

Table 9.3. Input parameters for example 5.

Parameter	Value
$q$ [cm/hour]	0.271
$D$ [cm <sup>2</sup> /hour]	1.167
$\rho$ [g/cm <sup>3</sup> ]	0.884
$\theta$ [-]	0.633
$c_0$ [mmol/L]	10.0
$k_s$ [cm <sup>3</sup> /g]	1.687
$\beta$ [-]	1.615

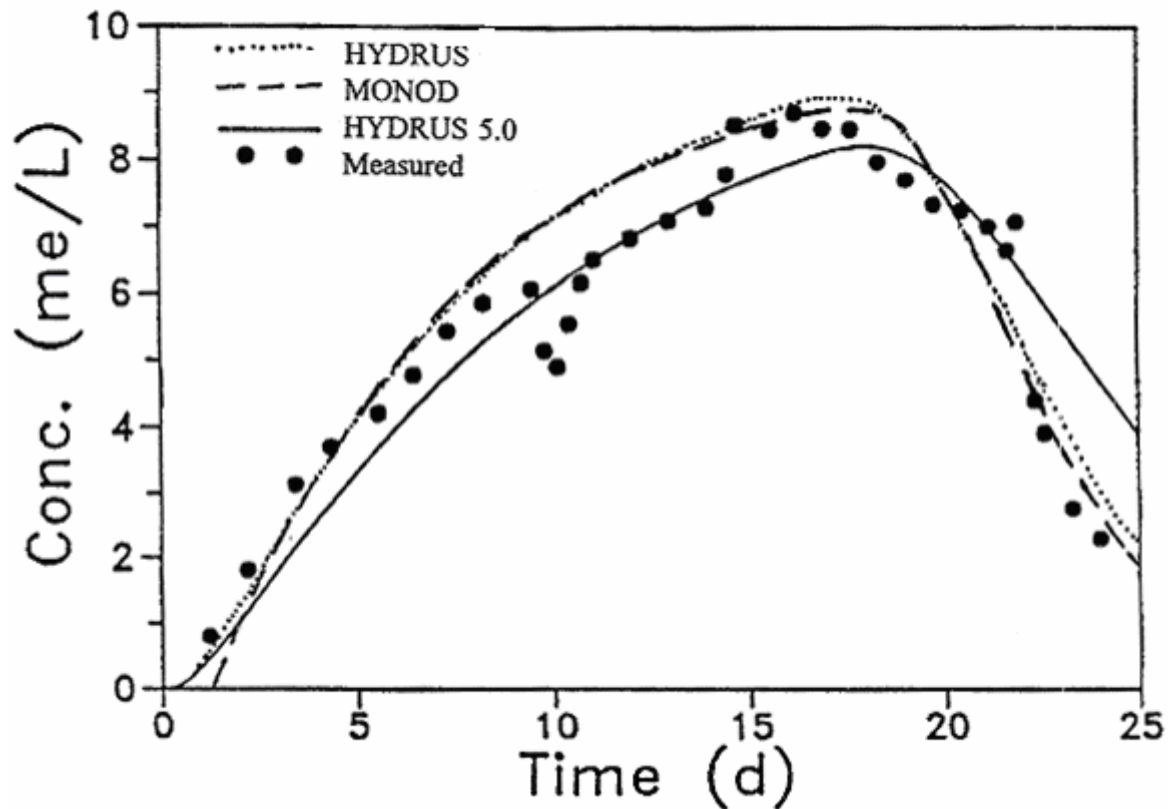


Figure 9.17. Mg breakthrough curves for Abist loam calculated with the MONOD, HYDRUS, and HYDRUS codes (data points from *Selim et al.* [1978]).

The Langmuir adsorption isotherm can also be used to model the exchange of homovalent ions. Parameters in the Langmuir adsorption isotherm for homovalent ion exchange may be derived as follows. Ion exchange for two ions with valences  $n$  and  $m$  can be expressed in a generalized form as [Sposito, 1981]

$$K_{ex} = \left( \frac{\bar{a}_1}{a_2} \right)^m \left( \frac{a_1}{\bar{a}_2} \right)^n \quad (9.11)$$

where  $K_{ex}$  is the dimensionless thermodynamic equilibrium constant, and  $a$  and  $\bar{a}$  denote the ion activities in the soil solution and on the exchange surfaces [-], respectively:

$$a_i = \gamma_i c_i \quad i = 1, 2 \quad (9.12)$$

$$\bar{a}_i = \xi_i s_i \quad i = 1, 2$$

where  $c_i$  [ML<sup>-3</sup>] (mmol/l) and  $s_i$  [MM<sup>-1</sup>] (mmol/kg) are solution and exchangeable concentrations, respectively, and  $\gamma_i$  and  $\xi_i$  are activity coefficients in the soil solution [L<sup>3</sup>M<sup>-1</sup>] (l/mmol) and on the exchange surfaces [MM<sup>-1</sup>] (kg/mmol), respectively. Substituting (9.12) into (9.11) gives

$$K_{12} = K_v \frac{\gamma_1^m}{\gamma_2^2} = K_{ex} \frac{\xi_2^n}{\xi_1^m} \frac{\gamma_1^m}{\gamma_2^n} = \frac{s_1^m c_2^n}{s_2^n c_1^m} \quad (9.13)$$

where  $K_v$  denotes the Vanselow selectivity coefficient [-], while  $K_{12}$  will be simply referred to as the selectivity coefficient [-]. Assuming that both the total solution concentration,  $C_T$  [ML<sup>-3</sup>] (mmol/l), and the cation exchange capacity,  $S_T$  [MM<sup>-1</sup>] (mmol/kg), are time invariant, i.e.,

$$\begin{aligned} nc_1 + mc_2 &= C_T \\ ns_1 + ms_2 &= S_T \end{aligned} \quad (9.14)$$

the Langmuir parameters  $k_s$  and  $\eta$  in (3.3) for the incoming solute become

$$\begin{aligned} k_s &= \frac{K_{12} S_T}{C_T} \\ \eta &= \frac{\vartheta(K_{12} - 1)}{C_T} \end{aligned} \quad (9.15)$$

whereas for the solute initially in the soil column:

$$\begin{aligned} k_s &= \frac{S_T}{K_{12} C_T} \\ \eta &= \frac{\vartheta(1 - K_{12})}{K_{12} C_T} \end{aligned} \quad (9.16)$$

The parameter  $\nu$  in (9.15) and (9.16) equals 1 for monovalent ions, and 2 for divalent ions.

The selectivity coefficient  $K_{12}$  for example 5 was measured by *Selim et al.* [1987] ( $K_{12}=0.51$ ). From the total solution concentration ( $C_T=10$  mmol/l) and the known cation exchange capacity ( $S_T=62$  mmol/kg), it follows that the parameters in the Langmuir adsorption isotherm for the incoming solute (Mg) are  $k_s=3.126$  and  $\eta=-0.098$ , while those for the solute initially in the soil profile (Ca) the parameters are  $k_s=12.157$  and  $\eta=0.192$ . The observed Ca breakthrough curve is shown in Figure 9.18, together with the simulated breakthrough curves obtained with the HYDRUS and MONOC codes [*Selim et al.*, 1987]. Note the close agreement between the numerical results and the experimental data.

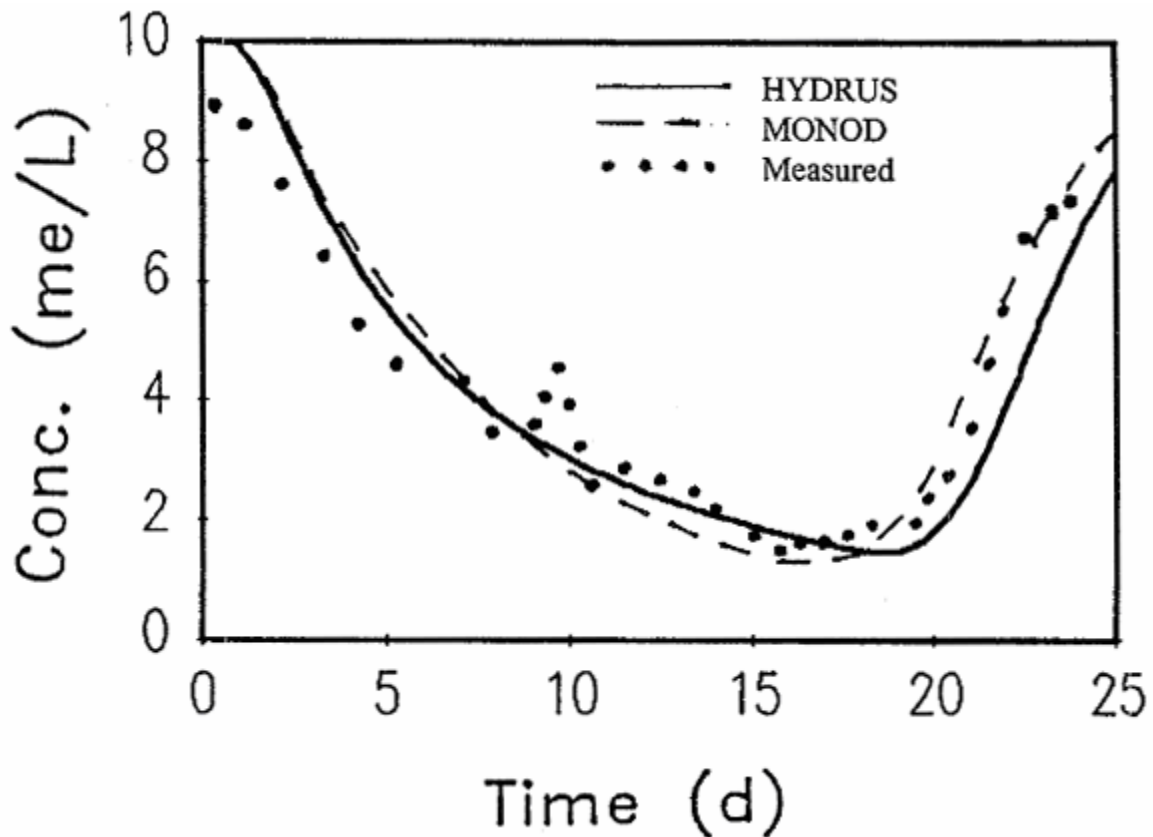


Figure 9.18. Ca breakthrough curves for Abist loam calculated with the MONOD and HYDRUS codes (data points from *Selim et al.* [1978]) (example 5).



### 9.1.6. Example 6 - One-Dimensional Solute Transport with Nonequilibrium Adsorption

This example considers the movement of a boron ( $\text{H}_3\text{BO}_4$ ) pulse through Glendale clay loam [van Genuchten, 1981]. The numerical simulation uses solute transport parameters that were fitted to the breakthrough curve with the CFITIM parameter estimation model [van Genuchten, 1981] assuming a two-site chemical nonequilibrium sorption model analogous to the formulation discussed in Section 3, but for steady-state water flow. Input parameters for example 6 are listed in Table 9.4. Figure 9.19 compares HYDRUS numerical results with the experimental data, and with a numerical simulation assuming physical non-equilibrium and nonlinear adsorption [van Genuchten, 1981].

Table 9.4. Input parameters for example 6.

Parameter	Value
$q$ [cm/day]	17.12
$D$ [cm <sup>2</sup> /day]	49.0
$\theta$ [-]	0.445
$\rho$ [g/cm <sup>3</sup> ]	1.222
$c_0$ [mmol/L]	20.0
$k_s$ [cm <sup>3</sup> /g]	1.14
$\beta$ [-]	1.0
$\eta$ [-]	0.0
$f$ [-]	0.47
$\omega$ [1/day]	0.320
$t_p$ [day]	5.06

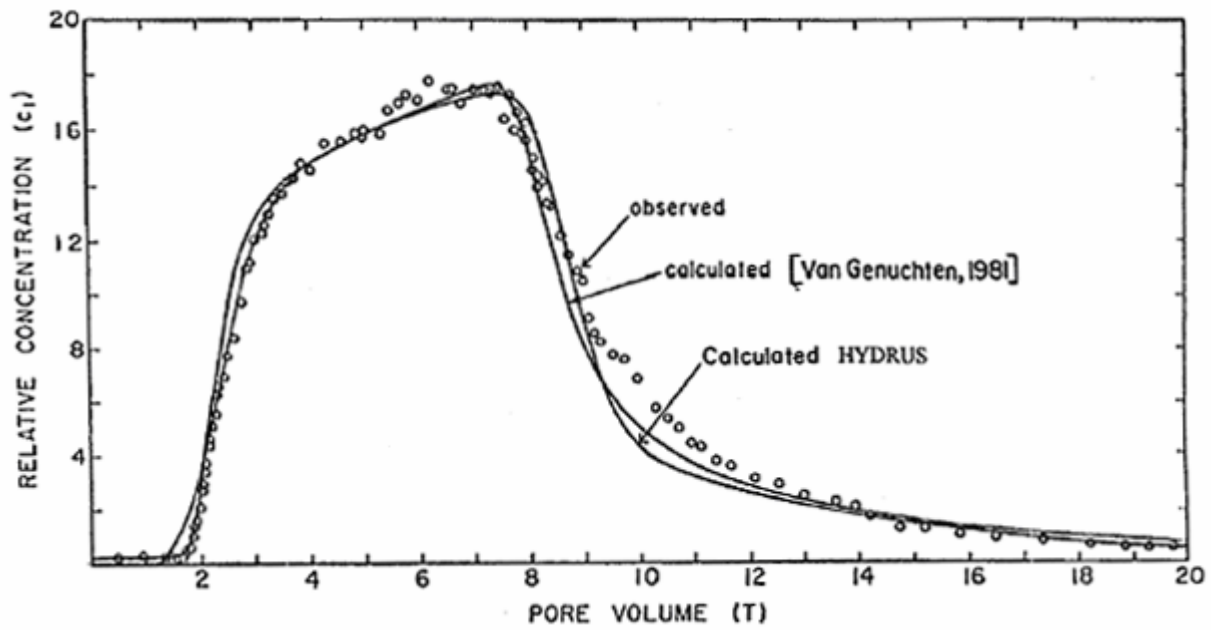
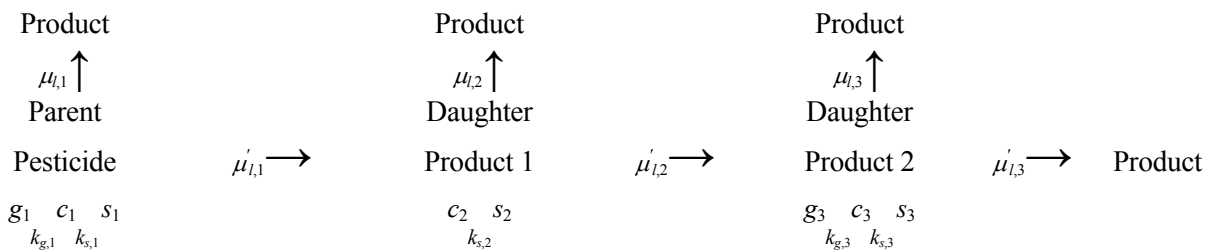


Figure 9.19. Observed and calculated effluent curves for Boron movement through Glendale clay (data points from *van Genuchten* [1981]) (example 6).

### 9.1.7. Example 7 - Water and Solute Infiltration Test

This example corresponds to example 4 in the SWMS\_2D and HYDRUS-2D manuals [Šimůnek *et al.*, 1992, 1999]. The example concerns the movement of water and a dissolved solute from a single-ring infiltrometer into the soil profile consisting of two layers: a 40-cm thick A-horizon, and an underlying B/C-horizon. The hydraulic functions of the two soil layers are the same as those used in Example 2. The axisymmetric flow system and associated finite element mesh for the ponded infiltration experiment are shown in Figure 9.19. The soil profile had an initial temperature of 20°C, whereas the infiltrated water had a temperature of 30°C and contained an organic (parent) compound (the pesticide aldicarb) which is known to degrade by oxidation into two sequential daughter products (sulfone and sulfoxide) [Ou *et al.*, 1988]. Each of the three solutes also undergoes hydrolytical first-order decay that leads to products which are not simulated or monitored during their subsequent transport (i.e., oxime, sulfone oxime, and sulfoxide oxime) [Ou *et al.*, 1988]. All major solutes adsorb onto the solid phase, and volatilization is considered for the first and the third solutes. The reaction pathway is schematically given by:



The example is used here to illustrate variably-saturated water flow, heat movement, and solute transport in a layered and radially symmetric three-dimensional soil profile.

Calculations were carried out over a period of 10 days. The pressure head profile obtained in example problem 2 at the beginning of June 1982 was taken as the initial condition for the water flow equation, similarly as in example 4 of Šimůnek *et al.* [1992]. The soil profile was assumed to be initially free of any solutes. All sides of the flow region were considered to be impervious, except for a small portion around the origin at the surface (the ponded surface inside the ring infiltrometer) where constant pressure head and concentration flux boundary conditions were imposed, as well as the lower right corner where the groundwater level was kept constant. The concentration of the infiltrating water was free of any solute except for the first five days of the simulation during which time the infiltrating water contained the parent solute of unit concentration. Boundary condition

(3.40) was used for the non-ponded part of the soil surface, thereby assuming the existence of a stagnant boundary layer of thickness  $d$  at the soil surface through which volatile solutes moved to the atmosphere by gas diffusion only. Water and solute extraction by plant roots was not considered.

Tables 9.5, 9.6, and 9.7 list the unsaturated soil hydraulic, heat and solute transport parameters, respectively. The solute and heat transport parameters were assumed to be the same for the two soil layers. The heat transport parameters  $b_1$ ,  $b_2$ ,  $b_3$ ,  $C_n$ ,  $C_o$ , and  $C_w$  in Table 9.6 were taken from *Chung and Horton* [1987]. The solute parameters  $k_s$ ,  $k_g$ ,  $\mu_w$ ,  $\mu_w'$ , and  $D_g$  in Table 9.7 were taken from *Wagenet and Hutson* [1987].

Figure 9.21 presents the initial and steady-state pressure head profiles. The steady-state profile for water flow was reached after approximately 2 or 3 days. Temperature profiles at times 1 and 10 days are shown in Figure 9.22. The heat front moved relatively slowly into the soil profile in comparison with the solute front (shown later) because of the high volumetric heat capacity of the relatively wet soil. Figures 9.23, 9.24, and 9.25 show concentration profiles for all three solutes at times 2.5, 5, 7.5, and 10 days. After its application in the infiltrating water during the first five days of the simulation (Fig. 9.23a, b), the first (parent) solute is transported further by water flow and gaseous diffusion, as well as is being degraded by two first-order decay reactions, such that the soil profile is practically free of this solute after 10 days (Fig. 9.23c, d). The second solute exists exclusively because of first-order degradation of the first solute. Hence, the second solute initially corresponds mainly with the first solute, but subsequently moves faster through the soil profile because of less sorption. Note that the highest concentrations of the second solute were reached after complete application of the first solute (Fig. 9.24c, d). Similar features as for the second solute also apply to the third solute. In particular, notice that the soil profile is almost free of this solute after 2.5 days (Fig. 9.25a), and that the highest concentrations of the third solute (while being much smaller than those for the first two solutes) were reached at the end of the simulation (Fig. 9.25d).

Table 9.5. Hydraulic input parameters for example 7.

Parameter	1st layer	2nd layer
$\theta_s = \theta_m = \theta_k$	0.399	0.339
$\theta_r = \theta_a$	0.000	0.000
$K_s = K_k$ [m/day]	0.298	0.454
$\alpha$ [1/m]	1.74	1.39
$n$ [-]	1.38	1.60

Table 9.6. Heat transport input parameters for example 7.

Parameter	Value
$\theta_n$ [-]	0.600 <sup>+</sup> (0.660 <sup>*</sup> )
$\theta_o$ [-]	0.001
$\lambda_L$ [m]	0.005
$\lambda_T$ [m]	0.001
$b_1$ [Wm <sup>-1</sup> K <sup>-1</sup> ]	0.243
$b_2$ [Wm <sup>-1</sup> K <sup>-1</sup> ]	0.393
$b_3$ [Wm <sup>-1</sup> K <sup>-1</sup> ]	1.534
$C_n$ [Jm <sup>-3</sup> K <sup>-1</sup> ]	1.92*10 <sup>6</sup>
$C_o$ [Jm <sup>-3</sup> K <sup>-1</sup> ]	2.51*10 <sup>6</sup>
$C_w$ [Jm <sup>-3</sup> K <sup>-1</sup> ]	4.18*10 <sup>6</sup>
$T_i$ [°C]	20
$T_0$ [°C]	30

<sup>+</sup> for the first layer

<sup>\*</sup> for the second layer

Table 9.7. Solute transport input parameters for example 7.

Parameter	Value
$\rho$ [kg/m <sup>3</sup> ]	1300
$D_w$ [m <sup>2</sup> /day]	0.00374
$D_g$ [m <sup>2</sup> /day]	0.432
$D_L$ [m]	0.005
$D_T$ [m]	0.001
$k_{s,1}$ [m <sup>3</sup> /kg]	0.0001
$k_{s,2}$ [m <sup>3</sup> /kg]	0.00005
$k_{s,3}$ [m <sup>3</sup> /kg]	0.0002
$k_{g,1}$ [-]	$1.33 \cdot 10^{-7}$
$k_{g,2}$ [-]	0.0
$k_{g,3}$ [-]	$1.33 \cdot 10^{-3}$
$\mu_{w,1}$ [1/day]	0.2
$\mu_{w,2}$ [1/day]	0.01
$\mu_{w,3}$ [1/day]	0.005
$\mu'_{w,1}$ [1/day]	0.36
$\mu'_{w,2}$ [1/day]	0.024
$\mu'_{w,3}$ [1/day]	0.0024
$c_{0,1}$ [-]	1.0
$c_{0,2}$ [-]	0.0
$c_{0,3}$ [-]	0.0
$d$ [m]	0.005

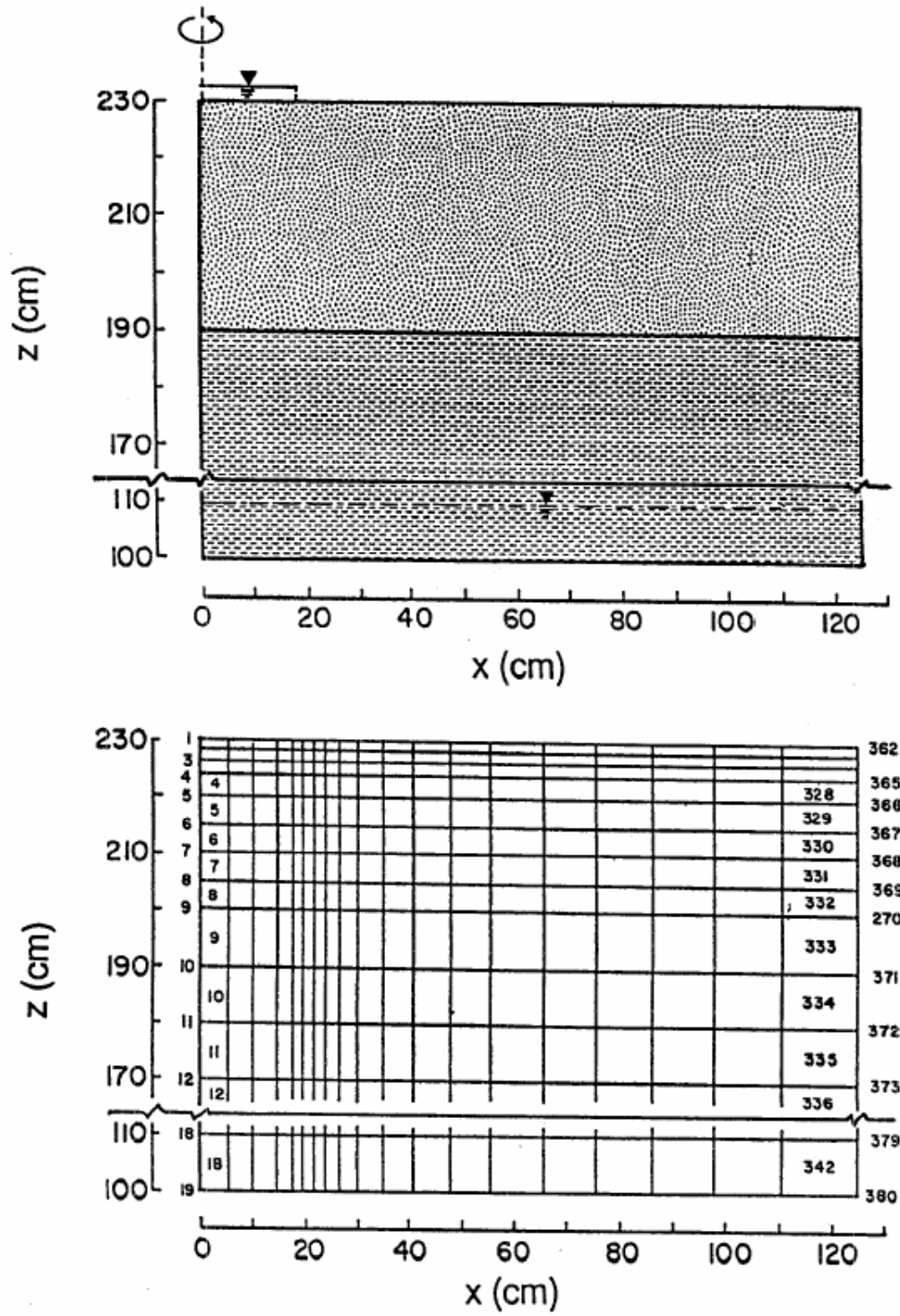


Figure 9.20. Flow system and finite element mesh for example 7.

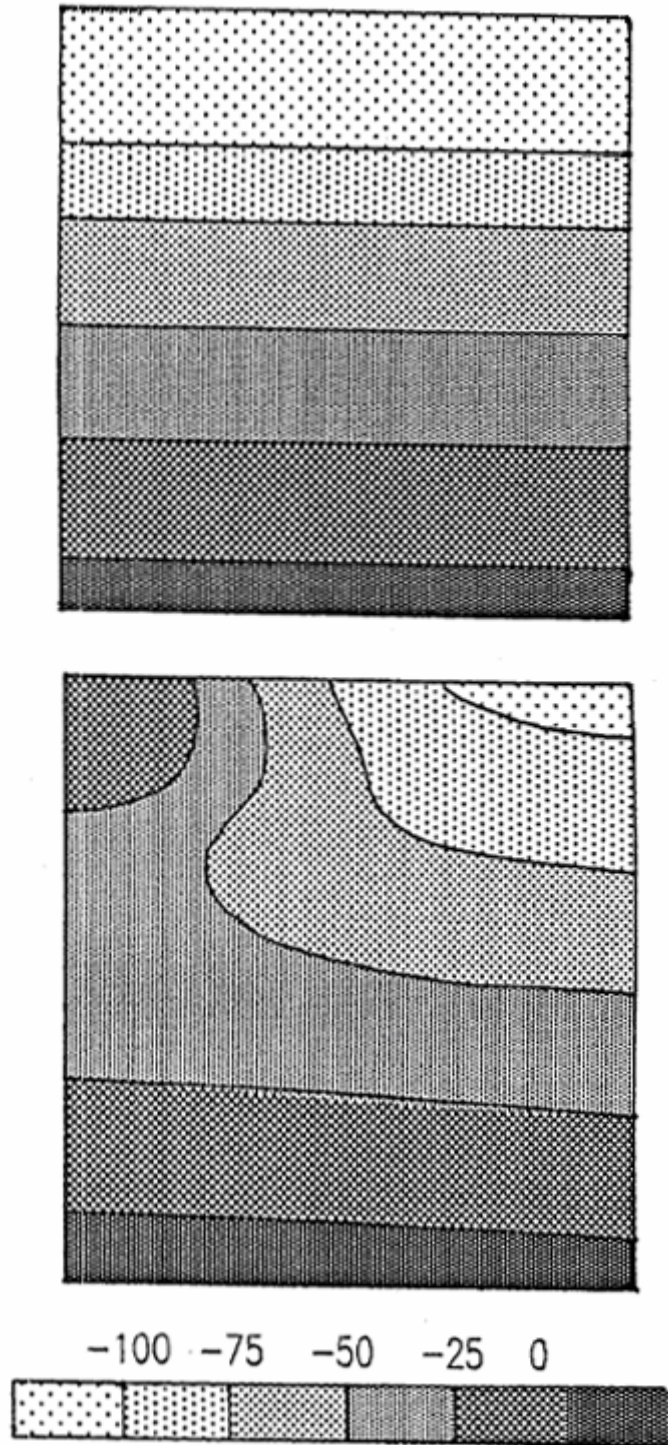


Figure 9.21. Initial (top) and steady state (bottom) pressure head profiles for example 7.



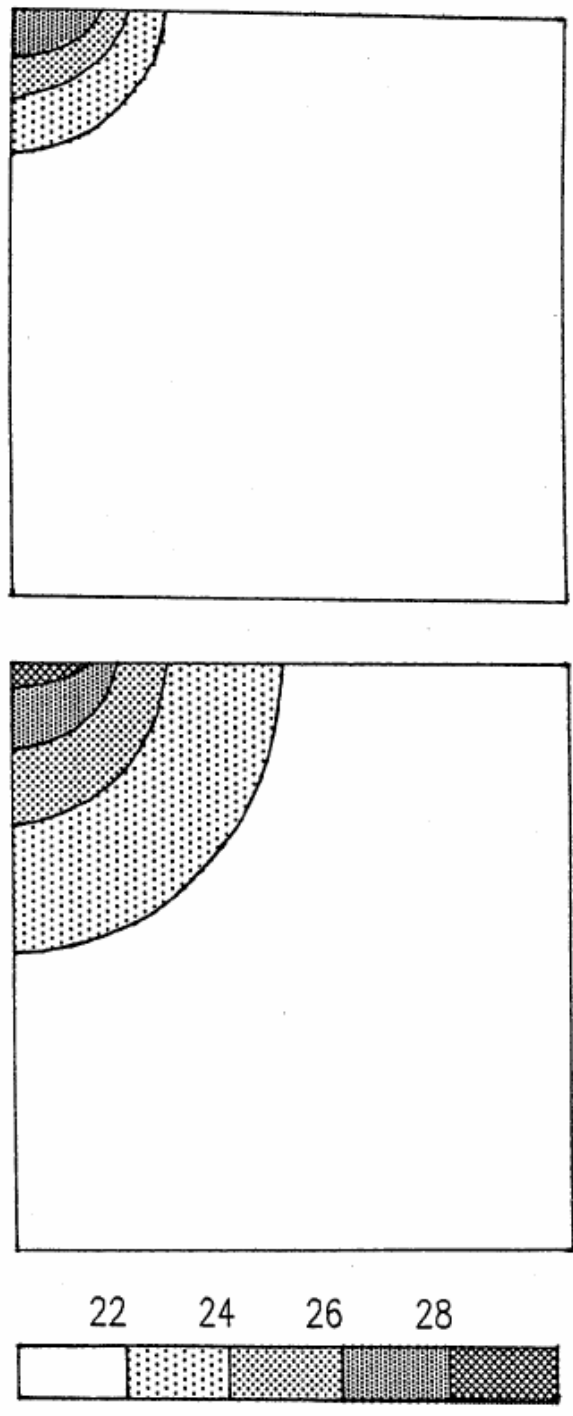


Figure 9.22. Temperature profiles after 1 (top) and 10 days (bottom) for example 7.

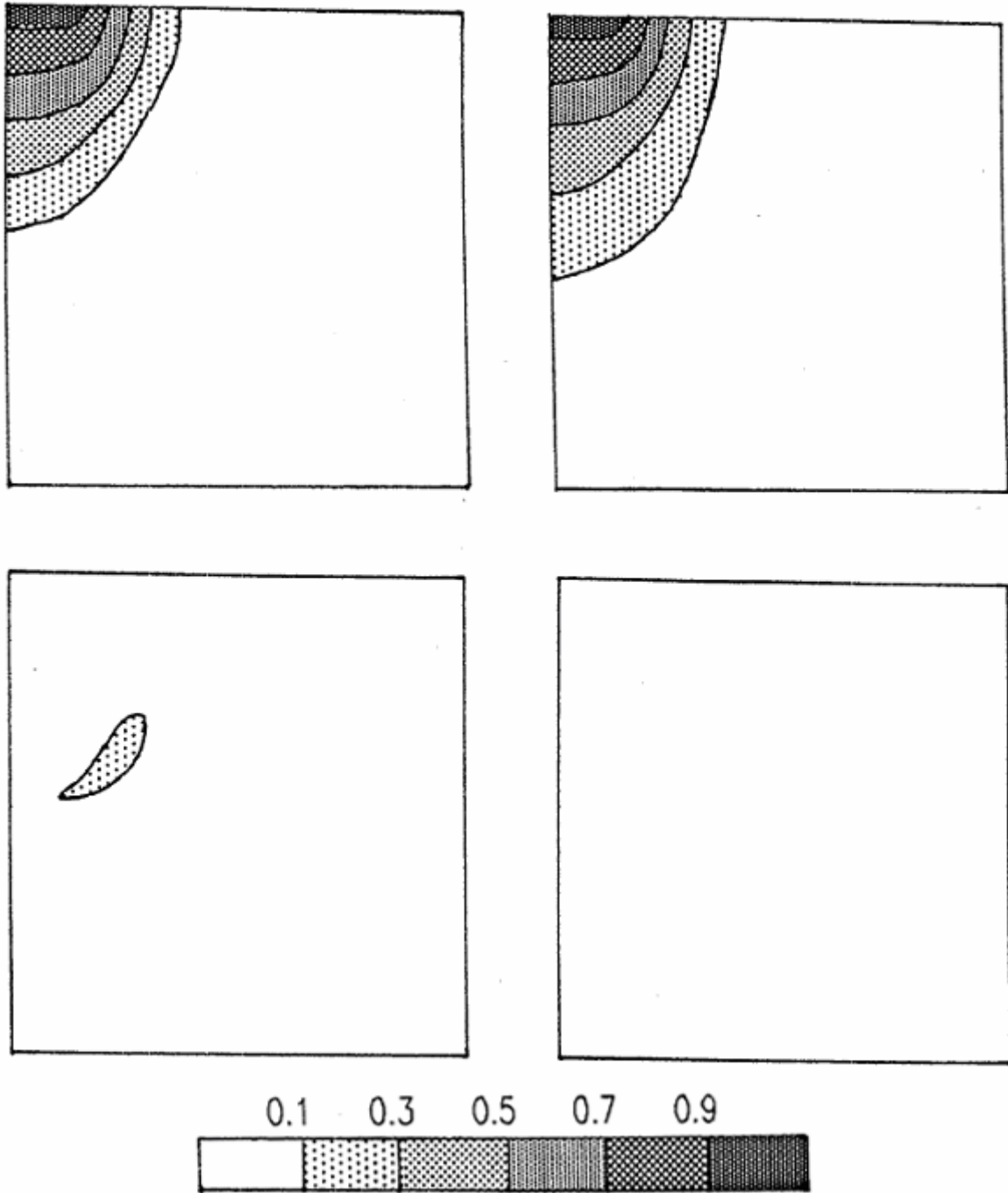


Figure 9.23. Concentration profiles for the first solute after 2.5, 5, 7.5, and 10 days for example 7.

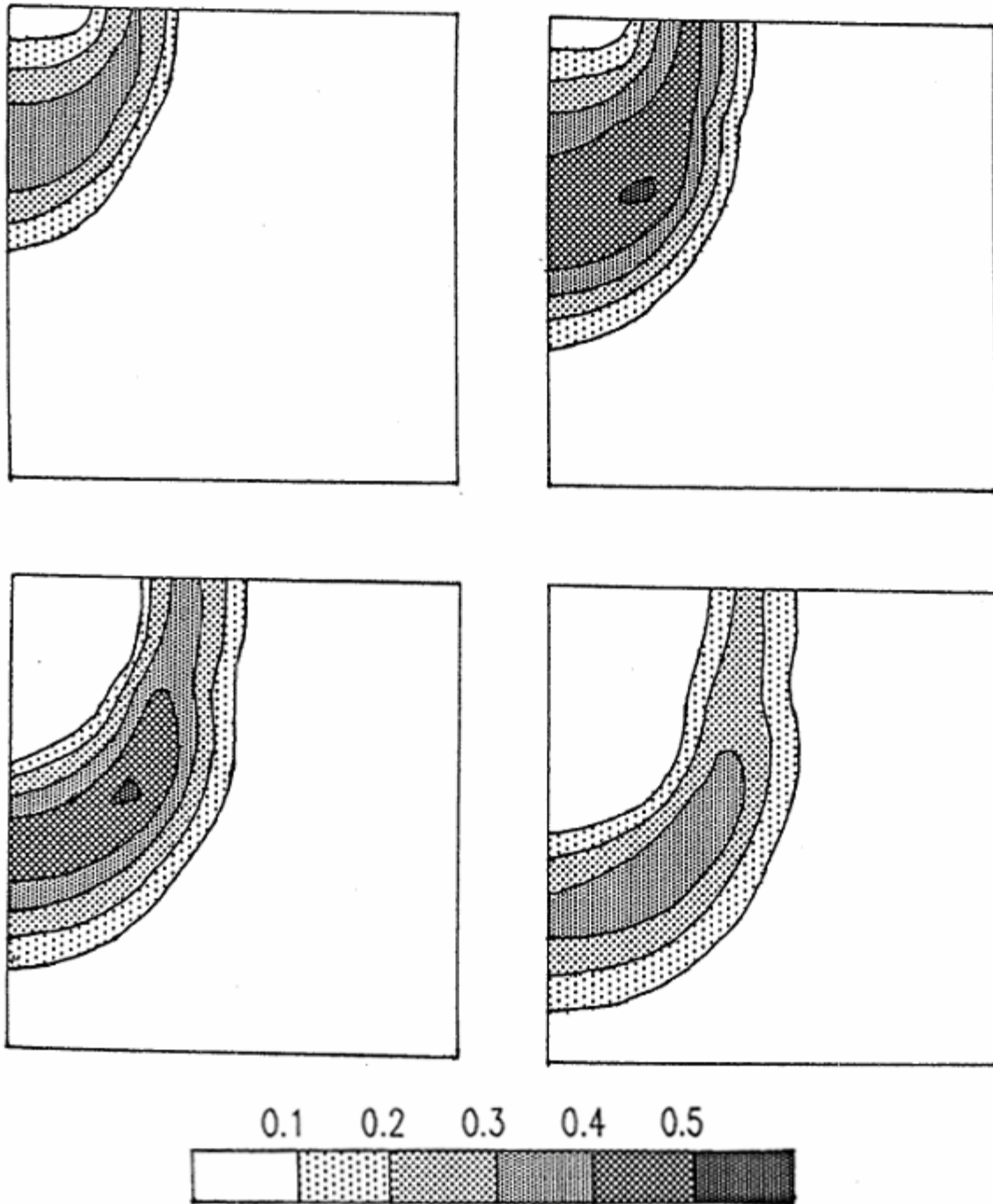


Figure 9.24. Concentration profiles for the second solute after 2.5, 5, 7.5, and 10 days for example 7.

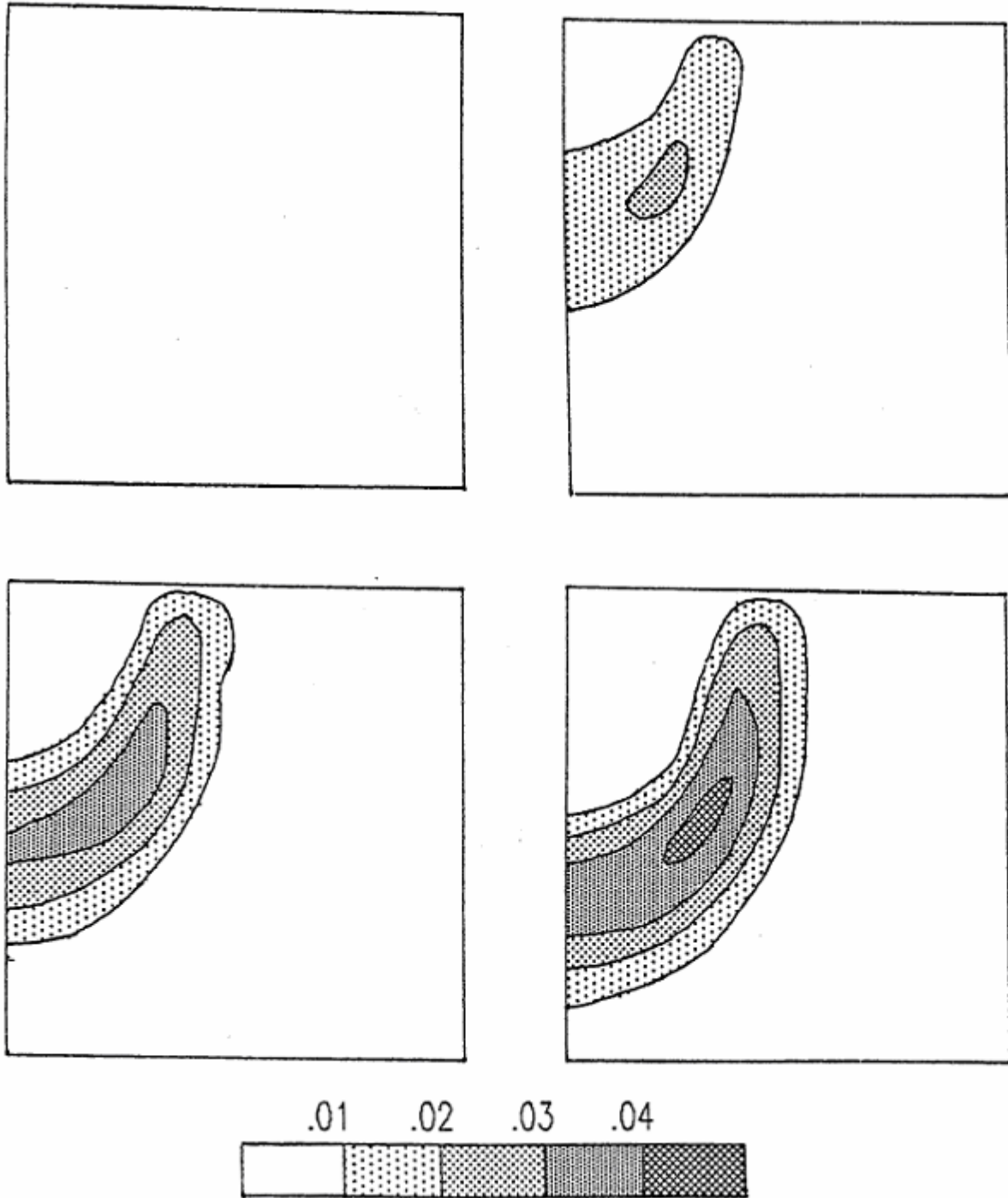


Figure 9.25. Concentration profiles for the third solute after 2.5, 5, 7.5, and 10 days for example 7.

### 9.1.8. Example 8 - Contaminant Transport From a Waste Disposal Site

This test problem concerns contaminant transport from a waste disposal site (or possibly a landfill) into a unconfined aquifer containing a pumping well downgradient of the disposal site as shown in Figure 9.26. Water was assumed to infiltrate from the disposal site into the unsaturated zone under zero-head ponded conditions. The concentration of the contaminant leaving the disposal site was taken to be 1.0 during the first 50 days, and zero afterwards. The waste disposal site itself had lateral dimensions of  $10 \times 40 \text{ m}^2$ . Initially, the water table decreased from a height of 28 m above the base of the aquifer at the left-hand side (Figure 9.26) to 26 m on the right-hand side of the flow domain. The initial pressure head in the unsaturated zone was assumed to be at equilibrium with the initial water table, i.e., no vertical flow occurred. The transport experiment started when the water table in the fully penetrated well at  $x = 170 \text{ m}$  ( $y = 0$ ) was suddenly lowered to a height of 18 m above the bottom of the unconfined aquifer. We assumed that at that same time ( $t = 0$ ) infiltration started to occur from the disposal site. Prescribed hydraulic head conditions  $h + z = 28 \text{ m}$  and  $h + z = 26 \text{ m}$  were imposed along the left-hand ( $x = 0$ ) and right-hand ( $x = 260 \text{ m}$ ) side boundaries ( $-50 \leq y \leq 50 \text{ m}$ ). A prescribed hydraulic head condition of  $h + z = 18 \text{ m}$  was used to represent the well along a vertical below the water table ( $z \leq 18$ ) at  $x = 170 \text{ m}$  and  $y = 0 \text{ m}$ , while a seepage face was defined at that location along the vertical above the water table ( $z > 18$ ). No-flow conditions were assumed along all other boundaries, including the soil interface. Hydraulic and transport parameters used in the analysis are listed in Table 9.8. We selected the retention hydraulic parameters for a coarse-textured soil with a relatively high saturated hydraulic conductivity,  $K_s$ , in order to test the HYDRUS code for a comparatively difficult numerical problem.

Because of symmetry about the  $y$  axis, only half of the flow region was simulated. The solution domain defined by  $0 \leq x \leq 260$ ,  $0 \leq y \leq 50$ , and  $0 \leq z \leq 38 \text{ m}$  was discretized into a rectangular grid comprised of 10560 elements and 12144 nodes (Figure 9.27). Nodal spacings were made relatively small in regions near the disposal site and near the pumping well where the highest head gradients and flow velocities were expected. The variably saturated flow problem was solved using HYDRUS assuming an iteration head tolerance of 0.01 m and a water content tolerance of 0.0001.

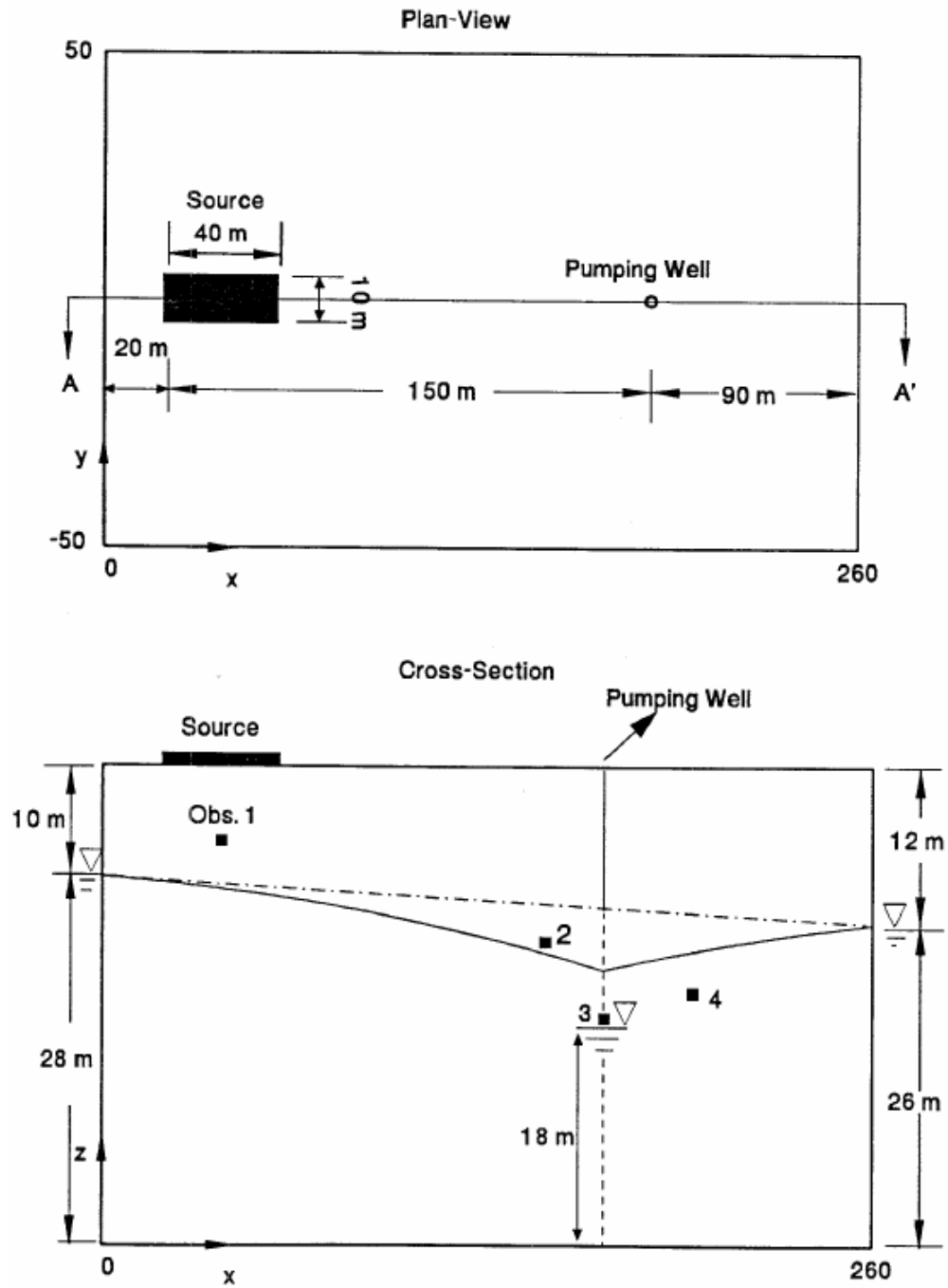


Figure 9.26. Geometry and boundary conditions for example 8 simulating three-dimensional flow and contaminant transport in a pumped variably-saturated aquifer.

Table 9.8. Input parameters for example 8.

<i>Hydraulic Parameters</i>		<i>Transport Parameters</i>	
$\theta_s = \theta_m = \theta_k$	0.450	$\rho$ [kg/m <sup>3</sup> ]	1400
$\theta_r = \theta_a$	0.05	$D_d$ [m <sup>2</sup> /day]	0.01
$K_s = K_k$ [m/day]	5.0	$D_L$ [m]	1.0
$\alpha$ [1/m]	4.1	$D_T$ [m]	0.25
$n$ [-]	2.0	$k$ [m <sup>3</sup> /kg]	0.0
		$\mu_w$ [1/day]	0.0
		$\mu_s$ [1/day]	0.0
		$\gamma_w$ [1/day]	0.0
		$\gamma_s$ [1/day]	0.0
		$c_0$	1.0

Computed water table elevations are plotted in Figure 9.28a and 9.28b along longitudinal ( $y=0$ ) and transverse ( $x=170$  m) planes through the pumping well, respectively. The results show a relatively strong direct interaction between the infiltrating water and the saturated zone after only a short period of time; water flow reached approximately steady state about 1.5 days after the experiment started. The velocity field and streamlines in a longitudinal section through the pumping well are presented in Figure 9.29. Note that the length of the seepage face along the well was determined to be approximately 5 meters. The calculated well discharge rate for the fixed water table ( $z = 18$  m) was calculated to be 39.6 m<sup>3</sup>/day. A concentration contour plot ( $c = 0.1$ ) is presented in Figure 9.30. This figure shows that contaminant transport was strongly affected by well pumping. Note that although the contaminant source was located 10 m above the initial groundwater table, and 150 m upgradient of the pumping well, the solute reached the pumping well after only 200 days of pumping. Figure 9.31 gives a two-dimensional view of calculated concentration distributions at several times in a horizontal plane ( $z = 20$  m).

Finally, Figure 9.32 presents solute breakthrough curves observed at observation node 1

( $x = 40$  m,  $z = 32$  m), node 2 ( $x = 150$  m,  $z = 24$  m), node 3 ( $x = 170$  m,  $z = 18$  m), and node 4 ( $x = 200$  m,  $z = 20$  m). These observation nodes are all on a vertical cross-section ( $y = 0$ ) as shown in Figure 9.26b. Notice that the breakthrough curves differ considerably in shape and especially peak concentrations. Although the breakthrough curve at observation node 1 immediately below the disposal site was very steep, no numerical oscillations were observed here. This shows that HYDRUS is able to solve the present solute transport problem involving sharp concentration distributions without generating non-physical oscillations. However, the efficiency of the numerical simulation for this example was limited by the need for relatively small time steps so as to satisfy the grid Courant criterion (Section 6.3.6). Although water flow had reached approximately steady-state within less than 2 days, the time step for the solute transport problem was only 0.073 day because of relatively large flow velocities near the well.

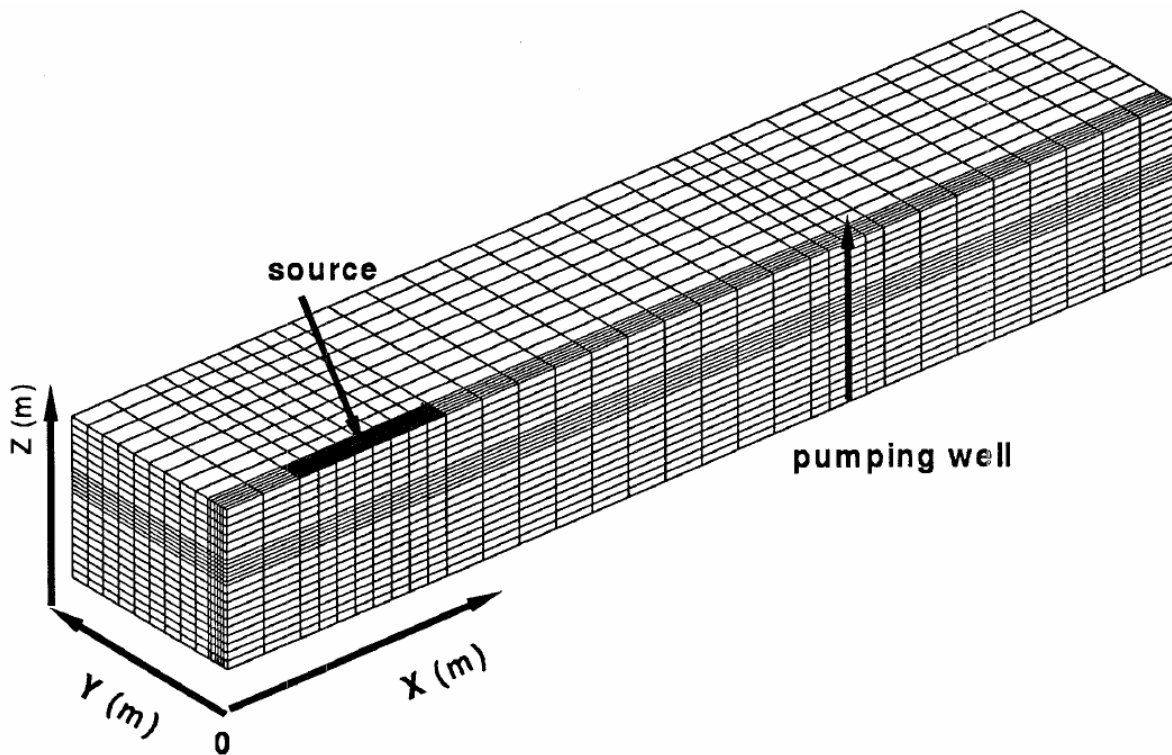


Figure 9.27. Finite element mesh for example 8.



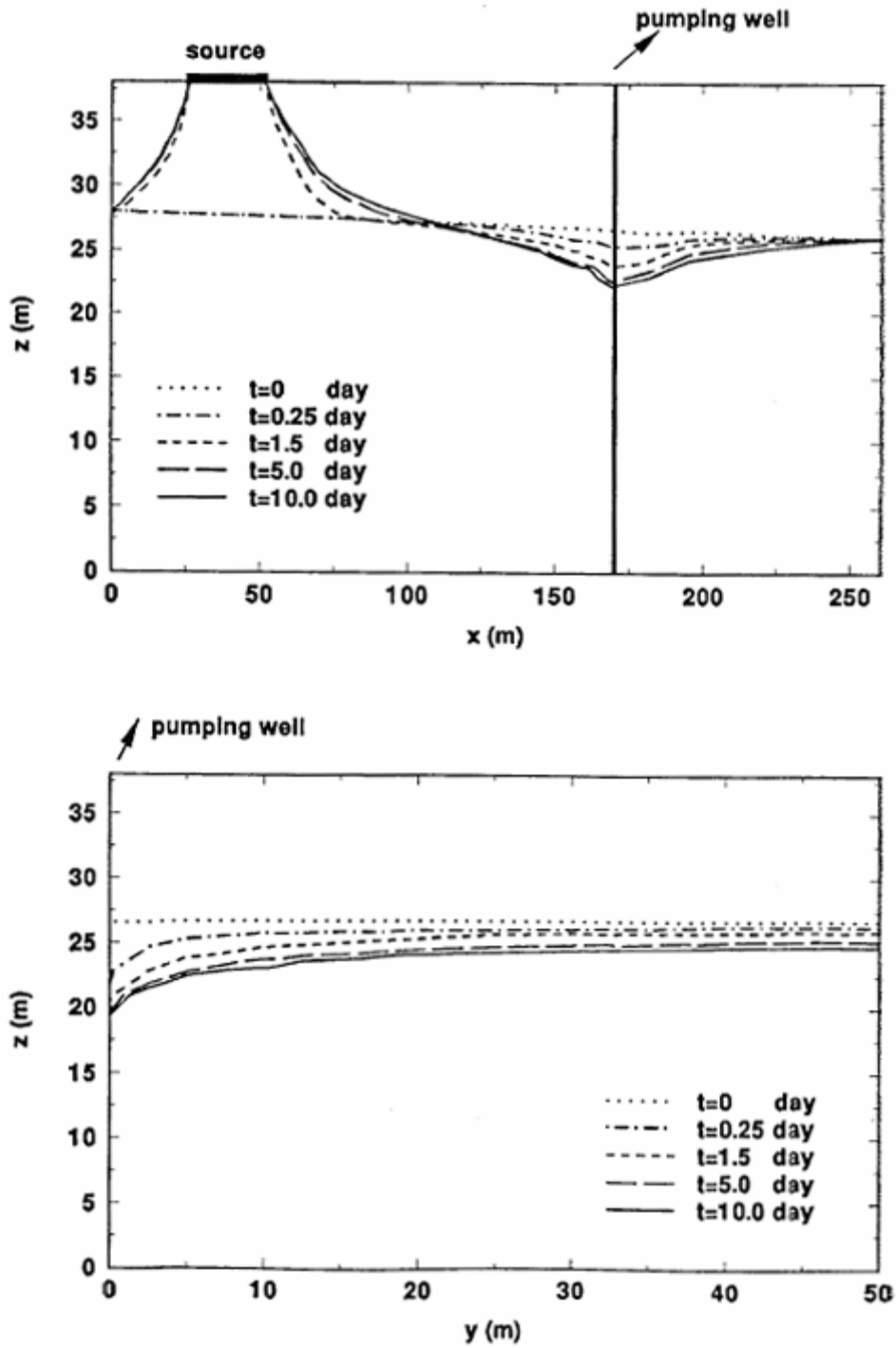


Figure 9.28. Calculated (a) longitudinal ( $y=0$ ) and (b) transverse ( $x=170$  m) elevations of the groundwater table.



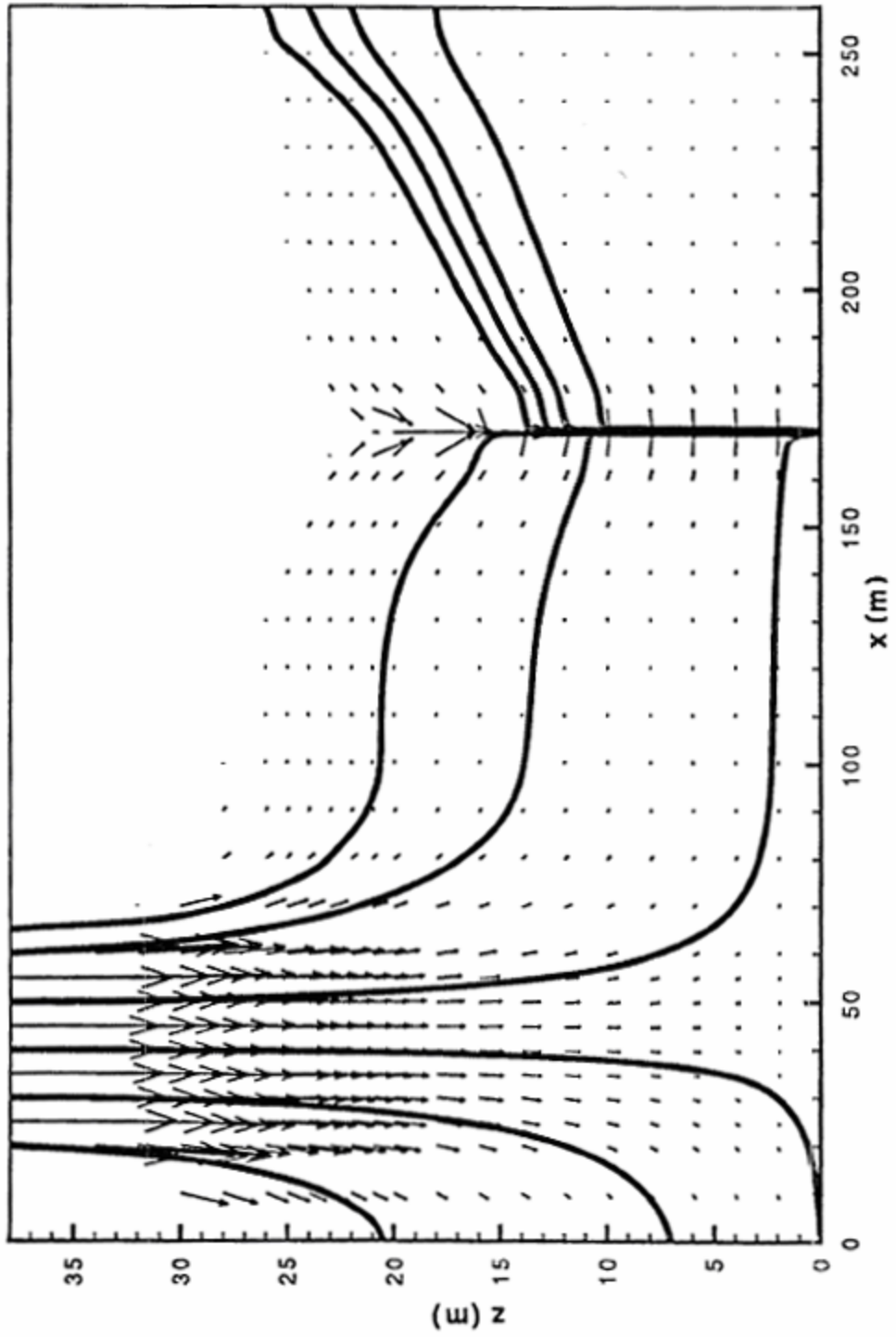


Figure 9.29. Computed velocity field and streamlines at  $t = 10$  days.

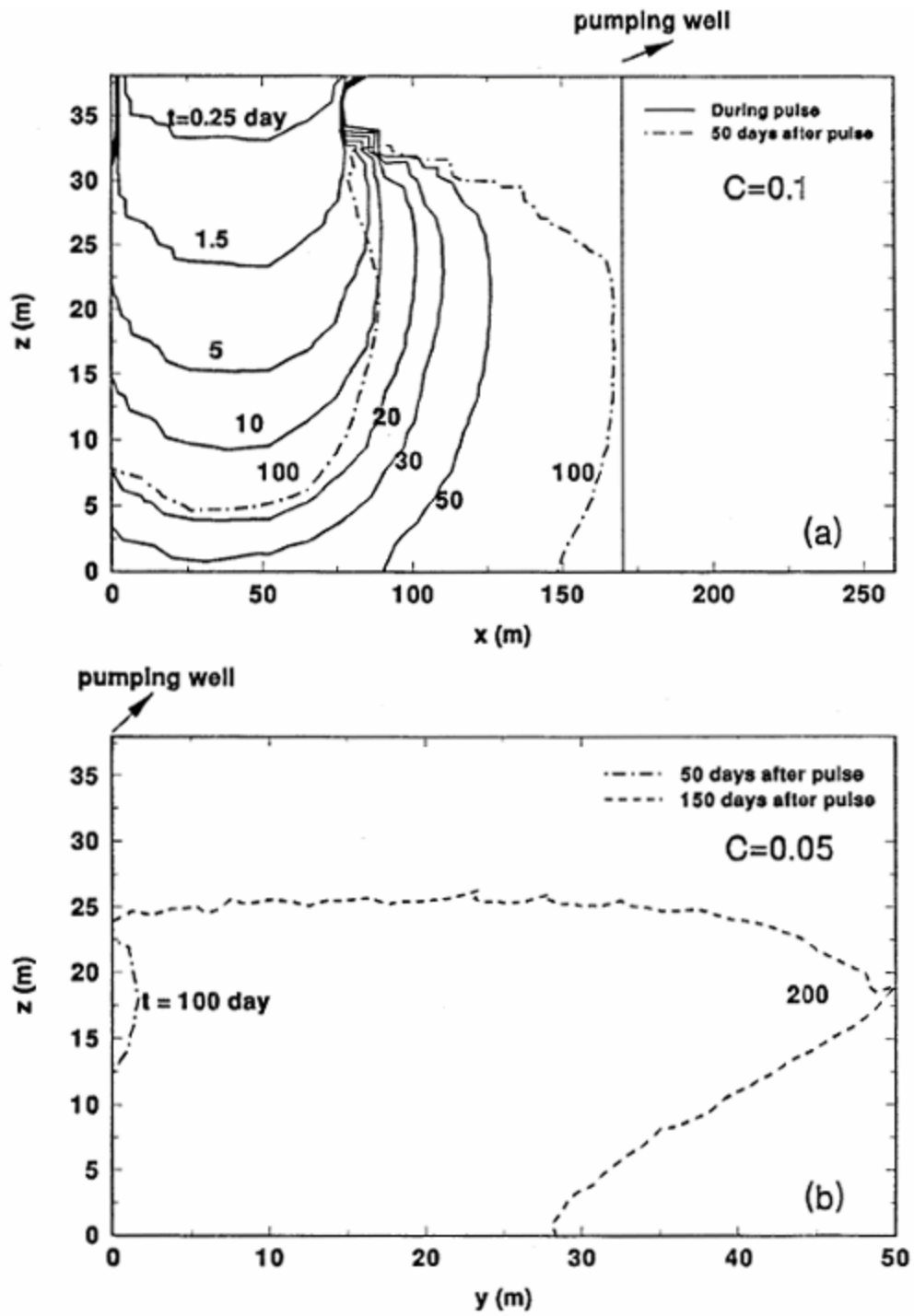


Figure 9.30. Concentration contour plots for (a)  $c=0.1$  in a longitudinal cross-section ( $y=0$ ), and (b)  $c=0.05$  in a transverse cross-section ( $x=170$  m).

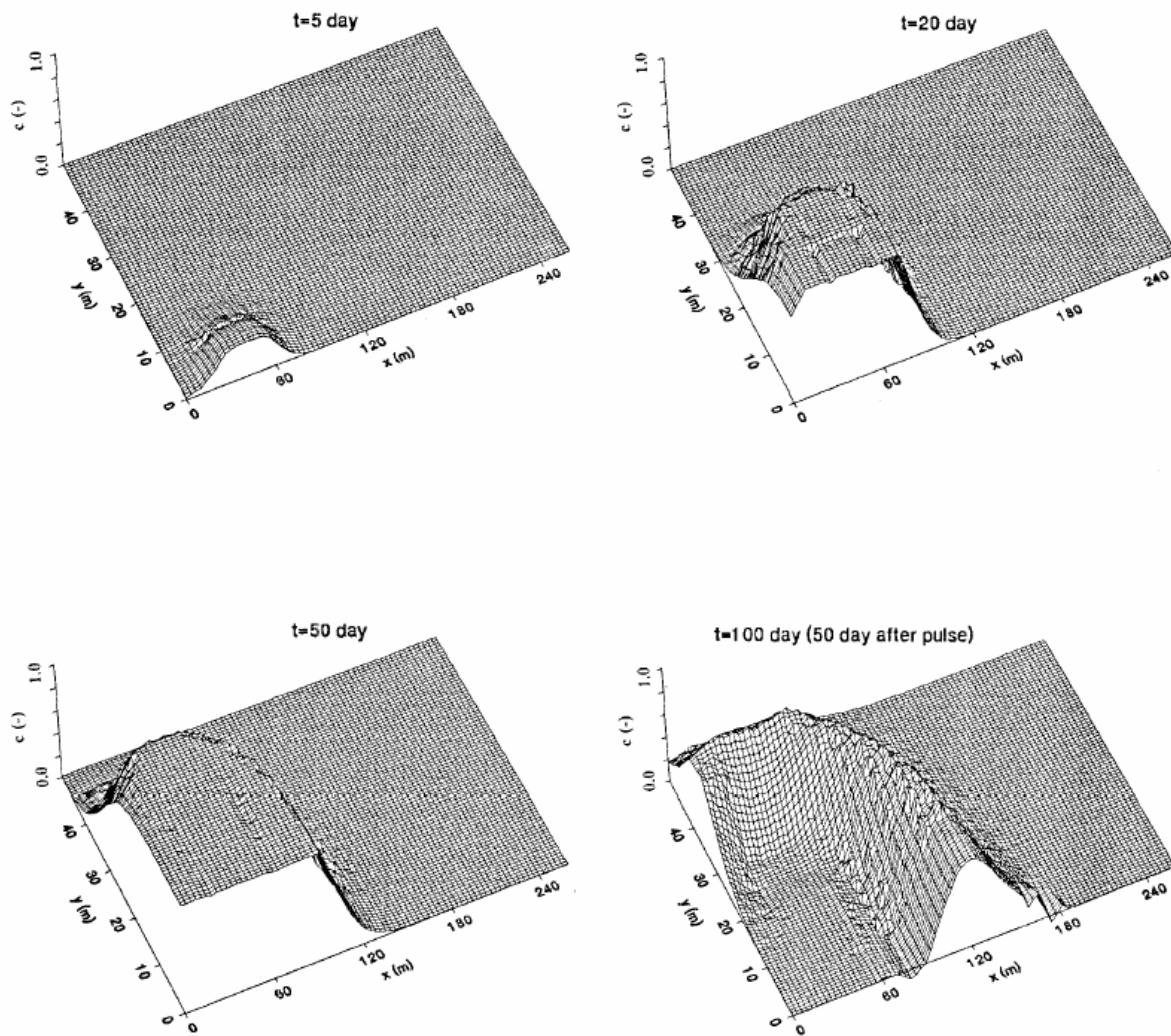


Figure 9.31. Concentration distributions in a horizontal plane located at  $z = 20$  m for  $t = 10, 50, 100,$  and  $200$  days.

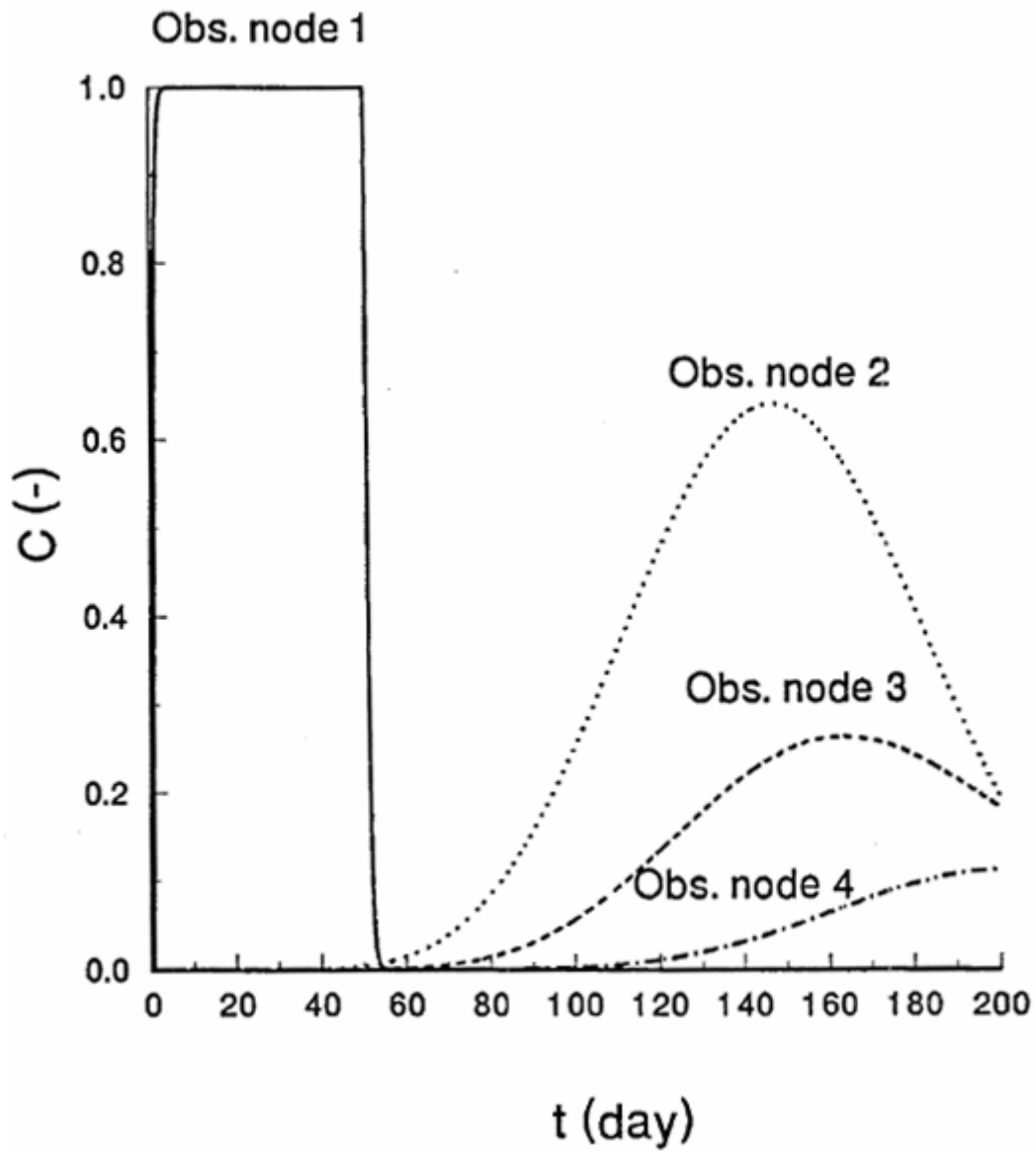


Figure 9.32. Breakthrough curves at observation node 1 ( $x = 40$  m,  $z = 32$  m), node 2 ( $x = 150$  m,  $z = 24$  m), node 3 ( $x = 170$  m,  $z = 18$  m), and node 4 ( $x = 200$  m,  $z = 20$  m).

## 9.2. Inverse Example Problems

In this section we discuss three methods recently proposed for estimating the soil hydraulic properties by numerical inversion of the Richards' equation. One method currently being developed involves the use of tension disc permeameter data [Šimůnek and van Genuchten, 1996, 1997] (example 9), while a second method uses data collected with a modified cone penetrometer [Gribb, 1996; Gribb et al., 1998] (example 10). The third method involves the use of a multiple extraction device [Inoue et al., 1998] (example 11). All these inverse problems are solved using 2D solver.

### 9.2.1. Example 9 - Tension Disc Infiltrometer

Šimůnek and van Genuchten [1997] suggested the use of multiple tension infiltration experiments in combination with knowledge of the initial and final water contents for estimating soil hydraulic properties. An evaluation of the numerical stability and parameter uniqueness using numerically generated data with superimposed stochastic and deterministic errors showed that a combination of the multiple cumulative tension infiltration data, a measured final water content, and an initial condition expressed in terms of the water content, provided the most promising parameter estimation approach for practical applications [Šimůnek and van Genuchten, 1997].

The experiment was used to estimate the soil hydraulic characteristics of a two-layered soil system involving a crusted soil in a Sahel region [Šimůnek et al., 1998]. Here we will report only results for the sandy subsoil. Data were obtained with a tension disc diameter of 25 cm and with supply tensions of 11.5, 9, 6, 3, 1, and 0.1 cm. Figure 9.33 shows measured and optimized cumulative infiltration curves and their differences. The small breaks in the cumulative infiltration curve (Fig. 9.33) were caused by brief removal of the infiltrometer from the soil surface to resupply it with water and to adjust the tension for a new time interval. Very close agreement between the measured and optimized cumulative infiltration curves was obtained; the largest deviations were generally less than 60 ml, which constituted only about 0.5% of the total infiltration volume. Figure 9.34 shows a comparison of the parameter estimation results against results obtained using Wooding's analysis. Both methods give almost identical unsaturated hydraulic conductivities for pressure heads between -2 and -10.25 cm. However, the hydraulic conductivity at the highest pressure head interval was overestimated by a factor of two using Wooding's analysis. Šimůnek et al. [1998] further compared the numerical inversion results with hydraulic properties estimated from available soil textural information using a neural-network-based pedotransfer function approach.

Relatively good agreement between the inverse and neural network predictions was obtained.

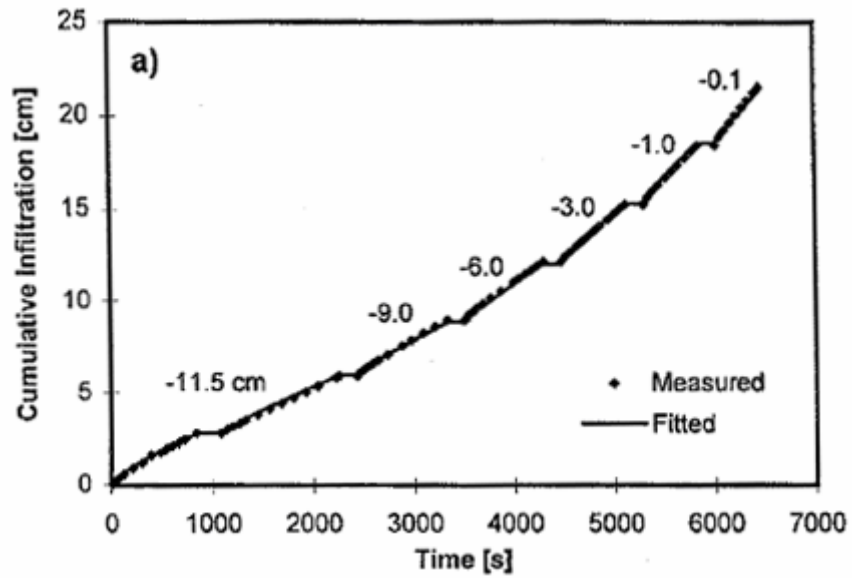


Figure 9.33. Measured and optimized cumulative infiltration curves for a tension disc infiltrometer experiment (example 9).

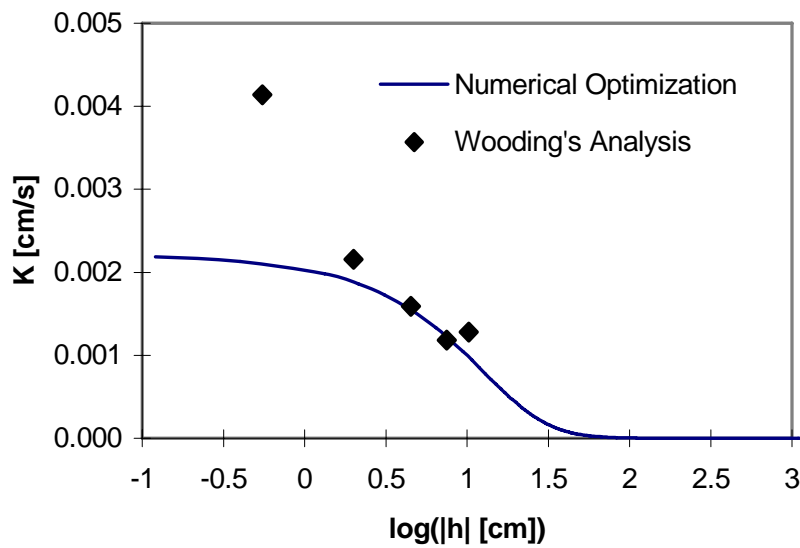


Figure 9.34. Unsaturated hydraulic conductivities at particular pressure heads, calculated using Wooding's analytical solution and the complete function obtained by numerical inversion (example 9).



### 9.2.2. Example 10 - Cone Penetrometer

While tension infiltrometer experiments provide relatively quick estimates of the hydraulic properties, they can be used only at the soil surface. By comparison, a new cone penetrometer method currently under development [Gribb, 1996; Gribb *et al.*, 1998; Kodešová *et al.*, 1998] can be used at depth. Cone penetrometers were originally used to obtain soil strength characteristics by measuring the tip resistance and sleeve friction during penetration at a constant rate. To obtain the hydraulic properties, a modified cone penetrometer, instrumented with a porous filter close to the penetrometer tip and two tensiometer rings 5 and 9 cm above the filter, is used (Fig. 9.35). The device is pushed into a soil to the desired depth, and a constant head is applied to the 5-cm filter. The volume of water imbibed into the soil is monitored, as are tensiometer ring readings registering the advancement of the wetting front for a short period of time (300-500 s).

Gribb [1996] gave a detailed numerical analysis of this experiment, including a study of the identifiability of the soil hydraulic parameters. She showed that the inverse solution was least sensitive to  $n$  and  $\theta_s$ , and most sensitive to  $K_s$  and  $\alpha$ . The method was recently used to estimate the hydraulic parameters of a sandy soil in a laboratory aquifer system measuring 5 x 5 x 3 m [Gribb *et al.*, 1998; Kodešová *et al.*, 1998; Šimůnek *et al.*, 1999].

Figure 9.36 shows observed flow data, as well as results of the numerical inversion. Excellent agreement between measured and optimized values was obtained for the inverse solution with four optimized parameters. Gribb *et al.* [1998] and Kodešová *et al.* [1998] presented retention curves obtained with selected laboratory methods and the parameter estimation technique. The optimized curves were close to wetting curves determined in the laboratory. Gribb *et al.* [1998] showed that the estimated saturated hydraulic conductivities were similar to those obtained with other test methods, such as the Guelph permeameter, slug tests, and laboratory constant head tests. Finally, Šimůnek *et al.* [1999] further used the redistribution part of the experiment to also estimate hysteresis in the soil water retention curve.

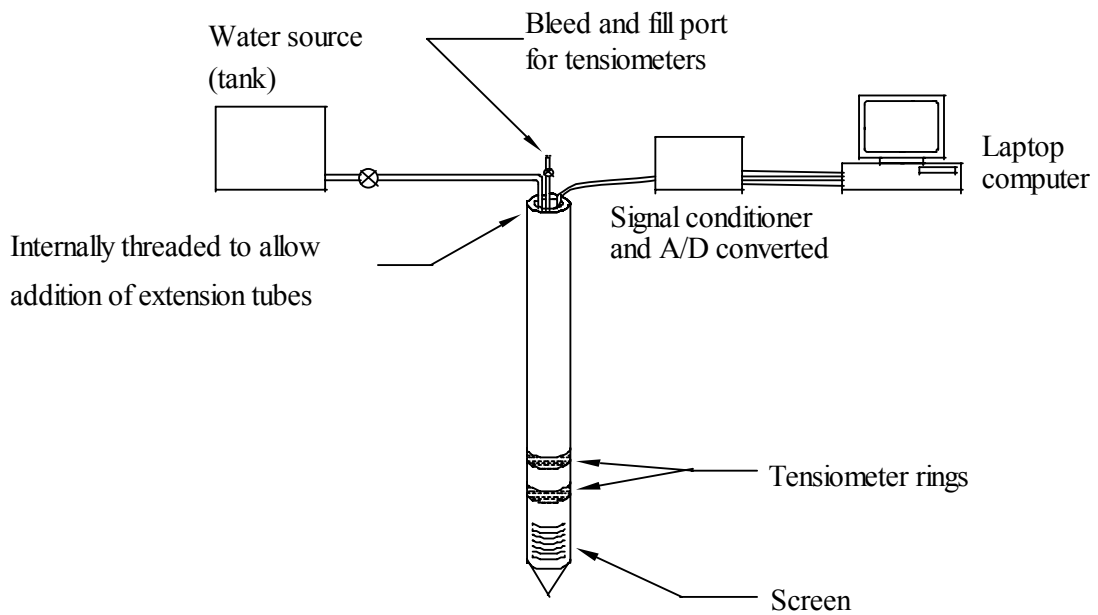


Figure 9.35. Schematic of the modified cone penetrometer (example 10).

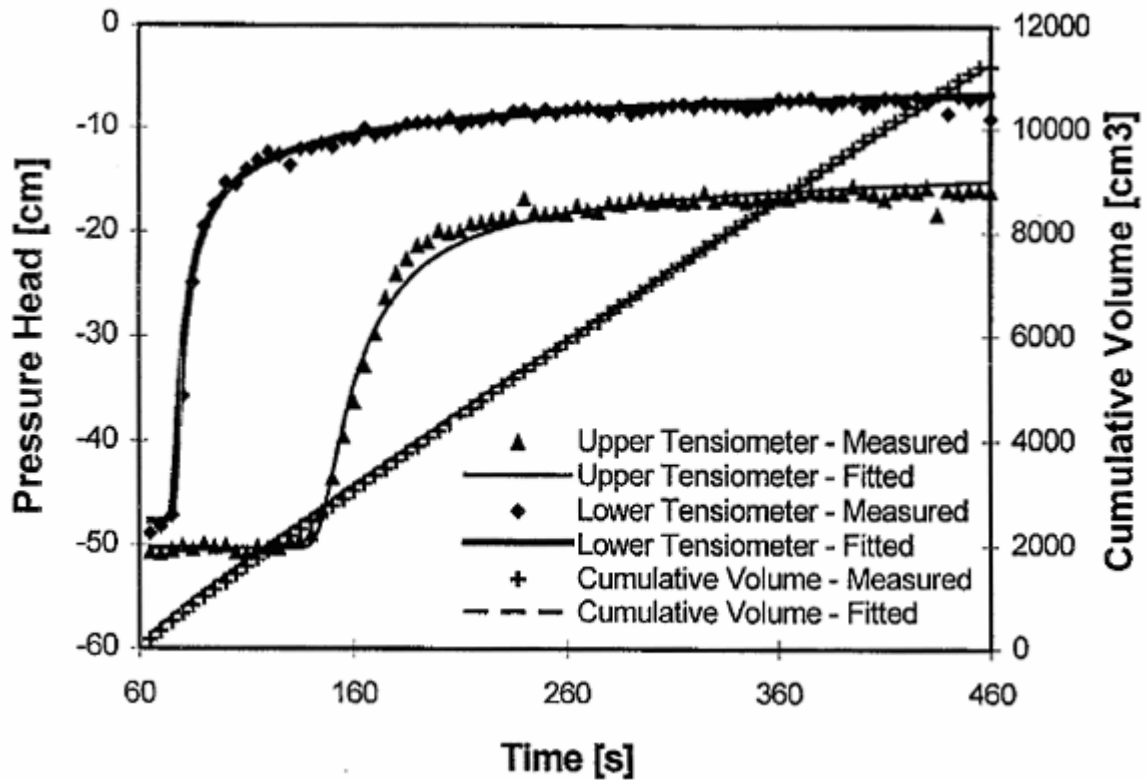


Figure 9.36. Comparison of observed and optimized cumulative infiltration curves and tensiometer readings for the modified cone penetrometer test (example 10).

### 9.2.3. Example 11 - Multiple-Step Extraction Experiment

The tension infiltrometer and cone penetrometer methods provide information about the wetting branches of the soil hydraulic properties. By comparison, a multiple step extraction device can be used to obtain draining branches. The device consists of a ceramic soil solution sampler (Fig. 9.37), which is inserted into an initially wet soil profile and subjected to a series of vacuum extraction pressures. The cumulative amount of soil solution extracted during an experiment, as well as pressure heads at various locations near the extraction device, are monitored during the experiment and subsequently used in an objective function for the nonlinear minimization problem. *Inoue et al.* [1998] first evaluated the feasibility of the vacuum extraction technique using numerically generated data, and concluded that the method is well suited for loamy-textured soils, but not necessarily for sandy soils. They tested the method in the laboratory and in the field. Here we briefly discuss one laboratory application.

The experiment [*Inoue et al.*, 1998] was carried out on a Columbia fine sandy loam. The center of the ceramic ring (with a radius of 3 cm, and a length of 3 cm) was located 6.3 cm below the soil surface. The tensiometers were installed at the following positions:  $T_1(r,z)=(4,-6.3)$  cm,  $T_2=(6,-6.3)$ ,  $T_3=(6,-24)$ . Five vacuum extraction steps were applied:  $h_{ex}=-35$  cm for 25 h,  $h_{ex}=-65$  cm for  $25 < t < 73$  h,  $h_{ex}=-125$  cm for  $73 < t < 217$  h,  $h_{ex}=-240$  cm for  $217 < t < 339$  h, and finally  $h_{ex}=-480$  cm for  $339 < t < 605$  h. Experimental data, as well as the final results of the numerical inversion, are presented in Figure 9.38. The saturated hydraulic conductivity of the ceramic ring was optimized simultaneously with van Genuchten's hydraulic parameters. Agreement between measured and calculated values in Figure 9.38 was relatively good. *Inoue et al.* [1998] compared the optimized soil hydraulic functions with independently measured data.

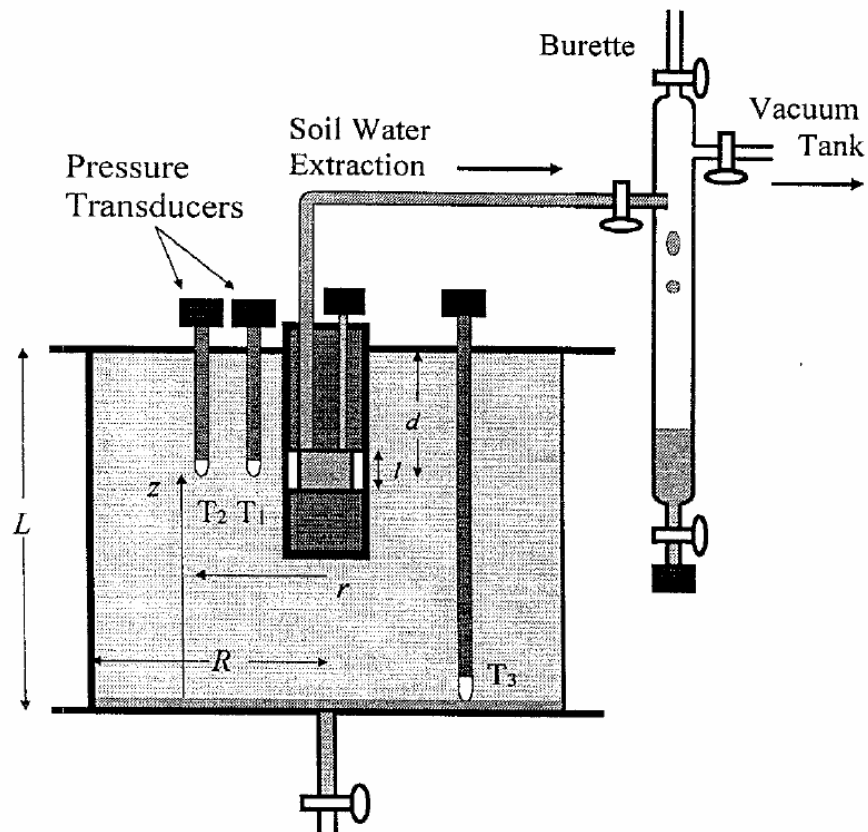


Figure 9.37. Layout of laboratory multistep extraction experiment (example 11).

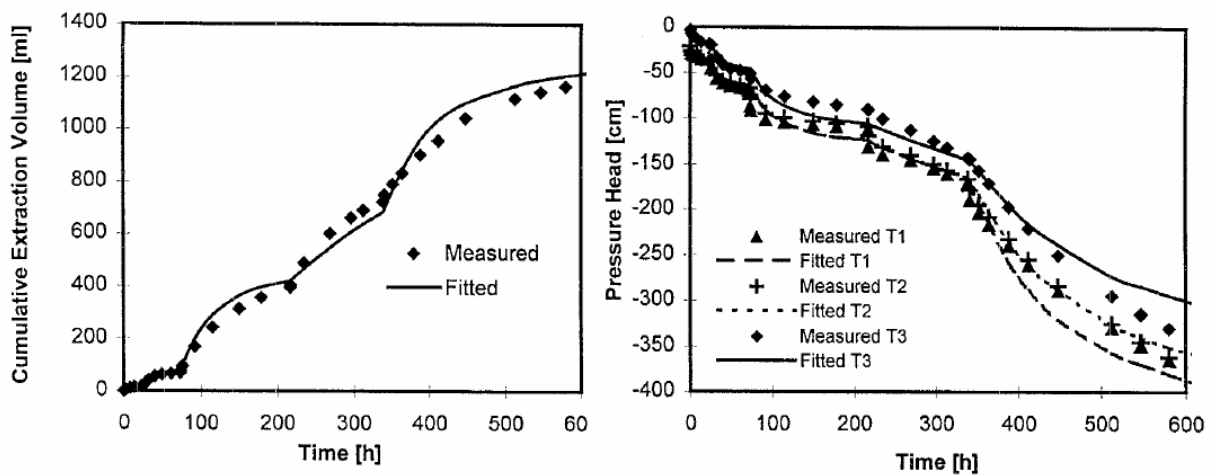


Figure 9.38. Comparison of measured (symbols) and optimized (lines) cumulative extraction (a) and pressure head (b) values (example 11).

## 10. INPUT DATA

The input data for HYDRUS are given in seven separate input files. These input files consist of one or more input blocks identified by the letters from A through M. The input files and blocks must be arranged as follows:

### SELECTOR.IN

- A. Basic Information
- B. Material Information
- C. Time Information
- D. Solute Transport Information
- E. Heat Transport Information
- F. Root Water Uptake Information

### MESHTRIA.TXT

- G. Finite Element Mesh Information

### DOMAIN.DAT

- H. Nodal Information
- I. Element Information

### BOUNDARY.IN

- J. Boundary Information

### ATMOSPH.IN

- K. Atmospheric Information

### DIMENSIO.IN

- L. Dimension Information

### FIT.IN

- M. Inverse Solution Information

The various input blocks are described in detail below. Tables 10.1 through 10.13 describe the data required for each input block. All data are read in using list-directed formatting (free format). Comment lines are provided at the beginning of, and within, each input block to facilitate, among other things, proper identification of the function of the block and the input variables. The comment lines are ignored during program execution; hence, they may be left blank but should not be omitted. All input files must be placed into one subdirectory. Output files are printed into the same subdirectory. An additional file **Level\_01.dir**, which specifies the path to the input and output file subdirectory must be given in the same directory as the executable **HYDRUS** codes if numerical

solvers are to be run outside of the GUI. The program assumes that all input data are specified in a consistent set of units for mass M, length L, and time T. The values of temperature should be specified in degrees Celsius.

Most of the information in Tables 10.1 through 10.13 should be self-explanatory. Several input files can be alternatively entered using binary files, e.g. the DOMAIN.DAT file can be replaced with the binary DOMAIN.IN file, and the MESHTRIA.TXT file can be replaced with the MESHTRIA.000 (or MESHGEN2.PMG) binary file. Binary files are utilized by default when the HYDRUS user interface is used.

Table 10.1. Block A - Basic information.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Selector.in file; set equal to 3 for current version.
2,3	-	-	Comment lines.
4	Char	<i>Hed</i>	Heading.
5	-	-	Comment line.
6	Char	<i>LUnit</i>	Length unit (e.g., 'cm').
7	Char	<i>TUnit</i>	Time unit (e.g., 'min').
8	Char	<i>MUnit</i>	Mass unit for concentration (e.g., 'g', 'mol', '-').
9	-	-	Comment line.
10	Integer	<i>Kat</i>	Type of flow system to be analyzed: 0 for a horizontal (areal) system 1 for axisymmetric flow 2 for vertical flow in a cross-section
			Records 9 and 10 are provided only for two-dimensional problems.
11	-	-	Comment line.
12	Integer	<i>MaxIt</i>	Maximum number of iterations allowed during any time step (usually 10).
12	Real	<i>TolTh</i>	Absolute water content tolerance for nodes in the unsaturated part of the flow region [-] (its recommended value is 0.001). <i>TolTh</i> represents the maximum desired absolute change in the value of the water content, $\theta$ , between two successive iterations during a particular time step.
12	Real	<i>TolH</i>	Absolute pressure head tolerance for nodes in the saturated part of the flow region [L] (its recommended value is 1 cm). <i>TolH</i> represents the maximum desired absolute change in the value of the pressure head, $h$ , between two successive iterations during a particular time step.
12	Logical	<i>lUnitW</i>	Set this logical variable equal to <b>.true.</b> when the initial condition is specified in terms of the pressure head. Set this logical variable equal to <b>.false.</b> when the initial condition is specified in terms of the water content.
13	-	-	Comment line.
14	Logical	<i>lWat</i>	Set this logical variable equal to <b>.true.</b> when transient water flow is considered. Set this logical variable equal to <b>.false.</b> when steady-state water flow is to be calculated.
14	Logical	<i>lChem</i>	Set this logical variable equal to <b>.true.</b> if solute transport is to be considered.
14	Logical	<i>SinkF</i>	Set this variable equal to <b>.true.</b> if water extraction from the root zone is imposed.

Table 10.1. (continued)

Record	Type	Variable	Description
14	Logical	<i>ShortF</i>	<b>.true.</b> if information is to be printed only at preselected times, but not at each time step (T-level information, see Section 11.1), <b>.false.</b> if information is to be printed at each time step or at each <i>n</i> -time steps.
14	Logical	<i>lPrint</i>	Set this logical variable equal to <b>.true.</b> if information about the pressure heads, water contents, temperatures, and concentrations in observation nodes, and the water and solute fluxes is to be printed at a constant time interval <i>tPrintInterval</i> .
14	Logical	<i>lScreen</i>	Set this logical variable equal to <b>.true.</b> if information is to be printed on the screen during code execution.
14	Logical	<i>AtmInf</i>	<b>.true.</b> if atmospheric boundary conditions are supplied via the input file ATMOSPH.IN, <b>.false.</b> if the file ATMOSPH.IN is not provided (i.e., in case of time independent boundary conditions).
14	Logical	<i>lTemp</i>	Set this logical variable equal to <b>.true.</b> if heat transport is to be considered.
14	Logical	<i>lWDep</i>	<b>.true.</b> if hydraulic properties are to be considered as temperature dependent. <b>.false.</b> otherwise (see Section 2.5).
14	Logical	<i>lEquil</i>	<b>.true.</b> if equilibrium solute transport is considered. <b>.false.</b> if nonequilibrium solute transport is considered for at least one solute species.
14	Logical	<i>lExter</i>	Set this logical variable equal to <b>.true.</b> if an external mesh generator is to be used to generate the finite element mesh (i.e., when using MESHGEN-2D). Set this logical variable equal to <b>.false.</b> if an internal mesh generator for simple quadrilateral domains is to be used to generate the finite element mesh.
14	Logical	<i>lInv</i>	Set this logical variable equal to <b>.true.</b> if the soil hydraulic or solute transport parameters are to be estimated from measured data (available only for 2D applications). Set this logical variable equal to <b>.false.</b> if only the direct solution for a particular problem is to be carried out.
15	-	-	Comment line.
16	Logical	<i>lEnter</i>	Set this logical variable equal to <b>.true.</b> if the Enter key is to be pressed at the end of simulation.
16	Logical	<i>lDummy</i>	Logical dummy variable (repeat 7 times).
17	-	-	Comment line.
17	Integer	<i>nPrintSteps</i>	Information to the screen and output files is not printed at each time step, but after each <i>nPrintSteps</i> .
17	Real	<i>tPrintInterval</i>	A constant time interval after which information about the pressure heads, water contents, temperatures, and concentrations in observation nodes, and the water and solute fluxes is to be printed.



Table 10.1. (continued)

Record	Type	Variable	Description
17	Logical	<i>lEnter</i>	Set this logical variable equal to <b>.true.</b> if the Enter key is to be pressed at the end of simulation.

Table 10.2. Block B - Material information.

Record	Type	Variable	Description
1,2	-	-	Comment lines.
3	Integer	<i>NMat</i>	Number of soil materials. Materials are identified by the material number, <i>MatNum</i> , specified in Block H.
3	Integer	<i>N Lay</i>	Number of subregions for which separate water balances are being computed. Subregions are identified by the subregion number, <i>LayNum</i> , specified in Block I.
3	Real	<i>ha</i>	Absolute value of the upper limit [L] of the pressure head interval below which a table of hydraulic properties will be generated internally for each material ( <i>h<sub>a</sub></i> must be greater than 0.0; e.g. 0.001 cm) (see Section 5.3.11).
3	Real	<i>hb</i>	Absolute value of the lower limit [L] of the pressure head interval for which a table of hydraulic properties will be generated internally for each material (e.g. 1000 m). One may assign to <i>h<sub>b</sub></i> the highest (absolute) expected pressure head to be expected during a simulation. If the absolute value of the pressure head during program execution lies outside of the interval [ <i>h<sub>a</sub></i> , <i>h<sub>b</sub></i> ], then appropriate values for the hydraulic properties are computed directly from the hydraulic functions (i.e., without interpolation in the table). Zero values for both <i>h<sub>a</sub></i> and <i>h<sub>b</sub></i> should be specified when interpolation tables are not to be used.
3	Integer	<i>NAniz</i>	Number of anisotropy tensors used in the transport domain (minimum number is 1). This value needs to be provided only for three-dimensional applications.
4	-	-	Comment line.
5	Integer	<i>iModel</i>	Soil hydraulic properties model: = 0; <i>van Genuchten's</i> [1980] model with six parameters. = 1; modified <i>van Genuchten's</i> model with ten parameters, <i>Vogel and Císlarová</i> [1988]. = 2; <i>Brooks and Corey's</i> [1964] model with six parameters. = 3; <i>van Genuchten's</i> [1980] model with air-entry value of -2 cm and with six parameters. = 4; <i>Kosugi's</i> [1996] model with six parameters. = 5; dual porosity model of <i>Durner</i> [1994] with nine parameters. = 6; dual-porosity system with transfer proportional to the effective saturation (9 parameters) (see Sections 2.1.2 and 2.8). = 7; dual-porosity system with transfer proportional to the pressure head (11 parameters) (see Sections 2.1.2 and 2.8).
5	Integer	<i>iHyst</i>	Hysteresis in the soil hydraulic properties: = 0; No hysteresis = 1; Hysteresis in the retention curve only = 2; Hysteresis in both the retention and hydraulic conductivity functions = 3; Hysteresis using <i>Bob Lenhard's</i> model [ <i>Lenhard et al.</i> , 1991; <i>Lenhard and Parker</i> , 1992].
6	-	-	Comment line.

Table 10.2. (continued)

Record	Type	Variable	Description
7	Integer	$iKappa$	= -1 if the initial condition is to be calculated from the main drying branch. = 1 if the initial condition is to be calculated from the main wetting branch.  Records 6 and 7 are provided only when $iHyst > 0$ .
8	-	-	Comment line.
9	Real	$Par(1,M)$	Parameter $\theta_r$ for material $M$ [-].
9	Real	$Par(2,M)$	Parameter $\theta_s$ for material $M$ [-].
9	Real	$Par(3,M)$	Parameter $\alpha$ for material $M$ [ $L^{-1}$ ].
9	Real	$Par(4,M)$	Parameter $n$ for material $M$ [-].
9	Real	$Par(5,M)$	Parameter $K_s$ for material $M$ [ $LT^{-1}$ ].
9	Real	$Par(6,M)$	Parameter $l$ for material $M$ [-].
			The following four parameters are specified only when $iModel=1$ .
9	Real	$Par(7,M)$	Parameter $\theta_m$ for material $M$ [-].
9	Real	$Par(8,M)$	Parameter $\theta_a$ for material $M$ [-].
9	Real	$Par(9,M)$	Parameter $\theta_k$ for material $M$ [-].
9	Real	$Par(10,M)$	Parameter $K_k$ for material $M$ [ $LT^{-1}$ ].
			The following four parameters are specified only when $iModel=0$ and $iHyst>1$ .
9	Real	$Par(7,M)$	Parameter $\theta_m$ for material $M$ [-].
9	Real	$Par(8,M)$	Parameter $\theta_s^w$ for material $M$ [-].
9	Real	$Par(9,M)$	Parameter $\alpha^w$ for material $M$ [ $L^{-1}$ ].
9	Real	$Par(10,M)$	Parameter $K_s^w$ for material $M$ [ $LT^{-1}$ ].
			The following three parameters are specified only when $iModel=5$ [Durner, 1994].
9	Real	$Par(7,M)$	Parameter $w$ for material $M$ [-]. The weighting factor for the sub-curve for the second overlapping subregion.
9	Real	$Par(8,M)$	Parameter $\alpha$ for material $M$ [ $L^{-1}$ ] for the second overlapping subregion.
9	Real	$Par(9,M)$	Parameter $n$ for material $M$ [-] for the second overlapping subregion.
			The following four parameters are specified only when $iModel=6$ (dual-porosity system with transfer proportional to the water content gradient).
9	Real	$Par(7,M)$	Parameter $\theta_r^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(8,M)$	Parameter $\theta_s^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(9,M)$	Parameter $\omega$ (mass transfer coefficient in (2.60)) for material $M$ [-].
			The following four parameters are specified only when $iModel=7$ (dual-porosity system with transfer proportional to the pressure head gradient).
9	Real	$Par(7,M)$	Parameter $\theta_r^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(8,M)$	Parameter $\theta_s^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(9,M)$	Parameter $\alpha^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(10,M)$	Parameter $n^{im}$ for the immobile region of material $M$ [-].
9	Real	$Par(11,M)$	Parameter $K_a$ (mass transfer coefficient in (2.64)) for material $M$ [-].

Table 10.2. (continued)

Record	Type	Variable	Description
			Record 9 information is provided for each material $M$ (from 1 to $NMat$ ). If $IWDep=\mathbf{true}$ . (Block A) then the soil hydraulic parameters $Par(i,M)$ must be specified at reference temperature $T_{ref}=20^{\circ}\text{C}$ .
10	-	-	Comment line.
11	Real	$c11(i)$	First principal component, $K_1^A$ , of the first dimensionless tensor $\mathbf{K}^A$ which describes the local anisotropy of the hydraulic conductivity.
11	Real	$c22(i)$	Second principal component, $K_2^A$ .
11	Real	$c33(i)$	Third principal component, $K_3^A$ .
11	Real	$a11(i)$	Cosines of the angle between $K_1^A$ and the $x$ -coordinate axis.
11	Real	$a22(i)$	Cosines of the angle between $K_2^A$ and the $y$ -coordinate axis.
11	Real	$a33(i)$	Cosines of the angle between $K_3^A$ and the $z$ -coordinate axis.
11	Real	$a12(i)$	Cosines of the angle between $K_1^A$ and the $y$ -coordinate axis.
11	Real	$a13(i)$	Cosines of the angle between $K_1^A$ and the $z$ -coordinate axis.
11	Real	$a23(i)$	Cosines of the angle between $K_2^A$ and the $z$ -coordinate axis.
			Record 11 information is provided for each anisotropy tensor ( $i$ from 1 to $NAniz$ ).
			Records 10 and 11 are provided only for three-dimensional problems.

Table 10.3. Block C - Time information.

Record	Type	Variable	Description
1,2	-	-	Comment lines.
3	Real	<i>dt</i>	Initial time increment, $\Delta t$ [T]. Initial time step should be estimated in dependence on the problem being solved. For problems with high pressure gradients (e.g. infiltration into an initially dry soil), $\Delta t$ should be relatively small.
3	Real	<i>dtMin</i>	Minimum permitted time increment, $\Delta t_{min}$ [T].
3	Real	<i>dtMax</i>	Maximum permitted time increment, $\Delta t_{max}$ [T].
3	Real	<i>dMul</i>	If the number of required iterations at a particular time step is less than or equal to <i>ItMin</i> , then $\Delta t$ for the next time step is multiplied by a dimensionless number $dMul \geq 1.0$ (its value is recommended not to exceed 1.3).
3	Real	<i>dMul2</i>	If the number of required iterations at a particular time step is greater than or equal to <i>ItMax</i> , then $\Delta t$ for the next time step is multiplied by $dMul2 \leq 1.0$ (e.g. 0.33).
3	Integer	<i>ItMin</i>	If the number of required iterations at a particular time step is less than or equal to <i>ItMin</i> , then $\Delta t$ for the next time step is multiplied by a dimensionless number $dMul \geq 1.0$ (its value is recommended not to exceed 1.3).
3	Integer	<i>ItMax</i>	If the number of required iterations at a particular time step is greater than or equal to <i>ItMax</i> , then $\Delta t$ for the next time step is multiplied by $dMul2 \leq 1.0$ (e.g. 0.33).
3	Integer	<i>MPL</i>	Number of specified print-times at which detailed information about the pressure head, water content, flux, temperature, concentrations, and the water and solute balances will be printed.
4	-	-	Comment line.
5	Real	<i>tInit</i>	Initial time of the simulation [T].
5	Real	<i>tMax</i>	Final time of the simulation [T].
6	-	-	Comment line.
7	Real	<i>TPrint(1)</i>	First specified print-time [T].
7	Real	<i>TPrint(2)</i>	Second specified print-time [T].
.	.	.	.
.	.	.	.
7	Real	<i>TPrint(MPL)</i>	Last specified print-time [T]. (Maximum six values on one line.)

Table 10.4. Block D - Solute transport information.<sup>+</sup>

Record	Type	Variable	Description
1,2	-	-	Comment lines.
3	Real	<i>Epsi</i>	Temporal weighing coefficient. =0.0 for an explicit scheme. =0.5 for a Crank-Nicholson implicit scheme. =1.0 for a fully implicit scheme.
3	Logical	<i>IUpW</i>	<b>.true.</b> if upstream weighing formulation is to be used. <b>.false.</b> if the original Galerkin formulation is to be used.
3	Logical	<i>lArtD</i>	<b>.true.</b> if artificial dispersion is to be added in order to fulfill the stability criterion <i>PeCr</i> (see Section 6.4.6). <b>.false.</b> otherwise.
3	Logical	<i>ITDep</i>	<b>.true.</b> if at least one transport or reaction coefficient ( <i>ChPar</i> ) is temperature dependent. <b>.false.</b> otherwise. If <i>ITDep</i> = <b>.true.</b> , then all values of <i>ChPar</i> ( <i>i,M</i> ) should be specified at a reference temperature $T_r=20^{\circ}\text{C}$ .
3	Real	<i>cTola</i>	Absolute concentration tolerance [ $\text{ML}^{-3}$ ], the value is dependent on the units used (set equal to zero if nonlinear adsorption is not considered).
3	Real	<i>cTolR</i>	Relative concentration tolerance [-] (set equal to zero if nonlinear adsorption is not considered).
3	Integer	<i>MaxItC</i>	Maximum number of iterations allowed during any time step for solute transport - usually 10 (set equal to zero if nonlinear adsorption is not considered).
3	Real	<i>PeCr</i>	Stability criteria (see Section 6.4.6). Set equal to zero when <i>IUpW</i> is equal to <b>.true.</b> .
3	Integer	<i>NS</i>	Number of solutes in a chain reaction.
3	Logical	<i>ITort</i>	<b>.true.</b> if the tortuosity factor [ <i>Millington and Quirk</i> , 1961] is to be used. <b>.false.</b> if the tortuosity factor is assumed to be equal to one.
3	Integer	<i>lBacter</i>	Set equal to <b>.true.</b> if attachment/detachment approach is to be used to calculate nonequilibrium transport of viruses, colloids, or bacteria. Set equal to <b>.false.</b> if original formulations, i.e., physical nonequilibrium or two-site sorption is to be used to describe nonequilibrium solute transport.
3	Logical	<i>IFiltr</i>	Set this logical variable equal to <b>.true.</b> if the attachment coefficient is to be evaluated using the filtration theory (eq. (3.28)).
3	Integer	<i>nChPar</i>	Number of solute transport parameters specific for each solute.
4	-	-	Comment line.
5	Real	<i>ChPar</i> (1, <i>M</i> )	Bulk density of material <i>M</i> , $\rho$ [ $\text{ML}^{-3}$ ].
5	Real	<i>ChPar</i> (2, <i>M</i> )	Longitudinal dispersivity for material type <i>M</i> , $D_L$ [L].

Table 10.4. (continued)

Record	Type	Variable	Description
5	Real	$ChPar(3,M)$	Transverse dispersivity for material type $M$ , $D_T$ [L].
5	Real	$ChPar(4,M)$	Dimensionless fraction of the sorption sites classified as type-1, i.e., sites with instantaneous sorption, when the <b>chemical nonequilibrium</b> option is considered. Set equal to 1 if equilibrium transport is to be considered. Dimensionless fraction of the sorption sites in contact with mobile water when the <b>physical nonequilibrium</b> option is considered. Set equal to 1 if all sorption sites are in contact with mobile water.
5	Real	$ChPar(5,M)$	Immobile water content. Set equal to 0 when the <b>physical nonequilibrium</b> option is not considered.  Record 5 information is provided for each material $M$ (from 1 to $NMat$ ).
6	-	-	Comment line.
7	Real	$ChPar(6,M)$	Ionic or molecular diffusion coefficient in free water, $D_w$ [ $L^2T^{-1}$ ].
7	Real	$ChPar(7,M)$	Ionic or molecular diffusion coefficient in gas phase, $D_g$ [ $L^2T^{-1}$ ].
8	-	-	Comment line.
9	Real	$ChPar(8,M)$	Adsorption isotherm coefficient, $k_s$ , for material type $M$ [ $L^3M^{-1}$ ]. Set equal to zero if no adsorption is to be considered.
9	Real	$ChPar(9,M)$	Adsorption isotherm coefficient, $\eta$ , for material type $M$ [ $L^3M^{-1}$ ]. Set equal to zero if Langmuir adsorption isotherm is not to be considered.
9	Real	$ChPar(10,M)$	Adsorption isotherm coefficient, $\beta$ , for material type $M$ [-]. Set equal to one if Freundlich adsorption isotherm is not to be considered.
9	Real	$ChPar(11,M)$	Equilibrium distribution constant between liquid and gas phases, $k_g$ , material type $M$ [-].
9	Real	$ChPar(12,M)$	First-order rate constant for dissolved phase, $\mu_w$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(13,M)$	First-order rate constant for solid phase, $\mu_s$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(14,M)$	First-order rate constant for gas phase, $\mu_g$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(15,M)$	Rate constant, $\mu_w'$ , representing a first-order decay for the first solute and zero-order production for the second solute in the dissolved phase, material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(16,M)$	Same as above for the solid phase, $\mu_s'$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(17,M)$	Same as above for the gas phase, $\mu_g'$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(18,M)$	Zero-order rate constant for dissolved phase, $\gamma_w$ , material type $M$ [ $ML^{-3}T^{-1}$ ].
9	Real	$ChPar(19,M)$	Zero-order rate constant for solid phase, $\gamma_s$ , material type $M$ [ $T^{-1}$ ].
9	Real	$ChPar(20,M)$	Zero-order rate constant for gas phase, $\gamma_g$ , material type $M$ [ $ML^{-3}T^{-1}$ ].
9	Real	$ChPar(21,M)$	First-order rate coefficient for nonequilibrium adsorption, or the mass transfer coefficient for solute exchange between mobile and immobile liquid regions, $\omega$ , material type $M$ [ $T^{-1}$ ].  Parameters $ChPar(14,M)$ through $ChPar(21,M)$ are reinterpreted when the variable $iBacter=1$ .
9	Integer	$ChPar(14,M)$	Type of blocking, $iPsi$ , applied in (3.23) on the second sorption sites. = 0: No blocking. = 1: Langmuirian dynamics, (3.24).

Table 10.4. (continued)

Record	Type	Variable	Description
			= 2: Ripening, (3.25).
			= 3: random sequential adsorption model, (3.26).
			= 4: depth dependent blocking coefficient, (3.27).
9	Integer	<i>ChPar</i> (15, <i>M</i> )	ditto, for the first sorption sites.
9	Real	<i>ChPar</i> (16, <i>M</i> )	Parameter in the blocking function for the second sorption sites ( $s_{max}$ for (3.24), (3.25) and (3.26), $\beta$ in (3.27)).
9	Real	<i>ChPar</i> (17, <i>M</i> )	The first-order deposition (attachment) coefficient, $k_a$ [ $T^{-1}$ ], for the second sorption sites.
9	Real	<i>ChPar</i> (18, <i>M</i> )	The first-order entrainment (detachment) coefficient, $k_d$ [ $T^{-1}$ ], for the second sorption sites.
9	Real	<i>ChPar</i> (19, <i>M</i> )	Parameter in the blocking function for the first sorption sites.
9	Real	<i>ChPar</i> (20, <i>M</i> )	The first-order deposition (attachment) coefficient, $k_a$ [ $T^{-1}$ ], for the first sorption sites.
9	Real	<i>ChPar</i> (21, <i>M</i> )	The first-order entrainment (detachment) coefficient, $k_d$ [ $T^{-1}$ ], for the first sorption sites.
			Parameters <i>ChPar</i> (14, <i>M</i> ) through <i>ChPar</i> (21, <i>M</i> ) are further reinterpreted when the variable <i>iBacter</i> =1 and <i>IFilter</i> =true..
9	Integer	<i>ChPar</i> (14, <i>M</i> )	Diameter of the sand grains, $d_c$ [L].
9	Integer	<i>ChPar</i> (15, <i>M</i> )	Diameter of the particle, $d_p$ (e.g., virus, bacteria) (= 0.95 $\mu\text{m}$ = 0.95e-6 m) [L].
9	Real	<i>ChPar</i> (16, <i>M</i> )	Parameter $s_{max}$ in the blocking function for the second sorption sites (3.24).
9	Real	<i>ChPar</i> (17, <i>M</i> )	Sticking efficiency, $\alpha$ [-], for the second sorption sites.
9	Real	<i>ChPar</i> (18, <i>M</i> )	The first-order entrainment (detachment) coefficient, $k_d$ [ $T^{-1}$ ], for the second sorption sites.
9	Real	<i>ChPar</i> (19, <i>M</i> )	Parameter $s_{max}$ in the blocking function for the first sorption sites (3.24).
9	Real	<i>ChPar</i> (20, <i>M</i> )	Sticking efficiency, $\alpha$ [-], for the first sorption sites.
9	Real	<i>ChPar</i> (21, <i>M</i> )	The first-order entrainment (detachment) coefficient, $k_d$ [ $T^{-1}$ ], for the first sorption sites.
			Record 9 information is provided for each material <i>M</i> (from 1 to <i>NMat</i> ).
			Record 6 through 9 information are provided for each solute (from 1 to <i>NS</i> ).
10,11	-	-	Comment lines.
12	Real	<i>TDep</i> (6)	Activation energy for parameter <i>ChPar</i> (6, <i>M</i> ) [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ] (See Section 3.4). This parameter should be specified in $\text{J mol}^{-1}$ . Set equal to 0 if <i>ChPar</i> (6, <i>M</i> ) is temperature independent.
12	Real	<i>TDep</i> (7)	Same for parameter <i>ChPar</i> (7, <i>M</i> ) [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ].
13	-	-	Comment line.
14	Real	<i>TDep</i> (8)	Same for parameter <i>ChPar</i> (8, <i>M</i> ) [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ].
.	.	.	.
.	.	.	.
14	Real	<i>TDep</i> (21)	Same for parameter <i>ChPar</i> (21, <i>M</i> ) [ $\text{ML}^2\text{T}^{-2}\text{M}^{-1}$ ].



Table 10.4. (continued)

Record	Type	Variable	Description
			Records 11 through 14 information is provided only when the logical variable <i>ITDep</i> of record 3 is set equal to <b>.true.</b> .
15	-	-	Comment line.
16	Real	<i>cBound</i> (1,1)	Value of the concentration for the first time-independent BC [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=±1 is specified.
16	Real	<i>cBound</i> (1,2)	Value of the concentration for the second time-independent BC [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=±2 is specified.
.	.	.	.
16	Real	<i>cBound</i> (1,5)	Value of the concentration for the fifth time-independent BC [ML <sup>-3</sup> ]. If water uptake is specified, then <i>cBound</i> (1,5) is automatically used for the concentration of water removed from the flow region by root water uptake [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=±5 and no root solute uptake is specified.
16	Real	<i>cBound</i> (1,6)	Value of the concentration for the sixth time-independent BC [ML <sup>-3</sup> ]. If internal sources are specified, then <i>cBound</i> (1,6) is automatically used for the concentration of water injected into the flow region through internal sources [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=±6 and no internal sources are specified.
16	Real	<i>cBound</i> (1,7)	Concentration of the incoming fluid in equation (3.39) [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=-7 is specified.
16	Real	<i>cBound</i> (1,8)	Concentration above the stagnant boundary layer, <i>g<sub>am</sub></i> (see equation (3.39)) [ML <sup>-3</sup> ]. Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=-7 is specified.
16	Real	<i>cBound</i> (1,9)	Thickness of the stagnant boundary layer, <i>d</i> [L] (see equation (3.39)). Set equal to zero if no <i>KodCB</i> ( <i>n</i> )=-7 is specified.
			Record 16 information is provided for each solute (from 1 to <i>NS</i> ).
17	-	-	Comment line.
18	Real	<i>tPulse</i>	Time duration of the concentration pulse [T].

†Block D is not needed when the logical variable *IChem* in Block A is set equal to **.false.** .

Table 10.5. Block E - Heat transport information.<sup>+</sup>

Record	Type	Symbol	Description
1,2	-	-	Comment lines.
3	Real	$TPar(1,M)$	Volumetric solid phase fraction of material $M$ , $\theta_n$ [-].
3	Real	$TPar(2,M)$	Volumetric organic matter fraction of material $M$ , $\theta_o$ [-].
3	Real	$TPar(3,M)$	Longitudinal thermal dispersivity of material $M$ , $\lambda_L$ [L].
3	Real	$TPar(4,M)$	Transverse thermal dispersivity of material $M$ , $\lambda_T$ [L].
3	Real	$TPar(5,M)$	Coefficient $b_1$ in the thermal conductivity function [MLT <sup>-3</sup> K <sup>-1</sup> ] (e.g. Wm <sup>-1</sup> K <sup>-1</sup> ) (see equation (4.5)).
3	Real	$TPar(6,M)$	Coefficient $b_2$ in the thermal conductivity function [MLT <sup>-3</sup> K <sup>-1</sup> ] (e.g. Wm <sup>-1</sup> K <sup>-1</sup> ) (see equation (4.5)).
3	Real	$TPar(7,M)$	Coefficient $b_3$ in the thermal conductivity function [MLT <sup>-3</sup> K <sup>-1</sup> ] (e.g. Wm <sup>-1</sup> K <sup>-1</sup> ) (see equation (4.5)).
3	Real	$TPar(8,M)$	Volumetric heat capacity of solid phase of material $M$ , $C_n$ [ML <sup>-1</sup> T <sup>-2</sup> K <sup>-1</sup> ] (e.g. Jm <sup>-3</sup> K <sup>-1</sup> ).
3	Real	$TPar(9,M)$	Volumetric heat capacity of organic matter of material $M$ , $C_o$ [ML <sup>-1</sup> T <sup>-2</sup> K <sup>-1</sup> ] (e.g. Jm <sup>-3</sup> K <sup>-1</sup> ).
3	Real	$TPar(10,M)$	Volumetric heat capacity of liquid phase of material $M$ , $C_w$ [ML <sup>-1</sup> T <sup>-2</sup> K <sup>-1</sup> ] (e.g. Jm <sup>-3</sup> K <sup>-1</sup> ).
			Record 3 is required for each soil material $M$ (from 1 to $NMat$ ).
4	-	-	Comment line.
5	Real	$TBound(1)$	Value of the first time-independent thermal boundary condition [°C]. Set equal to zero if no $KodTB(n)=\pm 1$ is specified.
5	Integer	$TBound(2)$	Value of the second time-independent thermal boundary condition [°C]. Set equal to zero if no $KodTB(n)=\pm 2$ is specified.
.	.	.	.
.	.	.	.
5	Integer	$TBound(6)$	Value of the sixth time-independent thermal boundary condition [°C]. Set equal to zero if no $KodTB(n)=\pm 6$ is specified. If internal sources are specified, then $TBound(6)$ is automatically used for the temperature of water injected into the flow region through internal source.
6	-	-	Comment line.
7	Real	$Ampl$	Temperature amplitude at the soil surface [K] prescribed for nodes where $Kode(n)=\pm 4$ . Set equal to zero when no $Kode(n)=\pm 4$ is specified.
7	Real	$tPeriod$	Time interval for the completion of one temperature cycle (usually 1 day) [T].

<sup>+</sup> Block E need not be supplied if logical variables  $ITemp$  (Block A) is set equal to **false**.

Table 10.6. Block F - Root water uptake information.<sup>+</sup>

Record	Type	Variable	Description
1,2	-	-	Comment lines.
3	Integer	<i>iMoSink</i>	Type of root water uptake stress response function. = 0; <i>Feddes et al.</i> [1978] = 1; S-shaped, <i>van Genuchten</i> [1987]
3	Real	<i>OmegaC</i>	Critical root water uptake index. Set equal to zero for a noncompensated root water uptake and smaller than zero for compensated root water uptake [-].
4	-	-	Comment line.  The following records (records 5a, 6a, 7a) are given only if <i>iMoSink</i> =0.
5a	Real	<i>P0</i>	Value of the pressure head, $h_1$ (Fig. 2.1), below which roots start to extract water from the soil.
5a	Real	<i>P2H</i>	Value of the limiting pressure head, $h_3$ , below which the roots cannot extract water at the maximum rate (assuming a potential transpiration rate of $r2H$ ).
5a	Real	<i>P2L</i>	As above, but for a potential transpiration rate of $r2L$ .
5a	Real	<i>P3</i>	Value of the pressure head, $h_4$ , below which root water uptake ceases (usually equal to the wilting point).
5a	Real	<i>r2H</i>	Potential transpiration rate [ $LT^{-1}$ ] (currently set at 0.5 cm/day).
5a	Real	<i>r2L</i>	Potential transpiration rate [ $LT^{-1}$ ] (currently set at 0.1 cm/day). The above input parameters permit one to make the variable $h_3$ a function of the potential transpiration rate, $T_p$ ( $h_3$ presumably decreases at higher transpiration rates). HYDRUS currently implements the same linear interpolation scheme as used in several versions of the SWATRE code (e.g., <i>Wesseling and Brandyk</i> [1985]) and in the SWMS_2D [ <i>Šimůnek et al.</i> , 1992]. The scheme is based on the following interpolation: $h_3 = P2H + \frac{P2L - P2H}{r2H - r2L} (r2H - T_p) \quad \text{for } r2L < T_p < r2H$ $h_3 = P2L \quad \text{for } T_p \leq r2L$ $h_3 = P2H \quad \text{for } T_p \geq r2H$
6a	-	-	Comment line.
7a	Real	<i>POptm(1)</i>	Value of the pressure head, $h_2$ , below which roots start to extract water at the maximum possible rate (material number 1).
7a	Real	<i>POptm(2)</i>	As above (material number 2).
.	.	.	.
.	.	.	.
7a	Real	<i>POptm(NMat)</i>	As above (for material number <i>NMat</i> ).  The following record (record 5b) is given only if <i>iMoSink</i> =1.

Table 10.6. (continued)

Record	Type	Variable	Description
5b	Real	$P50$	Value of the pressure head, $h_{50}$ (Fig. 2.1), at which the root water uptake is reduced by 50%.
5b	Real	$P3$	Exponent $p$ in the S-shaped root water uptake stress response function. Recommended value is 3.
5b	Real	$PW$	Wilting point, i.e., the pressure head below which the root water uptake ceases. The following records are given only if $lChem=.true.$ .
8	-	-	Comment line.
9	Logical	$lSolRed$	<b>=.true.</b> : root water uptake is reduced due to salinity. <b>=.false.</b> : otherwise. The following records are given only if $lSolRed=.true.$ .
10	-	-	Comment line.
11	Logical	$lSolAdd$	<b>=.true.</b> if the effect of salinity stress is additive to the pressure head stress. <b>=.false.</b> if the effect of salinity stress is multiplicative to the pressure head stress.
12	-	-	Comment line. The following two values are specified when the root water uptake salinity stress response function is described with the S-shaped function (2.8) or (2.9), i.e., $lMsSink=.true.$ .
13a	Real	$c50$	Value of the osmotic head $h_{\phi 50}$ , at which the root water uptake is reduced by 50%. This value is specified only when $lSolAdd=.false.$ .
13a	Real	$P3c$	Exponent, $p$ , in the S-shaped root water uptake salinity stress response function. Recommended value is 3. This value is specified only when $lSolAdd=.false.$ . The following two values are specified when the root water uptake salinity stress response function is described with the threshold-slope function of <i>Maas</i> [1990], i.e., $lMsSink=.false.$ .
			$\alpha(h_\phi) = 1 \quad h_\phi^M \leq h_\phi < 0$ $\alpha(h_\phi) = \max[0, 1 - 0.01(h_\phi - h_\phi^M)_s] \quad h_\phi < h_\phi^M$
13a	Real	$c50$	Value of the minimum osmotic head (the salinity threshold) $h_\phi^M$ , above which root water uptake is not reduced. This value is specified only when $lSolAdd=.false.$ .

Table 10.6. (continued)

Record	Type	Variable	Description
13a	Real	$P3c$	Slope, $s_{\phi}$ , of the curve determining fractional root water uptake decline per unit increase in salinity below the threshold. This value is specified only when $lSolAdd=.false.$ .
13	Real	$aOsm(1)$	Osmotic coefficient, $a_1$ , for the first solute [ $L^4M^{-1}$ ].
13	Real	$aOsm(2)$	Osmotic coefficient, $a_2$ , for the second solute [ $L^4M^{-1}$ ].
.	.	.	.
13	Real	$aOsm(NSD)$	Osmotic coefficient, $a_n$ , for the last solute [ $L^4M^{-1}$ ].
13	Logical	$lMsSink$	= <b>.true.</b> : S-shaped root water uptake salinity stress response function. = <b>.false.</b> : threshold function according <i>Maas</i> [1990].

<sup>+</sup> Block F is not needed when the logical variable  $SinkF$  (Block A) is set equal to **.false.** .

Table 10.7a. Block G - Finite element mesh information for two-dimensional applications.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Meshtria.txt file; set equal to 1 for current version.
2	Integer	<i>iDummy</i>	Dummy variable. Set equal to 1.
2	Integer	<i>NumNP</i>	Number of nodal points.
2	Integer	<i>nEdges</i>	Number of mesh edges.
2	Integer	<i>NumEl</i>	Number of finite elements (only triangles are allowed).
3	Integer	<i>n</i>	Nodal number.
3	Real	<i>x(n)</i>	<i>x</i> -coordinate of node <i>n</i> [L] (always a horizontal coordinate).
3	Real	<i>z(n)</i>	<i>z</i> -coordinate of node <i>n</i> [L]. <i>z</i> is the vertical coordinate for problems involving vertical planar or axisymmetric flow. For axisymmetric flow, <i>z</i> coincides with the vertical axis of symmetry.  Record 3 information is required for each node <i>n</i> . Numbering of the nodes is arbitrary.
4	-	-	Comment line.
5	Integer	<i>e</i>	Edge number. Not read by the calculation module.
5	Integer	<i>iEpb(e)</i>	Number of the beginning node of edge <i>e</i> . Not read by the calculation module.
5	Integer	<i>iEpe(e)</i>	Number of the ending node of edge <i>e</i> . Not read by the calculation module.  Record 5 information is required for each edge <i>e</i> . Record 5 information is not read by the calculation module.
6	-	-	Comment line.
7	Integer	<i>t</i>	Triangular element number.
7	Integer	<i>KX(t,1)</i>	Global nodal number of the first triangle's vertex.
7	Integer	<i>KX(t,2)</i>	Global nodal number of the second triangle's vertex.
7	Integer	<i>KX(t,3)</i>	Global nodal number of the third triangle's vertex.  Record 7 information is required for each triangle <i>t</i> .

Table 10.7b. Block G - Finite element mesh information for three-dimensional applications.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Meshtria.txt file; set equal to 1 for current version.
2	-	-	Comment line.
3	-	-	Comment line.
4	Integer	<i>IGenMesh</i>	Set equal to 0 if simple structured finite element mesh for hexahedral transport domains is used. Set equal to 1 if unstructured finite element mesh is used.
5	-	-	Comment line.
6	Integer	<i>NumNP</i>	Number of nodal points.
6	Integer	<i>NumEl</i>	Number of finite elements (only tetrahedrals are allowed).
6	Integer	<i>IJ</i>	Number of nodes on the base of the hexahedral domain. Set equal to zero if simple hexahedral domain is not used.
6	Integer	<i>nNx</i>	Number of nodes in the <i>x</i> -direction of the hexahedral domain. Set equal to zero if simple hexahedral domain is not used.
6	Integer	<i>nNy</i>	Number of nodes in the <i>y</i> -direction of the hexahedral domain. Set equal to zero if simple hexahedral domain is not used.
6	Integer	<i>nNz</i>	Number of nodes in the <i>z</i> -direction of the hexahedral domain. Set equal to zero if simple hexahedral domain is not used.
7	-	-	Comment line.
8	Integer	<i>n</i>	Nodal number.
8	Real	<i>x(n)</i>	<i>x</i> -coordinate of node <i>n</i> [L].
8	Real	<i>y(n)</i>	<i>y</i> -coordinate of node <i>n</i> [L].
8	Real	<i>z(n)</i>	<i>z</i> -coordinate of node <i>n</i> [L]. <i>z</i> is the vertical coordinate.  Record 3 information is required for each node <i>n</i> .
9	-	-	Comment line.
10	-	-	Comment line.
11	Integer	<i>t</i>	Tetrahedral element number.
11	Integer	<i>KX(e,1)</i>	Global nodal number of the first corner node <i>i</i> .
11	Integer	<i>KX(e,2)</i>	Global nodal number of the second corner node <i>j</i> .
11	Integer	<i>KX(e,3)</i>	Global nodal number of the third corner node <i>k</i> .
11	Integer	<i>KX(e,4)</i>	Global nodal number of the fourth corner node <i>l</i> .
11	Integer	<i>KX(e,5)</i>	Global nodal number of the fifth corner node <i>m</i> .
11	Integer	<i>KX(e,6)</i>	Global nodal number of the sixth corner node <i>n</i> .
11	Integer	<i>KX(e,7)</i>	Global nodal number of the seventh corner node <i>o</i> .

Table 10.7b. (continued)

Record	Type	Variable	Description
11	Integer	$KX(e,8)$	Global nodal number of the eighth corner node $p$ . Indices $i, j, k, l, m, n, o$ and $p$ , refer to the corner nodes of an element $e$ taken in a certain orientation as described in Section 6.1. $KX(e,5)$ for tetrahedral and $KX(e,7)$ for triangular prismatic elements must be equal to zero.
11	Integer	$KX(e,9)$	Code specifying the subdivision of hexahedral and triangular prismatic elements into tetrahedrals (See Chapter 6.1 and Figure 6.1).  Record 11 information is required for each triangle $t$ .



Table 10.8. Block H - Nodal information.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Domain.dat file; set equal to 2 for current version.
2,3	-	-	Comment lines.
4	Integer	<i>NS</i>	Number of solutes in a chain reaction.
4	Integer	<i>iEquil</i>	This variable is read only if the user interface is used. = 1; Equilibrium solute transport is considered. = 0; Nonequilibrium solute transport is considered. Set equal to 1 if <i>lChem</i> is equal to <b>.false.</b>
5,6	-	-	Comment line.
7	Integer	<i>n</i>	Nodal number.
7	Integer	<i>Kode(n)</i>	Code specifying the type of boundary condition applied to a particular node. Permissible values are 0,1,±2, ±3, ±4,..., ± <i>NumKD</i> (see Section 8.3).
7	Real	<i>hNew(n)</i>	Initial value of the pressure head at node <i>n</i> [L] when variable <i>lInitW</i> in Block A is equal to <b>.true.</b> . Initial value of the water content at node <i>n</i> [L] when variable <i>lInitW</i> in Block A is equal to <b>.false.</b> . If <i>lWat</i> = <b>.false.</b> in Block A, then <i>hNew(n)</i> represents the initial guess of the pressure head (water content) for steady state conditions.
7	Real	<i>Q(n)</i>	Prescribed recharge/discharge rate at node <i>n</i> ; [L <sup>2</sup> T <sup>-1</sup> ] for planar flow, [L <sup>3</sup> T <sup>-1</sup> ] for axisymmetric flow. <i>Q(n)</i> is negative when directed out of the system. When no value for <i>Q(n)</i> is needed, set <i>Q(n)</i> equal to zero.
7	Integer	<i>MatNum(n)</i>	Index for material whose hydraulic and transport properties are assigned to node <i>n</i> .
7	Real	<i>Beta(n)</i>	Value of the water uptake distribution, <i>b(x,y,z)</i> [L <sup>-2</sup> ], in the soil root zone at node <i>n</i> . Set <i>Beta(n)</i> equal to zero if node <i>n</i> lies outside the root zone.
7	Real	<i>Axz(n)</i>	Nodal value of the dimensionless scaling factor $\alpha_h$ [-] associated with the pressure head.
7	Real	<i>Bxz(n)</i>	Nodal value of the dimensionless scaling factor $\alpha_K$ [-] associated with the saturated hydraulic conductivity.
7	Real	<i>Dxz(n)</i>	Nodal value of the dimensionless scaling factor $\alpha_\theta$ [-] associated with the water content.
7	Real	<i>Temp(n)</i>	Initial value of temperature at node <i>n</i> [°C] (if <i>lTemp</i> = <b>.false.</b> then set equal to 0 or any initial value, which is to be used with temperature dependent water flow and solute transport).
7	Real	<i>Conc(1,n)</i>	Initial value of the concentration of the first solute at node <i>n</i> [ML <sup>-3</sup> ] (do not have to be specified if <i>lChem</i> = <b>.false.</b> ).

Table 10.8. (continued)

Record	Type	Variable	Description
7	Real	<i>Conc(2,n)</i>	Initial value of the concentration of the second solute at node <i>n</i> [ML <sup>-3</sup> ] (must not be specified if <i>lChem=.true.</i> and <i>NS &lt; 2</i> ).
.	.	.	.
7	Real	<i>Conc(i,n)</i>	Initial value of the concentration of the last solute at node <i>n</i> [ML <sup>-3</sup> ] (must not be specified if <i>lChem=.true.</i> and <i>NS &lt; i</i> ).
7	Real	<i>Sorb(1,n)</i>	Initial value of the adsorbed concentration on type-2 sites or initial concentration in the immobile zone of the first solute at node <i>n</i> [ML <sup>-3</sup> ]. This variable does not have to be specified if <i>lChem=.false.</i> or <i>lEquil=.true.</i> .
7	Real	<i>Sorb(2,n)</i>	Initial value of the adsorbed concentration on type-2 sites or initial concentration in the immobile zone of the second solute at node <i>n</i> [ML <sup>-3</sup> ]. This variable does not have to be specified if <i>lChem=.false.</i> or <i>lEquil=.true.</i> or <i>NS &lt; 2</i> .
.	.	.	.
7	Real	<i>Sorb(NS,n)</i>	Initial value of the adsorbed concentration on type-2 sites or initial concentration in the immobile zone of the <i>NS</i> th solute at node <i>n</i> [ML <sup>-3</sup> ]. This variable does not have to be specified if <i>lChem=.false.</i> or <i>lEquil=.true.</i> .

Table 10.9. Block I - Element information.

Record	Type	Variable	Description
1,2	-	-	Comment lines.
3	Integer	$e$	Element number.
			The following 3 numbers (Record 3a) are only for two-dimensional applications.
3a	Real	$Angle(e)$	Angle in degrees between $K_1^A$ and the $x$ -coordinate axis assigned to each element $e$ .
3a	Real	$ConA1(e)$	First principal component, $K_1^A$ , of the dimensionless tensor $\mathbf{K}^A$ which describes the local anisotropy of the hydraulic conductivity assigned to element $e$ .
3a	Real	$ConA2(e)$	Second principal component, $K_2^A$ .
			The following number (Record 3b) is only for two-dimensional applications.
3b	Real	$iAniz(e)$	Index of anisotropy tensor (Record 11 of Block B) assigned to each element $e$ .
3	Integer	$LayNum(e)$	Subregion number assigned to element $e$ . In general, record 3 information is required for each element $e$ , starting with $e=1$ and continuing sequentially until $e=NumEl$ .

Table 10.10. Block J - Boundary information.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Boundary.in file; set equal to 3 for current version.
2,3	-	-	Comment lines.
4	Integer	<i>NumBP</i>	Number of boundary nodes for which <i>Kode(n)</i> is not equal to 0.
4	Integer	<i>NObs</i>	Number of observation nodes for which values of the pressure head, the water content, temperature (for <i>ITemp=.true.</i> ), and the solution and sorbed concentrations (for <i>IChem=.true.</i> ) are printed at each time level.
4	Logical	<i>SeepF</i>	<b>.true.</b> if one or more seepage faces is to be considered.
4	Logical	<i>FreeD</i>	Set this variable equal to <b>.true.</b> if a unit vertical hydraulic gradient boundary condition (free drainage) is used at the bottom boundary. Otherwise set equal to <b>.false.</b> .
4	Logical	<i>DrainF</i>	Set this logical variable equal to <b>.true.</b> if a drain is to be simulated by means of a boundary condition. Otherwise set equal to <b>.false.</b> . Section 5.3.7 explains how tile drains can be represented as boundary conditions in a regular finite element mesh.
4	Logical	<i>qGWLf</i>	Set this variable equal to <b>.true.</b> if the discharge-groundwater level relationship $q(GWL)$ given by equation (8.1) is used as the bottom boundary condition; $GWL=h-GWL0L$ , where $h$ is the pressure head at the boundary.
5	-	-	Comment line.
6	Logical	<i>Interp</i>	Logical variable indicating that time-variable boundary pressure heads should be interpolated with time.
6	Logical	<i>IVarBC</i>	Logical variable indicating that the time-variable boundary pressure head boundary condition should be changed to zero flux when the specified number is larger than 999999.
6	Logical	<i>IFluxHead</i>	Logical variable indicating that the zero flux boundary condition should be applied on the part of the boundary where the time-variable boundary pressure head is negative.
6	Logical	<i>lAtmHead</i>	Logical variable indicating that the atmospheric boundary condition should be applied on the part of the boundary where the time-variable boundary pressure head is negative.
6	Logical	<i>lSeepHead</i>	Logical variable indicating that the seepage face boundary condition should be applied on the part of the boundary where the time-variable boundary pressure head is negative.
6	Logical	<i>lAtmGWL</i>	Logical variable indicating that the time-variable flux boundary condition should be treated similarly as the atmospheric boundary conditions, i.e., with limiting pressure head values $hCritA$ and $hCritS$ .

Table 10.10. (continued)

Record	Type	Variable	Description
6	Logical	<i>lAtmSeep</i>	Logical variable indicating that the atmospheric boundary condition should be applied on the part of the boundary where the seepage face is not active.
6	Logical	<i>lSnow</i>	Logical variable indicating that the snow accumulates at the atmospheric boundary condition whenever temperatures are below zero.
7	-	-	Comment line.
8	Integer	<i>KXB(1)</i>	Global node number of the first of a set of sequentially numbered boundary nodes for which <i>Kode(n)</i> is not equal to zero.
8	Integer	<i>KXB(2)</i>	As above for the second boundary node.
.	.	.	.
.	.	.	.
8	Integer	<i>KXB(NumBP)</i>	As above for the last boundary node.
9	-	-	Comment line.
10	Real	<i>Width(1)</i>	Width [L] (for 2D applications) or surface area (for 3D applications) [L <sup>2</sup> ] of the boundary associated with boundary node <i>KXB(1)</i> . <i>Width(n)</i> includes half the boundary length for 2D applications (or one quarter of the boundary surface area for 3D applications) of each element connected to node <i>KXB(n)</i> along the boundary. The type of boundary condition assigned to <i>KXB(n)</i> is determined by the value of <i>Kode(n)</i> . In case of axisymmetric flow, <i>Width(n)</i> represents the area of the boundary strip [L <sup>2</sup> ] associated with node <i>KXB(n)</i> , and along a horizontal boundary should be calculated as $Width(j) = \frac{\pi}{3} [(x_{j-1} + 2x_j)(x_j - x_{j-1}) + (x_{j+1} + 2x_j)(x_{j+1} - x_j)]$
			If a unit vertical hydraulic gradient or a deep drainage boundary condition is specified at node <i>n</i> , then <i>Width(n)</i> represents only the horizontal component of the boundary.
10	Real	<i>Width(2)</i>	As above for node <i>KXB(2)</i> .
.	.	.	.
.	.	.	.
10	Real	<i>Width(NumBP)</i>	As above for node <i>KXB(NumBP)</i> .
11	-	-	Comment line.
12	Real	<i>rLen</i>	Width (for 2D) or surface area (for 3D) of soil surface associated with transpiration [L]; represents surface area [L <sup>2</sup> ] in case of axisymmetrical flow. Set <i>rLen</i> equal to zero for problems without transpiration.
13	-	-	Comment line.
14	Real	<i>GWL0L</i>	Reference position of groundwater table (usually the <i>z</i> -coordinate of the soil surface).
14	Real	<i>Aqh</i>	Value of the parameter <i>A<sub>qh</sub></i> [LT <sup>-1</sup> ] in the <i>q(GWL)</i> -relationship (equation (8.1));

set to zero if  $qGWL = \mathbf{false}$ .

Table 10.10. (continued)

Record	Type	Variable	Description
14	Real	$B_{qh}$	Value of the parameter $B_{qh}$ [ $L^{-1}$ ] in the $q(GWL)$ -relationship (equation (8.1)); set to zero if $qGWL = \mathbf{false}$ .  Records 13 and 14 are provided only when the logical variable $qGWL = \mathbf{true}$ .
15	-	-	Comment line.
16	Integer	$Node(1)$	Global node number of the first observation node for which values of the pressure head, the water content, temperature (for $ITemp = \mathbf{true}$ ), and the solution and sorbed concentrations (for $lChem = \mathbf{true}$ ) are printed at each time level. It does not have to be specified if $NObs = 0$ .
16	Integer	$Node(2)$	Same as above for the second observation node. It does not have to be specified if $NObs < 2$ .
.	.	.	.
16	Integer	$Node(NObs)$	Same as above for the last observation node.  Records 15 and 16 are provided only when the variable $NObs > 0$ .
17	-	-	Comment line.
18	Integer	$NPart$	Number of fictional particles, for which their trajectory is to be calculated.
19	Integer	$NodeP(1)$	The node number of the first fictional particle.
19	Integer	$NodeP(2)$	The second fictional particle.
.	.	.	.
19	Integer	$NodeP(NObs)$	The last fictional particle.  Records 17 through 19 are provided only for two-dimensional applications and when particle option is enabled.
20,21	-	-	Comment lines.
22	Integer	$NSeep$	Number of seepage faces expected to develop.
23	-	-	Comment line.
24	Integer	$NSP(1)$	Number of nodes on the first seepage face.
24	Integer	$NSP(2)$	Number of nodes on the second seepage face.
.	.	.	.
.	.	.	.
24	Integer	$NSP(NSeep)$	Number of nodes on the last seepage face.
25	-	-	Comment line.
26	Integer	$NP(1,1)$	Sequential global number of the first node on the first seepage face.
26	Integer	$NP(1,2)$	Sequential global number of the second node on the first seepage face.
.	.	.	.
.	.	.	.

26 Integer  $NP(1,NSP(1))$  Sequential global number of the last node on the first seepage face.

Table 10.10. (continued)

Record	Type	Variable	Description
			Record 26 information is provided for each seepage face. Records 20 through 26 information is not provided if the logical variable <i>SeepF</i> is set equal to <b>.false.</b> .
27,28	-	-	Comment lines.
29	Integer	$NDr$	Number of drains. See Section 5.3.7 for a discussion on how tile drains can be represented as boundary conditions in a regular finite element mesh.
29	Real	$DrCorr$	Additional reduction in the correction factor $C_d$ (See Section 5.3.7).
30	-	-	Comment line.
31	Integer	$ND(1)$	Global number of the first drain.
31	Integer	$ND(2)$	Global number of the second drain.
.	.	.	.
.	.	.	.
31	Integer	$ND(NDr)$	Global number of the last drain.
32	-	-	Comment line.
33	Integer	$NEID(1)$	Number of elements surrounding the first drain.
33	Integer	$NEID(2)$	Number of elements surrounding the second drain.
.	.	.	.
.	.	.	.
33	Integer	$NEID(NDr)$	Number of elements surrounding the last drain.
34	-	-	Comment line.
35	Real	$EfDim(1,1)$	Effective diameter of the first drain, $d_e$ [L] (see Section 5.3.7).
35	Real	$EfDim(2,1)$	Dimension of the square in finite element mesh representing the first drain, $D$ [L] (see Section 5.3.7).
			Record 35 information is provided for each drain.
36	-	-	Comment line.
37	Integer	$KEIDr(1,1)$	Global number of the first element surrounding the first drain.
37	Integer	$KEIDr(1,2)$	Global number of the second element surrounding the first drain.
.	.	.	.
.	.	.	.
37	Integer	$KEIDr(1,NEID(1))$	Global number of the last element surrounding the first drain.
			Record 37 information is provided for each drain. Records 27 through 37 are provided only if the logical variable <i>DrainF</i> is set equal to <b>.true.</b> .
38,39	-	-	Comment lines.

Table 10.10. (continued)

Record	Type	Variable	Description
40	Integer	<i>KodCB(1)</i>	Code specifying the type of boundary condition for solute transport applied to a particular node. Positive and negative signs indicate that first-, or second- or third- (depending upon the calculated water flux $Q$ ), type boundary conditions are implemented, respectively. In case of time-independent boundary conditions ( $Kode(1)=\pm 1, \pm 2, \pm 5, \text{ or } \pm 6$ ; See Block H), <i>KodCB(1)</i> also refers to the field <i>cBound</i> for the value of the solute transport BC. <i>cBound(i,abs(KodCB(1)))</i> is the value of the boundary condition for node <i>KXB(1)</i> (the first of a set of sequentially numbered boundary nodes for which <i>Kode(N)</i> is not equal to zero). Permissible values are $\pm 1, \pm 2, \dots, \pm 5, \pm 6, -7$ . When <i>KodCB(1)</i> equals -7, a special type of boundary condition for volatile solutes described by equations (3.39) and (3.40) is applied.
40	Integer	<i>KodCB(2)</i>	Same as above for the second boundary node.
.	.	.	.
.	.	.	.
40	Integer	<i>KodCB(NumBP)</i>	Same as above for the last boundary node.
			Records 38 through 40 are provided only if the logical variable <i>lChem</i> (Block A) is set equal to <b>.true.</b> .
41,42	-	-	Comment line.
243	Integer	<i>KodTB(1)</i>	Code specifying the type of boundary condition for heat transport applied to a particular node. Positive and negative signs mean that first-, or second- or third- (depending upon the calculated water flux $Q$ ) type boundary conditions will be implemented, respectively. In case of time-independent boundary conditions ( $Kode(1)=\pm 1, \pm 2, \pm 5, \text{ or } \pm 6$ ; See Block H), <i>KodTB(1)</i> refers to the vector <i>TBound</i> for the value of the heat transport BC. <i>TBound(abs(KodTB(1)))</i> is the value of the boundary condition for node <i>KXB(1)</i> (the first of a set of sequentially numbered boundary nodes for which <i>Kode(N)</i> is not equal to zero). Permissible values are $\pm 1, \dots, \pm 6$ .
43	Integer	<i>KodTB(2)</i>	Same as above for the second boundary node.
.	.	.	.
.	.	.	.
43	Integer	<i>KodTB(NumBP)</i>	Same as above for the last boundary node.
			Records 41 through 43 are provided only if the logical variable <i>lTemp</i> (Block A) is set equal to <b>.true.</b> .



Table 10.11. Block K - Atmospheric information.<sup>+</sup>

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Atmosph.in file; set equal to 3 for current version.
2,3	-	-	Comment lines.
4	Integer	<i>MaxAl</i>	Number of atmospheric data records.
5	-	-	Comment line.
6	Real	<i>hCritS</i>	Maximum allowed pressure head at the soil surface [L].
7	-	-	Comment line.
8	Real	<i>tAtm(i)</i>	Time for which the <i>i</i> -th data record is provided [T].
8	Real	<i>Prec(i)</i>	Precipitation [ $\text{LT}^{-1}$ ] (in absolute value).
8	Real	<i>rSoil(i)</i>	Potential evaporation rate [ $\text{LT}^{-1}$ ] (in absolute value).
8	Real	<i>rRoot(i)</i>	Potential transpiration rate [ $\text{LT}^{-1}$ ] (in absolute value).
8	Real	<i>hCritA(i)</i>	Absolute value of the minimum allowed pressure head at the soil surface [L].
8	Real	<i>rGWL(1)</i>	Drainage flux [ $\text{LT}^{-1}$ ] across the bottom boundary, or other time-dependent prescribed flux boundary condition (positive when water leaves the flow region), for nodes where <i>Kode(n)</i> =-3; set to zero when no <i>Kode(n)</i> =-3 boundary condition is specified.
8	Real	<i>GWL(1)</i>	Groundwater level [L] (usually negative), or other time-dependent prescribed head boundary condition, for nodes where <i>Kode(n)</i> =+3; set equal to zero when no <i>Kode(n)</i> =+3 is specified. The prescribed value of the pressure head is $h=\text{GWL}+\text{GWL0L}$ .
8	Real	<i>rGWL(2)</i>	Drainage flux [ $\text{LT}^{-1}$ ] for nodes where <i>Kode(n)</i> =-7; set to zero when no <i>Kode(n)</i> =-7 boundary condition is specified.
8	Real	<i>GWL(2)</i>	Groundwater level [L] for nodes where <i>Kode(n)</i> =+7; set equal to zero when no <i>Kode(n)</i> =+7 is specified.
8	Real	<i>rGWL(3)</i>	ditto for <i>Kode(n)</i> =-8.
8	Real	<i>GWL(3)</i>	ditto for <i>Kode(n)</i> =+8.
8	Real	<i>rGWL(4)</i>	ditto for <i>Kode(n)</i> =-9.
8	Real	<i>GWL(4)</i>	ditto for <i>Kode(n)</i> =+9.
8	Real	<i>Temp1(i)</i>	First time-dependent temperature [K] prescribed for nodes where <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 (must not be specified if <i>lTemp</i> = <b>false</b> . and <i>lChem</i> = <b>true</b> .; set equal to zero when no <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 or when the flux is directed out of the flow domain).

Table 10.11. (continued)

Record	Type	Variable	Description
8	Real	<i>Temp2(i)</i>	Second time-dependent temperature [K] prescribed for nodes where <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 (must not be specified if <i>lTemp</i> = <b>false</b> . and <i>lChem</i> = <b>true</b> .; set equal to zero when no <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 or when the flux is directed out of the flow domain).
8	Real	<i>Conc1(1,i)</i>	First time-dependent solute concentration [ML <sup>-3</sup> ] prescribed for nodes where <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 (does not need to be specified if <i>lChem</i> = <b>false</b> .; set equal to zero when no <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9, or when the flux is directed out of the flow domain).
8	Real	<i>crt(1,i)</i>	Second time-dependent solute concentration [ML <sup>-3</sup> ] prescribed for nodes where <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 (does not need to be specified if <i>lChem</i> = <b>false</b> .; set equal to zero when no <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9, or when the flux is directed out of the flow domain).
8	Real	<i>cht(1,i)</i>	Third time-dependent solute concentration [ML <sup>-3</sup> ] prescribed for nodes where <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9 (does not need to be specified if <i>lChem</i> = <b>false</b> .; set equal to zero when no <i>Kode(n)</i> = ±3, ±4, ±7, ±8, or ±9, or when the flux is directed out of the flow domain).
8	Real	<i>cPrec(2,i)</i>	Same as <i>cPrec(1,i)</i> for the second solute (does not need to be specified if <i>lChem</i> = <b>false</b> . or <i>NS</i> < 2).
8	Real	<i>crt(2,i)</i>	Same as <i>crt(1,i)</i> for the second solute (does not need to be specified if <i>lChem</i> = <b>false</b> . or <i>NS</i> < 2).
8	Real	<i>cht(2,i)</i>	Same as <i>cht(1,i)</i> for the second solute (does not need to be specified if <i>lChem</i> = <b>false</b> . or <i>NS</i> < 2).
			The last three entries are entered for each solute from 1 to <i>NS</i> .
			The total number of atmospheric data records is <i>MaxAl</i> ( <i>i</i> =1,2, ..., <i>MaxAl</i> ).

<sup>+</sup> Block K is not read in if the logical variable *AtmInf*(Block A) is set equal to **false**.

Table 10.12. Block L - Dimension Information.

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Dimensio.in file; set equal to 2 for current version.
2	-	-	Comment lines.
3	Integer	<i>NumNPD</i>	Maximum number of nodes in finite element mesh
3	Integer	<i>NumEID</i>	Maximum number of elements in finite element mesh
3	Integer	<i>NumBPD</i>	Maximum number of boundary nodes for which $Kode(n) \neq 0$
3	Integer	<i>MBandD</i>	Maximum dimension of the bandwidth of matrix <i>A</i>
3	Integer	<i>NSeepD</i>	Maximum number of seepage faces
3	Integer	<i>NumSPD</i>	Maximum number of nodes along a seepage face
3	Integer	<i>NDrD</i>	Maximum number of drains
3	Integer	<i>NEIDrD</i>	Maximum number of elements surrounding one drain
3	Integer	<i>NMatD</i>	Maximum number of materials
3	Integer	<i>NObsD</i>	Maximum number of observation nodes (maximum is 10)
3	Integer	<i>NSD</i>	Maximum number of solutes in a chain reaction.
3	Integer	<i>NAnisD</i>	Maximum number of anisotropy tensors for 3d applications. Set equal to 1 for 2D applications.

Table 10.13. Block M - Inverse solution information.<sup>+</sup>

Record	Type	Variable	Description
1	Char	<i>cVersion</i>	Set text equal to "Pcp_File_Version=".
1	Integer	<i>iVersion</i>	Version of the Fit.in file; set equal to 3 for current version.
2	Integer	<i>NCase</i>	Number of cases being considered (only for the first data set).
3	Char	<i>Title1</i>	Descriptive title for simulation.
4	Char	<i>Title2</i>	Descriptive title for simulation.
5	-	-	Comment line.
6	Integer	<i>NOBB</i>	Number of observed data.
6	Integer	<i>MIT</i>	Maximum number of iterations for the inverse problem.
6	Integer	<i>iWeight</i>	Type of weighting used for the data set. = 0; no internal weighting. = 1; weighting by mean ratio. = 2; weighting by standard deviation.
7	-	-	Comment line.
8	Logical	<i>lWatF</i>	Set this logical variable equal to <b>.true.</b> when the soil hydraulic parameters are to be optimized.
8	Logical	<i>lChemF</i>	Set this logical variable equal to <b>.true.</b> when the solute transport parameters are to be optimized.
8	Integer	<i>NMat</i>	Number of soil materials. Materials are identified by the material number, <i>MatNum</i> , specified in Block H.
8	Logical	<i>lTempF</i>	Set this logical variable equal to <b>.true.</b> when the heat transport parameters are to be optimized.
8	Integer	<i>iConcType</i>	Type of concentration data that are used in the objective function. = 0: resident concentrations in the liquid phase = 1: log resident concentrations in the liquid phase : area averaged resident concentrations in the liquid phase when iPos=0 = 2: outflow concentration = 3: concentration flux = 4: cumulative concentration flux = 5: total concentration (both liquid and sorbed phases, both equilibrium and nonequilibrium phases) = 6: temperature
9	-	-	Comment line.
10	Integer	<i>iModel</i>	Soil hydraulic properties model: = 0; <i>van Genuchten's</i> [1980] model containing six parameters. = 1; modified <i>van Genuchten's</i> model containing ten parameters, <i>Vogel and Císlerová</i> [1988].

Table. 10.13. (continued).

Record	Type	Variable	Description
			<p>= 2; <i>Brooks and Corey's</i> [1964] model containing six parameters.</p> <p>= 3; <i>van Genuchten's</i> [1980] model with air-entry value of -2 cm and with six parameters.</p> <p>= 4; <i>Kosugi's</i> [1996] model with six parameters.</p> <p>= 5; dual porosity model of <i>Durner</i> [1994] with nine parameters.</p> <p>= 6; dual-porosity system with transfer proportional to the effective saturation (9 parameters) (see Sections 2.1.2 and 2.8).</p> <p>= 7; dual-porosity system with transfer proportional to the pressure head (11 parameters) (see Sections 2.1.2 and 2.8).</p>
10	Integer	<i>iHyst</i>	<p>Hysteresis in the soil hydraulic properties:</p> <p>= 0; no hysteresis</p> <p>= 1; hysteresis in the retention curve only</p> <p>= 2; hysteresis in both the retention and hydraulic conductivity functions</p> <p>= 3; Hysteresis using Bob Lenhard's model [<i>Lenhard et al.</i>, 1991; <i>Lenhard and Parker</i>, 1992].</p>
10	Logical	<i>ANiz</i>	= <b>.true.</b> is the coefficient of anisotropy is to be optimized.
11	-	-	Comment line.
12	Integer	<i>iQSame</i>	<p>Parameter constraints</p> <p>= 0: <math>\theta_s^d &gt; \theta_s^w</math></p> <p>= 1: <math>\theta_s^d = \theta_m^d</math>, <math>\theta_s^w = \theta_m^w</math></p> <p>= 2: <math>\theta_s^d = \theta_s^w = \theta_m</math></p>
12	Logical	<i>lAw2Ad</i>	<p><b>.true.</b> if parameter constraint <math>\alpha^w = 2 \alpha^d</math> is to be considered.</p> <p><b>.false.</b> if no constraint on <math>\alpha^w</math> and <math>\alpha^d</math> is imposed.</p>
12	Logical	<i>lKSame</i>	<p><b>.true.</b> if parameter constraint <math>K_s^w = K_s^d</math> is to be considered.</p> <p><b>.false.</b> if no constraint on <math>K_s^w</math> and <math>K_s^d</math> is imposed.</p>
12	Integer	<i>iKappa</i>	<p>= -1 if the initial condition is to be calculated from the main drying branch.</p> <p>= 1 if the initial condition is to be calculated from the main wetting branch.</p> <p>Records 11 and 12 are provided only when <i>iHyst</i> &gt; 0.</p> <p>Records 9 through 12 are specified only when the logical variable <i>lWatF</i> is equal to <b>.true.</b></p>
13	-	-	Comment line.
14	Integer	<i>NS</i>	<p>Number of solutes (must be equal to 1).</p> <p>Records 13 and 14 are specified only when the logical variable <i>lChemF</i> is equal to <b>.true.</b></p>
15	-	-	Comment line.
16	Real	<i>Par(1,M)</i>	Initial estimate of parameter $\theta_r$ for material <i>M</i> [-].
16	Real	<i>Par(2,M)</i>	Initial estimate of parameter $\theta_s$ for material <i>M</i> [-].
16	Real	<i>Par(3,M)</i>	Initial estimate of parameter $\alpha$ for material <i>M</i> [L <sup>-1</sup> ].

Table. 10.13. (continued).

Record	Type	Variable	Description
16	Real	$Par(4,M)$	Initial estimate of parameter $n$ for material $M$ [-].
16	Real	$Par(5,M)$	Initial estimate of parameter $K_s$ for material $M$ [ $LT^{-1}$ ].
16	Real	$Par(6,M)$	Initial estimate of parameter $l$ for material $M$ [-].
			The following four parameters are specified only when $iModel=1$ .
16	Real	$Par(7,M)$	Initial estimate of parameter $\theta_m$ for material $M$ [-].
16	Real	$Par(8,M)$	Initial estimate of parameter $\theta_a$ for material $M$ [-].
16	Real	$Par(9,M)$	Initial estimate of parameter $\theta_k$ for material $M$ [-].
16	Real	$Par(10,M)$	Initial estimate of parameter $K_k$ for material $M$ [ $LT^{-1}$ ].
			The following four parameters are specified only when $iModel=0$ and $iHyst>1$ .
16	Real	$Par(7,M)$	Initial estimate of parameter $\theta_m$ for material $M$ [-].
16	Real	$Par(8,M)$	Initial estimate of parameter $\theta_s^w$ for material $M$ [-].
16	Real	$Par(9,M)$	Initial estimate of parameter $\alpha^w$ for material $M$ [ $L^{-1}$ ].
16	Real	$Par(10,M)$	Initial estimate of parameter $K_s^w$ for material $M$ [ $LT^{-1}$ ].
17	Integer	$Index(1,M)$	Parameter estimation index for parameter $\theta_r$ , material $M$ [-]. = 0; Coefficient is known and kept constant during optimization. = 1; Coefficient is unknown and estimated by curve fitting the data.
17	Integer	$Index(2,M)$	Parameter estimation index for parameter $\theta_s$ , material $M$ [-].
17	Integer	$Index(3,M)$	Parameter estimation index for parameter $\alpha$ , material $M$ [-].
17	Integer	$Index(4,M)$	Parameter estimation index for parameter $n$ , material $M$ [-].
17	Integer	$Index(5,M)$	Parameter estimation index for parameter $K_{s_s}$ , material $M$ [-].
17	Integer	$Index(6,M)$	Parameter estimation index for parameter $l$ , material $M$ [-].
			The following four parameter estimation indices are specified only when $iModel=1$ .
17	Integer	$Index(7,M)$	Parameter estimation index for parameter $\theta_m$ , material $M$ [-].
17	Integer	$Index(8,M)$	Parameter estimation index for parameter $\theta_a$ , material $M$ [-].
17	Integer	$Index(9,M)$	Parameter estimation index for parameter $\theta_k$ , material $M$ [-].
17	Integer	$Index(10,M)$	Parameter estimation index for parameter $K_{k_s}$ , material $M$ [-].
			The following four parameter estimation indices are specified only when $iModel=0$ and $iHyst>1$ .
17	Integer	$Index(7,M)$	Parameter estimation index for parameter $\theta_m$ , material $M$ [-].
17	Integer	$Index(8,M)$	Parameter estimation index for parameter $\theta_s^w$ , material $M$ [-].
17	Integer	$Index(9,M)$	Parameter estimation index for parameter $\alpha^w$ , material $M$ [-].
17	Integer	$Index(10,M)$	Parameter estimation index for parameter $K_s^w$ , material $M$ [-].
18	Real	$BMn(1,M)$	Minimum constraint for parameter $\theta_r$ for material $M$ [-] (dummy value if $Index(1,M)=0$ ).
18	Real	$BMn(2,M)$	Minimum constraint for parameter $\theta_s$ , material $M$ [-].
18	Real	$BMn(3,M)$	Minimum constraint for parameter $\alpha$ , material $M$ [ $L^{-1}$ ].
18	Real	$BMn(4,M)$	Minimum constraint for parameter $n$ , material $M$ [-].
18	Real	$BMn(5,M)$	Minimum constraint for parameter $K_{s_s}$ , material $M$ [ $LT^{-1}$ ].
18	Real	$BMn(6,M)$	Minimum constraint for parameter $l$ , material $M$ [-].

Table 10.13. (continued).

Record	Type	Variable	Description
			The following four minimum parameter constraints are specified only when $iModel=1$ .
18	Real	$BMn(7,M)$	Minimum constraint for parameter $\theta_m$ , material $M$ [-].
18	Real	$BMn(8,M)$	Minimum constraint for parameter $\theta_a$ , material $M$ [-].
18	Real	$BMn(9,M)$	Minimum constraint for parameter $\theta_k$ , material $M$ [-].
18	Real	$BMn(10,M)$	Minimum constraint for parameter $K_k$ , material $M$ [ $LT^{-1}$ ].
			The following four minimum parameter constraints are specified only when $iModel=0$ and $iHyst>1$ .
18	Real	$BMn(7,M)$	Minimum constraint for parameter $\theta_m$ , material $M$ [-].
18	Real	$BMn(8,M)$	Minimum constraint for parameter $\theta_s^w$ , material $M$ [-].
18	Real	$BMn(9,M)$	Minimum constraint for parameter $\alpha^w$ , material $M$ [ $L^{-1}$ ].
18	Real	$BMn(10,M)$	Minimum constraint for parameter $K_s^w$ , material $M$ [ $LT^{-1}$ ].
19	Real	$BMx(1,M)$	Maximum constraint for parameter $\theta_r$ , material $M$ [-] (dummy value if $Index(1,M)=0$ ).
19	Real	$BMx(2,M)$	Maximum constraint for parameter $\theta_s$ , material $M$ [-].
19	Real	$BMx(3,M)$	Maximum constraint for parameter $\alpha$ , material $M$ [ $L^{-1}$ ].
19	Real	$BMx(4,M)$	Maximum constraint for parameter $n$ , material $M$ [-].
19	Real	$BMx(5,M)$	Maximum constraint for parameter $K_s$ , material $M$ [ $LT^{-1}$ ].
19	Real	$BMx(6,M)$	Maximum constraint for parameter $l$ , material $M$ [-].
			The following four maximum parameter constraints are specified only when $iModel=1$ .
19	Real	$BMx(7,M)$	Maximum constraint for parameter $\theta_m$ , material $M$ [-].
19	Real	$BMx(8,M)$	Maximum constraint for parameter $\theta_a$ , material $M$ [-].
19	Real	$BMx(9,M)$	Maximum constraint for parameter $\theta_k$ , material $M$ [-].
19	Real	$BMx(10,M)$	Maximum constraint for parameter $K_k$ , material $M$ [ $LT^{-1}$ ].
			The following four maximum parameter constraints are specified only when $iModel=0$ and $iHyst>1$ .
19	Real	$BMx(7,M)$	Maximum constraint for parameter $\theta_m$ , material $M$ [-].
19	Real	$BMx(8,M)$	Maximum constraint for parameter $\theta_s^w$ , material $M$ [-].
19	Real	$BMx(9,M)$	Maximum constraint for parameter $\alpha^w$ , material $M$ [ $L^{-1}$ ].
19	Real	$BMx(10,M)$	Maximum constraint for parameter $K_s^w$ , material $M$ [ $LT^{-1}$ ].
			Records 15 through 19 are specified only when logical variable $lWatF$ is equal to <b>.true.</b> and then must be provided for each material $M$ (from 1 to $NMat$ ). If $lWDep=.true.$ (Block A) then the soil hydraulic parameters $Par(i,M)$ must be specified at reference temperature $T_{ref}=20^\circ C$ .
20	-	-	Comment line.
21	Real	$ChPar(1,M)$	Initial estimate of bulk density of material $M$ , $\rho$ [ $ML^{-3}$ ].
21	Real	$ChPar(2,M)$	Initial estimate of longitudinal dispersivity for material type $M$ , $D_L$ [L].
21	Real	$ChPar(3,M)$	Initial estimate of transverse dispersivity for material type $M$ , $D_L$ [L].

Table 10.13. (continued).

Record	Type	Variable	Description
21	Real	$ChPar(4,M)$	Initial estimate of dimensionless fraction of the sorption sites classified as type-1, i.e., sites with instantaneous sorption when the <b>chemical nonequilibrium</b> option is considered. Set equal to 1 if equilibrium transport is to be considered. Dimensionless fraction of the sorption sites in contact with mobile water when the <b>physical nonequilibrium</b> option is considered. Set equal to 1 if all sorption sites are in contact with mobile water.
21	Real	$ChPar(5,M)$	Initial estimate of the immobile water content. Set equal to 0 when the <b>physical nonequilibrium</b> option is not considered.
21	Real	$ChPar(6,M)$	Initial estimate of the ionic or molecular diffusion coefficient in free water, $D_w$ [ $L^2 T^{-1}$ ].
21	Real	$ChPar(7,M)$	Initial estimate of the ionic or molecular diffusion coefficient in the gas phase, $D_g$ [ $L^2 T^{-1}$ ].
21	Real	$ChPar(8,M)$	Initial estimate of the adsorption isotherm coefficient, $k_s$ , for material type $M$ [ $L^3 M^{-1}$ ]. Set equal to zero if no adsorption is to be considered.
21	Real	$ChPar(9,M)$	Initial estimate of the adsorption isotherm coefficient, $\eta$ , for material type $M$ [ $L^3 M^{-1}$ ]. Set equal to zero if a Langmuir adsorption isotherm is not to be considered.
21	Real	$ChPar(10,M)$	Initial estimate of the adsorption isotherm coefficient, $\beta$ , for material type $M$ [-]. Set equal to one if a Freundlich adsorption isotherm is not to be considered.
21	Real	$ChPar(11,M)$	Initial estimate of the equilibrium distribution constant between the liquid and gas phases, $k_g$ , material type $M$ [-].
21	Real	$ChPar(12,M)$	Initial estimate of the first-order rate constant for the dissolved phase, $\mu_w$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(13,M)$	Initial estimate of the first-order rate constant for the solid phase, $\mu_s$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(14,M)$	Initial estimate of the first-order rate constant for the gas phase, $\mu_g$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(15,M)$	Initial estimate of the rate constant, $\mu_w'$ , representing first-order decay for the first solute and zero-order production for the second solute in the dissolved phase, material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(16,M)$	Initial estimate of the rate constant for the solid phase, $\mu_s'$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(17,M)$	Initial estimate of the rate constant for the gas phase, $\mu_g'$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(18,M)$	Initial estimate of the zero-order rate constant for the dissolved phase, $\gamma_w$ , material type $M$ [ $ML^{-3}T^{-1}$ ].
21	Real	$ChPar(19,M)$	Initial estimate of the zero-order rate constant for the solid phase, $\gamma_s$ , material type $M$ [ $T^{-1}$ ].
21	Real	$ChPar(20,M)$	Initial estimate of the zero-order rate constant for the gas phase, $\gamma_g$ , material type $M$ [ $ML^{-3}T^{-1}$ ].
21	Real	$ChPar(21,M)$	Initial estimate of the first-order mass transfer coefficient for nonequilibrium adsorption, $\omega$ , material type $M$ [ $T^{-1}$ ].
22	Integer	$Index(1,M)$	Parameter estimation index for parameter $ChPar(1,M)$ . = 0; Coefficient is known and kept constant during optimization. = 1; Coefficient is unknown and estimated by curve fitting the data.



Table. 10.13. (continued).

Record	Type	Variable	Description
22	Integer	$Index(21,M)$	Parameter estimation index for parameter $ChPar(21,M)$ .
23	Real	$BMn(1,M)$	Minimum constraint for parameter $ChPar(1,M)$ (dummy value if $Index(1,M)=0$ ).
.	.	.	.
23	Real	$BMn(21,M)$	Minimum constraint for parameter $ChPar(21,M)$ .
24	Real	$BMx(1,M)$	Maximum constraint for parameter $ChPar(1,M)$ (dummy value if $Index(1,M)=0$ ).
.	.	.	.
24	Real	$BMx(21,M)$	Maximum constraint for parameter $ChPar(21,M)$ .
<p>Records 20 through 24 are specified only when the logical variable <math>IChemF</math> is equal to <b>.true.</b>, in which case they must be provided for each material <math>M</math> (from 1 to <math>NMat</math>).</p> <p>Records 20 through 24 are specified similarly for heat transport parameters when the logical variable <math>ITempF</math> is equal to <b>.true.</b> In such case they must be provided for each material <math>M</math> (from 1 to <math>NMat</math>).</p>			
25	-	-	Comment line.
26	Real	$HO(i)$	Observation data. Time $t$ for $iType(i)=0,1,2,3,4$ ; Pressure head $h$ for $iType(i)=5,6$ ; Dummy for $iType(i)=7,8,9,10,11$ ;
26	Real	$FO(i)$	Observation data (see description with variable $iType$ ). When $iType(i)=2$ and $iPos(i)=0$ , then $FO(i)$ represents the total volume of water in the entire flow domain. When $iType(i)=4$ and $iPos(i)=0$ , then $FO(i)$ represents the average concentration of the entire flow domain. Type of concentration data depends on $iConcType$ .
26	Integer	$iType(i)$	Type of observed data: = 0: cumulative boundary water flux versus time = 1: $h(x,t)$ measurement = 2: $\theta(x,t)$ measurement = 3: boundary flux versus time = 4: $Conc(x,t)$ measurement = 5: $h(\theta)$ measurement = 6: $K(h)$ measurement = 7: prior knowledge of parameter $\alpha$ = 8: prior knowledge of parameter $n$ = 9: prior knowledge of parameter $\theta_r$ = 10: prior knowledge of parameter $\theta_s$ = 11: prior knowledge of parameter $K_s$

Table. 10.13. (continued).

Record	Type	Variable	Description
26	Integer	$iPos(i)$	Position of the observation node for $iType(i)=1,2,4$ (and $iConcType=0, 1, 6$ ); allowed values are 1, 2,... $NObs$ . When $iType(i)=0$ or 3 (and 4 when $iConcType=2, 3, 4$ ); then $iPos(i)$ is equal to $Kode(n)$ representing a particular type of boundary condition, e.g., 1 for a constant b.c., 2 for a seepage face, 3 for a variable b.c., 4 for an atmospheric b.c., 5 for a internal drains, and 6 for deep or free drainage. When $iType(i)=5,6,7,8,9,10$ , or 11, then $iPos(i)$ represents the material number $M$ ; allowed values are 1, 2,... $NMat$ .
26	Real	$Weight(i)$	Weight associated with a particular data point.

<sup>+</sup> Block M is not needed if only the direct solution is calculated or for three-dimensional applications.

## 11. OUTPUT DATA

The program output consists of  $14+3n_s$  output files organized into 3 groups:

T-level information

H\_MEAN.OUT  
V\_MEAN.OUT  
CUM\_Q.OUT  
RUN\_INF.OUT  
SOLUTEx.OUT  
OBSNOD.OUT

P-level information

H.OUT  
TH.OUT  
CONCx.OUT  
SORBCx.OUT  
TEMP.OUT  
V.OUT  
BOUNDARY.OUT  
BALANCE.OUT

A-level information

A\_LEVEL.OUT

In addition, some of the input data are printed to files CHECK.OUT and FIT.OUT. Separate output files SOLUTEx.OUT, CONCx.OUT and SORBx.OUT are created for each solute. The various output files are described in detail below. The file CHECK.OUT summarizes the most important input variables, including the hydraulic and transport properties of each soil material. Results of the inverse solution are written to an output file FIT.OUT (Table 11.8). All output files are directed to the same directory as the input files, and must be created by the user prior to program execution (the directory is created automatically if the user interface is used).

*T-level information* - This group of output files contains information, which is printed at the end of each time step (or after  $n$  type steps). Printing can be suppressed by setting the logical variable *ShortF* in input Block A equal to .true.; the information is then printed only at selected print times. Output files printed at the T-level are described in Tables 11.1 through 11.5. Output file OBSNOD.OUT brings the information about the time change of the pressure head, water content, temperature, and solution and sorbed concentrations, in specified observation nodes.

*P-level information* - P-level information is printed only at prescribed print times. The following output files are printed at the P-level:

H.OUT	Nodal values of the pressure head
TH.OUT	Nodal values of the water content
CONCx.OUT	Nodal values of the solution concentrations
SORBx.OUT	Nodal values of the nonequilibrium concentrations
TEMP.OUT	Nodal values of the temperature
V.OUT	Nodal values of the $x$ - and $y$ -components of the Darcian flux vector
BOUNDARY.OUT	This file contains information about each boundary node, $n$ , for which $Kode(n) \neq 0$ , including the discharge/recharge rate, $Q(n)$ , the boundary flux, $q(n)$ , the pressure head $h(n)$ , the water content $\theta(n)$ , the temperature $Temp(n)$ , and the concentration $Conc(n_s, n)$ .
BALANCE.OUT	This file gives the total amount of water, heat and solute inside each specified subregion, the inflow/outflow rates to/from that subregion, together with the mean pressure head ( $hMean$ ), mean temperature ( $TMean$ ) and the mean concentration ( $cMean$ ) over each subregion (see Table 11.6). Absolute and relative errors in the water and solute mass balances are also printed to this file.

The output files H.OUT, TH.OUT, CONCx.OUT, SORBx.OUT, TEMP.OUT, and V.OUT provide binary output of the specific variables. The user interface can convert these binary files into the ASCII files H.TXT, TH.TXT, CONCx.TXT, SORBx.TXT, TEMP.TXT, and V.TXT.

*A-level information* - A-level information is printed each time a time-dependent boundary condition is specified. The information is directed to output file A\_LEVEL.OUT (Table 11.7).

Table 11.1. H\_MEAN.OUT - mean pressure heads.

---

<i>hAtm</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm 4$ (i.e., along part of a boundary controlled by atmospheric conditions) [L].
<i>hRoot</i>	Mean value of the pressure head over a region for which $Beta(n)>0$ (i.e., within the root zone) [L].
<i>hKode3</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm 3$ (i.e., along part of a boundary where the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is imposed) [L].
<i>hKode1</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm 1$ (i.e., along part of a boundary where time-independent pressure heads and/or fluxes are imposed) [L].
<i>hSeep</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm 2$ (i.e., along seepage faces) [L].
<i>hKode5</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm 5$ [L].
.	.
.	.
.	.
<i>hKodeN</i>	Mean value of the pressure head calculated over a set of nodes for which $Kode(n)=\pm NumKD$ [L].

---

Table 11.2. V\_MEAN.OUT - mean and total water fluxes.\*

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<i>rAtm</i>	Potential surface flux per unit atmospheric boundary ( <i>Kode(n)=±4</i> ) [ $L T^{-1}$ ].
<i>rRoot</i>	Potential transpiration rate, $T_p$ [ $L T^{-1}$ ].
<i>vAtm</i>	Mean value of actual surface flux per unit atmospheric boundary ( <i>Kode(n)=±4</i> ) [ $L T^{-1}$ ].
<i>vRoot</i>	Actual transpiration rate, $T_a$ [ $L T^{-1}$ ].
<i>vKode3</i>	Total value of the bottom or other flux across part of a boundary where the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is imposed ( <i>Kode(n)=±3</i> ), [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup> .
<i>vKode1</i>	Total value of the boundary flux across part of a boundary where time-independent pressure heads and/or fluxes are imposed, including internal sinks/sources ( <i>Kode(n)=±1</i> ), [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup> .
<i>vSeep</i>	Total value of the boundary flux across a potential seepage face ( <i>Kode(n)=±2</i> ), [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup> .
<i>vKode5</i>	Total value of the flux across a boundary containing nodes for which <i>Kode(n)=±5</i> , [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup> .
.	.
.	.
.	.
<i>vKodeN</i>	Total value of the flux across a boundary containing nodes for which <i>Kode(n)=±NumKD</i> , [ $L^2 T^{-1}$ ] or [ $L^3 T^{-1}$ ] <sup>+</sup> .
<i>Runoff</i> <sup>#</sup>	Average surface run off per unit atmospheric boundary ( <i>Kode(n)=±4</i> ) [ $L T^{-1}$ ].
<i>Evapor</i> <sup>#</sup>	Average evaporation flux per unit atmospheric boundary ( <i>Kode(n)=±4</i> ) [ $L T^{-1}$ ].
<i>Infiltr</i> <sup>#</sup>	Average infiltration flux per unit atmospheric boundary ( <i>Kode(n)=±4</i> ) [ $L T^{-1}$ ].
<i>SnowLayer</i> <sup>#</sup>	Surface snow layer [L].

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<sup>+</sup> For plane (2D) and axisymmetric (or 3D) flow, respectively

\* Boundary fluxes are positive when water is removed from the system.

# Only for two-dimensional problems.

Table 11.3. CUM\_Q.OUT - total cumulative water fluxes.\*

---

<i>CumQAP</i>	Cumulative total potential surface flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQRP</i>	Cumulative total potential transpiration rate, [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQA</i>	Cumulative total actual surface flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQR</i>	Cumulative total actual transpiration rate, [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQ3</i>	Cumulative total value of the bottom or other boundary flux across part of a boundary where the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is imposed ( <i>Kode(n)=±3</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQ1</i>	Cumulative total value of the flux across part of a boundary along which time-independent pressure heads and/or fluxes are imposed, including internal sinks/sources ( <i>Kode(n)=±1</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQS</i>	Cumulative total value of the flux across a potential seepage faces ( <i>Kode(n)=±2</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQ5</i>	Cumulative total value of the flux across a boundary containing nodes for which <i>Kode(n)=±5</i> , [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
.	.
.	.
.	.
<i>CumQN</i>	Cumulative total value of the flux across a boundary containing nodes for which <i>Kode(n)=±NumKD</i> , [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>cRunoff</i> <sup>#</sup>	Cumulative surface run off across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>cEvapor</i> <sup>#</sup>	Cumulative evaporation flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>cInfiltr</i> <sup>#</sup>	Cumulative infiltration flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .

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<sup>+</sup> For plane (2D) and axisymmetric (or 3D) flow, respectively

\* Boundary fluxes are positive when water is removed from the system.

# Only for two-dimensional problems.

Table 11.4. RUN\_INF.OUT - time and iteration information.

---

<i>TLevel</i>	Time-level (current time-step number) [-].
<i>Time</i>	Time, $t$ , at current time-level [T].
<i>dt</i>	Time step, $\Delta t$ [T].
<i>IterW</i>	Number of iterations for water flow [-].
<i>IterC</i>	Number of iterations for solute transport [-].
<i>ItCum</i>	Cumulative number of iterations [-].
<i>Peclet</i>	Maximum local Peclet number [-].
<i>Courant</i>	Maximum local Courant number [-].

---



Table 11.5. SOLUTEx.OUT - actual and cumulative concentration fluxes.\*

<i>CumCh0</i>	Cumulative amount of solute removed from the flow region by zero-order reactions (positive when removed from the system), [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>CumCh1</i>	Cumulative amount of solute removed from the flow region by first-order reactions, [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>CumChR</i>	Cumulative amount of solute removed from the flow region by root water uptake <i>S</i> , [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>CumChN</i>	Cumulative amount of solute being transferred to either kinetic adsorption sites (type-2 sorption sites), or to the immobile liquid region, [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>ChemS1</i>	Cumulative solute flux across part of a boundary along which time-independent pressure heads and/or fluxes are imposed, including internal sink/sources ( <i>Kode(n)</i> = ±1), [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>ChemS2</i>	Cumulative solute flux across a potential seepage faces ( <i>Kode(n)</i> = ±2), [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>ChemS3</i>	Cumulative solute flux across part of a boundary along which the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is imposed ( <i>Kode(n)</i> = ±3), [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>ChemS4</i>	Cumulative total solute flux across the atmospheric boundary ( <i>Kode(n)</i> = ±4), [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>ChemS5</i>	Cumulative total solute flux across an internal or external boundary containing nodes for which <i>Kode(n)</i> = ±5, [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
.	.
<i>ChemSN</i>	Cumulative total solute flux across an internal or external boundary containing nodes for which <i>Kode(n)</i> = ± <i>NumKD</i> , [ML <sup>-1</sup> ] or [M] <sup>+</sup> .
<i>qc1</i>	Total solute flux across part of a boundary along which time-independent pressure heads and/or fluxes are imposed ( <i>Kode(n)</i> = ±1), [ML <sup>-1</sup> T <sup>-1</sup> ] or [MT <sup>-1</sup> ] <sup>+</sup> .
<i>qc2</i>	Total solute flux across a potential seepage face ( <i>Kode(n)</i> = ±2), [ML <sup>-1</sup> T <sup>-1</sup> ] or [MT <sup>-1</sup> ] <sup>+</sup> .
<i>qc3</i>	Total solute flux calculated across a boundary containing nodes for which <i>Kode(n)</i> = ±3 (i.e., along part of a boundary where the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is specified), [ML <sup>-1</sup> T <sup>-1</sup> ] or [MT <sup>-1</sup> ] <sup>+</sup> .
<i>qc4</i>	Total solute flux across the atmospheric boundary ( <i>Kode(n)</i> = ±4), [ML <sup>-1</sup> T <sup>-1</sup> ] or [MT <sup>-1</sup> ] <sup>+</sup> .
.	.
<i>qcN</i>	Total solute flux across an internal or external boundary containing nodes for which <i>Kode(n)</i> = ± <i>NumKD</i> , [ML <sup>-1</sup> T <sup>-1</sup> ] or [MT <sup>-1</sup> ] <sup>+</sup> .
<i>cMean1</i>	Mean concentration across part of a boundary along which time-independent pressure heads and/or fluxes are imposed ( <i>Kode(n)</i> = ±1) [ML <sup>-3</sup> ].
.	.
<i>cMean N</i>	Mean concentration across an internal or external boundary containing nodes for which <i>Kode(n)</i> = ± <i>NumKD</i> , [ML <sup>-3</sup> ].

<sup>+</sup> For plane (2D) and axisymmetric (or 3D) flow, respectively

\* The same output file is created for each solute from 1 to NS. Values of the solute flux and the cumulative solute flux are positive when solute is removed from the system.

Table 11.6. BALANCE.OUT - mass balance variables.

---

<i>Area (Volume)</i>	Area of the entire flow domain or a specified subregion, $[L^2]$ or $[L^3]^+$ .
<i>VolumeW</i>	Volume of water in the entire flow domain or in a specified subregion, $[L^2]$ or $[L^3]^+$ .
<i>InFlow</i>	Inflow/Outflow to/from the entire flow domain or to/from a specified subregion, $[L^2T^{-1}]$ or $[L^3T^{-1}]^+$ .
<i>hMean</i>	Mean pressure head in the entire flow domain or in a specified subregion $[L]$ .
<i>HeatVol</i>	Amount of heat in the entire flow domain or in a specified subregion, $[MLT^{-2}]$ or $[ML^2T^{-2}]^+$ .
<i>TMean</i>	Mean temperature in the entire flow domain or in a specified subregion $[K]$ .
<i>ConcVol</i>	Amount of solute in the entire flow domain or in a specified subregion. This variable is given for all solutes from 1 to <i>NS</i> , $[ML^{-1}]$ or $[M]^+$ .
<i>cMean</i>	Mean concentration in the entire flow domain or in a specified subregion. This variable is given for all solutes from 1 to <i>NS</i> $[ML^{-3}]$ .
<i>ConcVII</i>	Amount of solute in the entire flow domain or in a specified subregion in the non-equilibrium phase (solute in the immobile water or kinetically sorbed solute). This variable is given for all solutes from 1 to <i>NS</i> , $[ML^{-1}]$ or $[M]^+$ .
<i>SorbVII</i>	Amount of kinetically sorbed solute in the entire flow domain or in a specified subregion. This variable is given for all solutes from 1 to <i>NS</i> (for 3D applications), $[ML^{-1}]$ or $[M]^+$ .
<i>cMeanIm</i>	Mean concentration in the entire flow domain or in a specified subregion in the non-equilibrium phase (solute in the immobile water or kinetically sorbed solute (called <i>sMeanIm</i> in 3D applications)). This variable is given for all solutes from 1 to <i>NS</i> $[ML^{-3}]$ .
<i>WatBalT</i>	Absolute error in the water mass balance of the entire flow domain, $[L^2]$ or $[L^3]^+$ .
<i>WatBalR</i>	Relative error in the water mass balance of the entire flow domain [%].
<i>CncBalT</i>	Absolute error in the solute mass balance of the entire flow domain. This variable is given for all solutes from 1 to <i>NS</i> , $[ML^{-1}]$ or $[M]^+$ .
<i>CncBalR</i>	Relative error in the solute mass balance of the entire flow domain. This variable is given for all solutes from 1 to <i>NS</i> [%].

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<sup>+</sup> For plane (2D) and axisymmetric (or 3D) flow, respectively

Table 11.7. A\_LEVEL.OUT - mean pressure heads and total cumulative fluxes.\*

---

<i>CumQAP</i>	Cumulative total potential flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQRP</i>	Cumulative total potential transpiration rate, [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQA</i>	Cumulative total actual flux across the atmospheric boundary ( <i>Kode(n)=±4</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQR</i>	Cumulative total actual transpiration rate, [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>CumQ3</i>	Cumulative total bottom or other flux across a boundary along which the groundwater level, the bottom flux, or other time-dependent pressure head and/or flux is imposed ( <i>Kode(n)=±3</i> ), [L <sup>2</sup> ] or [L <sup>3</sup> ] <sup>+</sup> .
<i>hAtm</i>	Mean value of the pressure head calculated over a set of nodes for which <i>Kode(n)=±4</i> [L].
<i>hRoot</i>	Mean value of the pressure head over a region for which <i>Beta(n)&gt;0</i> (i.e., the root zone) [L].
<i>hKode3</i>	Mean value of the pressure head over a set of nodes for which <i>Kode(n)=±3</i> [L].

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<sup>+</sup> For plane (2D) and axisymmetric (or 3D) flow, respectively

\* Boundary fluxes are positive when water is removed from the system.

Table 11.8. FIT.OUT - information related to parameter estimation.

---

<i>SSQ</i>	Value of the objective function $\phi$ being minimized during the parameter optimization process.
<i>S.E.Coeff</i>	Standard error.
<i>RSQUARE</i>	$r^2$ value for regression of observed versus fitted values.
<i>Quantity</i>	Measured data, e.g., the pressure head, water content, cumulative flux.
<i>Type</i>	Type of measured data (see Table 10.13).
<i>Position</i>	Position of the measurement (see Table 10.13).
<i>Weight</i>	Weight associated with a particular data point.
<i>Residual</i>	Residual between measured and fitted quantity.

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